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**Modeling Transient Thermalhydraulic Behavior of a
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by

Abdullah S. Al-Kheliewi

A THESIS

submitted to

Oregon State University

in partial fulfillment of
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Andrew C. Klein

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The results show that this design is suitable for space applications and does not show any deficiency in the

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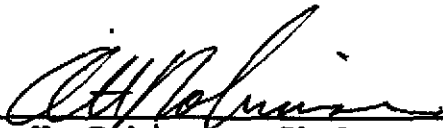
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APPROVED:



Andrew C. Klein, Ph.D.
Assoc. Professor of Nuclear Engineering in charge of major



Alan H. Robinson, Ph.D.
Head of department of Nuclear Engineering

Thomas J. Maresh, Ph.D.
Dean of Graduate School

Date thesis is presented September 20, 1993

Typed by Abdullah S. Al-Kheliewi

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Modeling Transient Thermalhydraulic Behavior of a Thermionic Fuel Element for Nuclear Space Reactors

Chapter 1

Literature Review

1.1 Space Reactors

Nuclear power reactors play an important role in every aspect of today's technology not only on our planet but in outer space. For space missions, it has been found that nuclear technology can be useful in providing power for systems operation in earth orbit, on the moon, on Mars, and in deep space.

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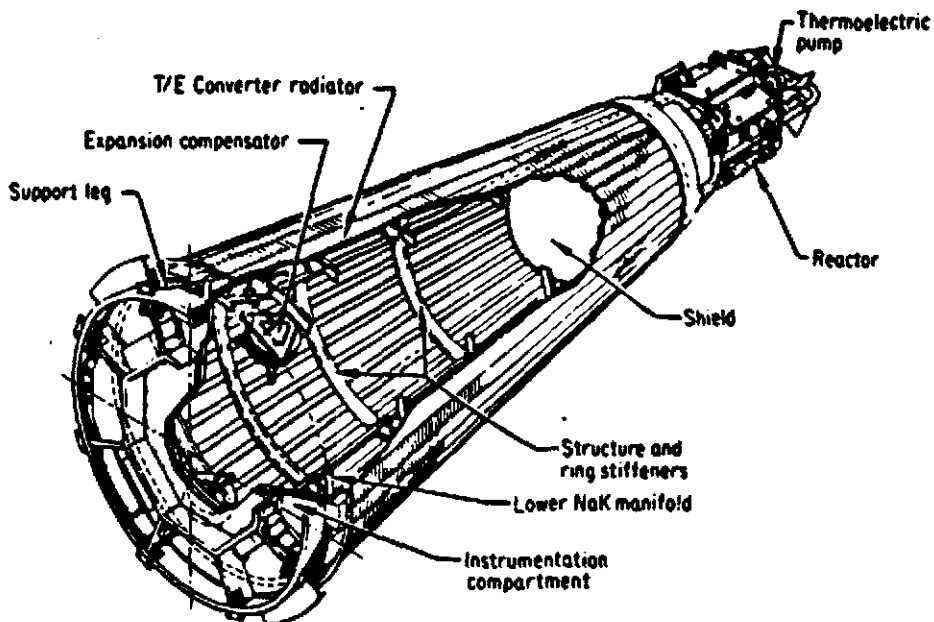


Figure 1.1. SNAP-10A Nuclear Space Reactor

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Current U.S. space reactor development effort is focused on the SP-100 reactor, a joint program of the Defense Advanced Research Projects Agency, the Department of Energy's Office of Nuclear Energy, and NASA's Office of Aeronautics and Space Technology [2,55]. The SP-100, as shown in Figure 1.2, is a thermoelectric reactor designed to generate 100 KW of electricity continuously for seven years. The SP-100 is a fast spectrum reactor, fueled with about 190 Kg of uranium nitride fuel enriched to an average of 96% U-235 and cooled by liquid lithium metal. The reactor core is small (less than 1 m³) [2].

Two types of nuclear power systems were implemented by the former USSR, "TOPAZ" and "TOPAZ-II" [7,52,56]. TOPAZ depends in its operation on multicell thermionic converters, while TOPAZ-II depends in its operation on single cell thermionic converters. The Soviets have sold TOPAZ reactors to the U.S. The former Soviet Union has moved far ahead of the U.S. in operational use of space nuclear power. TOPAZ thermionic reactors, each providing 10 Kw of power, were launched in 1987 into high orbits of about 800 naut. mi.

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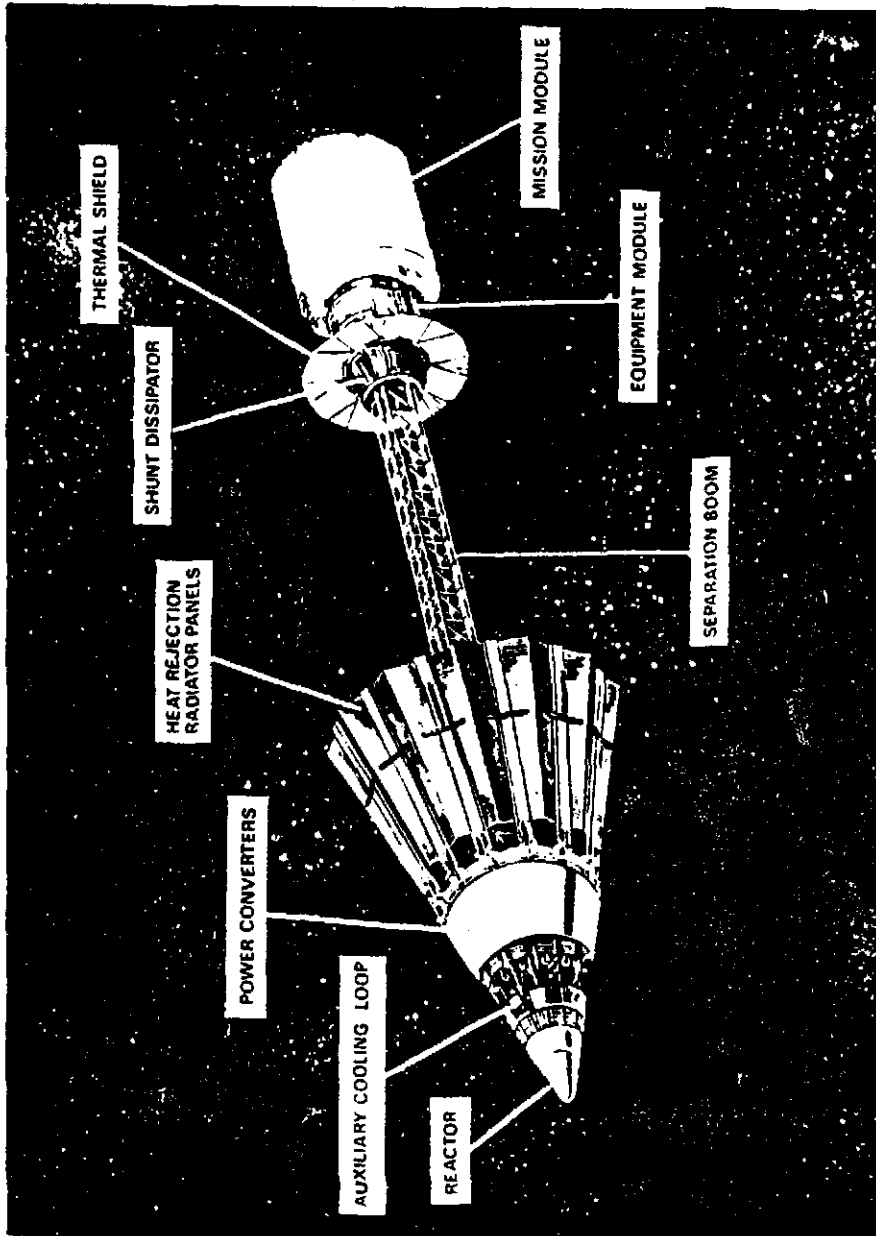


Figure 1.2 SP-100 reactor deployed configuration
(Source: Jet Propulsion Laboratory)

Most of nuclear space reactors depend in their operation on thermionic converters [1] because of the following advantages listed below:

1. No moving parts connected to the reactor and modular structure, which gives high reliability performance.
2. High rejection temperatures that allows a reduction in overall size of the power system.
3. The conversion of heat to electricity is of higher efficiency.
4. Quiet operation.

1.2 Thermionic Converter

1.2.1 Historical Introduction:

Thermionic emission phenomenon was first known by Edison in 1883, according to his patent application " I have discovered that if a conducting substance is interposed anywhere in the vacuous space within the globe of an incandescent electric lamp and said conducting substance is connected outside the lamp with one terminal, preferably the positive one of the incandescent conductor, a portion of the current will, when the lamp is in operation, pass through the shunt circuit thus formed, which shunt includes a portion of the vacuous space within the lamp. The current I have found to be proportional to the degree of incandescence of the

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1.2.2 Basic Physical Principles:

The thermionic conversion system is a device in which heat is converted directly to electricity. Thermionic conversion phenomenon is based on a device called a thermionic converter (see Figure 1.3) which consists of a metal surface connected to the heat source and a secondary surface acting as an electron collector. The emitter emits electrons upon heating by a heat source and all emitted electrons transfer through the interelectrode space between the emitter and collector. Upon reaching the collector surface, which is kept at a temperature lower than that of the emitter to prevent any back emission toward the emitter that may affect the output power and efficiency of the thermionic converter, the electrons condense and return to the hot electrode via the electrical leads and the electrical load connected between the emitter and the collector. The flow of electrons through the electrical load is sustained by the temperature difference between the emitter and the collector [1,4,9-14].

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Chapter 1

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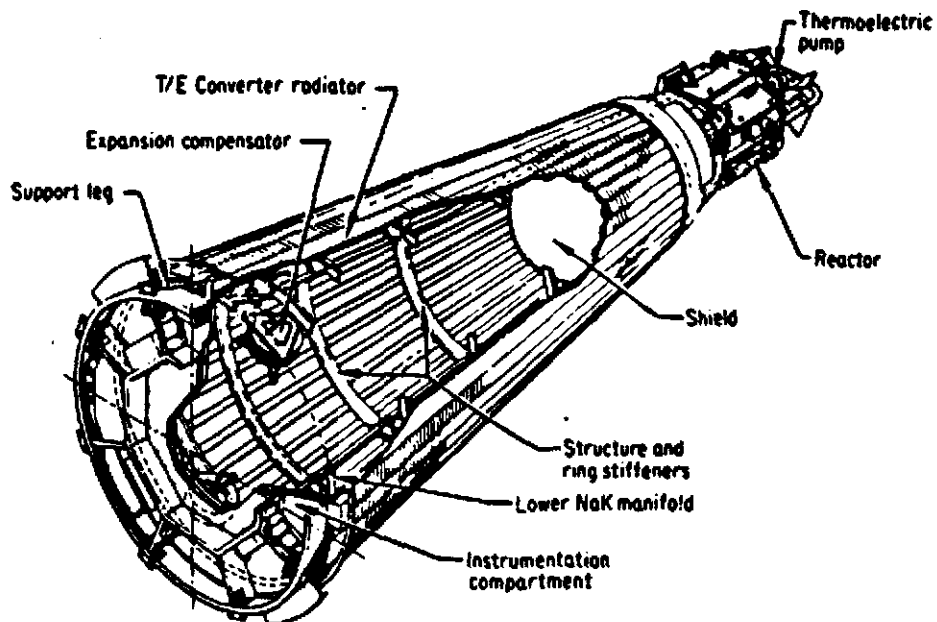


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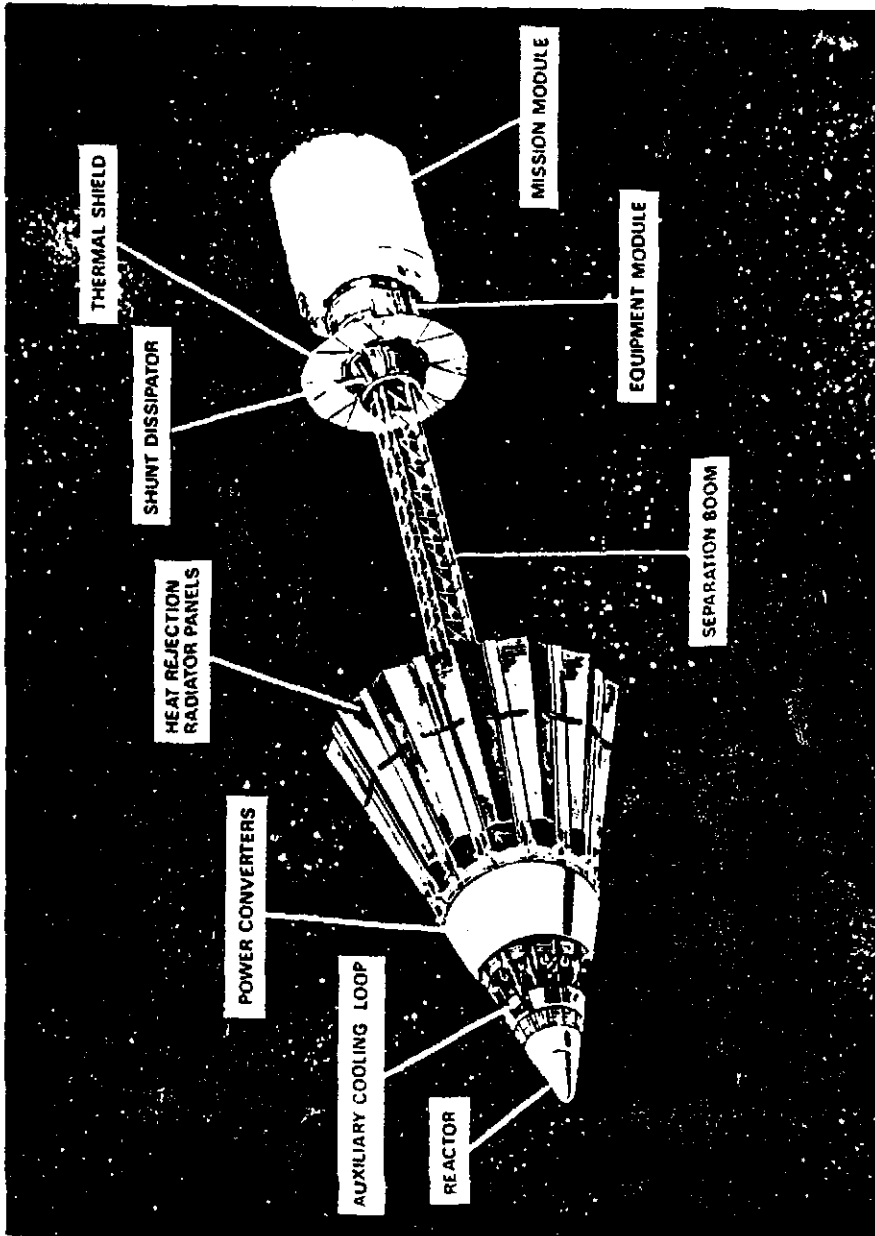


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To understand the operation of a thermionic converter, it is important to discuss several surface and solid phenomena, such as conduction electron energies, thermionic emission, and surface ionization; as well as space phenomena, such as negative space charge and plasma transport properties.

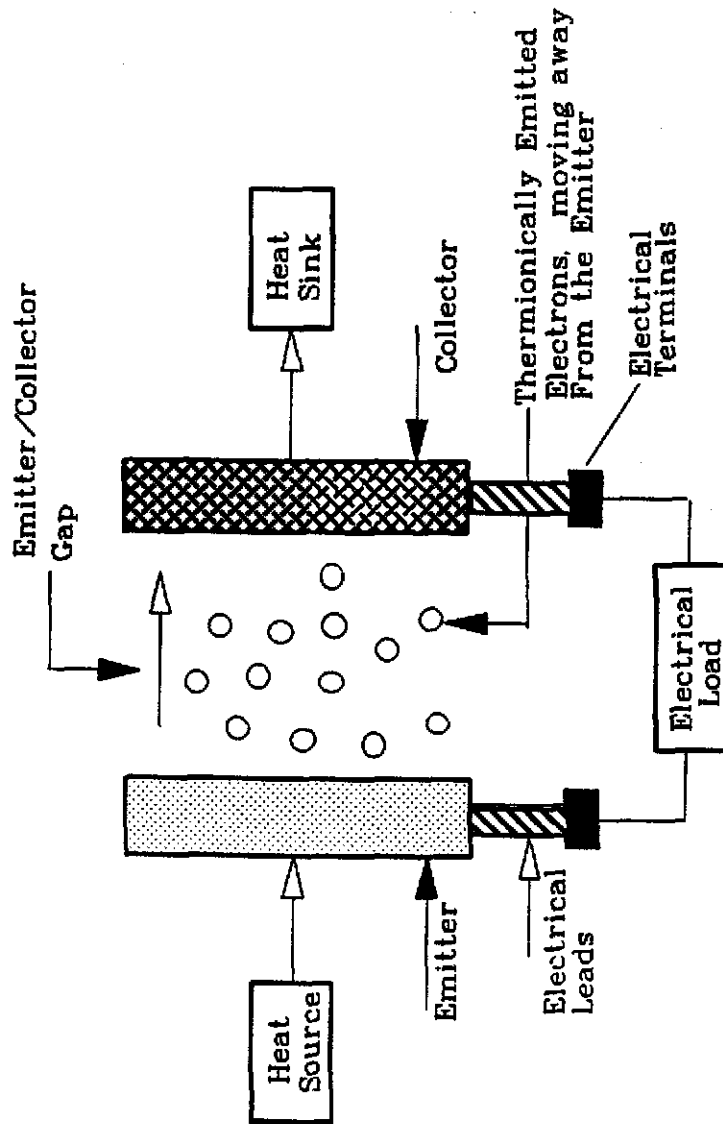


Figure 1.3 Thermionic Energy Converter

1.2.2.1 Solid Phenomena: The thermionic properties of any thermionic converter depend greatly on the crystallographical distribution of the surface of the emitter and the collector. The atom is made up of a positively charged nucleus surrounded by a different number of negatively charged electrons. The number of orbits and the number of electrons in each orbit depend actually on the type of the atom and consequently on the type of material. There are attractive forces between the nucleus and the surrounding electrons due to the opposite charges they carry. The valence (free) electrons are those types of electrons that are located usually in the outer or the far orbit from the nucleus so that they are weakly bound to the nucleus and free to move around inside the metal, while the nearby electrons are tightly bound to the nucleus. The valence (conduction) electrons are responsible for the mechanism of heat and electric conduction in metals. At the surface boundary, a potential energy barrier exists, since there are no positive ions on one side of the boundary to give the free electrons equal attractive forces. The electrons are attracted then by their image forces. The free electrons need more energy to boil them out of the metal into free space [9-14].

1.2.2.2 Surface Phenomena: The electron leaving a solid surface experiences a net positive charge inside the metal at the boundary. The electron needs energy to overcome the

potential barrier and to be released from the emitter surface. This needed energy must be equal to the work required to raise it from the Fermi level, which is the highest energy level occupied by free electrons at absolute zero temperature (0°K) at which none of the electrons can escape, to a point outside the metal. This energy is called the work function of the metal and varies according to the type of material and some other factors. The work function can also be defined as the energy required to overcome the force exerted on the electron from its image force of positive charge of magnitude e as shown in Figure 1.4. The work function of a material depends somewhat on the crystallographic face exposed. The work function for most materials falls in the range from 1 to 6 eV. At low temperatures, some electrons possess enough initial

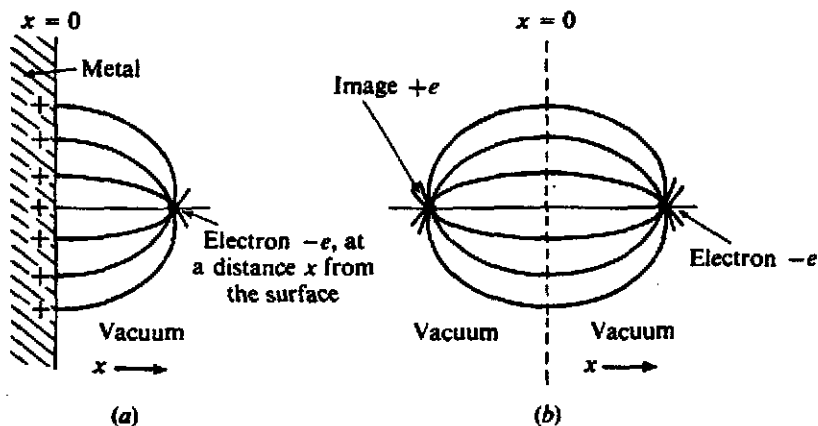


Figure 1.4 Image forces exerted on electron in surface metal [13].

kinetic energy to exceed the potential barrier of the emitter, which is equal to the product of the electron charge e and the work function in volts ($e\phi$ V), and get into the emitter-collector gap and reach the collector surface, while others do not. The situation is different at high temperatures due to an increase in the number of electrons that possess enough kinetic energy to leave the emitter surface.

The rate of electron emission is given by the Richardson-Dushman equation,

$$J = \frac{4\pi em_e k^2}{h^3} T^2 \exp \frac{-\phi}{KT} \quad (1.1)$$

where

J = Rate of electrons emitted in amp/cm²

e = Electron charge

m_e = Mass of electron (9.10909×10^{-28} gm)

h = Planck's constant (4.13576×10^{-15} ev sec)

T = Surface temperature, °K

ϕ = Work function, volt

K = Boltzman constant = 8.62×10^{-5} ev/°K

Equation 1.1 can be written as

$$J = AT^2 \exp \frac{-\phi}{kT} \quad (1.2)$$

where

$$\begin{aligned} A &= \text{Richardson's constant} \\ &= 4\pi em_e k^2 / h^3 \\ &= 120 \text{ amp/cm}^2 \cdot \text{K}^2 \end{aligned}$$

The Richardson-Dushman equation is only valid in a vacuum, and in a gas when the electron mean free path (mfp) is considerably greater than the distance from the emitter to the potential barrier [25]. The electrodes (emitter and collector) in a thermionic converter have different Fermi levels; the emitter has a low Fermi level whereas the collector has a relatively high Fermi level. The electron [13] in the emitter surface needs a larger energy to be lifted out of the emitter than would a corresponding electron to be lifted out of the collector. Thus the emitter work function is greater than the collector work function.

1.2.2.3 Space (Gap) Phenomena: There are two phenomena that better describe the operation of thermionic converters. The first one is the emission phenomenon which depends mainly on the emitter-collector materials, properties of the surface, and crystallographic structure of the surface. The second one is the transport phenomenon which describes the processes in which electrons migrate from the emitter and interact in the emitter/collector space.

In the interelectrode space between the emitter and the collector, the electrons (charged particles act as a working fluid in the emitter/collector space) are emitted from the

refractory metal that possesses a high electron emission rate (usually tungsten) and condense on the collector surface. The speed of these electrons is limited in which they take some time (in terms of nano-seconds) to reach the collector. During the electrons' travel, they form a cloud of free negative electrons called "negative space charge".

This cloud of electrons will repel electrons emitted later back toward the emitter unless they have sufficient initial kinetic energy to overcome the repulsion and reach the collector surface. There is no doubt that the negative space charge affects the output current and consequently the efficiency of the thermionic converter and some precautions must be taken to suppress the electrostatic effect of this negative space charge. The classification of thermionic converters is based mainly on the type of suppression of the negative charges. Suppression can be achieved by several methods. These methods are described as follows:

1.2.3 Close-Space Vacuum Thermionic Converter:

In a vacuum thermionic converter, heat is supplied to the emitter surface and some electrons gain energy that raise them up from Fermi level until they reach the minimum potential or the emitter work function, ϕ_E as shown in Figure 1.5. The electrons still need an extra potential to overcome the space charge potential barrier so that they may not return to the emitter surface. The potential required is $(V_E - \phi_E)$ which is

the potential difference between the top of the potential barrier [40] and the Fermi level of the emitter. Therefore the effective emitter (cathode) work function V_C is given by

$$V_E = \phi_E + V_{ES}$$

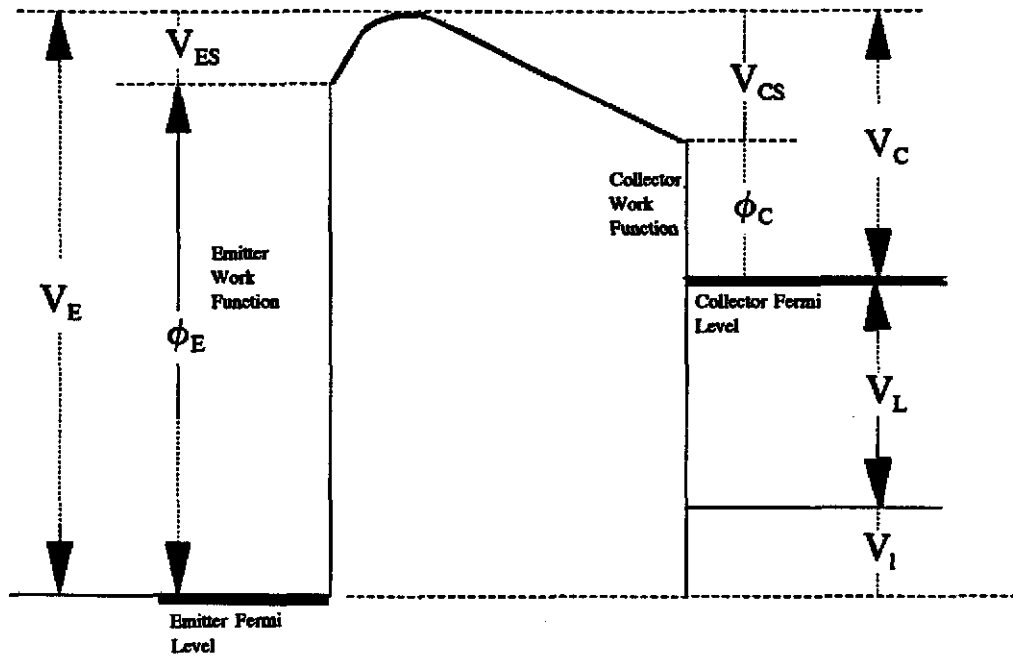


Figure 1.5 Potential diagram of a vacuum thermionic converter.

The electron that possesses a potential, equivalent to the effective work function, overcomes the hump or the potential peak and is accelerated towards the collector (anode) surface. Upon reaching the collector surface, the electron falls down on a potential energy scale by an amount equal to the work function of the collector surface and releases an effective collector potential V_C and an energy eV_C until it

reaches the collector Fermi level. This energy appears as heat in the collector surface and is given by

$$V_C = \phi_C + V_{Cs}$$

$$eV_C = e(\phi_C + V_{Cs})$$

It is extremely important that the collector work function should be smaller than the emitter work function to allow a net potential difference which can be connected to a useful load, V_L , between the emitter/collector surfaces. The energy loss through electrical leads, V_L , as a result of their electrical resistance should be subtracted from the useful (electrical) energy before reaching the emitter Fermi level.

The space between the two electrodes in a vacuum thermionic converter is very narrow so that no appreciable space charge can build up in the evacuated space between them. It has been found that a spacing of 0.001 cm (10μ) or less is standard for these types of converters (Figure 1.6) as was confirmed experimentally by Hatsopoulos and Kaye [14] in 1958. They obtained an estimated 12-13% efficiency at this spacing.

It has been concluded [1] that a close-space vacuum converter is not practical and has some disadvantages such as:

1. Difficulty of manufacturing prevents the attainment of interelectrode gap (spacing) of less than about 10μ .
2. No materials have been found to be usable as an emitter in a vacuum converter because all materials produce excessive evaporation which is not desirable because it (a)

limits the useful life of the emitter, (b) causes an electrical short between the emitter and the collector, and (c) alters the work function of the collector and makes it approach that of the emitter. All these undesirable effects can be avoided by introduction of a suitable rarefied vapor such as cesium.

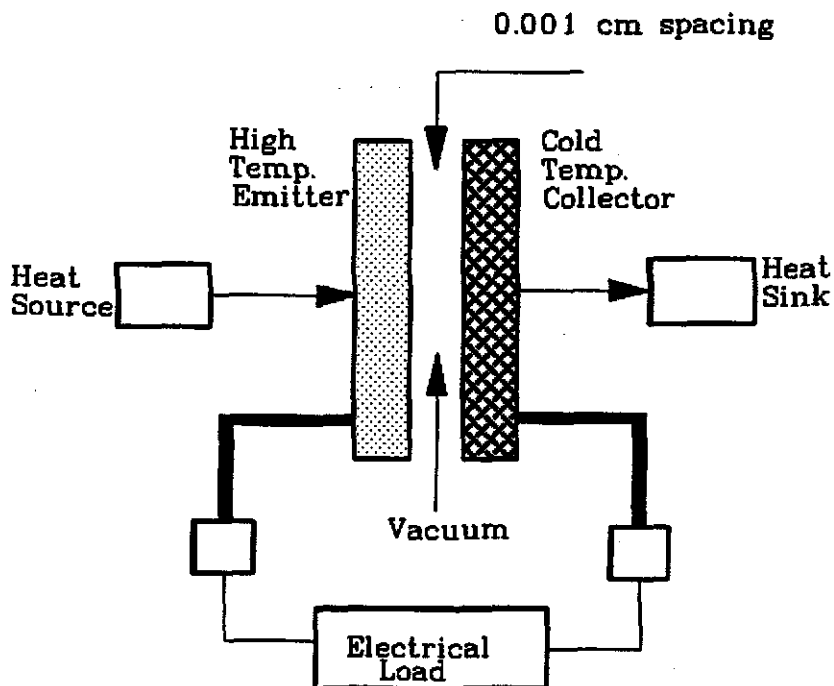


Figure 1.6 Close-space vacuum thermionic converter

1.2.4 Cesium Vapor Thermionic Converter:

The best way to overcome the negative space charge in the emitter/collector gap is to introduce a rarefied cesium vapor. The reasons for choosing this kind of vapor are because of 1)

its low ionization potential (3.89 eV), lower than that of the emitter, to completely neutralize the cesium atoms which impinge on the emitter surface and lose their outermost electrons then evaporate as positive ions, and 2) it is the most easily ionizable of all the stable gases. (see Figure 1.7).

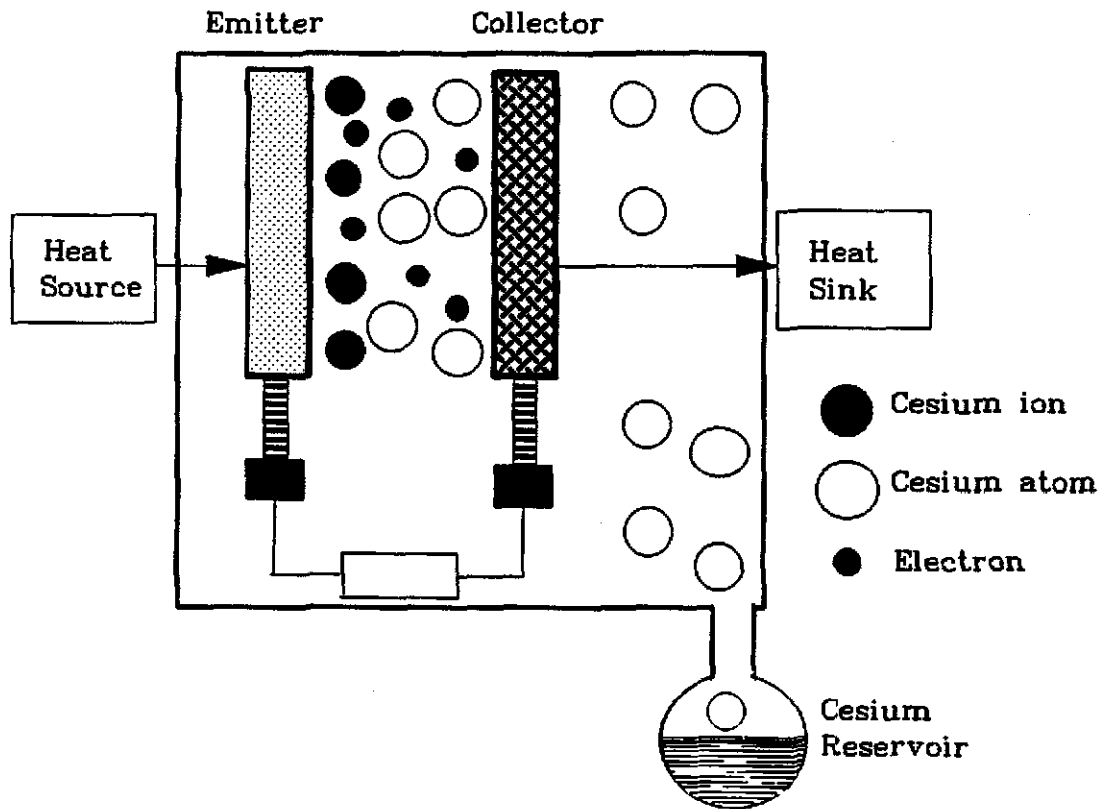


Figure 1.7 Cesium Thermionic Converter

The cesium atoms will be partially ionized when touching the hot emitter surface and consequently some ions are formed. The positive charge of the cesium ions will neutralize the

negative charge of the electron cloud.

There are two modes for the operation of thermionic converters. These modes are 1) ignited (ball of fire) mode and 2) unignited mode. In the latter, a cesium atom comes into contact with a hot surface (contact ionization) if the ionization potential of the atom is lower than the work function of the surface. The valence electron of the gas atom detaches from the atom and attaches instead to the surface material. If the surface is hot enough, the electron is then emitted, and an electron ion- pair are produced at the surface. The plasma (a mixture of positive and negative charged particles) is maintained entirely by thermionic emission of positive ions from the emitter. The rate of production depends mainly upon the cesium vapor pressure, which in turn depends upon the cesium reservoir temperature. It has been found that for the most effective rate of electrical power the emitter temperature must be at least 3.6 times the cesium reservoir temperature [9,33,47]. The motive diagram for the unignited plasma is shown in Figure 1.8. In the unignited mode, at low cesium vapor pressure (10^{-4} mm Hg), the mean free path of electrons in the emitter/collector gap is larger than the gap itself so the inelastic collisions are negligible. Also the negative space charge is partially neutralized, while at high cesium pressure, where the collisional processes are considered, it is completely neutralized. This mode of operation is impractical because 1)

it requires high emitter surface temperatures (>1900 °K) that may cause some metallurgical problems and 2) the output power densities and currents are small.

In the ignited mode as illustrated in Figure 1.9, part of the electric power generated by the converter [33] is dissipated internally in the interelectrode gas by collisional processes. This mode of operation is more efficient than the unignited mode because of the high power densities output and efficiencies. The cesium vapor pressure is relatively high (1 mm Hg or higher) and the electron collisions are taken into consideration. The electron mean free path is much smaller than the emitter/collector space. The majority of all thermionic converters in operation today operates in the ignited mode [13]. The so called ball of fire mode refers to an external power source, whereas the arc, or ignited, mode refers to internal heating by the emission current. This mode of operation can be classified into two regions: one of bright plasma and the second of dark plasma. In the dark region the electrons do not possess enough energy to ionize significant number of cesium atoms but neutralization occurs due to the ion flow from the bright region which is caused by the inelastic collisions. Ions produced in this mode are capable not only of neutralization of cesium vapor, but also of producing a strong positive space charge. The ideal performance in the ignited mode can be achieved by firstly complete reduction of the negative space charge and secondly

by reduction of the large internal voltage drop. This reduction as shown in Figure 1.10, is simply to minimize the product of the cesium vapor pressure times the emitter/collector gap.

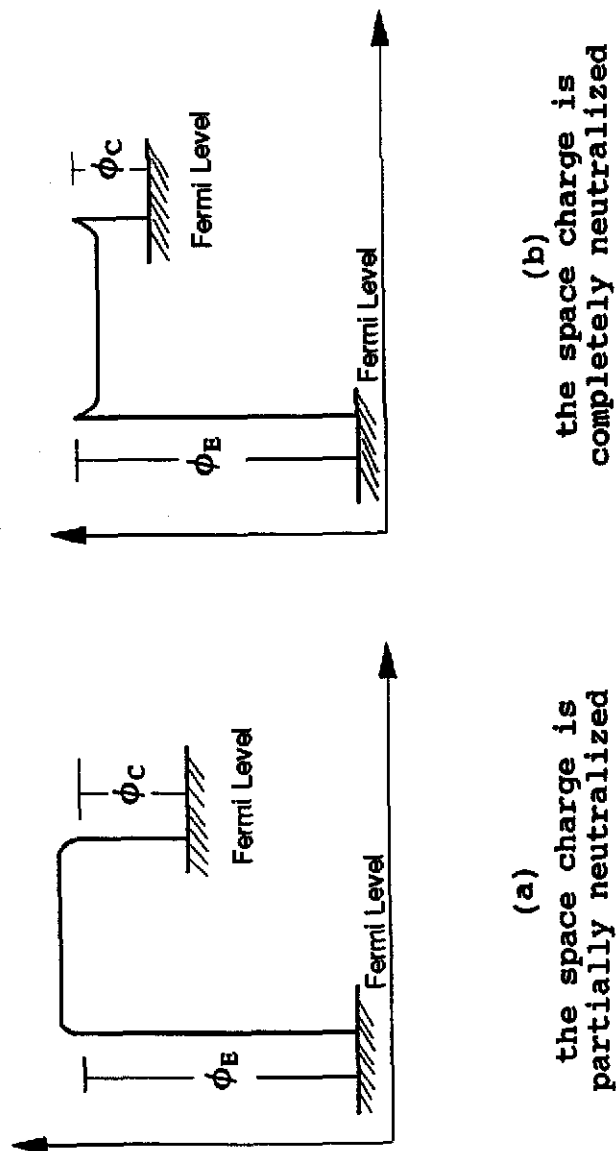


Figure 1.8 Motive Diagram (Unignited mode)

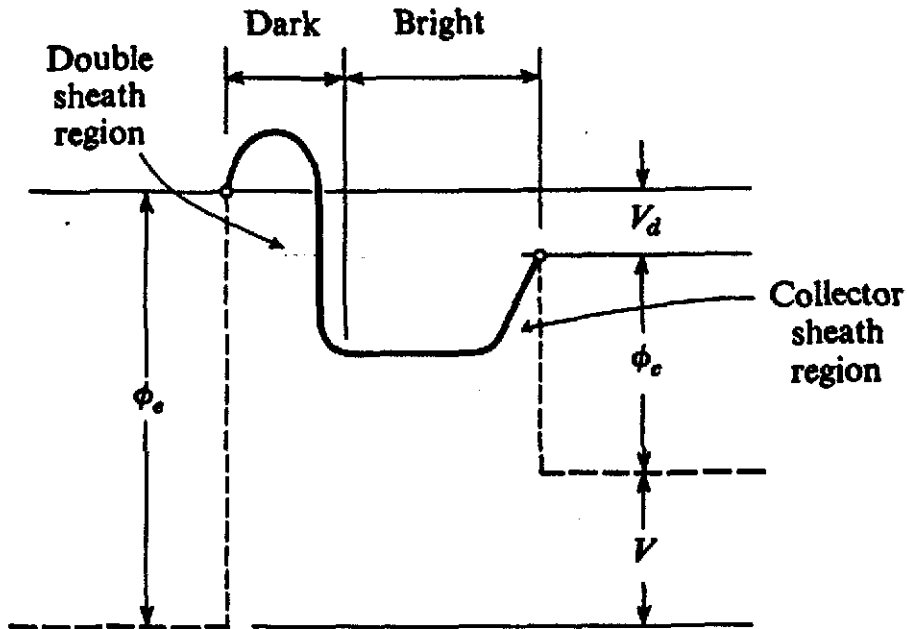


Figure 1.9 Motive Diagram (Ignited mode) [15]

1.2.5 The Ideal Thermionic Converter:

The ideal thermionic converter assumes that there is no negative space charge that may affect the transmission of electrons from the emitter to the collector. The potential between the barrier heights of the electrodes (emitter and collector) must be continuous [33]. The motive diagram for the ideal diode thermionic converter is illustrated in Figure 1.10. For an electron to move into the interelectrode gap, it

must experience forces that overcome the potential energy barrier or the emitter work function ϕ_E . An energy barrier $V + \phi_C$ must be overcome to allow an electron to move into the gap and reach the collector surface when the electrode potential energy difference (output voltage) V is greater than the contact potential energy difference $V_0 = \phi_B - \phi_C$. When V is less than V_0 , a barrier ϕ_E must be overcome. Neglecting electron emission from the collector, the output current density of the ideal diode thermionic converter is given by the Richardson-Dushman equation:

$$J = AT_E^2 \exp\left(-\frac{V + \phi_C}{kT_E}\right) \quad \text{for } V > V_0 \quad (1.3)$$

$$J = AT_E^2 \exp\left(-\frac{\phi_E}{kT_E}\right) \equiv J_{s_e} \quad \text{for } V < V_0 \quad (1.4)$$

where J_{s_e} is the saturation current density for the emitter

The total heat that must be supplied to the emitter is

$$q_E = q_c + q_r + q_d$$

where

$$q_c = J(\phi_E + 2kT_E) = \text{Emitter electron cooling}$$

$$q_r = \sigma \varepsilon (T_E^4 - T_C^4) = \text{Heat removed by radiation}$$

$$q_d = \text{Heat conducted down the emitter lead}$$

The optimum ideal performance for the ideal thermionic converter depends mainly on the optimum choice of thermionic properties values that allows the attainment of the maximum possible ideal efficiency [1]. Emitter temperatures between about (1500 to 2000 °K) define the region of most attractive operation of ideal thermionic converter. It has been found that [1] at an emitter temperature of 2300 °K, the output current density is about 100 amp/cm² which seems attractive but in reality it is impractical because of the difficulty of handling high current densities and because of the extreme difficulty and expense of operating the heat source at very high temperatures. An ideal current between 5 and 50 amp/cm² can be achieved in the presence of suitable materials. The heat radiation flux term, Q_{rad} , reduces the efficiency of the ideal thermionic converter at higher temperatures because the emissivity of refractory metals increases with temperature. The optimum emissivity value falls in the range (0.1 to 0.2). The <0.1 emissivity is not maintainable and >0.2 emissivity is not desirable [1,25]. For the collector work function, ϕ_c is restricted to values greater than about 1.5 ev. The collector temperature should not exceed 1000 °K. At the same time the collector temperature can not be taken at very low temperatures because of the need to reject heat at a reasonable temperature level.

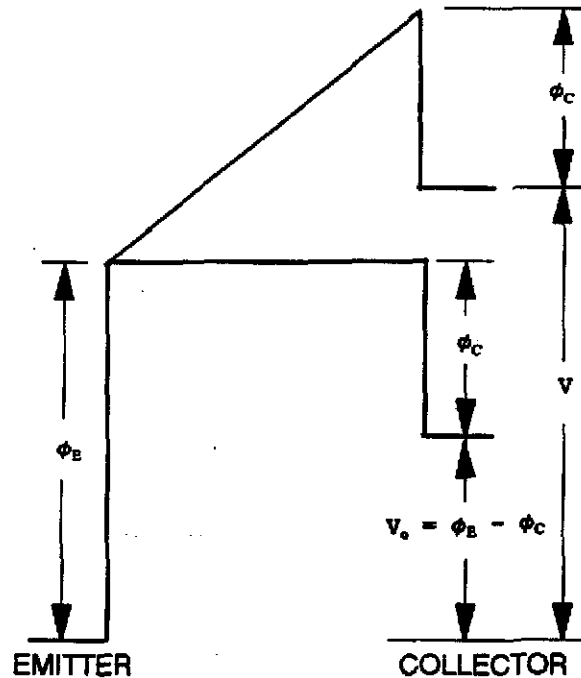


Figure 1.10 The ideal Motive Diagram of Thermionic Converter.

1.2.6 Heat Sources:

The emitter in a thermionic reactor needs to be heated in order to emit electrons into the emitter/collector gap. There are many kinds of heat sources that may be of use for this purpose. The choice of the heat source depends mainly on the type of application, time of operation, space, cost, and several other factors.

For thermionic converters, there are three kinds of heat sources to be listed as: 1) Chemical source; 2) Solar source; and 3) Nuclear source.

1. Chemical source: Fossil fuel can be used but can not be recommended as a heat source for thermionic reactors due to the following deficiencies:

- a. Large mass that takes large space which is not desirable for space applications.
- b. Limited life due to the fast rate of burn-up of the chemical feed stock.
- c. Regular maintenance is always needed to avoid poisoning converter elements by their products and corrosion.
- d. Ventilation is required to expel the undesirable smoke into space which may, in turn, cause some hazards.

2. Solar source: Solar energy is a very cheap source of energy and is not life-limited as in the case of chemical source. Parabolic reflectors are required to concentrate the heat on the emitter surface. This type of heat sources is not practical due to its high cost and large size.

3. Nuclear source: Nuclear fuel is the most efficient source of energy for thermionic reactors for several considerations:

- a. Long life in space due to the long half live of uranium-235 (i.e., 7.13×10^8 years). The fuel burn-up rate is so small because the electrical power produced in thermionic systems is so small.
- b. Low maintenance requirements due to the safety precautions for these types of reactors. In the case of any unexpected failure in the operating system, the shut down and emergency systems

overcome the problem.

- c. Small size core. The fission of a single uranium-235 nucleus is accompanied by the release of about 200 MeV of energy, while the energy released by a combustion of one carbon-12 atom is 4 ev. Hence, the fission of uranium yields something like 3 million times as much energy as the combustion of the same mass of carbon. In other words, the energy produced by 1 kg of uranium is equivalent to the energy produced by 2,700 metric tons of coal[57].

The only disadvantage of a nuclear fuel is the requirements for heavy masses of shielding to prevent any radioactive release in space.

1.2.7 Efficiency:

The efficiency of a thermionic converter depends on many factors such as: 1) The temperature of the emitter and collector, 2) The cesium reservoir temperature, 3) The type of materials used as emitter or collector, 4) The suppression of the negative electron space charge, 5) The pressure of the cesium vapor, 6) The work function of both the emitter and the collector, 7) The size of the emitter/collector gap, 8) emissivity characteristics of the emitter and collector surfaces, 9) The electrical power output, and finally 10) the impurities on the emitter and collector surfaces [1]. The

efficiency can be defined as the electrical power output per unit area of emitter divided by the emitter heat input per unit area of emitter.

$$\text{The power output} = (J_E - J_C) (V_E - V_C)$$

where

J_E = Emitter current density (amp/cm²).

J_C = Collector current density (amp/cm²).

$(J_E - J_C)$ = Net current flow between emitter and collector (amp/cm²).

$(V_E - V_C)$ = Output voltage (volt).

The efficiency of thermionic converter can be given as

$$\eta = \frac{(J_E - J_C) (V_E - V_C - V_L)}{Q^{Rad} + Q^k + [Q_L - \frac{Q_d}{2}] + Q^{EC} - Q^{CH}} \quad (1.5)$$

where

Q^{Rad} = Radiation heat flux (watt/cm²).

Q^{EC} = Emitter electron cooling (watt/cm²).

$$= J_E (eV_E + 2kT_E)$$

Q^{CH} = Collector electron heating (watt/cm²).

$$= J_C (eV_C + 2kT_C)$$

Q^k = Heat conduction through cesium and structural components. (watt/cm²).

V_L = Voltage drop across the leads (volt).

$(Q_L - Q_d/2)$ = Heat conduction through electrical leads (watt/cm²).

$Q_d/2$ = One half of the Joulean heat generated in the leads that transfers back to the emitter.

The emitter surface temperature is very high with respect to the collector surface temperature so the current flow towards the emitter is very small because the back emission of electrons is very small so that it can be negligible (i.e. $J_e = 0$) so that the net current is J_E . Equation 1.5 can be rearranged and written as

$$\eta = \frac{J_E V}{Q^{Rad} + Q^{EC} + Q_k + [Q_L - \frac{Q_d}{2}]} \quad (1.6)$$

where

$$V = V_E - V_C - V_L$$

$$J = J_E$$

If the voltage drop across the leads is considered small, one can play with equation (1.6) by variation of many parameters. For example, if $V_E = V_C$, that leads to zero efficiency. As V_C is lowered, η increases until, at some point, the collector begins to back-emit. The efficiency goes through a maximum [25] at the V_C value given by $(V_C = V_E T_C/T_E)$. At this optimum value of V_C the back emission is

$$J_a = \left(\frac{T_C}{T_E}\right)^2 J_E \quad (1.7)$$

If V_C is lowered further, the back emission rapidly increases, and η falls to zero when $J_C = J_E$.

1.2.8 Heat Transfer in the Emitter/Collector Gap [1]:

As shown in Figure 1.11, energy is transferred away in the radial direction from the emitter surface by the following three modes:

1. Heat conduction rate through the following media:

a. Heat conduction rate, $(Q_L - Q_d/2)$ through the leads connected to the emitter and collector is:

$$Q_L = k_L \frac{S_L}{l_L} (T_E - T_C) \quad (1.8)$$

where k_L , S_L , and l_L are the thermal conductivity, the cross-sectional area and the length of the electrical leads respectively.

$$-\frac{1}{2} Q_d = -\frac{1}{2} S J V_L \quad (1.9)$$

where

Q_d = The Joulean heat rate

V_L = The voltage drop across the leads.

- b. Heat conduction rate through the cesium vapor. Let Q_C be the heat conduction rate through the cesium vapor.
- c. Heat conduction rate through the structural components.

Now, let Q_{k1} be the heat conduction rate through the structural components connected to the emitter.

The total heat conduction rate through the gap is given by:

$$Q_k = Q_{k1} + Q_{CS} = g_k (T_E - T_C) \quad (1.10)$$

where g_k is the sum of the thermal conductances g_{k1} of structural materials connected to the emitter and g_v of the vapor.

2. Thermal radiation rate, Q_r

$$Q_r = S \sigma_0 \epsilon (T_E^4 - T_C^4) \quad (1.11)$$

where σ_0 is the Stephan-Boltzman constant (= 5.67×10^{-12} watt/cm²-k⁴) and ϵ is the net effective thermal emissivity.

3. Electron cooling rate, Q_E :

- a. The Energy flux associated with electrons travelling from the emitter to the collector is

$$S J_{EC} \frac{\psi_{\max} + 2kT_E}{e} \quad (1.12)$$

where Ψ_{\max} is the maximum value of the interelectrode motive.

- b. The Energy flux associated with electrons returning to the emitter through the electrical load is given by:

$$-SJ_{EC} \frac{\mu_E}{e} \quad (1.13)$$

- c. The energy flux associated with electrons flowing from the collector to the emitter in the emitter/collector gap is given by:

$$-SJ_{CE} \frac{\Psi_{\max} + 2kT_c}{e} \quad (1.14)$$

- d. The energy flux associated with electrons leaving the emitter through the electrical load is:

$$SJ_{CE} \frac{\mu_E}{e} \quad (1.15)$$

Thus the electron cooling rate, Q_E is:

$$Q_E = \frac{SJ_{EC}(\Psi_{\max} - \mu_E + 2kT_E) - SJ_{CE}(\Psi_{\max} - \mu_E + 2kT_C)}{e} \quad (1.16)$$

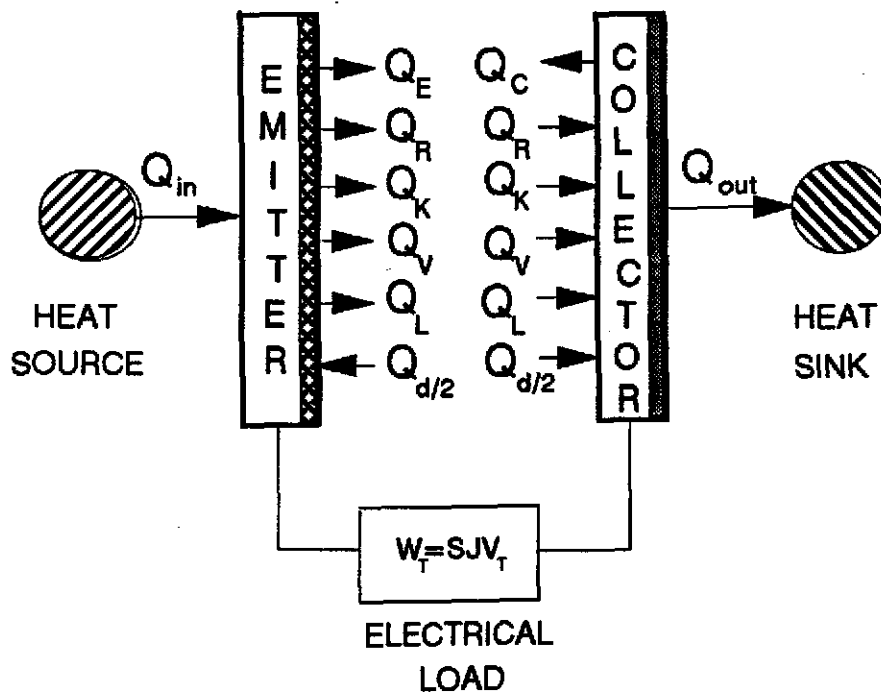


Figure 1.11 Energy Transfer Modes in a Thermionic Converter

1.3 Thermionic Fuel Element (TFE)

Thermionic fuel elements are used extensively in nuclear space reactors for power generation purposes. The heat source in the TFE is the nuclear fuel. The fuel is completely enclosed by the emitter material (Figure 1.12), and waste heat is removed from the collector by fluid convection.

Thermionic fuel elements (TFEs) for incore reactors can be either multicell or single cell. In the multicell type, also known as flashlight, all the thermionic cells are grouped in thermionic fuel elements. In the single cell configuration,

the thermionic converter is enclosed in the TFE. Single fuel elements have many advantages:

1. Simulation task is possible due to using an electrical heater instead of nuclear fuel for ground base tests before launching to space.
2. Simplicity of removing gas fission fragments from fuel elements.
3. Possibility of additional TFEs in a fully assembled reactor [1].

The various components of a typical TFE include:

a. **Void:** The void is located at the center and extended along the axial direction of the TFE. It serves as a vent to expel the fission gas products which arise from the nuclear fission process in the nuclear fuel during operation. These may have an effect on the life span of the TFE. It also prevents any swelling in the fuel that may arise from trapping of fission products in the fuel lattice. Densification of fuel during reactor operation, when the fuel temperature reaches a maximum, can be prevented due to the existence of the void. The size of the void is directly proportional to the size and weight of the fuel.

b. **Fuel:** The heat source used in the TFE is uranium dioxide enriched with 95% uranium 235. The nuclear fuel used in the TFE has the following advantages:

1. High density (advantageous for size reduction of

reactor in space applications).

2. Solidarity and durability at high operational

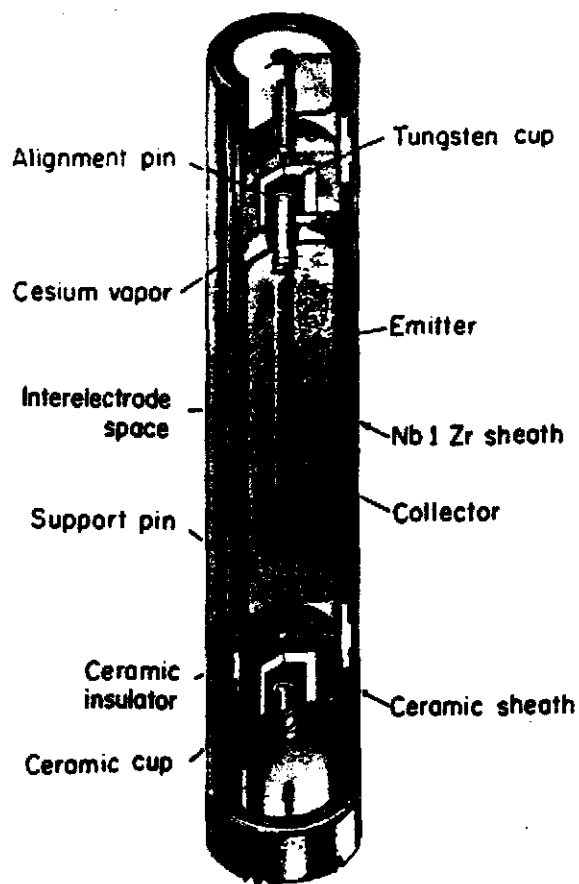


Figure 1.12 Thermionic Fuel Element

temperatures(due to the ceramic composition).

3. Low neutron absorption cross section of

oxygen that prolongs the life time of the fuel.

4. Excellent chemical and mechanical integrity.

c. **Emitter:** The emitter in this design is adjacent to the fuel so that there is no fuel/emitter gap. Heat is transferred directly from the fuel to the emitter by the conduction mode.

The emitter is a refractory metal made of tungsten (W) material that is being used in many thermionic reactors for the following considerations:

1. High melting point (3700 °K). This high temperature is compatible to the fuel melting point temperature and is of great importance in case of the loss of flow accident (LOFA) in which all thermionic parts and reactor components can be prevented from any expected damage in case of fuel melt down.
2. High electron emission at higher temperatures (1900 °K). The higher the emitter temperature the higher the emission rate and the higher the reactor efficiency and the higher the reactor power output.
3. High work function.
4. Low emissivity rate that reduces the transferred heat loss by radiation.

Unfortunately, most of the tungsten isotopes are highly neutron absorbing materials and are not recommended for use in

thermionic reactors due to the reduction of the fuel life and minimization of the reactor efficiency. Fortunately one isotope (^{184}W) is exceptional [47] due its low neutron absorption advantage. Hence the emitter should be highly enriched with this isotope. The only disadvantage is the fabrication cost but it is worthy for the benefits.

d. Emitter/Collector gap: The gap is filled with cesium vapor that neutralizes the negative charge and eases the transportation of emitted electrons from the emitter to the collector. It is considered to be the most important region in the TFE through which many energy transformations take place.

e. Collector: The collector works as a sink to collect the emitted electrons from the emitter. The collector material is made of niobium which has a low work function. This work function is lower than that of the emitter and is kept at low temperature lower than that of the emitter.

f. Insulator: The insulator sheath is made of Al_2O_3 to electrically insulate the collector and prevent any current leakage that may affect the efficiency of the thermionic converter. Also, the insulator in a thermionic converter should be a good heat conductor.

g. Cladding: To prevent any discharge of radioactive materials during the reactor operation. The cladding is usually made of niobium.

h. Coolant: The liquid metal coolant keeps the thermionic fuel element temperature within safe limits. It flows along

the outside axial length of the cladding. The coolant used is eutectic NaK (78% K) which 1) possesses a very high thermal conductivity to transfer more heat from the contiguous surface of cladding and 2) has a wide useful range of temperature in the liquid phase. The 22% sodium in the coolant prevents any corrosion that may arise from any adjacent surface due to the long operation in space.

i. **Liner:** The main purpose of the liner is to retain the liquid metal coolant from discharging outside the TFE. The liner is made of stainless steel that withstands the elevated temperatures. It also protects the ZrH block (moderator) from the coolant.

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Chapter 2

Theory

2.1 Introduction

The temperature distribution throughout a thermionic fuel element (TFE) is a function of many factors:

1. The location of the node point along the radial and axial positions in the TFE. There are different materials which have different thermal conductivities and specific heat terms.
2. There are some nodes which lie on the interface between two layers, in this case, any temperature dependent physical properties terms can be averaged.
3. The thickness of each layer as well as the number of regions in each material (see Table 2.1).

A steady state computer code (TFEHX) for calculating the steady state temperature distribution along the axial and radial directions has been developed. The TFEHX computer code is one of the most complete descriptions of a thermionic system in existence, and the first combined thermionic-thermal-neutronic code developed in the United States [7]. This code needs to be developed to accommodate the transient thermalhydraulic behavior of the TFE. This task was accomplished using TFETC (Thermionic Fuel Element Transient

Code) which is a newer version of TFEHX that has been developed by the author of this thesis. The heat transfer mechanism varies throughout the TFE according to the physical properties of materials from region to region. Also the emitter/collector gap has a great effect on the heat transfer mechanism as well as the liquid metal coolant which is adjacent to the cladding surface. All these modes of heat transfer need to be taken care of by introducing a suitable partial differential equation.

Table 2.1 Thermionic Fuel Pin Parameters

Region	Inner Radius (cm)	Outer Radius (cm)	Thick- ness (cm)	Mater- ial
Fission Gas Plenum	-----	0.15	0.15	Void
Fuel	0.15	0.60	0.45	UO ₂
Emitter	0.60	0.75	0.15	Tungsten
Gap	0.75	0.80	0.05	Cesium Vapor
Collector	0.80	0.90	0.10	Niobium
Insulator	0.90	0.95	0.05	Al ₂ O ₃
Cladding	0.95	1.00	0.05	Niobium
Coolant	1.00	1.25	0.25	NaK (Eutectic)
Liner	1.25	1.255	0.005	Stainless Steel

The unsteady state nonhomogeneous heat conduction partial differential equation (equation 2.1) is required and suitable for solving the temperature distribution along the TFE pin.

$$\nabla \cdot k(r, z, t) \nabla T(r, z, t) + g(r, z, t) = \rho(r, z, t) C_p(r, z, t) \frac{\partial T(r, z, t)}{\partial t} \quad (2.1)$$

where

k = Thermal conductivity of a material in the TFE, W/m. $^{\circ}$ K.

C_p = Specific heat of a material in the TFE, J/Kg. $^{\circ}$ K.

ρ = Density of a material in the TFE, Kg/cm 3 .

g = Rate at which heat is generated in the fuel, watt.

T = Temperature at any point in the TFE, $^{\circ}$ K.

t = Transient time of reactor operation, sec.

Some physical properties such as thermal conductivity, density, and specific heat are location and time dependent and need to be determined at various temperatures. For some solid materials such as fuel, emitter, collector, and insulator the density has to be constant for each material (i.e., does not vary with temperature variation) and that is true due to the fact that thermal expansion for solids is very small. The exceptional case is for a coolant (NaK) in which the density

changes at different temperatures. On the other hand, thermal conductivity and specific heat differ with temperature variation and should be calculated for all time steps as a function of temperature.

2.2 TFE Configuration

Figure 2.1 shows the top view of the TFE. The detailed description of all regions of the TFE is presented in chapter 1 of this thesis. The following describes the regions at which the only effective heat transfer mechanism is conduction.

These regions are:

1. Fuel/fuel interface.
2. Fuel/emitter interface.
3. Collector/insulator interface.
4. Insulator/cladding interface.

The effective heat transfer mechanism in the cladding/coolant interface is convection. The most important modes of heat transfer that play an important role in the TFE operation are the ones that lie in the emitter/collector gap. The energy is transferred away from the emitter surface to the collector surface in the positive r-direction by the following three modes [4]:

1. Thermal conduction of cesium vapor.
2. Thermal radiation between the emitter and the collector.

3. Thermionic heat transfer processes which include:
- a. Energy transferred away by the emitted electrons which is greater than that converted into electricity.
 - b. Thermal radiation from the ignited cesium plasma back to the emitter surface.

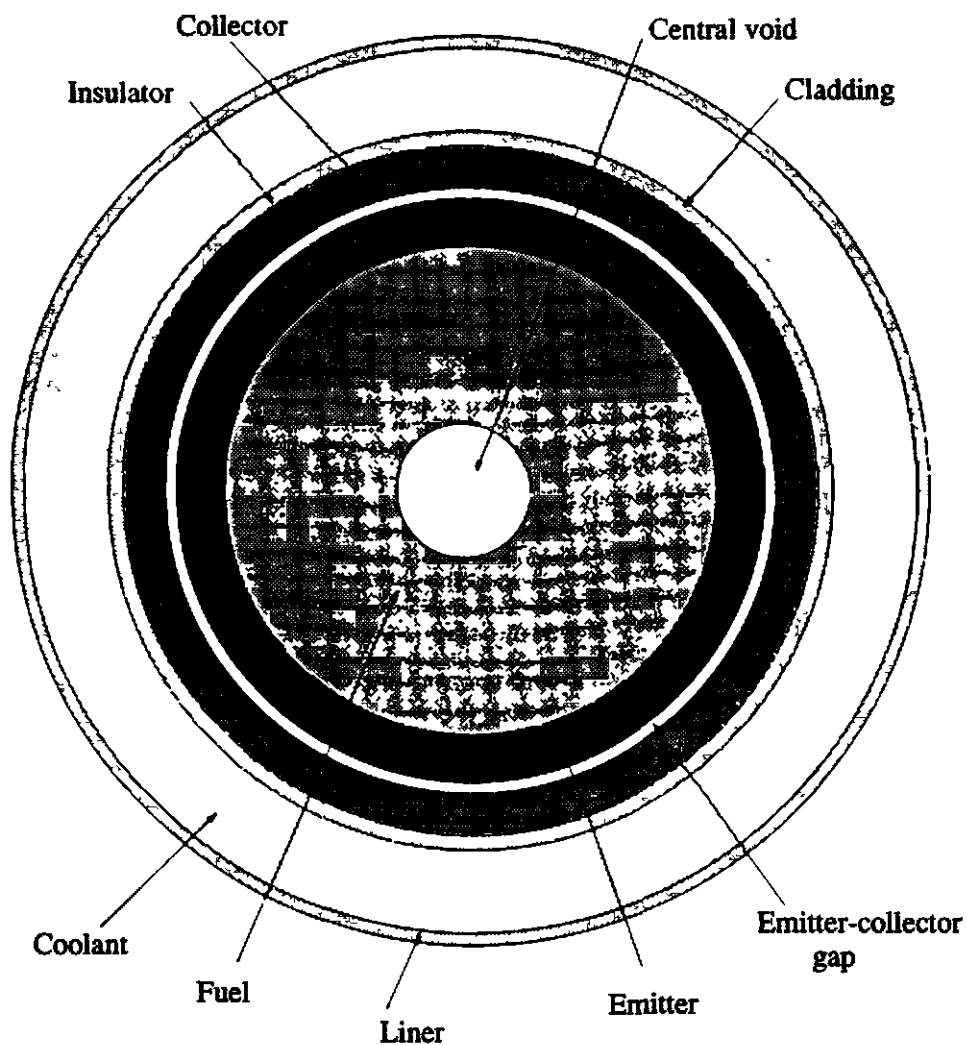


Figure 2.1 TFE Configuration

For the heat conduction flux through cesium vapor across the emitter/collector gap, a Kitrilakis and Meeker correlation [5] is used as follows:

$$Q_k^{cond} = \frac{k_{Cs}(T_{e,k} - T_{c,k})}{d + 1.15 \times 10^{-5} \frac{(T_{e,k} - T_{c,k})}{P_{Cs}}} \left[2\pi r_e \frac{(Z_{k+1} - Z_{k-1})}{2} \right] \quad (2.2)$$

where

$T_{e,k}$ = Emitter temperature (°K).

$T_{c,k}$ = Collector temperature (°K).

k_{Cs} = Thermal conductivity of cesium vapor,
W/cm.°K.

P_{Cs} = Pressure of cesium vapor at a cesium reservoir
temperature (torr).

r_e = Emitter outside radius, cm.

d = Emitter/collector gap, cm.

The pressure p_{Cs} is given by the following correlation:

$$P_{Cs} = 2.45 \times 10^8 \frac{\exp\left(\frac{8910}{T_r}\right)}{\sqrt{T_r}} \quad (2.3)$$

The thermal radiation term Q^{Rad} between the emitter and collector is given by the following equation:

$$Q_k^{Rad} = \sigma \epsilon_e F_{e-c} (T_{e,k}^4 - T_{c,k}^4) \left[2\pi r_e \left(\frac{Z_{k+1} - Z_{k-1}}{2} \right) \right] \quad (2.4)$$

where

σ = Stefan-Boltzman constant (5.67×10^{-12} Watts/cm²°K⁴)

ϵ_e = Thermal emissivity of the emitter surface.

F_{e-c} = View factor from the emitter surface to the collector surface ($F_{e-c} = 1$ for the emitter surface).

The electron cooling energy transfer term Q_k^{EEC} is computed using the TECMDL computer code [8] and can be given by:

$$Q^{EEC} = J_E \left(V_E + 2 \frac{kT_E}{e} \right) \quad (2.5)$$

where

J_E = Current density of the emitter surface, amp/cm².

V_E = Voltage across the emitter surface, volt.

T_E = Emitter temperature, °K.

k = Boltzman constant = 8.62×10^{-5} ev/°K.

For the thermalhydraulic transient calculations of the TFE, the TFETC is modeled to accommodate three different situations namely:

1. Start up.
2. Loss of Flow Accident.
3. Shut down.

2.2.1 start up

The reactor thermal power (P_{th}) is assumed to rise exponentially with time as follows:

$$P_{th} = P_{ss} \cdot [1 - e^{(-t/\tau)}] \quad (2.6)$$

where

P_{th} = Thermal power during start up, watt.

P_{ss} = Steady state power, watt

t = Transient time for start up, sec.

τ = Power rise coefficient, sec.

There are four different cases in which the thermal power rises until it reaches the steady state value. These values are:

1. $\tau = 100$ sec.
2. $\tau = 300$ sec.
3. $\tau = 600$ sec.
4. $\tau = 1200$ sec.

2.2.1.1 Helium Heating:

Thermal conductivity of helium is relatively high compared to cesium so it can be used as a heating element in the emitter/collector gap to speed up the heating process. At a certain temperature, around 900 °K, the helium heating is stopped and cesium vapor takes place. The temperature at which the helium heating is stopped is part of the input file of the TFETC code.

2.2.1.2 Electron cooling:

The electron cooling for the emitter surface is negligible at low temperatures at the beginning of the start up process. At certain temperatures (1500-2000 °K), the electron cooling is effective. The temperature at which the electron cooling starts is part of the input file of the TFETC code.

2.2.2 Loss of Flow Accident (LOFA)

In a loss of flow accident four cases of pump failure are discussed. These cases are listed below

1. Complete pump failure (1/1).
2. 50% pump failure (1/2).
3. 33% pump failure (1/3).
4. 25% pump failure (1/4).

The mass flow rate in LOFA behaves according to the following equation:

$$m(t) = m_0 \cdot [A + B \cdot e^{-t/\tau}] \quad (2.7)$$

where

m_0 = Mass flow rate before LOFA begins.

$m(t)$ = Mass flow rate after LOFA begins.

t = Transient time, sec.

$A = 0.0$ for 1/1 pump failure.

$= 0.50$ for 1/2 pump failure.

$= 0.67$ for 1/3 pump failure.

$= 0.75$ for 1/4 pump failure.

$B = 1.0$ for 1/1 pump failure.

$= 0.50$ for 1/2 pump failure.

$= 0.33$ for 1/3 pump failure.

$= 0.25$ for 1/4 pump failure.

Different values of rising mass flowrate coefficients, τ are discussed for LOFA. The smaller the τ , the faster the loss of coolant and vice versa. Three values have been chosen for describing four different schemes of LOFA

1. $\tau = 30$ sec.
2. $\tau = 120$ sec.
3. $\tau = 600$ sec.

2.2.3 Shut down

The only shut down technique that has been considered is prompt jump according to the following equation:

$$P_{ch} = P_{ss} \left[\frac{1 - \beta \rho'}{1 - \rho'} \right] e^{(-t/T)} \quad (2.8)$$

where

- P_m = Thermal power before shut down.
- β = Total delayed fraction.
- ρ' = Negative reactivity insertion, \$
- T = Reactor period, sec.

Different negative reactivity insertions have been used for different shut down schemes. The values of T are taken according to Figure 2.2.

$$\begin{aligned} \rho' &= -\$0.1, \\ \rho' &= -\$0.3, \\ \rho' &= -\$0.9, \\ \rho' &= -\$3.0 \end{aligned}$$

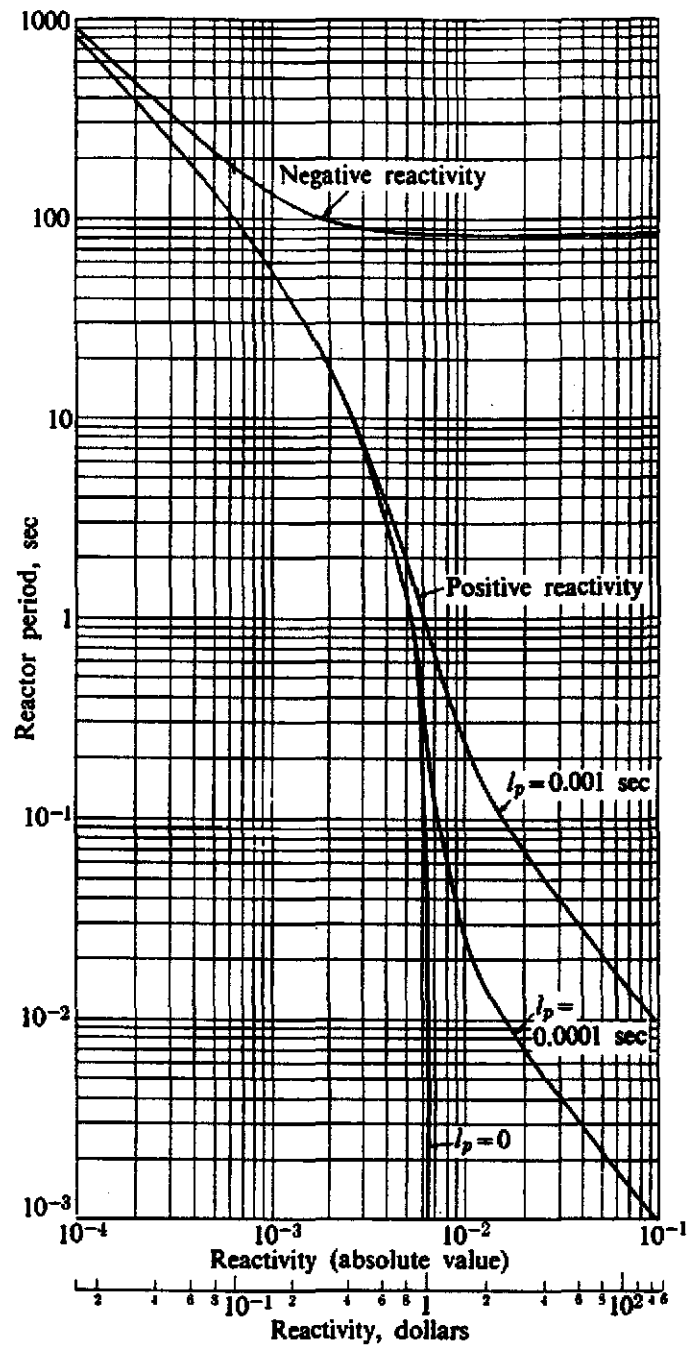


Figure 2.2 Reactor period as a function of positive and negative reactivity for a U-235 fueled reactor [1].

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Chapter 3
Method of Analysis

3.1 Introduction:

This chapter is intended to describe the model used to calculate the temperature distribution throughout the radial and axial directions of the thermionic fuel element (TFE) as a function of time by using a finite difference method. Most of the heat is transferred, throughout the TFE's layers, by conduction except at the cladding/coolant interface. The heat through the emitter/collector gap is transferred by conduction, radiation, and electron cooling. The heat conduction equation in polar cylindrical coordinates can be written as :

$$k\left[\frac{1}{r}\frac{\partial}{\partial r}\left(r\frac{\partial T}{\partial r}\right) + \frac{1}{r^2}\frac{\partial^2 T}{\partial \theta^2} + \frac{\partial^2 T}{\partial z^2}\right] + g = \rho C_p \frac{\partial T}{\partial t} \quad (3.1)$$

because of the symmetry in the TFE, $\frac{\partial T}{\partial \theta}$ can be taken to be zero. Thus equation 3.1 can be written as :

$$k\left[\frac{1}{r}\frac{\partial}{\partial r}\left(r\frac{\partial T}{\partial r}\right) + \frac{\partial^2 T}{\partial z^2}\right] + g = \rho C_p \frac{\partial T}{\partial t}$$

Using the Laplacian operator in cylindrical coordinates yields

$$k(r,z,t)\nabla^2 T(r,z,t) + g(r,z,t) = \rho(r,z,t)C_p(r,z,t)\frac{\partial T(r,z,t)}{\partial t} \quad (3.2)$$

The unsteady state heat conduction partial differential equation for the TFE can also be written as:

$$\nabla \cdot \{k(r, z, t)\nabla T(r, z, t)\} + g(r, z, t) = \rho(r, z, t)C_p(r, z, t)\frac{\partial T(r, z, t)}{\partial t} \quad (3.3)$$

Integrating the above equation over an arbitrary volume V gives

$$\int_V \nabla \cdot \{k(r, z, t)\nabla T(r, z, t)\} dV + \int_V g(r, z, t) dV = \int_V \rho(r, z, t)C_p(r, z, t)\frac{\partial T(r, z, t)}{\partial t} dV$$

Using the Divergence theorem gives

$$\int_A \{k(r, z, t)\nabla T(r, z, t)\} \cdot ndA + \int_V g(r, z, t) dV = \int_V \rho(r, z, t)C_p(r, z, t)\frac{\partial T(r, z, t)}{\partial t} dV \quad (3.4)$$

Now, the TFE is modeled at several discrete mesh points in the radial (r) and axial (z) directions at time t . Let V represents the volume of a ring element which is located at radial mesh point i and axial mesh point j at time $k+1$ as shown in Figure 3.1. This ring has a radial thickness Δr and axial length Δz . Let A_1, A_2, A_3 , and A_4 be the areas of the four outside surfaces of the ring

Equation 3.4 can now be written as follows :

$$\begin{aligned}
& k_{i+1/2,j,k} \left(\frac{\partial T}{\partial r} \right)_1 r . n_1 A_1 + k_{i,j+1/2,k} \left(\frac{\partial T}{\partial z} \right)_2 z . n_2 A_2 + \\
& k_{i-1/2,j,k} \left(\frac{\partial T}{\partial r} \right)_3 r . n_3 A_3 + k_{i,j-1/2,k} \left(\frac{\partial T}{\partial z} \right)_4 z . n_4 A_4 + \\
& g_{ij,k} . 2\pi r \Delta r \Delta z = (\rho C_p)_{ij,k} \frac{\partial T_{ij,k}}{\partial t} 2\pi r_i \Delta r \Delta z \quad (3.5)
\end{aligned}$$

where n_1, n_2, n_3 , and n_4 are the outward normal vectors to the surfaces 1,2,3, and 4, respectively. The energy balance on the volume about a mesh point $(i,j,k+1)$ which is not located on an outer surface of the pin or on the emitter or collector surfaces is shown in Figure 3.2. The subscripts on the partial derivatives are computed at these surfaces.

The $k_{i+1/2,j,k}$ value is the average thermal conductivity along the surface A_1 . It is computed at a temperature which is the average of the two temperatures $T_{i,j,k}$ and $T_{i+1,j,k}$.

The other thermal conductivity values are calculated in a similar way. Density and specific heat values vary with respect to the temperature variations and the temperature varies in accordance with each time step.

$$\frac{\partial T(i,j,k)}{\partial t} = \frac{T_{i,j,k+1} - T_{i,j,k}}{\Delta t} \quad (3.6)$$

where

$T_{i,j,k+1}$ is the temperature at point $(i,j,k+1)$

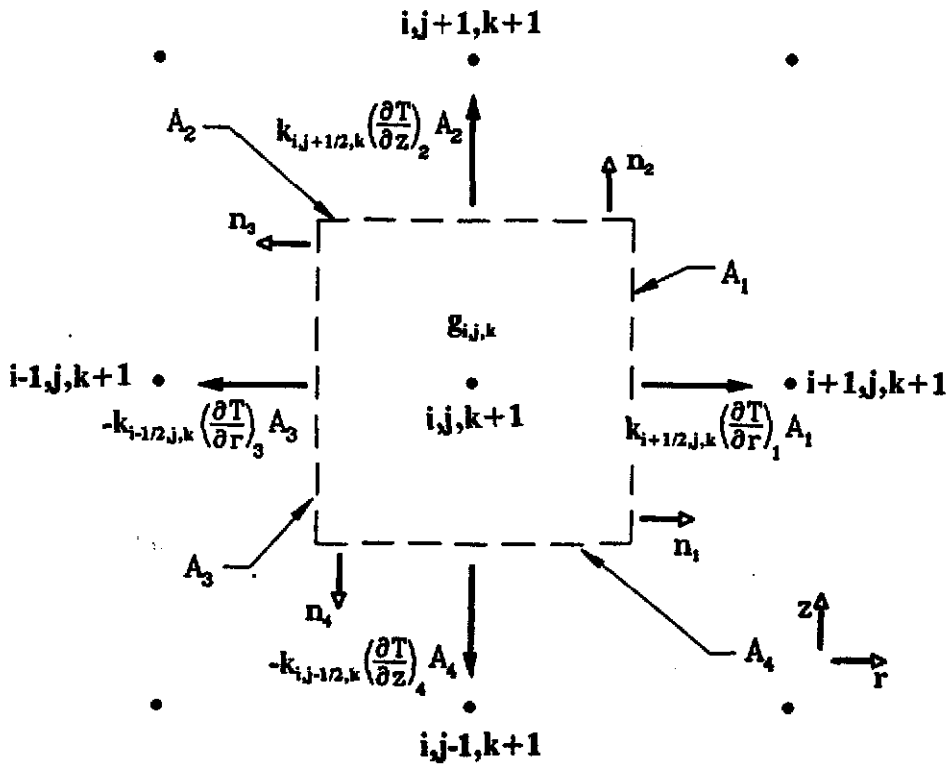


Figure 3.1 Energy balance on a ring volume about point $(i, j, k+1)$.

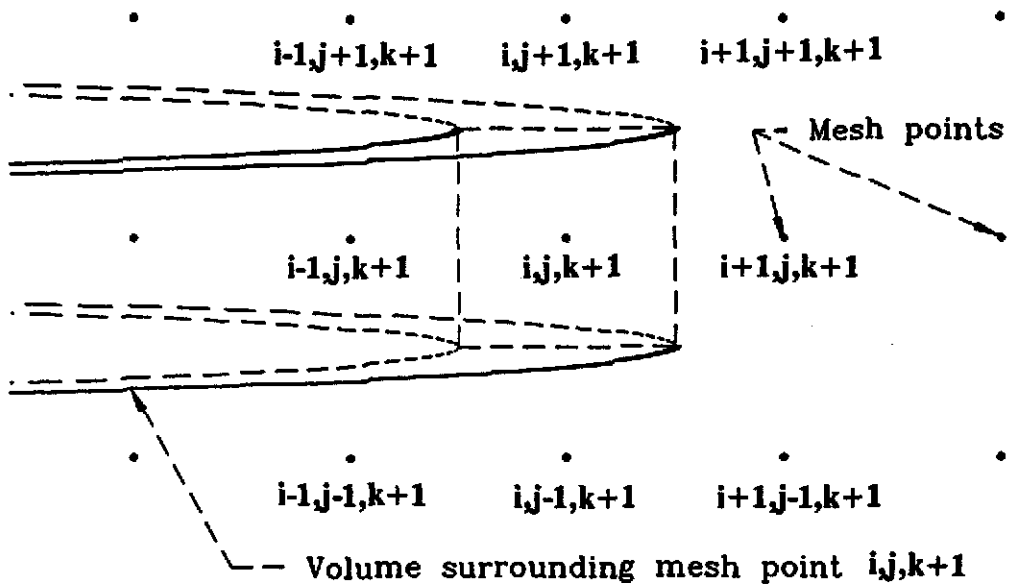


Figure 3.2 Cylindrical ring volume about the mesh point $(i, j, k+1)$.

$T_{i,j,k}$ is the temperature at point (i,j,k)

Δt is the time increment in seconds

If the point $(i,j,k+1)$ happens to lie on an interface between two materials as shown in Figure 3.3, then the thermal conductivities are computed as before for each of the two materials; then these two values are averaged to obtain an effective thermal conductivity for the surface.

From equation 3.5

$$r.n_1 = 1$$

$$z.n_2 = 1$$

$$r.n_3 = -1$$

$$z.n_4 = -1$$

3.1.1 Discretization Method

The implicit method [13] is used for solving the unsteady state heat conduction PDE. The main advantage of this method is its stability for any time increment. The temperature in the implicit method is advanced one time step and a system of linear simultaneous equations has to be solved at each time step. Thus as many as 100 temperatures should be determined at each time step in both r and z directions. In other words, each value of $i=1$ to $i=10$ has to be matched with all values of j (i.e., $j=1$

to $j=10$) so that a matrix of 100×100 is formed which has a banded structure of size 10.

Using this fact, and computing the partial derivatives in equation 3.5 as finite differences, leads to the following equation :

$$\begin{aligned}
 & k_{i+1/2,j,k} \left(\frac{T_{i+1,j,k+1} - T_{i,j,k+1}}{r_{i+1} - r_i} \right) A_1 + k_{i,j+1/2,k} \left(\frac{T_{i,j+1,k+1} - T_{i,j,k+1}}{Z_{j+1} - Z_j} \right) A_2 \\
 & k_{i-1/2,j,k} \left(\frac{T_{i-1,j,k+1} - T_{i,j,k+1}}{r_i - r_{i-1}} \right) A_3 + k_{i,j-1/2,k} \left(\frac{T_{i,j-1,k+1} - T_{i,j,k+1}}{Z_j - Z_{j-1}} \right) A_4 \\
 & g_{i,j,k} 2\pi r_i \Delta r \Delta z = (\rho C_p)_{i,j,k} \left(\frac{T_{i,j,k+1} - T_{i,j,k}}{t_{k+1} - t_k} \right) 2\pi r_i \Delta r \Delta z \quad (3.7)
 \end{aligned}$$

3.1.2. Boundary Conditions

Adiabatic boundary conditions are assumed at the fuel pin extremities

$$\left(\frac{\partial T}{\partial Z} \right)_{Z=Z_{\min.}} = 0, \quad \left(\frac{\partial T}{\partial Z} \right)_{Z=Z_{\max.}} = 0 \quad (3.8)$$

$$\left(\frac{\partial T}{\partial r} \right)_{r=r_{\min.}} = 0, \quad \left(\frac{\partial T}{\partial r} \right)_{r=r_{\max.}} = h(T_{clad} - T_{cool}) \quad (3.9)$$

3.1.3. Initial Conditions

$$T(r, z, 0) = f(r, z) \quad (3.10)$$

where $f(r, z)$ is the given forcing function

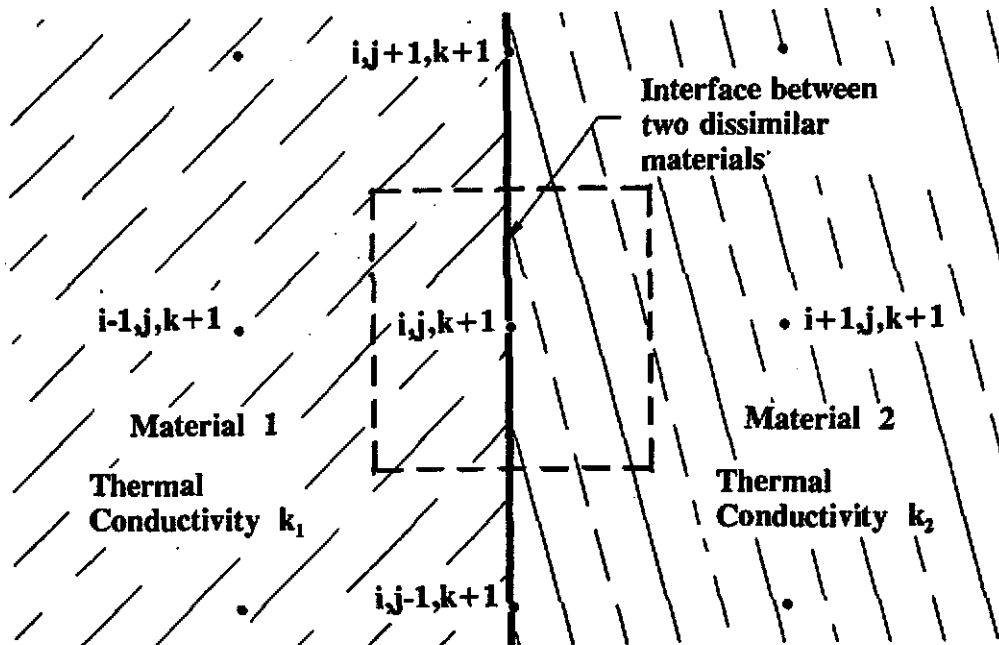


Figure 3.3 A mesh point $(i, j, k+1)$, which lies on a material interface.

3.1.4. Stability Calculations:

The implicit method is stable for any Δt . It is considered to be more complicated than the explicit method because for each time step along the radial or axial directions of a cylindrical mesh point, it assumes that the $T_{i-1, j, k+1}$, $T_{i, j, k+1}$, $T_{i+1, j, k+1}$, $T_{i, j+1, k+1}$ and $T_{i, j-1, k+1}$ values are unknown, in other words, for each single time step there are five unknown values for temperature discretized in each equation.

Equation 3.7 can be rearranged to be used in the TFETC code as follows:

$$\begin{aligned}
& k_{i+1/2,j,k} \left(\frac{A_1}{r_{i+1}-r_i} \right) T_{i+1,j,k+1} + k_{i,j+1/2,k} \left(\frac{A_2}{z_{j+1}-z_j} \right) T_{i,j+1,k+1} + \\
& k_{i-1/2,j,k} \left(\frac{A_3}{r_i-r_{i-1}} \right) T_{i-1,j,k+1} + k_{i,j-1/2,k} \left(\frac{A_4}{z_j-z_{j-1}} \right) T_{i,j-1,k+1} - \\
& [k_{i+1/2,j,k} \left(\frac{A_1}{r_{i+1}-r_i} \right) + k_{i,j+1/2,k} \left(\frac{A_2}{z_{j+1}-z_j} \right) + k_{i-1/2,j,k} \left(\frac{A_3}{r_i-r_{i-1}} \right) \\
& + k_{i,j-1/2,k} \left(\frac{A_4}{z_j-z_{j-1}} \right) - (\rho C_p)_{i,j,k} \left(\frac{2\pi r_i \Delta r \Delta z}{t_{k+1}-t_k} \right)] T_{i,j,k+1} \\
& = -g_{i,j,k} 2\pi r_i \Delta r \Delta z - (\rho C_p)_{i,j,k} \left(\frac{2\pi r_i \Delta r \Delta z}{t_{k+1}-t_k} \right) T_{i,j,k} \quad (3.11)
\end{aligned}$$

Equation 3.11 is valid for all interior mesh points of the fuel emitter region. It is not valid for the following mesh points :

1. Those mesh points located at the upper and lower limits of the pin (i.e., the top and the bottom).
2. Those on the emitter and collector radial surfaces.
3. Those on the surface of the void region located at the center of the TFE.
4. Those on the outside radial surface of the cladding.

Equations for these points are derived in the following sections. The stability equation can be derived easily from equation 3.11. The stability equation enhances the fact that the implicit method is stable for any time step.

$$\frac{-(\rho C_p)_{i,j,k} \frac{2\pi \Delta r \Delta z}{\Delta t}}{-[k_{i+1/2,j,k} \left(\frac{A_1}{r_{i+1}-r_i}\right) + k_{i,j+1/2,k} \left(\frac{A_2}{z_{j+1}-z_j}\right) + k_{i-1/2,j,k} \left(\frac{A_3}{r_i-r_{i-1}}\right) + k_{i,j-1/2,k} \left(\frac{A_4}{z_j-z_{j-1}}\right) + (\rho C_p)_{i,j,k} \left(\frac{2\pi \Delta r \Delta z}{\Delta t}\right)]} > 0 \quad (3.12)$$

All values in the stability equation above are positive.

For the sake of accuracy, Δt has to be very small so that the truncation error $O[\Delta t + (\Delta r)^2 + (\Delta z)^2]$ can be reduced.

3.2.1 Fuel Pellet/Central Void Interface-Top of the TFE

The energy balance for the mesh point at this location is shown in Figure 3.4. The top of the fuel and the central void surfaces, in the TFE, are assumed to be adiabatic (i.e., heat flow equals zero). Therefore, heat transfer does not occur in the positive r and negative z directions. When all these terms are removed from equation 3.10, the equation for the temperature at this mesh point results in:

$$k_{3/2,j_{\max},k} \left(\frac{A_1}{r_2-r_1}\right) T_{2,j_{\max},k+1} + k_{1,j_{\max}-1/2,k} \left(\frac{A_4}{z_{j_{\max}}-z_{j_{\max}-1}}\right) T_{1,j_{\max}-1,k+1}$$

$$- [k_{3/2,j_{\max},k} \left(\frac{A_1}{r_2-r_1}\right) + k_{1,j_{\max}-1/2,k} \left(\frac{A_4}{z_{j-1}-z_j}\right)]$$

$$\begin{aligned}
 & -(\rho C_p)_{i,j_{\max},k} \left(\frac{2\pi r_1 (r_2 - r_1) (z_{j_{\max}} - z_{j_{\max}-1})}{t_{k+1} - t_k} \right) T_{i,j_{\max},k+1} \\
 & = -g_{i,j_{\max},k} 2\pi r_1 (r_2 - r_1) (z_{j_{\max}} - z_{j_{\max}-1}) \\
 & -(\rho C_p)_{i,j_{\max},k} \left(\frac{2\pi r_1 (r_2 - r_1) (z_{j_{\max}} - z_{j_{\max}-1})}{t_{k+1} - t_k} \right) T_{i,j_{\max},k} \quad (3.13)
 \end{aligned}$$

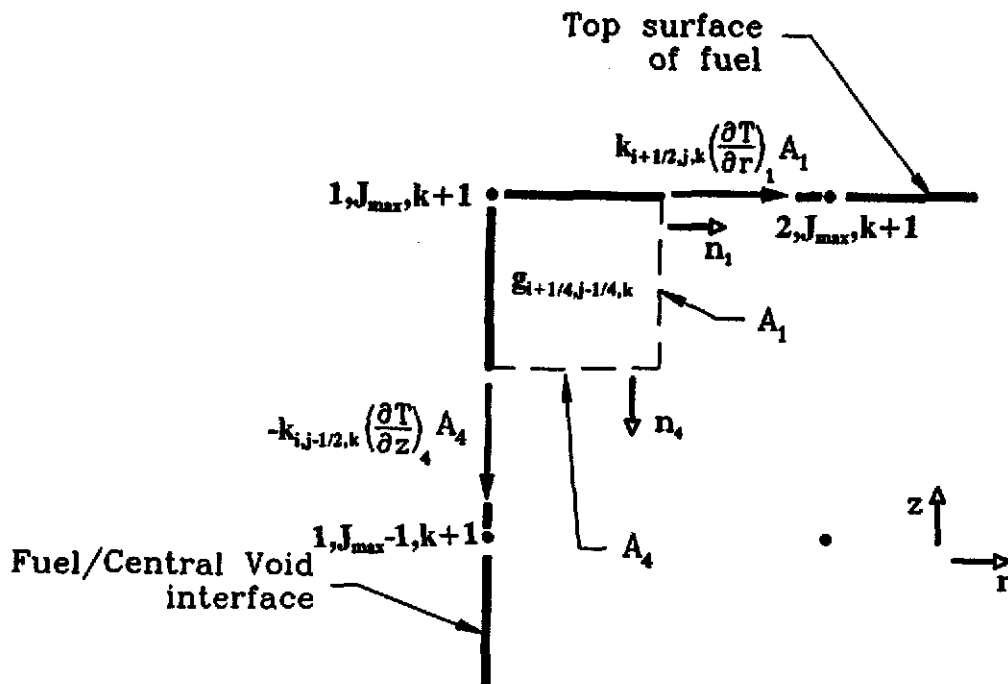


Figure 3.4 Energy balance for the mesh point $(1, J_{\max}, k+1)$, which is located at the top of the fuel pin and at the surface of the central void.

3.2.2 Fuel Pellet/Central Void Interface-TFE Bottom

The energy balance for the mesh point is shown in Figure 3.5. The bottom of the TFE is assumed to be an adiabatic surface. Thus the temperature $T_{1,1,k+1}$ at this location is:

$$\begin{aligned}
 & k_{3/2,1,k} \left(\frac{A_1}{r_2 - r_1} \right) T_{2,1,k+1} + k_{1,3/2,k} \left(\frac{A_2}{z_2 - z_1} \right) T_{1,2,k+1} \\
 & - \left[k_{3/2,1,k} \left(\frac{A_1}{r_2 - r_1} \right) + k_{1,3/2,k} \left(\frac{A_2}{z_2 - z_1} \right) - (\rho C_p)_{1,1,k} \left(\frac{2\pi r_1 (r_2 - r_1) (z_2 - z_1)}{t_{k+1} - t_k} \right) \right] T_{1,1,k+1} \\
 & = -g_{1,1,k} 2\pi r_1 (r_2 - r_1) (z_2 - z_1) - \\
 & (\rho C_p)_{1,1,k} \left(\frac{2\pi r_1 (r_2 - r_1) (z_2 - z_1)}{t_{k+1} - t_k} \right) T_{1,1,k} \quad (3.14)
 \end{aligned}$$

3.2.3 Other Locations on the Fuel/Void Interface

The energy balance for these points is shown in Figure 3.6. The equations for the temperatures of these points are given as follows

$$\begin{aligned}
 & k_{3/2,j,k} \left(\frac{A_1}{r_2 - r_1} \right) T_{2,j,k+1} + k_{1,j+1/2,k} \left(\frac{A_2}{z_{j+1} - z_j} \right) T_{1,j+1,k+1} \\
 & + k_{1,j-1/2,k} \left(\frac{A_4}{z_j - z_{j-1}} \right) T_{1,j-1,k+1} - \left[k_{3/2,j,k} \left(\frac{A_1}{r_2 - r_1} \right) \right. \\
 & \left. + k_{1,j+1/2,k} \left(\frac{A_2}{z_{j+1} - z_j} \right) + k_{1,j-1/2,k} \left(\frac{A_4}{z_j - z_{j-1}} \right) \right. \\
 & \left. - (\rho C_p)_{1,j,k} \left(\frac{2\pi r_1 (r_2 - r_1) (z_{j+1} - z_j)}{t_{k+1} - t_k} \right) \right] T_{1,j,k+1} \\
 & = -g_{1,j,k} 2\pi r_1 (r_2 - r_1) (z_{j+1} - z_j)
 \end{aligned}$$

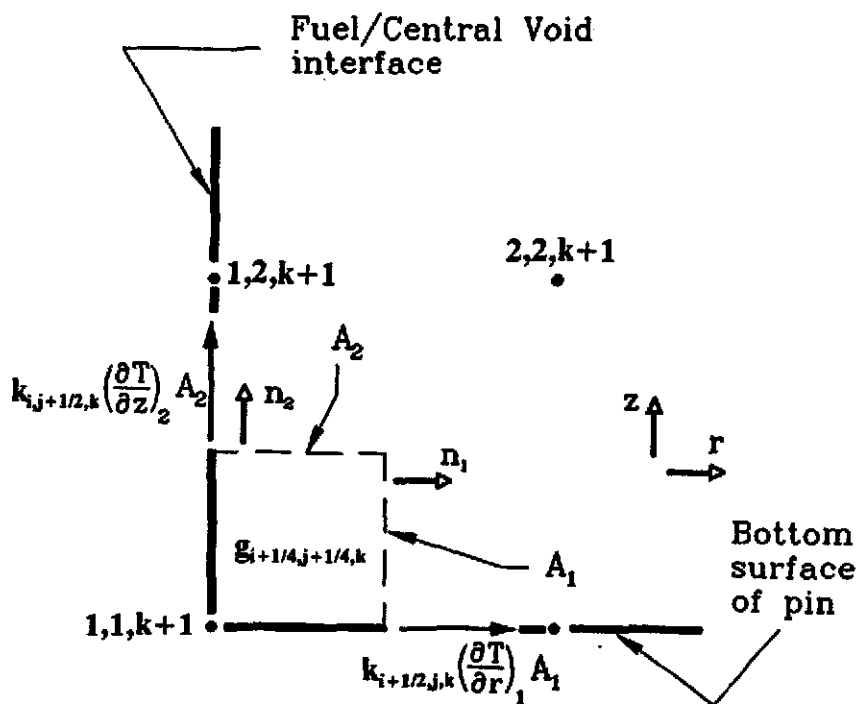


Figure 3.5 Energy balance for the mesh point $(1,1,k+1)$, which is located at the bottom of the pin and at the surface of the central void.

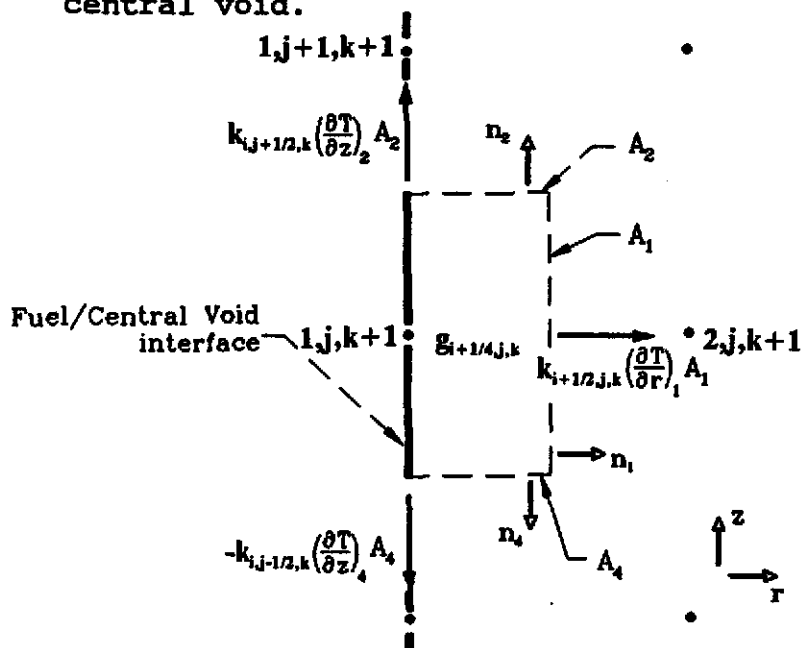


Figure 3.6 Energy balance for mesh points $(1,j,k+1)$, which are on the fuel/void interface, but which are not at the top or bottom.

$$-(\rho C_p)_{1,j,k} \left(\frac{2\pi r_1 (r_2 - r_1) (z_{j+1} - z_j)}{t_{k+1} - t_k} \right) T_{1,j,k} \quad (3.15)$$

3.2.4 Top Surface of the TFE:

The energy balance for these points is shown in Figure 3.7. The equations for the temperatures of these points are given in the following equation:

$$\begin{aligned} & k_{i+1/2,j_{\max},k} \left(\frac{A_1}{r_{i+1} - r_i} \right) T_{i+1,j_{\max},k+1} + k_{i-1/2,j_{\max},k} \left(\frac{A_3}{r_i - r_{i-1}} \right) T_{i-1,j_{\max},k+1} \\ & + k_{i,j_{\max}-1/2,k} \left(\frac{A_4}{z_{j_{\max}} - z_{j_{\max}-1}} \right) T_{i,j_{\max}-1,k+1} - \left[k_{i+1/2,j_{\max},k} \left(\frac{A_1}{r_{i+1} - r_i} \right) \right. \\ & \left. + k_{i-1/2,j_{\max},k} \left(\frac{A_3}{r_i - r_{i-1}} \right) + k_{i,j_{\max}-1/2,k} \left(\frac{A_4}{z_{j_{\max}-1} - z_{j_{\max}}} \right) \right. \\ & \left. - (\rho C_p)_{i,j_{\max},k} \left(\frac{2\pi r_i \Delta r (z_{j_{\max}} - z_{j_{\max}-1})}{t_{k+1} - t_k} \right) \right] T_{i,j_{\max},k+1} \\ & = -g_{i,j_{\max},k} 2\pi r_i \Delta r (z_{j_{\max}} - z_{j_{\max}-1}) \\ & - (\rho C_p)_{i,j_{\max},k} \left(\frac{2\pi r_i \Delta r (z_{j_{\max}} - z_{j_{\max}-1})}{t_{k+1} - t_k} \right) T_{i,j_{\max},k} \quad (3.16) \end{aligned}$$

3.2.5 Bottom Surface of the TFE:

The mesh points are located at the bottom surface of the TFE but are not located on any radial boundaries. The energy balance for these points is shown in Figure 3.8.

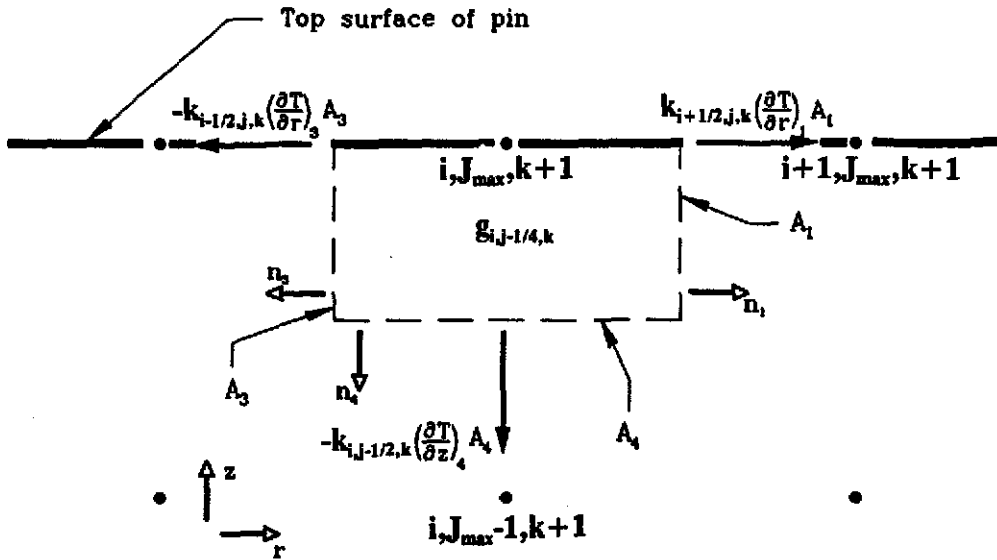


Figure 3.7 Energy balance on mesh points $(i, j_{\max}, k+1)$, which are located on the top of the TFE pin, but not on any radial boundaries.

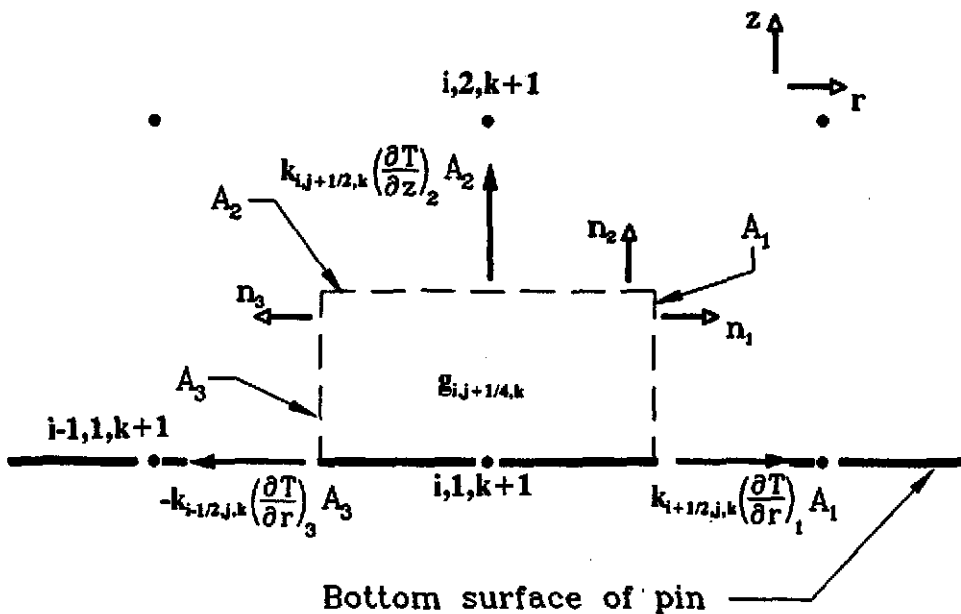


Figure 3.8 Energy balance for mesh points $(i, 1, k+1)$, which are located on the bottom of the TFE pin away from any radial boundaries.

The temperature equation is given as:

$$\begin{aligned}
& k_{i+1/2,1,k} \left(\frac{A_1}{r_{i+1}-r_i} \right) T_{i+1,1,k+1} + k_{i,3/2,k} \left(\frac{A_2}{z_2-z_1} \right) T_{i,2,k+1} \\
& + k_{i-1/2,1,k} \left(\frac{A_3}{r_i-r_{i-1}} \right) T_{i-1,1,k+1} - [k_{i+1/2,1,k} \left(\frac{A_1}{r_{i+1}-r_i} \right) \\
& + k_{i,3/2,k} \left(\frac{A_2}{z_2-z_1} \right) + k_{i-1/2,1,k} \left(\frac{A_3}{r_{i-1}-r_i} \right) \\
& - (\rho C_p)_{i,1,k} \left(\frac{2\pi r_i \Delta r (z_2-z_1)}{t_{k+1}-t_k} \right)] T_{i,1,k+1} \\
& = -g_{i,1,k} 2\pi r_i \Delta r (z_2 - z_1) \\
& - (\rho C_p)_{i,1,k} \left(\frac{2\pi r_i \Delta r (z_2-z_1)}{t_{k+1}-t_k} \right) T_{i,1,k} \tag{3.17}
\end{aligned}$$

3.2.6 Emitter Surface:

As shown in Figure 3.9, energy is transferred away from the surface of the emitter in the positive r-direction by different modes fully explained in Chapter 2. The equation for the temperatures at these points is:

$$\begin{aligned}
& k_{i,j+1/2,k} \left(\frac{A_2}{z_{j+1}-z_j} \right) T_{i,j+1,k+1} + k_{i-1/2,j,k} \left(\frac{A_3}{r_i-r_{i-1}} \right) T_{i-1,j,k+1} \\
& + k_{i,j-1/2,k} \left(\frac{A_4}{z_j-z_{j-1}} \right) T_{i,j-1,k+1} - [k_{i,j+1/2,k} \left(\frac{A_2}{z_{j+1}-z_j} \right) \\
& + k_{i-1/2,j,k} \left(\frac{A_3}{r_{i-1}-r_i} \right) + k_{i,j-1/2,k} \left(\frac{A_4}{z_{j-1}-z_j} \right)
\end{aligned}$$

$$\begin{aligned}
& -(\rho C_p)_{i,j,k} \left(\frac{2\pi r_i (r_i - r_{i-1}) (z_{j+1} - z_j)}{t_{k+1} - t_k} \right) T_{i,j,k+1} \\
& = -g_{i,j,k} 2\pi r_i (r_i - r_{i-1}) (z_{j+1} - z_j) \\
& -(\rho C_p)_{i,j,k} \left(\frac{2\pi r_i (r_i - r_{i-1}) (z_{j+1} - z_j)}{t_{k+1} - t_k} \right) T_{i,j,k} \\
& + Q_{j,k}^{Cond.} A_1 + Q_{j,k}^{Rad.} A_1 + Q_{ave}^{EEC} A_1 \tag{3.18}
\end{aligned}$$

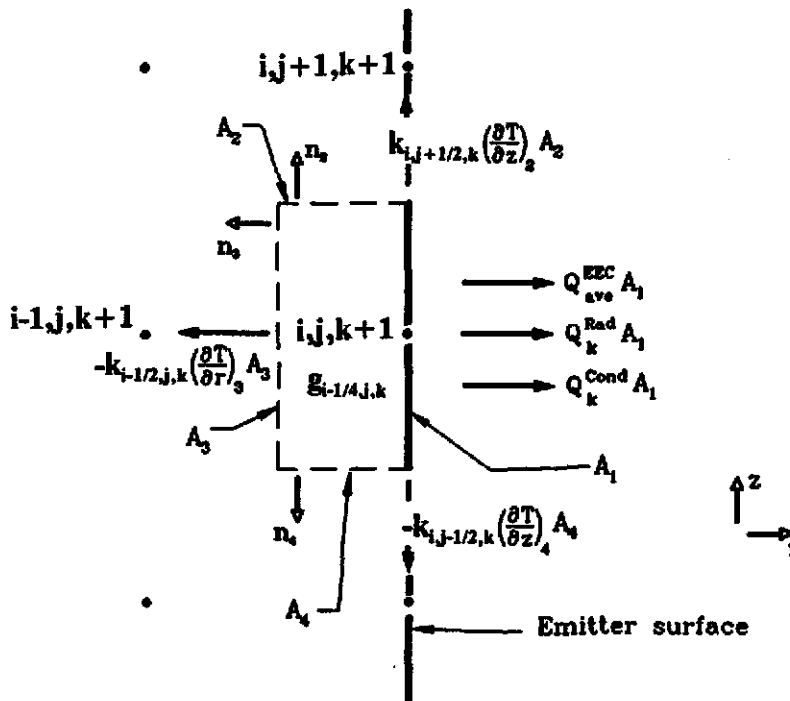


Figure 3.9 Energy balance for mesh points $(i, j, k+1)$, which are located along the emitter surface.

3.2.7 Emitter Surface-Top of the TFE:

As shown in Figure 3.10, the equation for the temperature at the mesh point $i, j_{max}, k+1$ is

$$k_{i-1/2,j_{max},k} \left(\frac{A_3}{r_i - r_{i-1}} \right) T_{i-1,j_{max},k+1} + k_{i,j_{max}-1/2,k} \left(\frac{A_4}{z_{j_{max}} - z_{j_{max}-1}} \right) T_{i,j_{max}-1,k+1}$$

$$\begin{aligned}
& -\left[k_{i-1/2, j_{\max}, k} \left(\frac{A_3}{r_{i-1} - r_i} \right) + k_{i, j_{\max}-1/2, k} \left(\frac{A_4}{z_{j_{\max}-1} - z_{j_{\max}}} \right) \right. \\
& \left. - (\rho C_p)_{i, j_{\max}, k} \left(\frac{2\pi r_i (r_i - r_{i-1}) (z_{j_{\max}} - z_{j_{\max}-1})}{t_{k+1} - t_k} \right) \right] T_{i, j_{\max}, k+1} \\
& = -g_{i, j_{\max}, k} 2\pi r_i (r_i - r_{i-1}) (z_{j_{\max}} - z_{j_{\max}-1}) \\
& - (\rho C_p)_{i, j_{\max}, k} \left(\frac{2\pi r_i (r_i - r_{i-1}) (z_{j_{\max}} - z_{j_{\max}-1})}{t_{k+1} - t_k} \right) T_{i, j_{\max}, k} \\
& + Q_{j_{\max}, k}^{Cond} A_1 + Q_{j_{\max}, k}^{Rad} A_1 + Q_{ave}^{EEC} A_1 \quad (3.19)
\end{aligned}$$

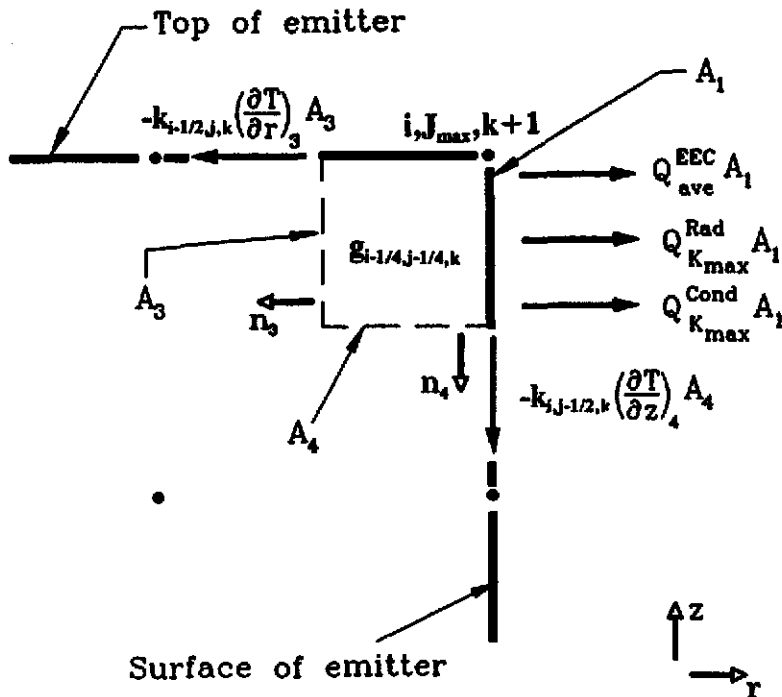


Figure 3.10 Energy balance for the mesh point $(i, j_{\max}, k+1)$, which is located at the top of the pin and on the emitter surface.

3.2.8 Emitter Surface-Bottom of the TFE:

As shown in Figure 3.11, the temperature equation at the mesh point $i,1,k+1$ is:

$$\begin{aligned}
 & k_{i,3/2,k} \left(\frac{A_2}{z_2 - z_1} \right) T_{i,2,k+1} + k_{i-1/2,1,k} \left(\frac{A_3}{r_i - r_{i-1}} \right) T_{i-1,1,k+1} \\
 & - \left[k_{i,3/2,k} \left(\frac{A_2}{z_2 - z_1} \right) + k_{i-1/2,1,k} \left(\frac{A_3}{r_i - r_{i-1}} \right) \right. \\
 & \left. - (\rho C_p)_{i,1,k} \left(\frac{2\pi r_i (r_i - r_{i-1})(z_2 - z_1)}{t_{k+1} - t_k} \right) \right] T_{i,1,k+1} \\
 & = -g_{i,1,k} 2\pi r_i (r_i - r_{i-1})(z_2 - z_1) \\
 & - (\rho C_p)_{i,1,k} \left(\frac{2\pi r_i (r_i - r_{i-1})(z_2 - z_1)}{t_{k+1} - t_k} \right) T_{i,1,k} \\
 & + Q_{1,k}^{Cond.} A_1 + Q_{1,k}^{Rad.} A_1 + Q_{ave}^{EEC} A_1 \quad (3.20)
 \end{aligned}$$

3.2.9 Collector Surface:

The energy balance for the collector surface is shown in Figure 3.12. The temperature equations for this surface were derived in a similar way to those for the emitter surface and are as follows:

$$k_{i,j+1/2,k} \left(\frac{A_2}{z_{j+1} - z_j} \right) T_{i,j+1,k+1} + k_{i+1/2,j,k} \left(\frac{A_1}{r_{i+1} - r_i} \right) T_{i+1,j,k+1}$$

$$\begin{aligned}
& +k_{i,j-1/2,k} \left(\frac{A_4}{z_j - z_{j-1}} \right) T_{i,j-1,k+1} - \left[k_{i+1/2,j,k} \left(\frac{A_1}{r_{i+1} - r_i} \right) \right. \\
& \quad \left. + k_{i,j+1/2,k} \left(\frac{A_2}{z_{j+1} - z_j} \right) + k_{i,j-1/2,k} \left(\frac{A_4}{z_{j-1} - z_j} \right) \right. \\
& \quad \left. - (\rho C_p)_{i,j,k} \left(\frac{2\pi r_i (r_{i+1} - r_i) (z_{j+1} - z_j)}{t_{k+1} - t_k} \right) \right] T_{i,j,k+1} \\
& = -g_{i,j,k} 2\pi r_i \Delta r \Delta z \\
& \quad - (\rho C_p)_{i,j,k} \left(\frac{2\pi r_i \Delta r \Delta z}{t_{k+1} - t_k} \right) T_{i,j,k} \\
& - Q_{jk}^{\text{Cond.}} A_3 - Q_{jk}^{\text{Rad.}} A_3 + Q_{ave}^{\text{CEH}} A_3 \quad (3.21)
\end{aligned}$$

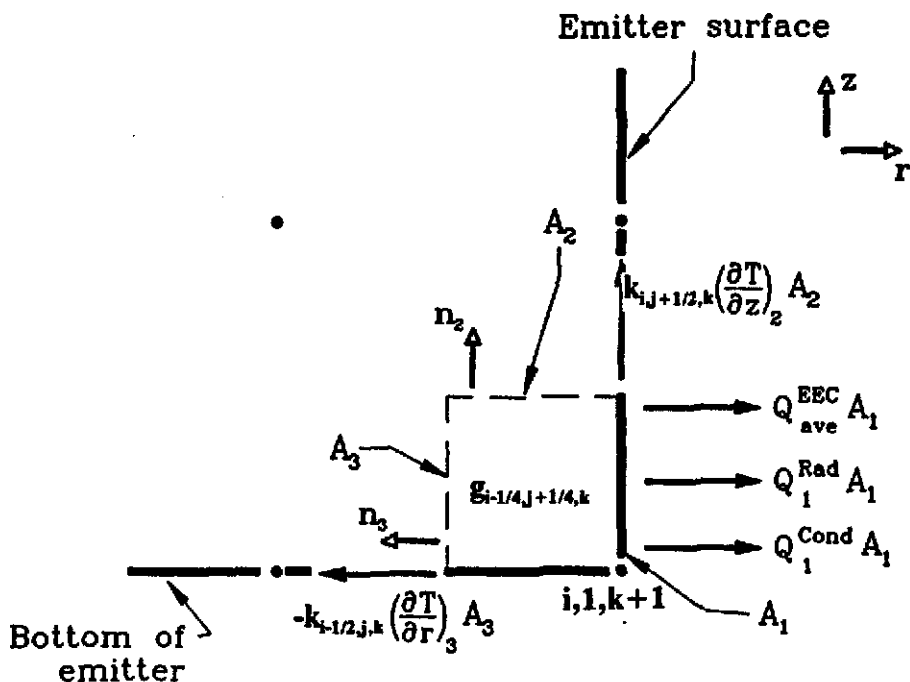


Figure 3.11 Energy balance for the mesh point (i, 1, k+1), which is located on the emitter surface at the bottom of the pin.

The Q_{ave}^{CEH} term differs from the Q_{ave}^{EEC} term in that the effect of the plasma radiation is added to Q_{ave}^{CEH} , whereas it is subtracted from Q_{ave}^{EEC} ; plasma radiation reduces the amount of heat removed from the emitter, but it increases the amount of heat added to the collector.

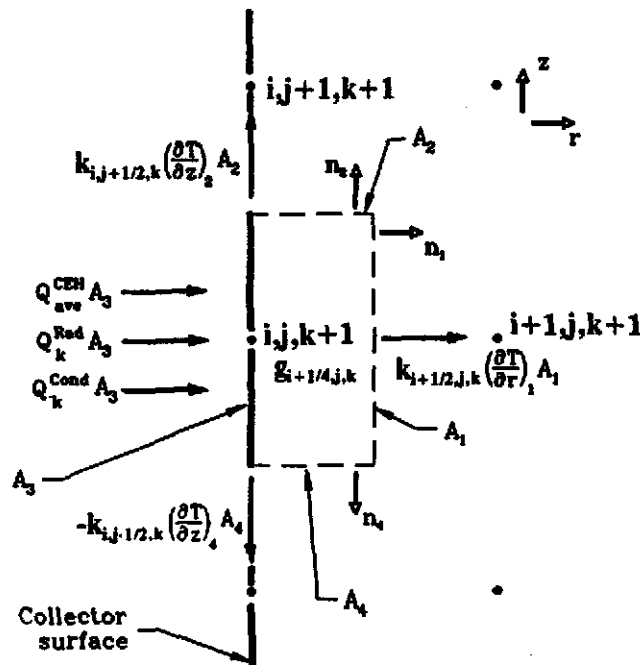


Figure 3.12 Energy balance for mesh points $(i, j, k+1)$, which are located on the collector surface.

3.2.10 Collector Surface-Top of the TFE:

Figure 3.13 shows the heat balance for the mesh point at the top of the collector surface. The temperature equation is given as:

$$\begin{aligned}
& k_{i+1/2, j_{\max}, k} \left(\frac{A_1}{r_{i+1} - r_i} \right) T_{i+1, j_{\max}, k+1} + k_{i, j_{\max}-1/2, k} \left(\frac{A_4}{z_{j_{\max}} - z_{j_{\max}-1}} \right) T_{i, j_{\max}-1, k+1} \\
& - \left[k_{i+1/2, j_{\max}, k} \left(\frac{A_1}{r_{i+1} - r_i} \right) + k_{i, j_{\max}-1/2, k} \left(\frac{A_4}{z_{j_{\max}-1} - z_{j_{\max}}} \right) \right. \\
& \left. - (\rho C_p)_{i, j_{\max}, k} \left(\frac{2\pi r_i (r_i - r_{i-1}) (z_{j_{\max}} - z_{j_{\max}-1})}{t_{k+1} - t_k} \right) \right] T_{i, j_{\max}, k+1} \\
& = -g_{i, j_{\max}, k} 2\pi r_i (r_i - r_{i-1}) (z_{j_{\max}} - z_{j_{\max}-1}) \\
& - (\rho C_p)_{i, j_{\max}, k} \left(\frac{2\pi r_i (r_i - r_{i-1}) (z_{j_{\max}} - z_{j_{\max}-1})}{t_{k+1} - t_k} \right) T_{i, j_{\max}, k} \\
& - Q_{j_{\max}, k}^{\text{Cond.}} A_3 - Q_{j_{\max}, k}^{\text{Rad.}} A_3 + Q_{\text{ave}}^{\text{CEH}} A_3 \quad (3.22)
\end{aligned}$$

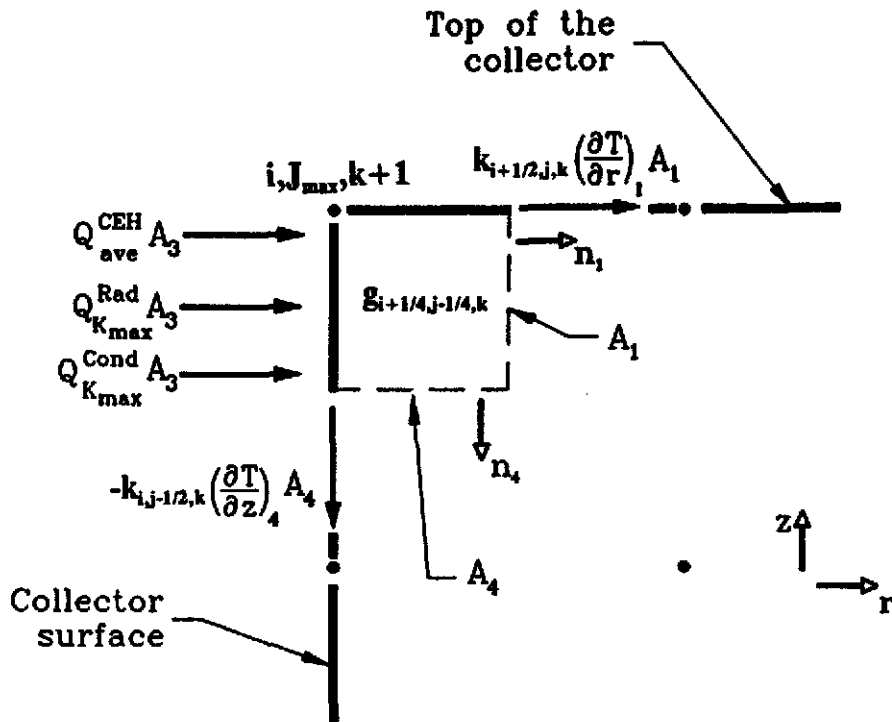


Figure 3.13 Energy balance for the mesh point $(i, j_{\max}, k+1)$, which is located at the top of the pin and on the collector surface.

3.2.11 Collector Surface-Bottom of the TFE:

Figure 3.14 shows the heat balance for the mesh point at the bottom of the collector surface. The temperature equation is:

$$\begin{aligned}
 & k_{i+1/2,1,k} \left(\frac{A_1}{r_{i+1}-r_i} \right) T_{i+1,1,k+1} + k_{i,3/2,k} \left(\frac{A_2}{z_2-z_1} \right) T_{i,2,k+1} \\
 & - [k_{i+1/2,1,k} \left(\frac{A_1}{r_{i+1}-r_i} \right) + k_{i,3/2,k} \left(\frac{A_2}{z_2-z_1} \right) \\
 & - (\rho C_p)_{i,1,k} \left(\frac{2\pi r_i (r_{i+1}-r_i)(z_2-z_1)}{t_{k+1}-t_k} \right)] T_{i,1,k+1} \\
 & = -g_{i,1,k} 2\pi r_i \Delta r (z_2 - z_1) \\
 & - (\rho C_p)_{i,1,k} \left(\frac{2\pi r_i \Delta r (z_2-z_1)}{t_{k+1}-t_k} \right) T_{i,1,k} \\
 & - Q_{1,k}^{Cond.} A_3 - Q_{1,k}^{Rad.} A_3 + Q_{ave}^{CEH} A_3 \quad (3.23)
 \end{aligned}$$

3.2.12 Cladding/Coolant Interface:

The energy balance for the mesh points at the cladding/coolant interface is shown in Figure 3.15. The temperature equations are:

$$\begin{aligned}
 & h_{j,k} (A_1) T_{j,k+1}^{Coolant} + k_{i,j+1/2,k} \left(\frac{A_2}{z_{j+1}-z_j} \right) T_{i,j+1,k+1} \\
 & + k_{i-1/2,j,k} \left(\frac{A_3}{r_i-r_{i-1}} \right) T_{i-1,j,k+1} + k_{i,j-1/2,k} \left(\frac{A_4}{z_j-z_{j-1}} \right) T_{i,j-1,k+1}
 \end{aligned}$$

$$\begin{aligned}
& -[h_{j,k}(A_1) + k_{i,j+1/2,k}(\frac{A_2}{z_{j+1}-z_j}) \\
& + k_{i-1/2,j,k}(\frac{A_3}{r_{i-1}-r_i}) + k_{i,j-1/2,k}(\frac{A_4}{z_{j-1}-z_j}) \\
& - (\rho C_p)_{i,j,k}(\frac{2\pi r_i \Delta r \Delta z}{t_{k+1}-t_k})] T_{i,j,k+1} \\
& = -g_{i,j,k} 2\pi r_i \Delta r \Delta z - (\rho C_p)_{i,j,k}(\frac{2\pi r_i \Delta r \Delta z}{t_{k+1}-t_k}) T_{i,j,k} \quad (3.24)
\end{aligned}$$

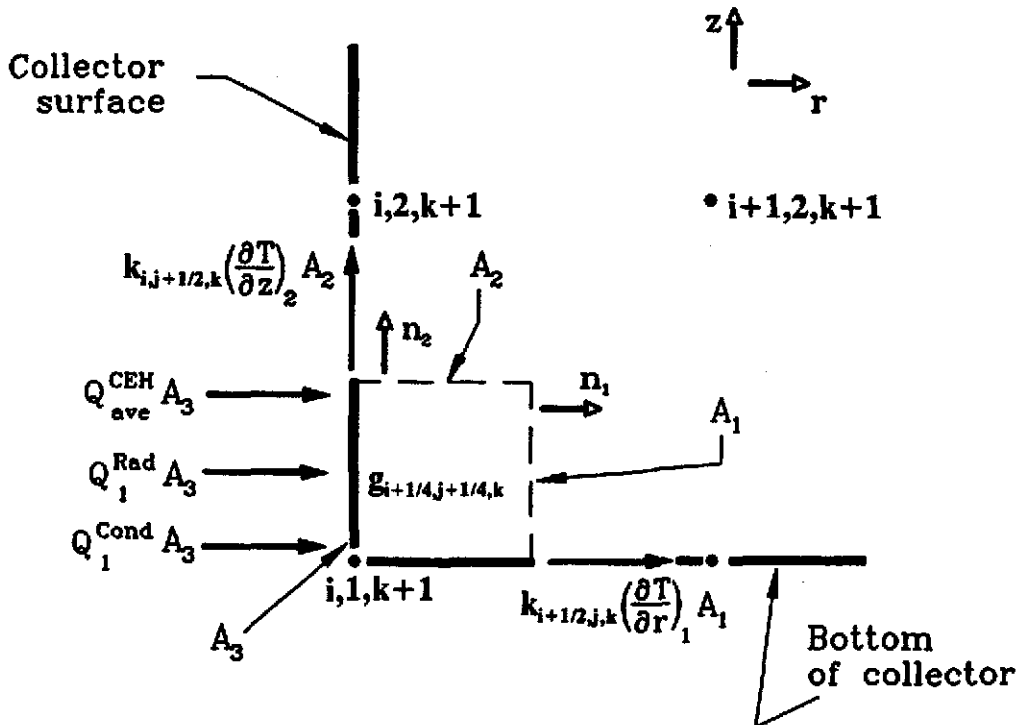


Figure 3.14 Energy balance for the mesh point $(i, 1, k+1)$, which is located at the bottom of the TFE and on the collector surface.

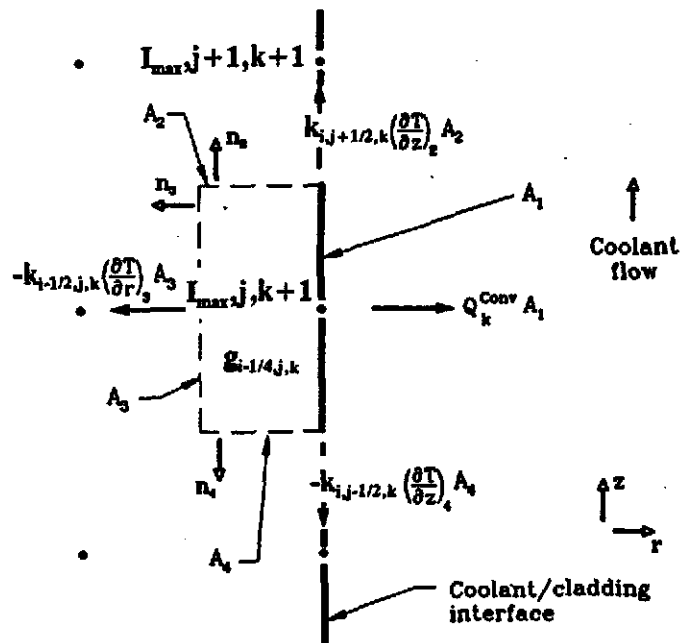


Figure 3.15 Energy balance for mesh points $(I_{\max}, j, k+1)$, which are located at the cladding/coolant interface.

3.2.13 Cladding/Coolant Interface-Top of the TFE:

The energy balance on the cladding/coolant interface at the top of the TFE is shown in Figure 3.16. The temperature equation for this point is as follows:

$$\begin{aligned}
 & h_{j_{\max},k}(A_1)T_{j_{\max},k+1}^{Coolant} + k_{i_{\max}-1/2,j_{\max},k}\left(\frac{A_3}{r_{i_{\max}}-r_{i_{\max}-1}}\right)T_{i_{\max}-1,j_{\max},k+1} \\
 & + k_{i_{\max},j_{\max}-1/2,k}\left(\frac{A_4}{z_{j_{\max}}-z_{j_{\max}-1}}\right)T_{i_{\max},j_{\max}-1,k+1} - [h_{j_{\max},k}(A_1) \\
 & + k_{i_{\max}-1/2,j_{\max},k}\left(\frac{A_3}{r_{i_{\max}-1}-r_{i_{\max}}}\right) + k_{i_{\max},j_{\max}-1/2,k}\left(\frac{A_4}{z_{j_{\max}-1}-z_{j_{\max}}}\right)]
 \end{aligned}$$

$$\begin{aligned}
 & -(\rho C_p)_{i_{\max},j_{\max},k} \left(\frac{2\pi r_{i_{\max}}(r_{i_{\max}} - r_{i_{\max}-1})(z_{j_{\max}} - z_{j_{\max}-1})}{t_{k+1} - t_k} \right) T_{i_{\max},j_{\max},k+1} \\
 & = -g_{i_{\max},j_{\max},k} (2\pi r_{i_{\max}}(r_{i_{\max}} - r_{i_{\max}-1})(z_{j_{\max}} - z_{j_{\max}-1})) \\
 & -(\rho C_p)_{i_{\max},j_{\max},k} \left(\frac{2\pi r_{i_{\max}}(r_{i_{\max}} - r_{i_{\max}-1})(z_{j_{\max}} - z_{j_{\max}-1})}{t_{k+1} - t_k} \right) T_{i_{\max},j_{\max},k} \quad (3.25)
 \end{aligned}$$

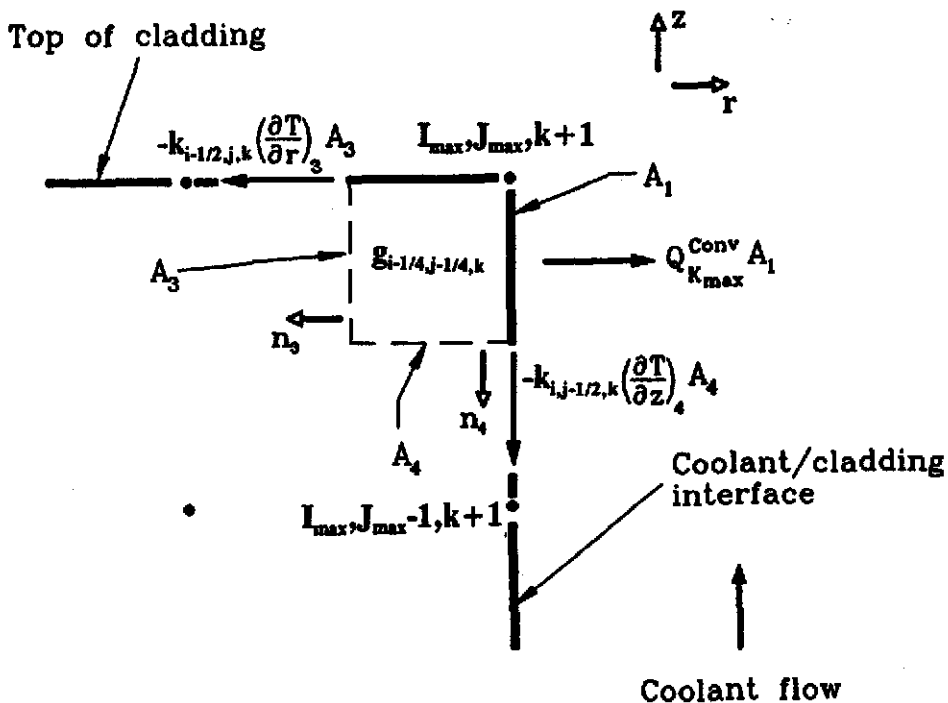


Figure 3.16 Energy balance at the mesh point $(I_{\max}, J_{\max}, k+1)$, which is located at the cladding/coolant interface and at the top of the TFE.

3.2.14 Cladding/Coolant Interface-Bottom of the TFE:

Figure 3.17 shows the energy balance for the mesh point at the bottom of the cladding/coolant interface of the TFE. The temperature equation for this point is:

$$\begin{aligned}
& h_{1,k}(A_1)T_{1,k+1}^{Coolant} + k_{i_{max},3/2,k}\left(\frac{A_2}{z_2-z_1}\right)T_{i_{max},2,k+1} \\
& + k_{i_{max}-1/2,1,k}\left(\frac{A_3}{r_{i_{max}}-r_{i_{max}-1}}\right)T_{i_{max}-1,1,k+1} - [h_{1,k}(A_1) \\
& + k_{i_{max},3/2,k}\left(\frac{A_2}{z_2-z_1}\right) + k_{i_{max}-1/2,1,k}\left(\frac{A_3}{r_{i_{max}}-r_{i_{max}-1}}\right) \\
& - (\rho C_p)_{i_{max},1,k}\left(\frac{2\pi r_{i_{max}}(r_{i_{max}}-r_{i_{max}-1})(z_2-z_1)}{t_{k+1}-t_k}\right)]T_{i_{max},1,k+1} \\
& = -g_{i_{max},1,k}(2\pi r_{i_{max}}(r_{i_{max}}-r_{i_{max}-1})(z_2-z_1)) \\
& - (\rho C_p)_{i_{max},1,k}\left(\frac{2\pi r_{i_{max}}(r_{i_{max}}-r_{i_{max}-1})(z_2-z_1)}{t_{k+1}-t_k}\right)T_{i_{max},1,k} \quad (3.26)
\end{aligned}$$

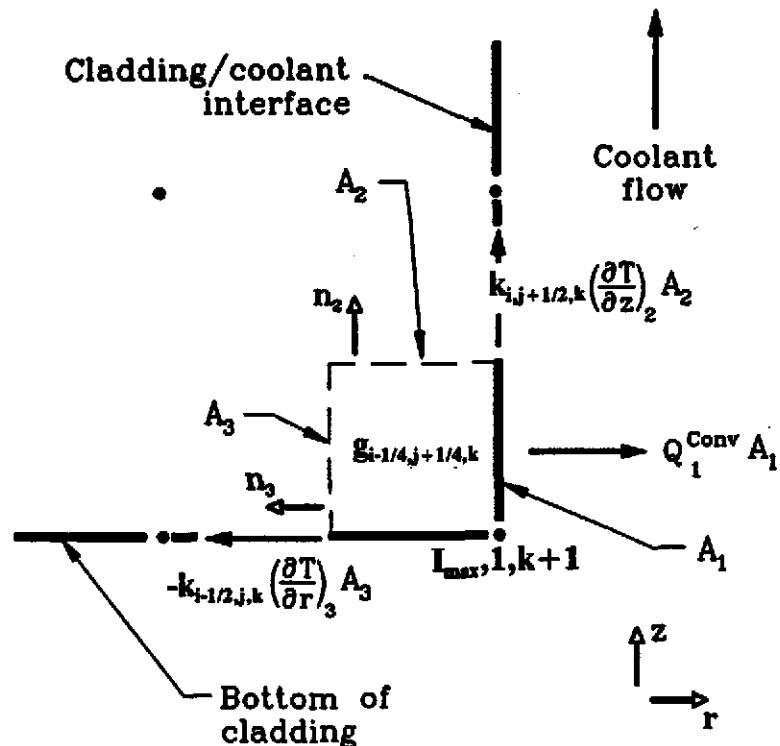


Figure 3.17 Energy balance at the mesh point $(I_{max, 1, k+1})$, which is located at the cladding/coolant interface and at the bottom of the TFE pin.

3.3 Coolant Transient Convection:

The heat convection subroutine TConvect is used to solve for the transient convection heat transfer in the coolant [12] by using the fully implicit scheme as follows.

$$\frac{Pq''}{A} = G \frac{\partial h}{\partial z} + \rho \frac{\partial h}{\partial t} \quad (3.27)$$

Applying the discretization method yields

$$\frac{\partial h}{\partial z} = \frac{h_{j,k+1} - h_{j-1,k+1}}{\Delta z} \quad (3.28)$$

$$\frac{\partial h}{\partial t} = \frac{h_{j,k+1} - h_{j,k}}{\Delta t} \quad (3.29)$$

where

h = Enthalpy, J/Kg.

G = Mass flowrate (Kg/sec.)

P = Heated parameter of channel, cm^2 .

A = Area of channel, cm^2 .

q'' = Heat flux at surface of channel, watt/cm^2 .

ρ = Density of the coolant, Kg/cm^3 .

Plugging equations 3.28 and 3.29 into equation (3.27) yields:

$$\frac{P}{A} q_{j,k}^{\approx} = G_k \frac{h_{j,k+1} - h_{j-1,k+1}}{\Delta z} + \rho_k \frac{h_{j,k+1} - h_{j,k}}{\Delta t} \quad (3.30)$$

$$\frac{\rho_k}{\Delta t} h_{j,k} + \frac{P}{A} q_{j,k}^{\approx} = \left(\frac{G_k}{\Delta z} + \frac{\rho_k}{\Delta t} \right) h_{j,k+1} - \frac{G_k}{\Delta z} h_{j-1,k+1}$$

but $dh = C_p dT$

$$\frac{\rho_k}{\Delta t} T_{j,k} + \frac{P}{AC_p} q_{j,k}^{\approx} = \left(\frac{G_k}{\Delta z} + \frac{\rho_k}{\Delta t} \right) T_{j,k+1} - \frac{G_k}{\Delta z} T_{j-1,k+1}$$

3.3.1 Stability

From equation 3.30

$$\frac{\frac{\rho_k}{\Delta t}}{\frac{G_k}{\Delta z} + \frac{\rho_k}{\Delta t}} > 0 \quad (3.31)$$

Equation 3.31 is true for all Δt and Δz

3.3.2 Initial Conditions

$$t=0, k=1$$

$$T_{j,1} = T_{\text{coolant}}$$

$$j = 1, N$$

3.3.3 Boundary Conditions

$$z=0, j=1$$

$$T_{1,k} = T_{\text{inlet}}$$

For $j=1$

$$\frac{\rho_k}{\Delta t} T_{1,k} + \frac{P}{AC_p} q_{1,k}^{\infty} = \left(\frac{G_k}{\Delta z} + \frac{\rho_k}{\Delta t} \right) T_{1,k+1}$$

$$\Rightarrow T_{1,k+1} = \left[\frac{G_k}{\Delta z} + \frac{\rho_k}{\Delta t} \right]^{-1} \cdot \left\{ \frac{\rho_k}{\Delta t} T_{1,k} + \frac{P}{AC_p} q_{1,k}^{\infty} \right\}$$

The general equation for transient convection in the coolant can be written as:

$$T_{j,k+1} = \left[\frac{G_k}{\Delta z} + \frac{\rho_k}{\Delta t} \right]^{-1} \left\{ \frac{\rho_k}{\Delta t} T_{j,k} + \frac{P}{AC_p} q_{j,k}^{\infty} + \frac{G_k}{\Delta z} T_{j-1,k+1} \right\} \quad (3.32)$$

3.4 Computer Code Implementation:

The spatial temperature distribution within the TFE is computed through finite volume analysis. The materials within the TFE [3] are subdivided into a series of small control volumes upon which an energy balance is performed. This results in a set of first-order nonhomogeneous partial differential equations which have variable coefficients, and which may be non-linear, depending on the location of the finite element within the TFE. Variable coefficients occur due to the temperature dependence of thermal conductivities, specific heats, and densities of the TFE materials. Nonlinear terms arise due

to the heat transfer processes across the emitter/collector gap (i.e., thermionic emission, thermal radiation, and conduction through the vapor) and due to convection to the coolant.

The fully implicit method is used to solve the system of linear equations for temperatures at each time step. In the TFE, as many as 100 temperatures need to be solved at each time step. All temperature coefficients are cast into a matrix which has a banded structure of 10. The implicit method is efficient and reliable due to its stability at any given time step.

Except for the transient specific codes and subroutines, much of the thermionic-specific internals of the TFETC are based on TFEHX, a steady state code for thermionic fuel element which in turn uses CYLCON6 for modifying the TFE. CYLCON6 is called by TIMPLCIT, a transient subroutine in the TFETC which solves for the fully implicit scheme. For solving the linear equation resulting from discretization of the heat transfer equation, the user has the option of selecting either a Gaussian elimination package, which was inherited from TFEHX, or a sparse linear solver called Y12M. Y12M solves sparse systems of linear algebraic equations by Gaussian elimination. The subroutine is a "black box subroutine" designed to solve efficiently problems which contain only one system with a single right hand side. For details, see

the documentation of Y12M is available on the internet by anonymous ftp from netlib at research.att.com in the directory Y12M; login as netlib[17].

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المؤلف الرئيسي:	Al Kheliewi, Abd Allah S.
مؤلفين آخرين:	Klein, Andrew C.(Super)
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Chapter 4

Results and Analysis

A transient code (TFETC) for calculating the temperature distribution throughout the radial and axial positions of a thermionic fuel element (TFE) has been successfully developed. It accommodates the variations of temperatures, thermal power, electrical power, voltage, and current density throughout the TFE as a function of time as well as the variations of heat fluxes arising from radiation, conduction, electron cooling, and collector heating. The thermionic fuel element transient code (TFETC) is designed to calculate all the above variables for three different cases namely: 1) Start-up; 2) Loss of flow accident; and 3) Shut down. In this chapter, the results obtained from the code are presented and analyzed. The results for the start up case are shown on Figures 4.1 through 4.11, those for the loss of flow accident (LOFA) on Figures 4.12 through 4.25, and finally those for the shut down case are on Figures 4.26 through 4.45.

4.1 Start up:

In Figure 4.1, the fuel temperature increases with time until it reaches the steady state temperature (2496°K). Many factors affect the fuel temperature profile of the TFE. Among these are a) thermal power rise coefficient, τ , b) helium

heating, c) heat removal, and d) onset of electron cooling (EC). Values of 100, 300, 600, and 1200 seconds were used for the power rise coefficient, τ . During start up, helium heating is used to raise the temperature of the collector surface of the TFE assembly. The emitter temperature T_{stop} , at which helium heating stops, is a user supplied input with a nominal value of 900 °K. Similarly, the emitter temperature, T_{start} , at which electron cooling begins, is a user supplied input with a nominal value of 1900 °K. When the heat generation in the fuel is high, i.e. $\tau=100$ sec., the net effect of electron cooling (EC) (which begins a little later) is small, hence the little dip in the fuel temperature. For an appreciably lower power rise ($\tau=1200$ sec.), however, the effect of EC is rather pronounced. Regardless of these transient effects, the fuel temperature does reach the steady state value for all τ 's.

The emitter temperature profiles follow a similar pattern to that of the fuel as shown in Figure 4.2, because the only heat transfer mode between the emitter and the fuel surfaces is conduction. Notice that all the temperature fluctuations in the emitter occur around 1900 °K, the EC temperature set-point.

The coolant temperatures, as shown on Figure 4.3, increase with time until the steady state temperature is reached for all power rise coefficients. The small dips are due to the nonlinear EC effects.

As expected, the thermal power (see Figure 4.4) increases exponentially until it attains the steady state value (3177 watts) according to the following equation:

$$P_{th} = P_{ss} \cdot [1 - e^{(-t/\tau)}]$$

where

$$\begin{aligned} P_{ss} &= \text{steady state thermal power} \\ &= 3177 \text{ watts.} \end{aligned}$$

The thermal power may reach the steady state value either in fast mode or slow mode depending on the power rise coefficient, τ . The electric power profile is a function of emitter electron cooling according to the following equation [2] :

$$P_E = \frac{Q^{EC}}{(V_E + 2 \frac{kT_E}{e})} \cdot V \quad (4.1)$$

where

- Q^{EC} = Electron cooling, watt/cm².
- V = Output voltage, volts.
- V_E = Emitter potential difference, volt.
- K = Boltzman constant = 8.62×10^{-5} ev/°K.
- e = Electron charge

It is obvious from equation 4.1 that the electric power, as shown in Figure 4.5, is directly proportional to the electron cooling which follows the profile illustrated in Figure 4.8. The electron cooling heat flux, Q^{EC} , increases with time without any fluctuations for fast start up but the situation is different for slow start up. Q^{EC} is computed directly by CYLCON6, while Q^{CH} is computed from

$$Q^{CH} = Q^{EC} - J.V$$

where

J = Current density, watt/cm².

V = Interelectrode voltage, volt.

Q^{CH} is shown on Figure 4.9, while the current density, J and interelectrode voltage V are shown on Figures 4.10 and 4.11 respectively. The voltage follows the pattern of electrical power according to the following equation

$$P_E = I.V$$

where I = total current input = 490 watts.

Radiation, Q^{Rad} and conduction, Q^{cond} through the emitter collector gap are shown on Figures 4.6 and 4.7 respectively. The dip in the curve of radiation heat flux is due to the nonlinearity in the following equation:

$$Q_k^{Rad} = \sigma \epsilon_e F_{e-c} (T_{e,k}^4 - T_{c,k}^4) [2\pi r_e (\frac{Z_{k+1} - Z_{k-1}}{2})]$$

where

σ = Stefan-Boltzman constant (5.67×10^{-12}
Watts/cm²k⁴)

ϵ_e = Thermal emissivity of the emitter surface.

F_{e-c} = View factor from the emitter surface to the
collector surface ($F_{e-c} = 1$ for the emitter
surface).

The cesium conductive heat flux, Q_k^{cond} , profile is affected by
the following equation:

$$Q_k^{cond} = \frac{k_{Cs} (T_{e,k} - T_{c,k})}{d + 1.15 \times 10^{-5} \frac{(T_{e,k} - T_{c,k})}{P_{Cs}}} \left[2\pi r_e \frac{(Z_{k+1} - Z_{k-1})}{2} \right] \quad (4.3)$$

where

$T_{e,k}$ = Emitter temperature (°K).

$T_{c,k}$ = Collector temperature (°K).

k_{Cs} = Thermal conductivity of cesium vapor (W/cm.°K).

P_{Cs} = Pressure of cesium vapor at a cesium reservoir
temperature (torr).

r_e = Emitter outside radius.

d = Emitter/collector gap (cm).

The TFETC code, for the start up case, works as expected
without showing any deficiency. All temperatures, powers,
fluxes, voltages, and currents behaved in a very consistent

manner by increasing from zero power until reaching the steady state values. The running time of the code in the case of start up can be summarized as follows:

For a transient time of 1000 seconds and Δt of 0.5 second, on IBM PC486 machine of 33 Mhz with a math coprocessor, it takes about two hours and forty minutes . While for a transient time of 9000 seconds, the execution time is about 23 hours. For $\Delta t < 0.5$ second, it takes a longer time for execution. Thermal power and coolant temperature for start up are in a good agreement with the results of the TOPAZ-II simulation [6].

4.2 Loss of Flow Accident (LOFA):

The second set of graphs, Figures 4.12 through 4.25 depict the results for the loss of flow accident (LOFA). The mass flow rate of the coolant for the LOFA case is modeled as

$$m(t) = m_0 [A + B.e^{-t/\tau}] \quad (4.4)$$

where

t = Transient time, sec.

$m(t)$ = Mass flow rate as a function of time, Kg/sec.

m_0 = Mass flow rate before LOFA begins, Kg/sec.

A, B = Pump failure coefficients. $(A+B) = 1$, $B \neq 0$

τ = Mass loss coefficient, sec.

In Figure 4.12, the mass flow rate for complete pump failure ($A=0.0$, $B=1.0$) decreases quickly or slowly depending on the mass loss coefficient, τ . In the case of a LOF accident, four different pump failure cases are studied. After a period of time (4000 sec.) as shown on Figure 4.13, the mass flow rates attain the steady state values. The fuel temperature increases with time during the LOFA. The rate of temperature rise and final steady state values being governed by the fraction of pump failure. For complete pump failure (i.e 1/1 pump failure), the fuel temperature increases up to 2497 °K then stops because the code is halted upon reaching the boiling temperature of the coolant in 34 seconds. If the reactor is not shut down, the fuel temperature continues to increase until reaching the melting point of the fuel. Also, the fuel temperature increases about one degree in a complete pump failure after 34 seconds. The slow increase in fuel temperature is due to the existence of the emitter/collector gap that rejects heat to the coolant. On the other hand, the fuel temperature rise is directly proportional to the type of pump failure. For 1/2 pump failure as in Figure 4.14, the highest attainable steady state fuel temperature is about 2499 °K while for 1/4 pump failure, the highest attainable steady state fuel temperature is about 2498 °K. This means that when the heat removal of the coolant is small the fuel temperature, as in the case of 1/2 pump failure, has a high steady state value but when the heat removal is large, the

fuel temperature, as in the case of 1/4 pump failure increases at a slower rate and attains a lower steady state value. In Figure 4.14, it should be noticed that the TFE design is reliable and efficient since the highest fuel temperature does not reach the melting point of the fuel. The heat removal in the coolant is a function of the mass flow rate. Figure 4.15 shows the emitter temperature profile for different pump failures. It has a similar profile as the fuel temperature because conduction is the only mode of heat transfer between the emitter and fuel surfaces.

In the case of a complete pump failure, as shown in Figure 4.16, the time needed for the coolant temperature to exceed the boiling point, which is 1057 °K, depends on the mass loss coefficient, τ . In the case with $\tau=30$ seconds, it takes about 34 seconds to reach the NaK coolant boiling point. However, it takes about 120 seconds and 580 seconds to reach the NaK coolant boiling point for mass loss coefficients of 120 and 600 respectively. The maximum coolant temperatures, in the case of mass loss coefficient, τ , of 30 seconds, at different pump failures (see Figure 4.17) are listed below

$T_{\max.} > 1057$ °K for 1/1 pump failure.

$T_{\max.} = 1017$ °K for 1/2 pump failure.

$T_{\max.} = 987$ °K for 1/3 pump failure.

$T_{\max.} = 977$ °K for 1/4 pump failure.

The coolant temperature may exceed its boiling point if an appropriate action is not taken. The reactor would probably have a set point to trip the reactor when the coolant exit temperature got too high. Also, if the coolant temperature gets high then in a zirconium hydride moderated reactor, like the ATI or TOPAZ-II designs, the hydrogen will begin to disassociate from the ZrH, and this will add negative reactivity, thereby shutting down the reactor.

The thermal power in LOFA keeps constant before tripping the reactor as shown in Figure 4.18. It starts decreasing after the reactor is shut down. In the case of 1/1 pump failure, the mass flowrate decreases quickly and the heat is accumulated in the collector and emitter surfaces without being removed. This, in turn, increases the emission of electrons from the emitter surface that would be significant according to the following equation:

$$\eta = (J_E - J_C) \cdot \frac{V}{\Sigma Q} \quad (4.5)$$

where

η = Efficiency of thermionic fuel element.

J_E = Emitter current density, watt/cm².

J_C = Collector current density, watt/cm².

V = Output voltage, volt.

$$\begin{aligned}
 \Sigma Q &= Q^{\text{Rad}} (\downarrow) + Q^{\text{EC}} (\uparrow) + Q^k (\downarrow) \\
 &= - 0.08 + 0.85 - 0.0036 \\
 &= 0.7664 \text{ watt/cm}^2
 \end{aligned}$$

The efficiency of the reactor will decrease according to the above equation. The electrical power drops off to its lowest value at a complete pump failure while it decreases a little until reaching the steady state value as in the cases of 1/2, 1/3, 1/4 pump failures, as shown in Figure 4.19. In the case of 1/2 pump failure, the maximum attainable power value is 315 watt. In the case of 1/3 pump failure, the maximum attainable power value is 314 watt. In the case of 1/4 pump failure, the maximum thermal power value is 307 watt.

The decrease of heat fluxes in Q^{Rad} and Q^k , as shown in Figures 4.20 and 4.21, is very small so their changes can be neglected. The decrease in Q^{Rad} is due to the back emission of the collector which affects the emissivity properties of the emitter surface. The electron cooling and collector heating terms are dependent on temperature variations. When the fuel temperature rises, the emitter temperature will rise too so the emission of electrons will increase. This increase in electron cooling is a function of heat removal which, in turn, is a function of the mass flowrate. In a complete loss of flow, the electron cooling increases by 0.8 watt/cm² in about 34 seconds (see Figure 4.22) while it does not increase by more than 0.1 watt/cm² in the case of loss of half pump

failure. The electrical current density is a function of electron cooling as shown in Figure 4.24.

4.3 Shut down:

In the case of shut down four types of negative reactivity insertions are introduced. These reactivities are:

$$\rho = - \$0.10$$

$$\rho = - \$0.30$$

$$\rho = - \$0.90$$

$$\rho = - \$3.0$$

The larger the negative reactivity insertion the faster the shut down of the reactor. The fuel temperature shows the most decrease for the case of $-\$3.0$ reactivity insertion without showing any oscillations in the curve (see Figure 4.26), because the heat generation in the fuel drops off abruptly according to the prompt jump approximation. The sharp change shown for the $-\$0.1$ and $-\$0.3$ insertions are due to 1) the change of shut down mode of thermal power from prompt jump to exponential, and 2) the weak absorption of thermal neutrons in the case of low negative reactivity insertions which allows some thermal neutrons, not absorbed yet, to generate heat to the fuel and these neutrons will die out eventually. In large reactivity insertions, most of the

thermal neutrons are absorbed so that the rest are not able to induce any significant change in the fuel temperature behavior.

The emitter temperature follows the same profile as the fuel temperature except that at low negative reactivity insertions (i.e., $-\$0.1$), when the heat removal from the emitter surface will be less than the heat supply just right after the prompt jump. The coolant temperature drops off to the coolant inlet temperature of 895 °K. It takes about 700 seconds to reach the inlet temperature in the case of $\$3.0$ negative reactivity insertion and 1500 seconds in the case of $\$0.1$ insertion. The heat transfer coefficients (ρ, C_p) vary with time as a function of heat generation to the fuel. The enthalpy equation is:

$$dh = C_p Dt$$

or

$$\int dh = \int C_p dT$$

and the transient implicit finite difference equation [7] for the coolant is given by:

$$T_{j,k+1} = \left[\frac{G_k}{\Delta Z} + \frac{\rho_k}{\Delta t} \right]^{-1} \left(\frac{\rho_k}{\Delta t} T_{j,k} + \frac{P}{AC_p} q_{j,k} + \frac{G_k}{\Delta Z} T_{j-1,k+1} \right) \quad (4.6)$$

where

C_p = Specific heat of coolant, J/Kg.°K.

ρ = Coolant density, Kg/cm³.

A = Flow area, cm².

P = Flow perimeter, cm.

G = Mass velocity, Kg/sec.cm².

q" = Heat flux at coolant channel surface, watt/cm².

The coolant temperature behaves according to the above equation. It is noticed that the coolant temperature is a function of some fixed and some variable parameters as follows:

T(Δz , Δt , P, A) Fixed Parameters

T(ρ , C_p , G_k , q") Variable Parameters

Equation 4.6 can be simplified by the following equation:

$$T_{j,k+1} = \frac{[\rho_k(t) T_{j,k} + \frac{q_{j,k}^*(t)}{C_p(t)} + G_k(t) T_{j-1,k+1}] (4.7)}{G_k(t) + \rho_k(t)}$$

The thermal power drops off sharply at large negative reactivity insertions and slower but with the same exponential pattern at low negative reactivity insertion as in Figure 4.29. The electrical power reaches zero at - β 0.1 insertion after 150 seconds and reaches zero at - β 3.0 insertion after 50 seconds as illustrated in Figure 4.30. The zero electrical power has to do with the emitter temperature set point Tstart. When the emitter temperature falls below this value, the CYLCON6 subroutine may not be able to converge and provide results for electrical power, hence, the call to CYLCON6 is

stopped and the electrical power is set to zero. The radiation heat flux from the emitter surface follows the behavior of the emitter temperature. The higher the emitter temperature the higher the radiation heat flux and vice versa (see Figure 4.31). The conductive heat flux profile of cesium in the emitter/collector gap follows the same pattern as the emitter surface temperature as shown in Figure 4.32. The behavior of electron cooling and collector heating in Figures 4.33 and 4.34 is due to the behavior of the electrical current according to the following equation:

$$Q^{EEC} = J_E \left(V_E + 2 \frac{kT_E}{e} \right) \quad (4.8)$$

where

J_E = Current density of the emitter surface, amp/cm².

V_E = Voltage across the emitter surface, volt.

T_E = Emitter temperature, °K.

K = Boltzman constant = 8.62×10^{-5} eV/°K.

The electron cooling (EC) is directly proportional to the current density as in the above equation. For the electron current density, it is stated that the current density increases at low output voltage values [3,4,5] and decreases at high output voltage according to the Richardson-Dushman equation. However, it is noticed in Figure 4.35 that the

current density, for a large negative reactivity insertion ($-\beta 3.0$), increases to 8.5 watt/cm^2 in a transient time of about 50 seconds then decreases to its lowest value (zero) due to zero electrical power. For the lowest negative reactivity insertion ($-\beta 0.1$), the highest attainable value of current density is 6.29 watt/cm^2 after about 150 seconds. The voltage drop during shut down follows the electrical power profile as shown in Figure 4.36.

4.4 Start up at Different EC temperatures:

The start up of the TFE has been tested at different electron cooling temperatures of 1500, 1900, and 2000 °K respectively. The behavior of the temperatures, electrical power, current density, thermal power, voltage, and heat fluxes are nearly the same. The fuel, emitter, and coolant temperatures, in a small portion of the curves, are high at 2000 °K and low at 1500 °K as shown in Figures 4.37, 4.38, and 4.39 respectively. The reason behind this behavior arises from the fact that the heat removal by electron cooling at 2000 °K starts a little bit later than the heat removal by electron cooling at 1500 °K which allows a small increase in the temperatures before they attain the steady state temperatures. The electrical power at 2000 °K starts after 320 seconds of start up while it starts after 300 seconds in the case of 1900 °K and after 240 seconds in the case of 1500 °K. Of course, the

electrical power depends on the current and in turn the current depends on the temperature difference between the emitter surface and the collector [1] surfaces. When the emitter and collector surface temperatures reach the steady state value then the electrical power will be stable and will attain the steady state value. The radiation heat flux (see Figure 4.41) is higher when the electron cooling starts late because the emissivity of the emitter surface increases with temperature increase and reaches its maximum value before the electron cooling starts. When the electron cooling starts earlier, however, the emissivity would not reach its maximum value because the heat removal starts earlier too. Figures 4.42 and 4.43 show that the electron cooling and collector heating heat fluxes are dependent on the emitter and collector surfaces respectively. The electron cooling starts earlier at 1500 °K and starts increasing until reaching the steady state value. The current density, as shown in Figure 4.44, is a function of the emitter and collector surface temperatures thus it follows the same profile. The voltage drop is a function of the electrical current and follows the same behavior.

4.5 The accuracy of the results:

There are two types of errors associated with the results. The first error is due to the discretization of the implicit

method [9] and the second one is due to the round-off error of Gaussian elimination [8]. The error from the implicit method is considered to be as a function of 1) the time step; 2) Δr ; and 3) Δz , where Δr and Δz are the radial thickness and axial length in respectively. The error arising from the Gaussian elimination depends somewhat on different parameters listed below:

1. Condition number of the matrix, $K(A)$.
2. Size of the matrix.
3. Floating point precision.
4. The inaccuracy in the matrix element.

The exact temperature is given by:

$$T_1 = T_{\text{exact}} \pm M[\Delta t_1 + (\Delta r)^2 + (\Delta z)^2] \pm EGAUSS \quad (4.9)$$

$$T_2 = T_{\text{exact}} \pm M[\Delta t_2 + (\Delta r)^2 + (\Delta z)^2] \pm EGAUSS \quad (4.10)$$

where

- Δr = Radial thickness of the TFE, cm.
- Δz = Axial thickness of the TFE, cm.
- Δt = Time increment, sec.
- T_1 = Computed temperature for Δt_1 at a given point, °K.
- T_2 = Computed temperature for Δt_2 at a given point, °K.

T_{exact} = Exact temperature at a given point, °K.

EGAUSS = Error arising from Gaussian.

M = Constant of the error arising from the implicit method.

M can be determined as follows:

$$M = \frac{T_2 - T_1}{\Delta t_2 - \Delta t_1} \quad (4.11)$$

where

Δt_2 = Time step at T_2 , sec.

Δt_1 = Time step at T_1 , sec.

$\Delta t_1 \ll \Delta t_2$

Substituting the value of M in equation 4.10 yields

$$T_2 = T_{\text{exact}} \pm \frac{T_2 - T_1}{\Delta t_2 - \Delta t_1} [\Delta t_2 + (\Delta r)^2 + (\Delta z)^2] \pm \text{EGAUSS} \quad (4.12)$$

The relative bound error associated with Gaussian elimination is given by the following equation:

$$\frac{\|T_{\text{exact}} - T_1\|}{\|T_{\text{exact}}\|} \leq K(A) \frac{\|E\|/\|A\|}{1 - K(A) \|E\|/\|A\|} \quad (4.13)$$

where

$K(A)$ = Condition of the matrix = $\|A\| \cdot \|A^{-1}\|$.

A = Matrix.

E = Error associated with a matrix A .

$$\|E\| \leq (2n+1)g2^p \quad (4.14)$$

where

g = Growth factor

n = Size of the matrix.

p = Binary floating point arithmetic.

If $K(A)$ is close to unity, the matrix A is well-conditioned and if it is large, the matrix A is ill-conditioned. The size of E in equation 4.13 depends on the precision of the arithmetic used in the computation. The typical values used in the TFETC code were as follows:

$\Delta t = 0.5$ sec.

$\Delta r = 0.125$ cm.

$\Delta z = 2.54$ cm.

The error associated with the discretization of the implicit method depends mainly on the number of nodes in both axial and radial directions. It decreases with increasing of the node points and increases with decreasing of the node points. The largest error associated with the implicit method is the one arises from Δz , so it is advisable to reduce the value of Δz to be less than 1.

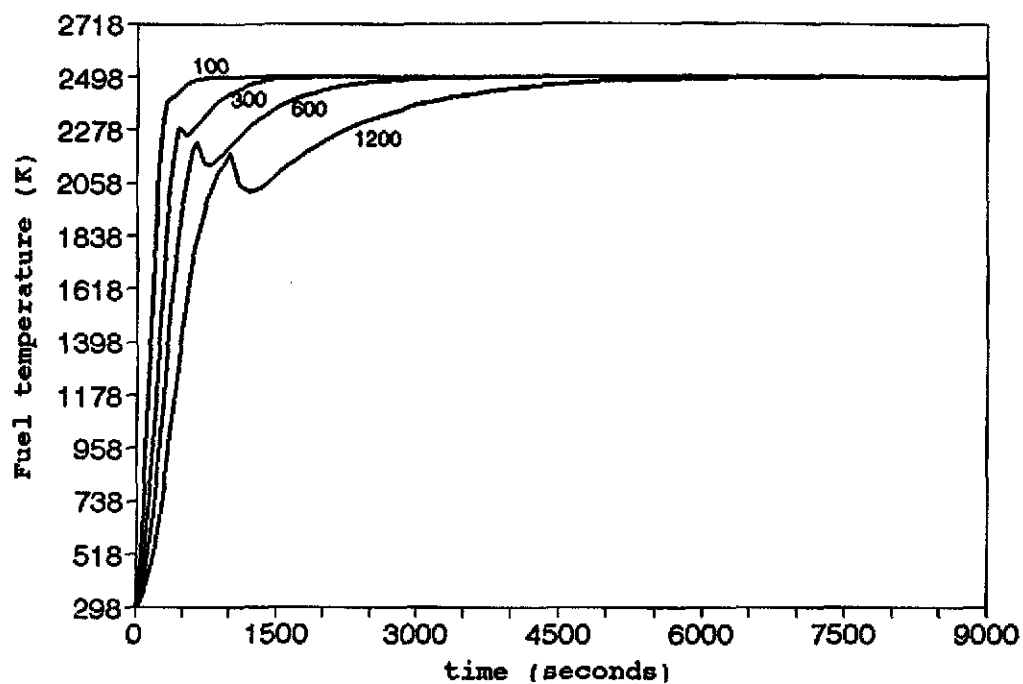


Figure 4.1 Fuel temperature profile for reactor start-up.

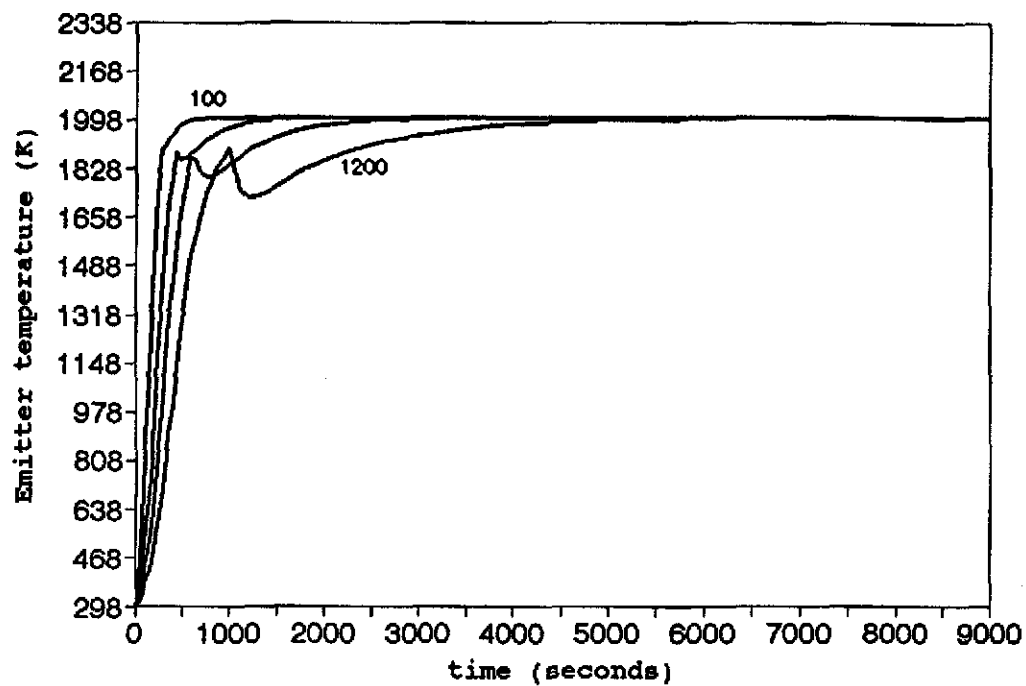


Figure 4.2 Emitter temperature profile for reactor start-up.

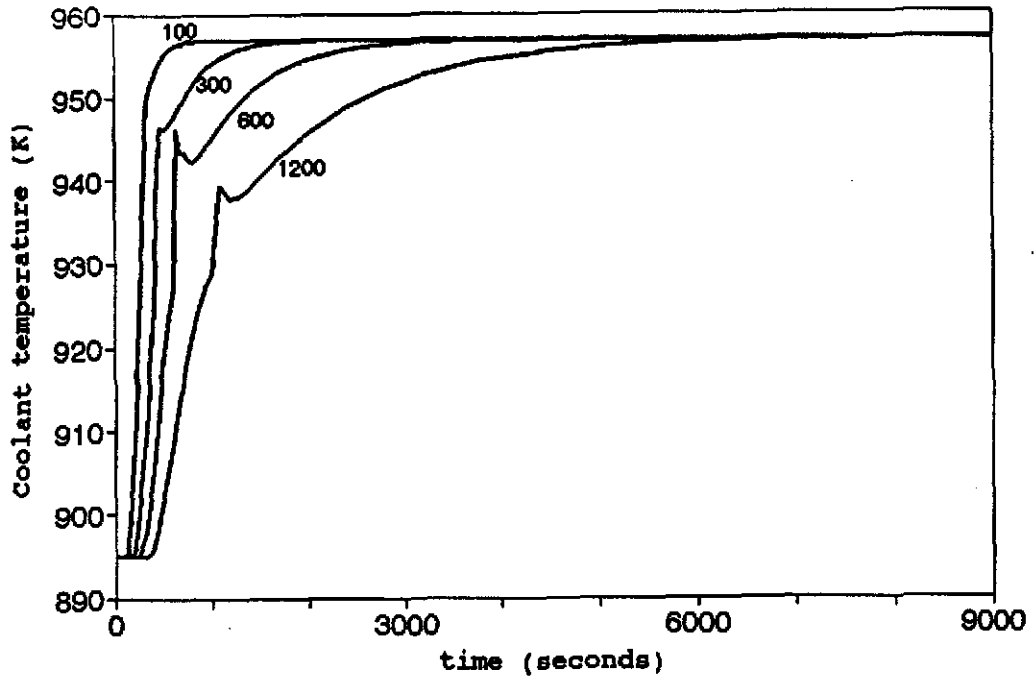


Figure 4.3 Coolant temperature profile for reactor start-up.

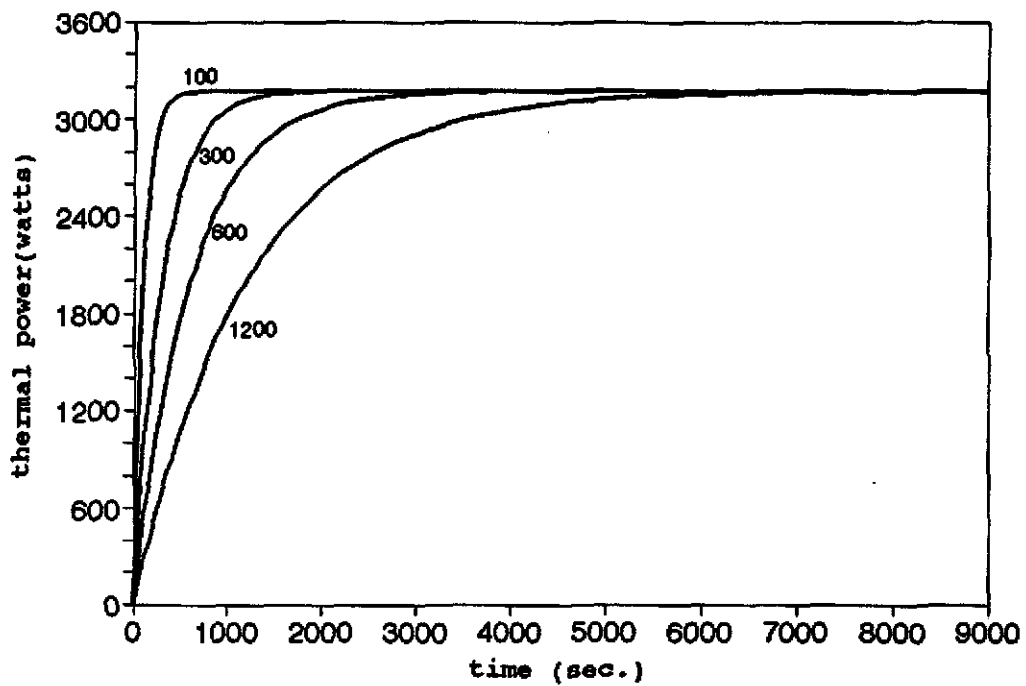


Figure 4.4 Thermal power profile for reactor start-up.

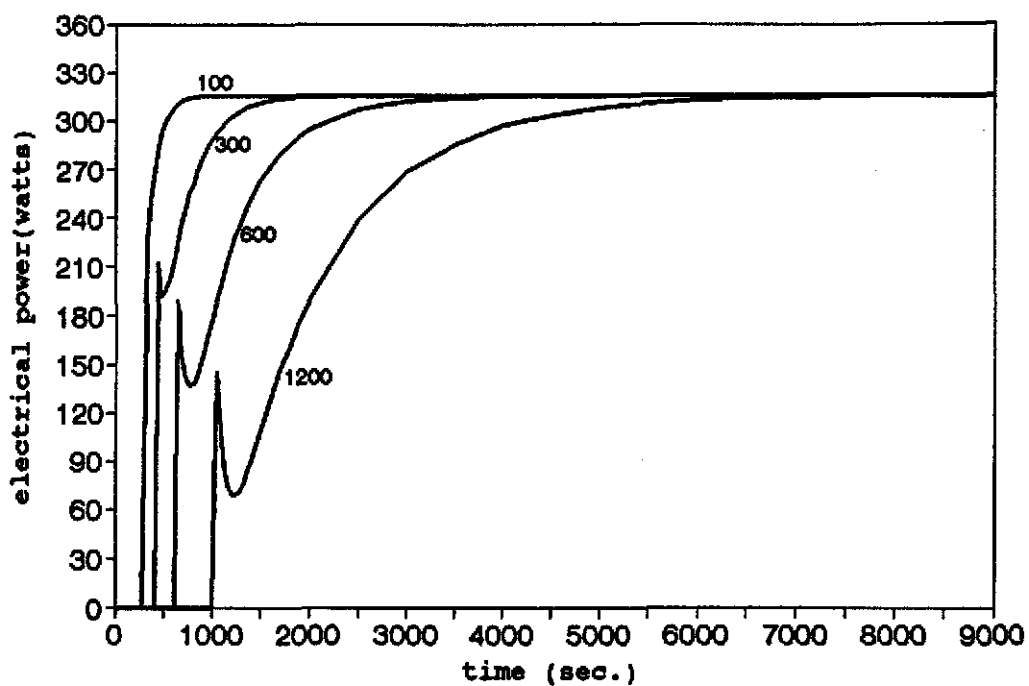


Figure 4.5 Electrical power profile for reactor start-up.

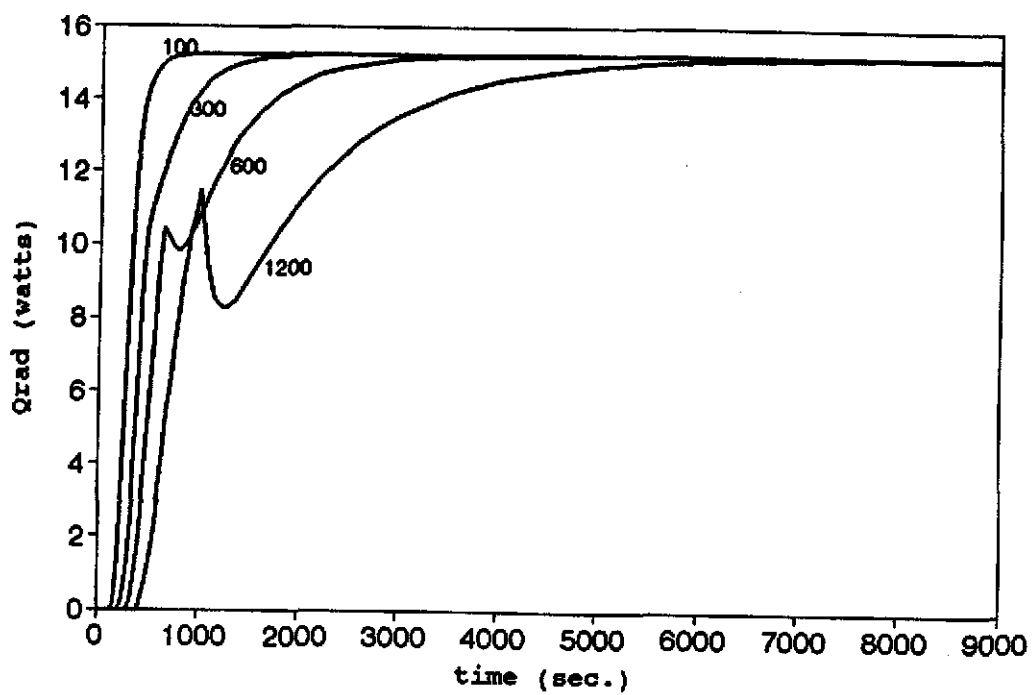


Figure 4.6 Radiation heat flux distribution for reactor start-up.

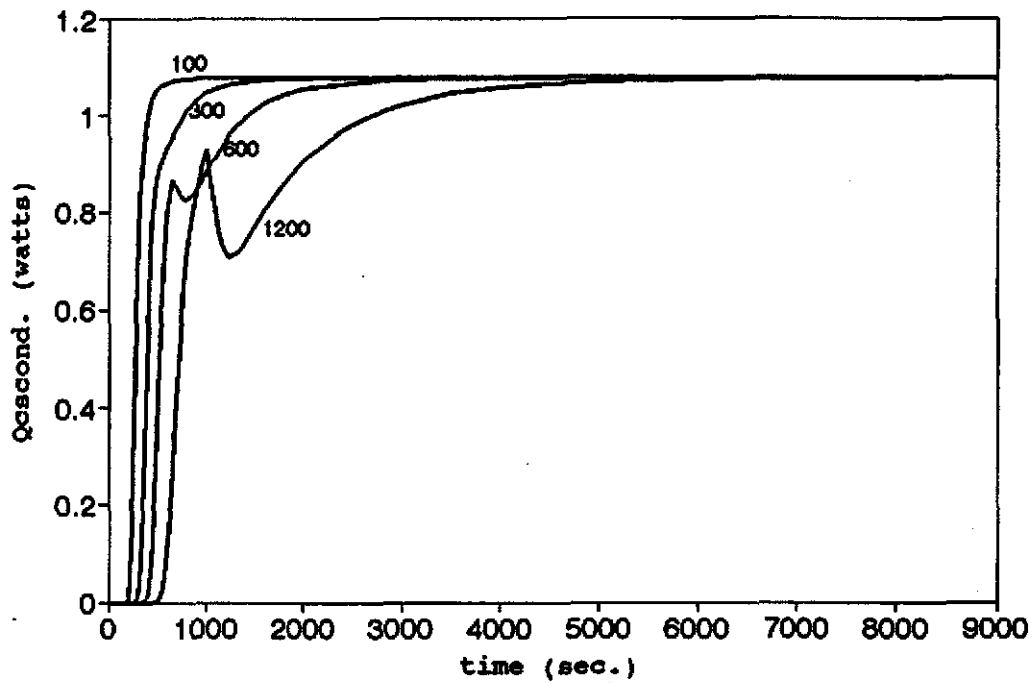


Figure 4.7 Conductive heat flux distribution of cesium for reactor start-up.

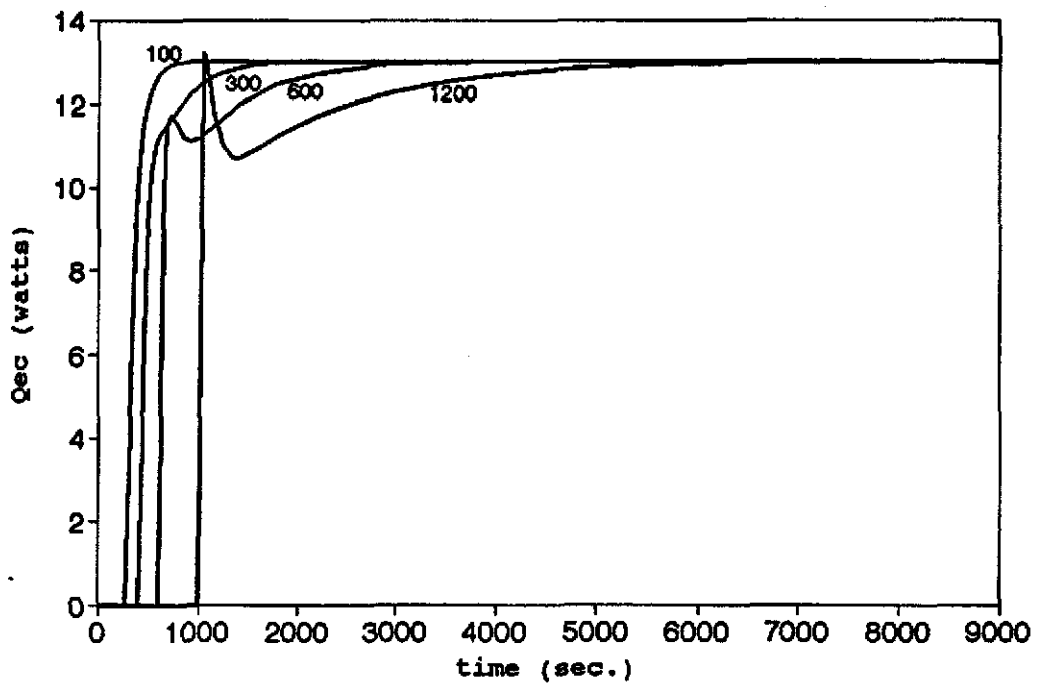


Figure 4.8 Heat flux distribution of emitter electron cooling for reactor start-up.

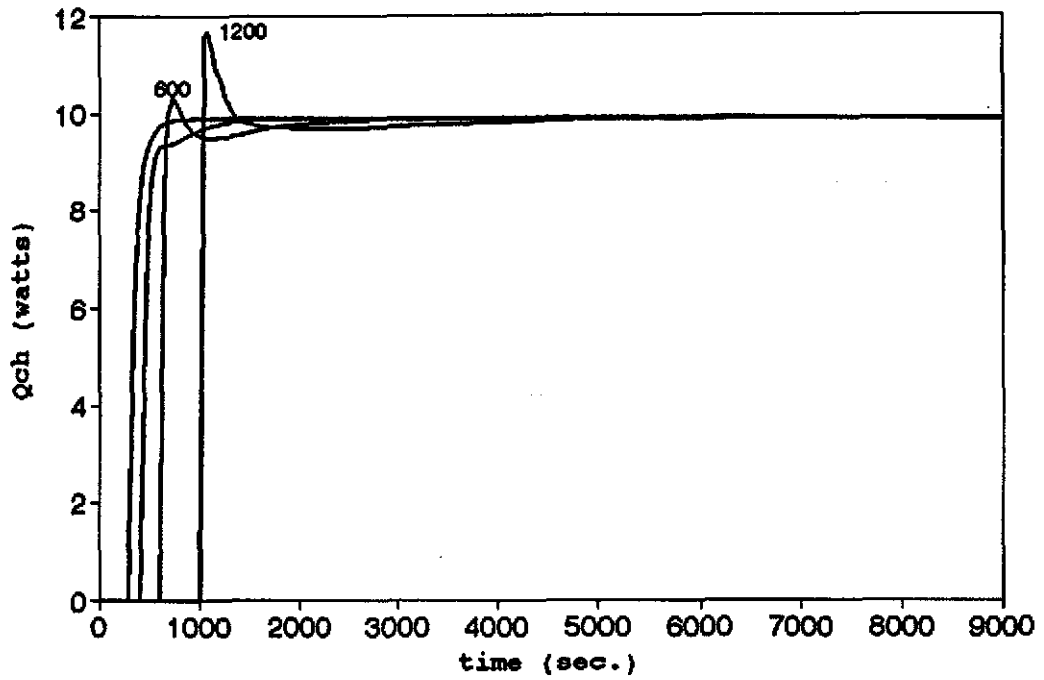


Figure 4.9 Heat flux distribution of collector electron heating for reactor start-up.

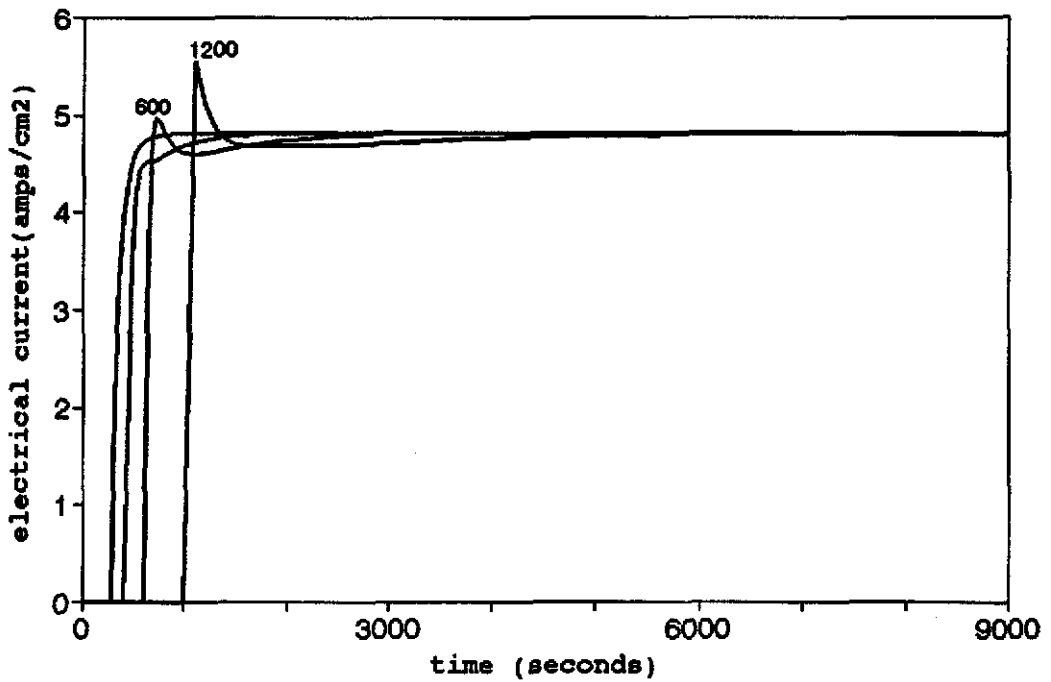


Figure 4.10 Electrical current profile for reactor start-up.

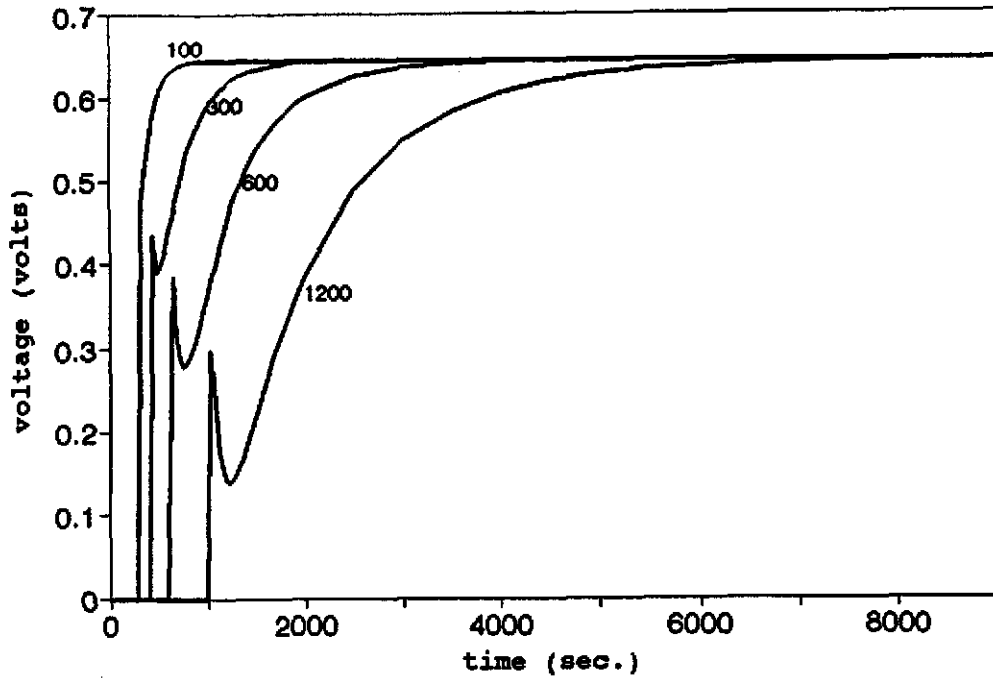


Figure 4.11 Electrical voltage profile for reactor start-up.

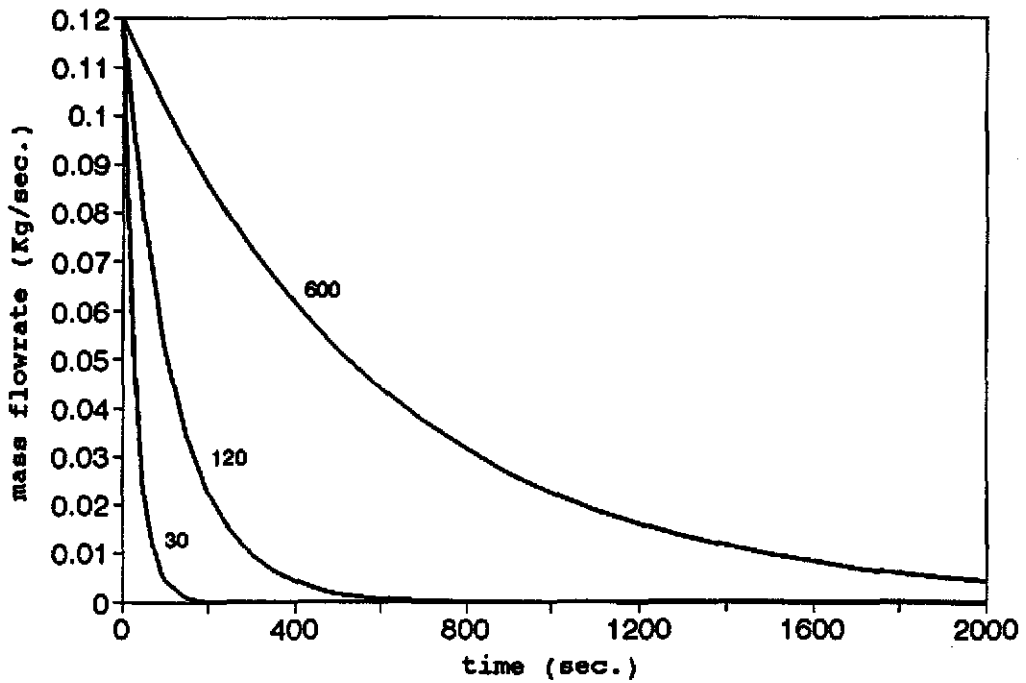


Figure 4.12 Mass flow rate for different decreasing exponential coefficients in LOF accident.

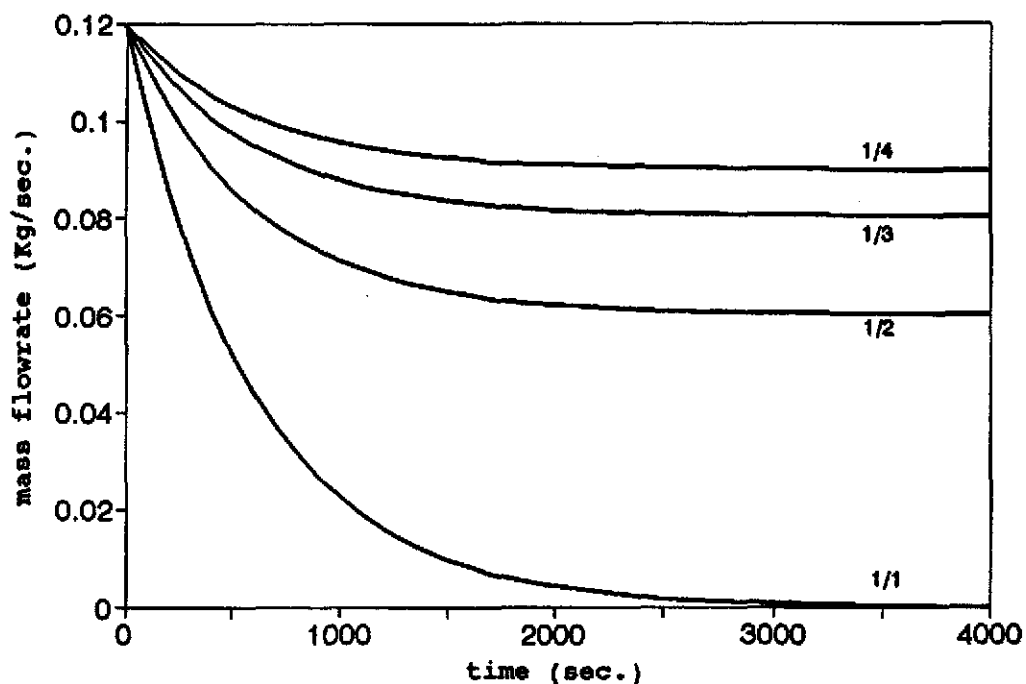


Figure 4.13 Mass flow rate distribution for different types of pump failures in LOF accident.

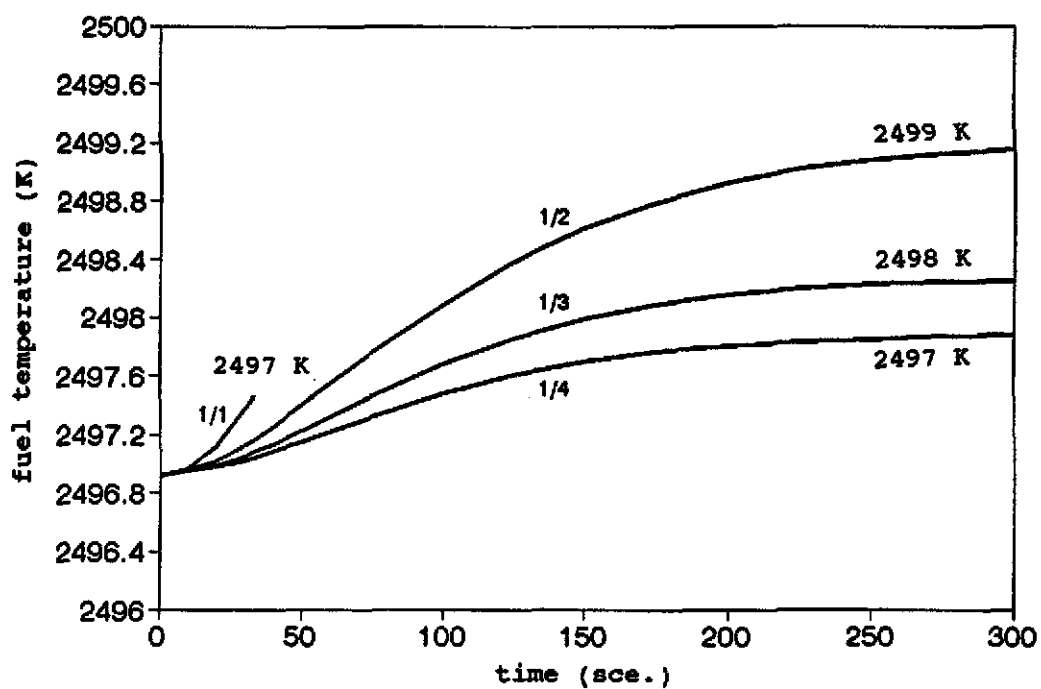


Figure 4.14 Fuel temperature profile for different types of pump failures at ($\tau = 30$ seconds).

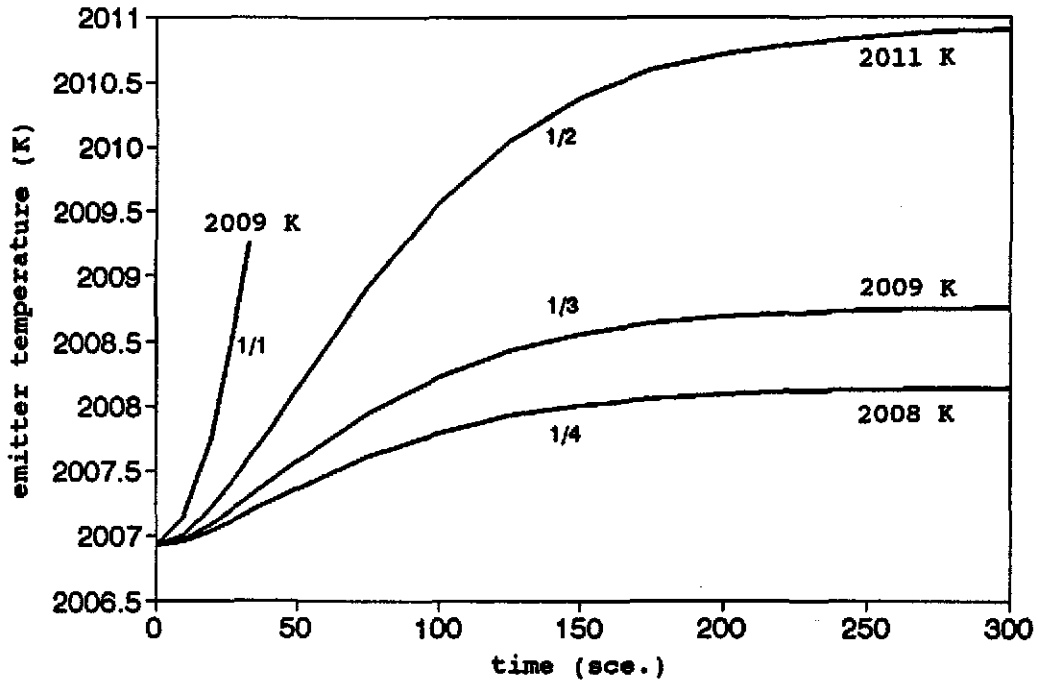


Figure 4.15 Emitter temperature profile for different types of pump failures at ($\tau = 30$ seconds).

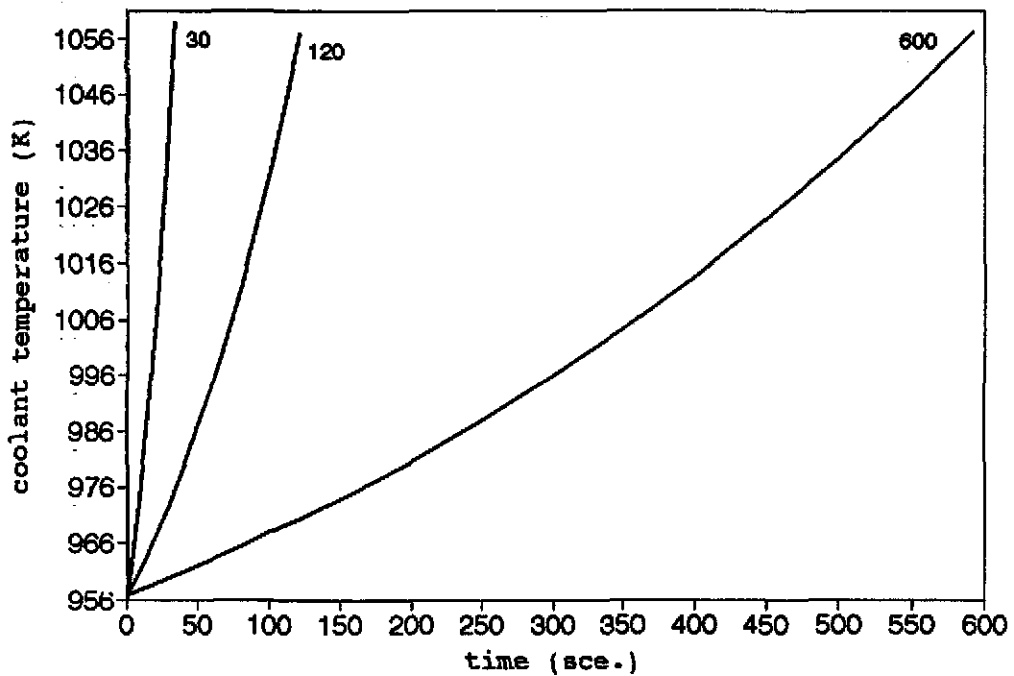


Figure 4.16 Coolant temperature profile for 1/1 pump failure at different decreasing exponential coefficients.

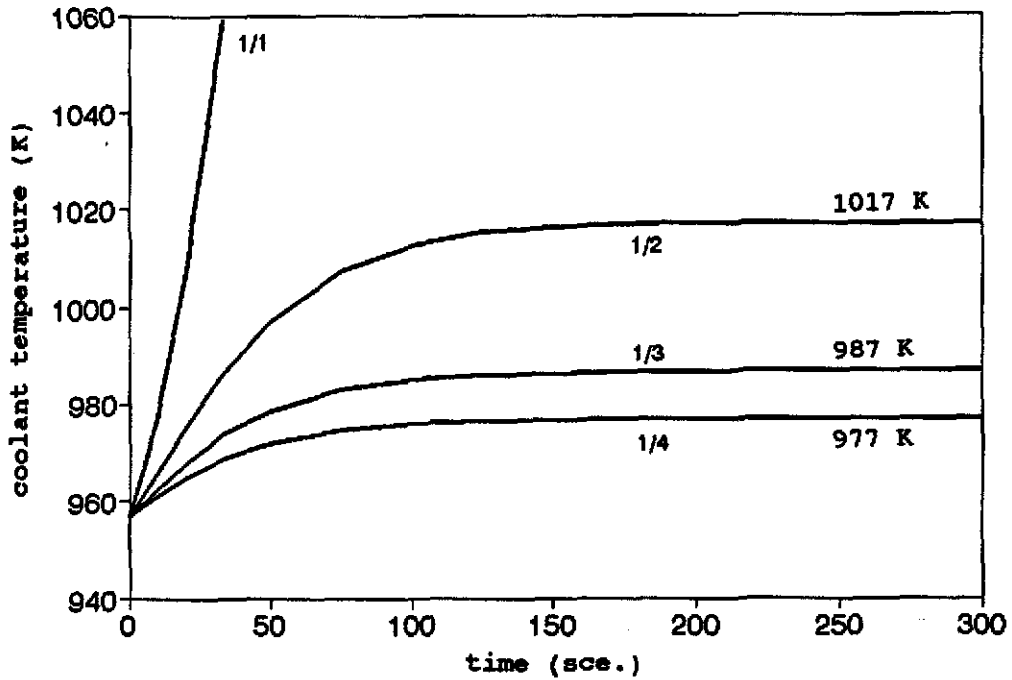


Figure 4.17 Coolant temperature profile for different types of pump failures at ($\tau = 30$ seconds).

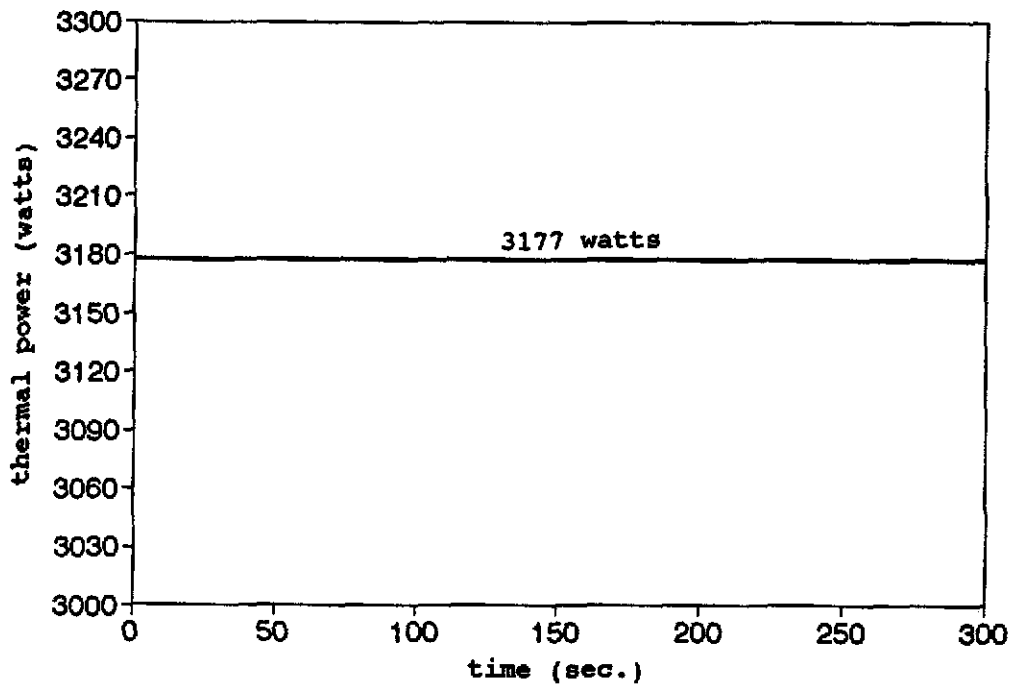


Figure 4.18 Thermal power distribution for LOF.

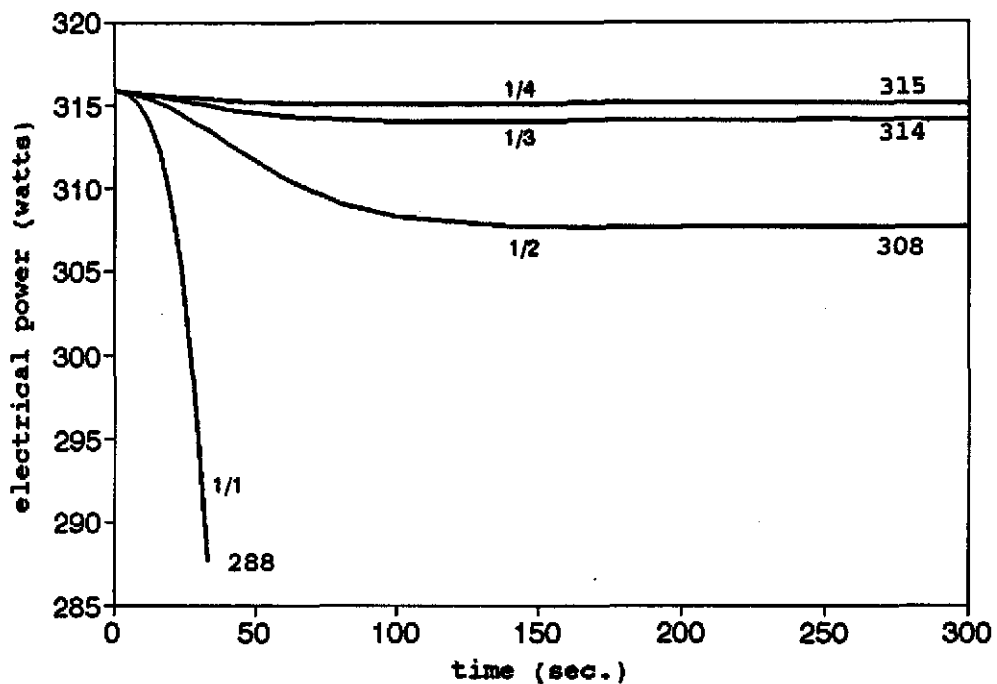


Figure 4.19 Electrical power profile for LOF accident at ($\tau = 30$ seconds).

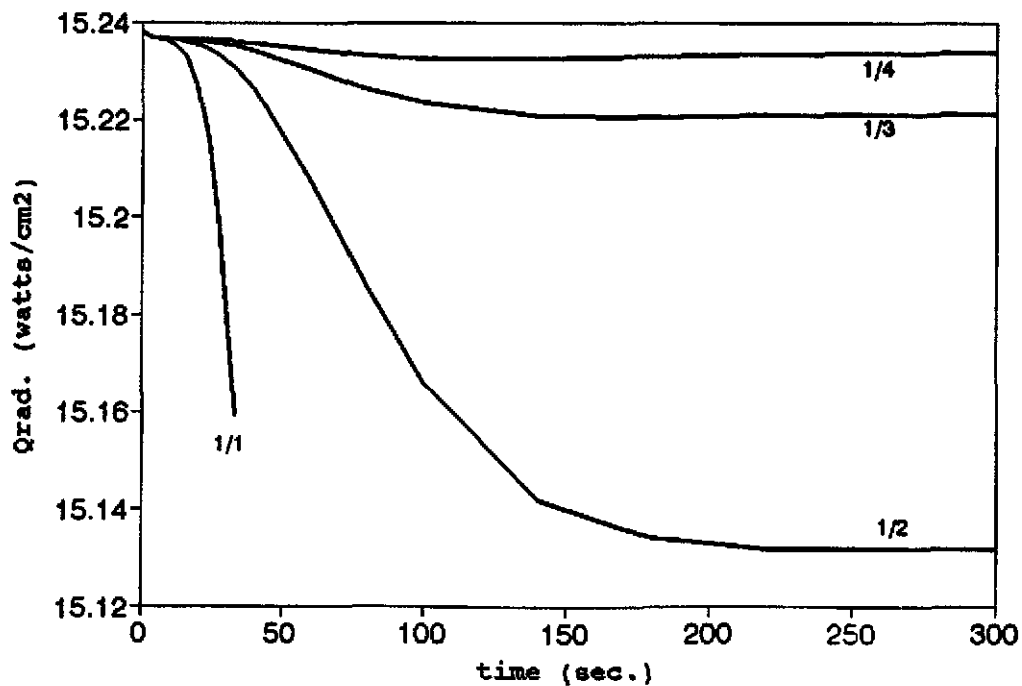


Figure 4.20 Radiation heat flux distribution for LOF accident at ($\tau = 30$ seconds).

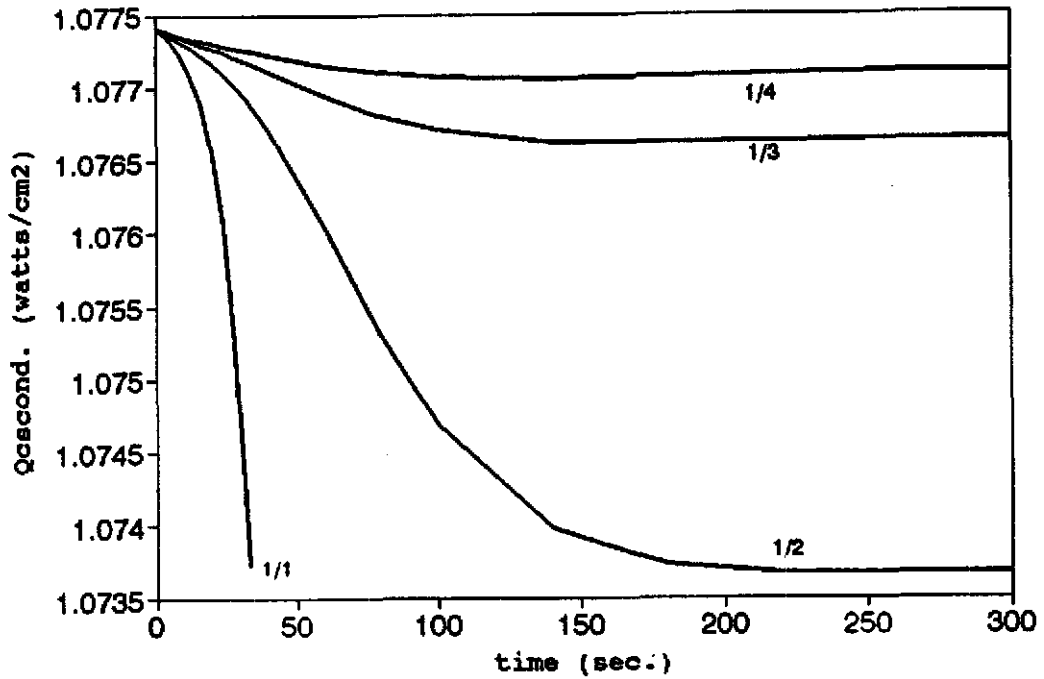


Figure 4.21 Conductive heat flux distribution of cesium for LOF accident at ($\tau = 30$ seconds).

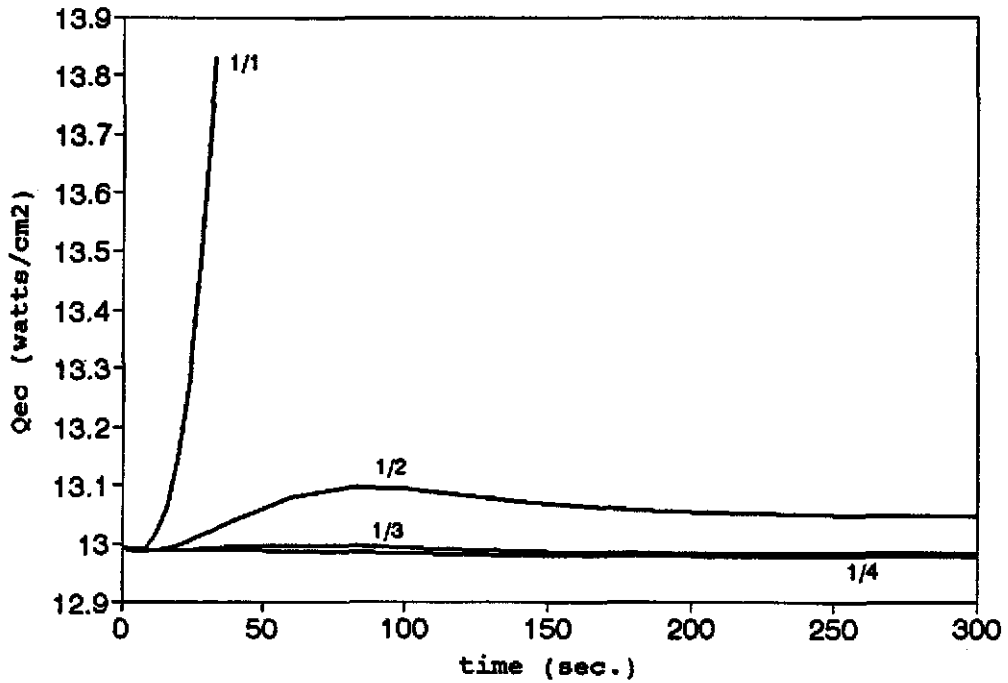


Figure 4.22 Heat flux distribution of emitter electron cooling for LOF accident at ($\tau = 30$ seconds).

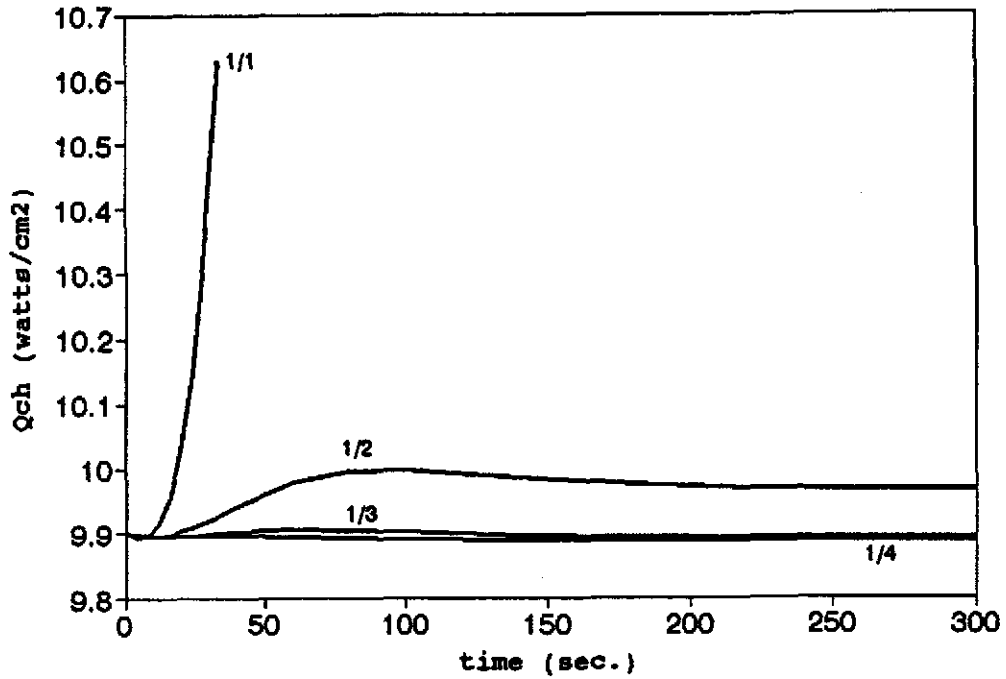


Figure 4.23 Heat flux distribution of collector electron heating for LOF accident at ($\tau = 30$ seconds).

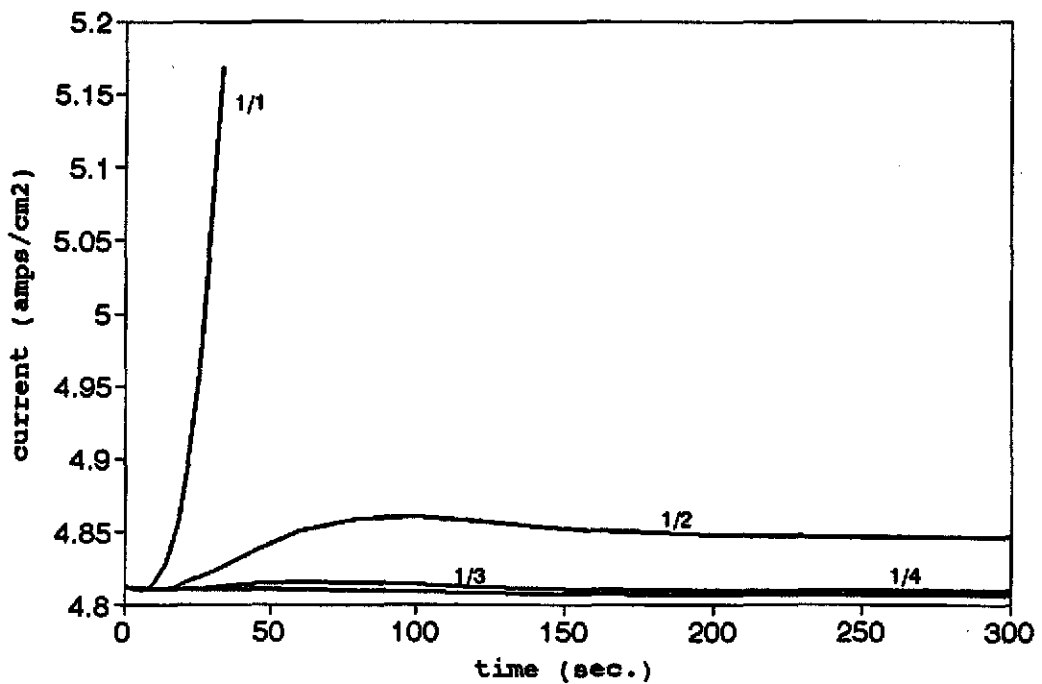


Figure 4.24 Electrical current profile for LOF accident at ($\tau = 30$ seconds).

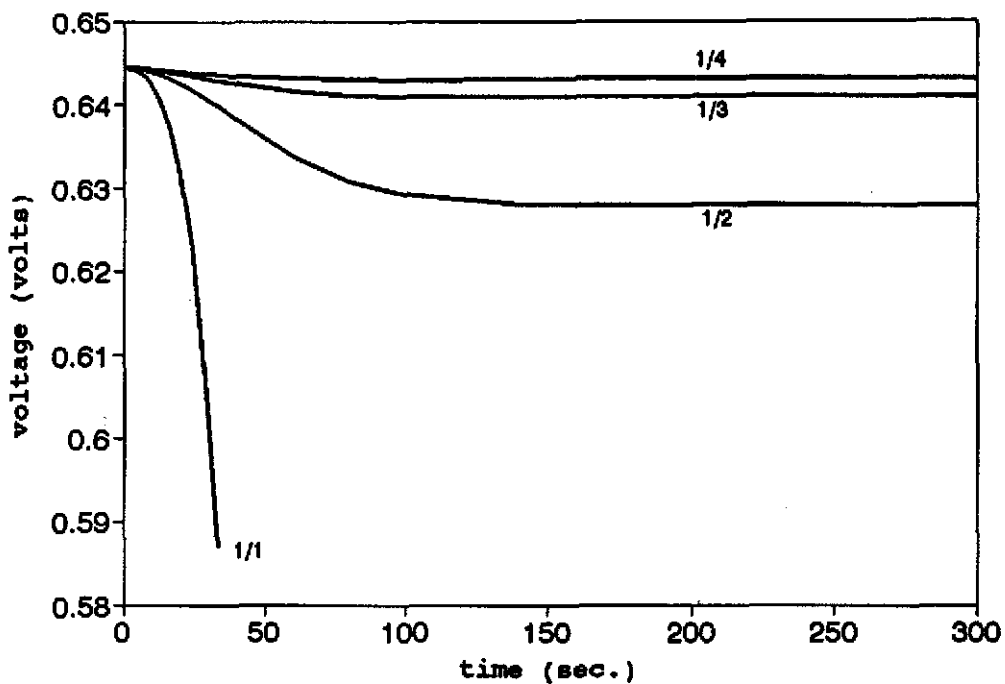


Figure 4.25 Electrical voltage profile for LOF accident at ($\tau = 30$ seconds).

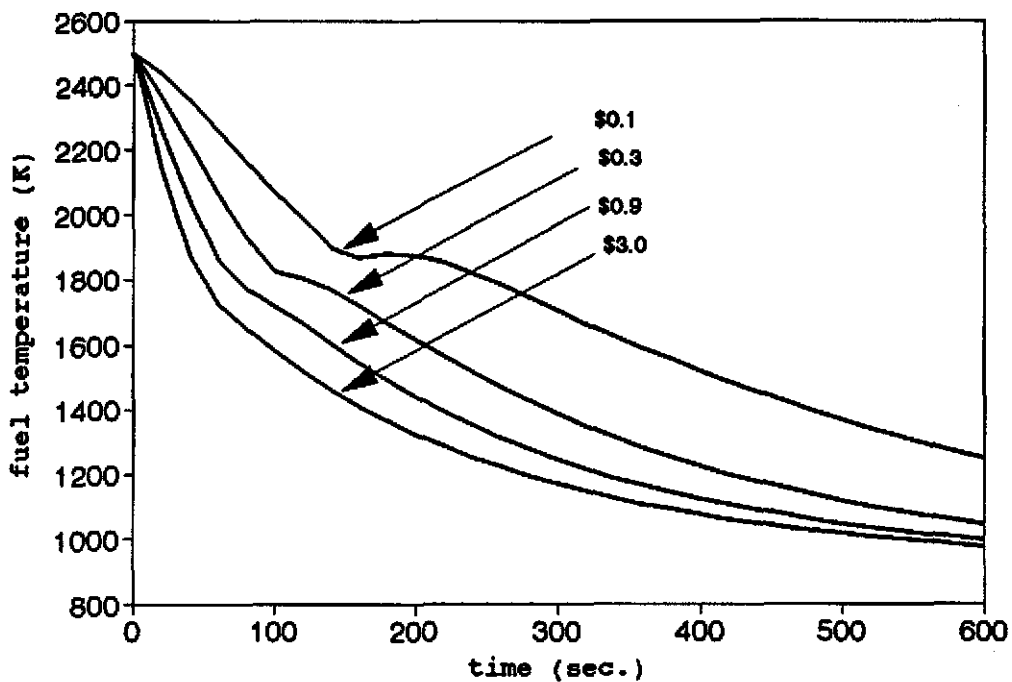


Figure 4.26 Fuel temperature profile for reactor shut down at different negative reactivity insertions.

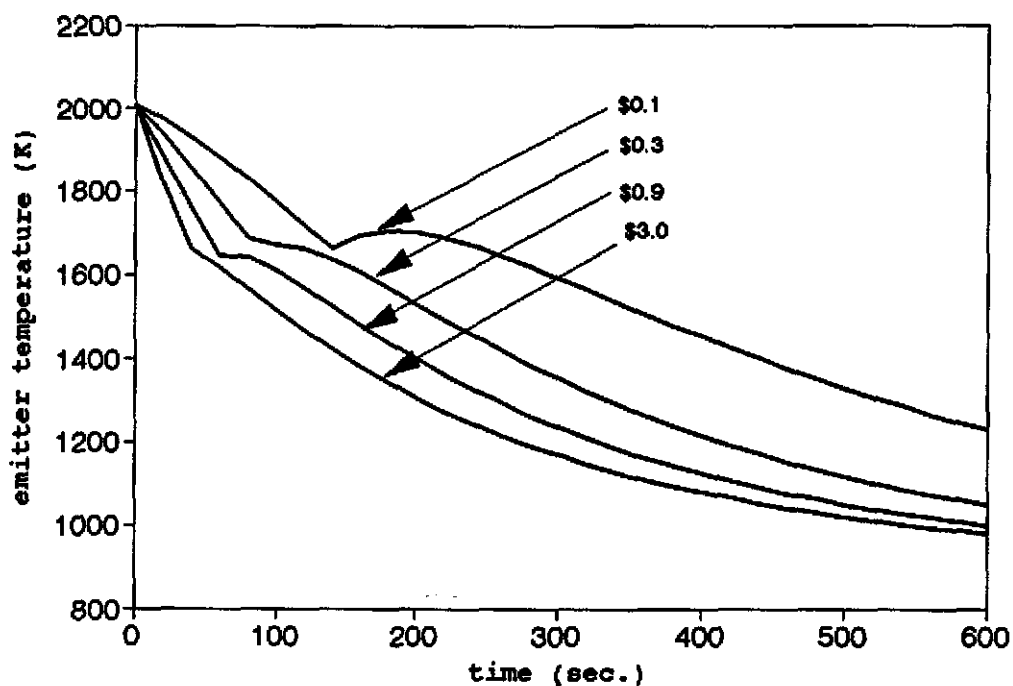


Figure 4.27 Emitter temperature profile for reactor shut down at different negative reactivity insertions.

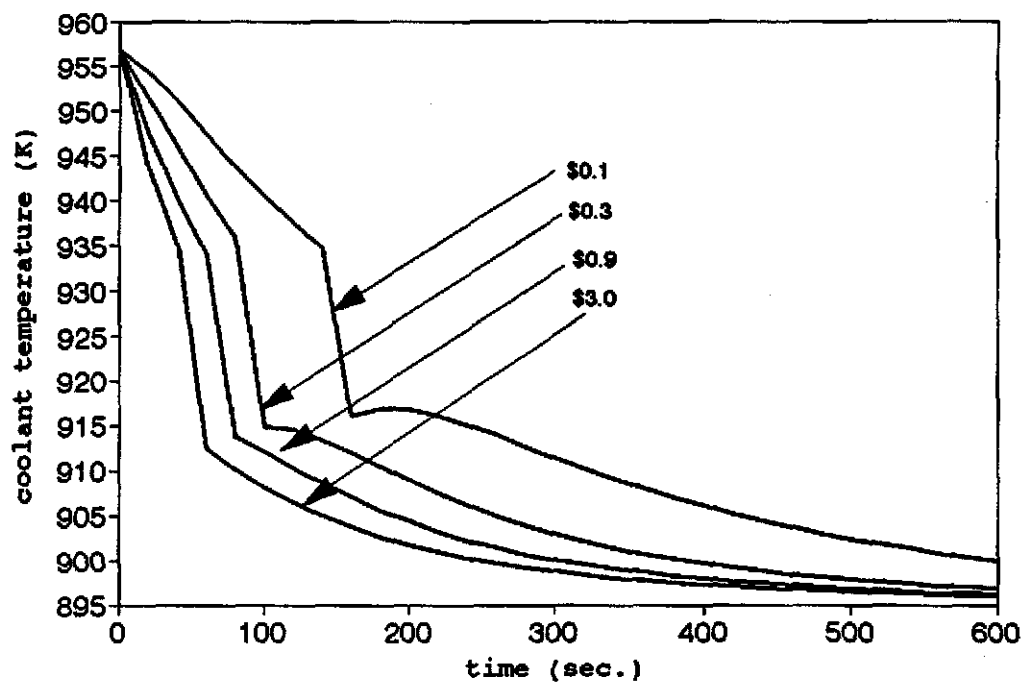


Figure 4.28 Coolant temperature profile for reactor shut down at different negative reactivity insertions.

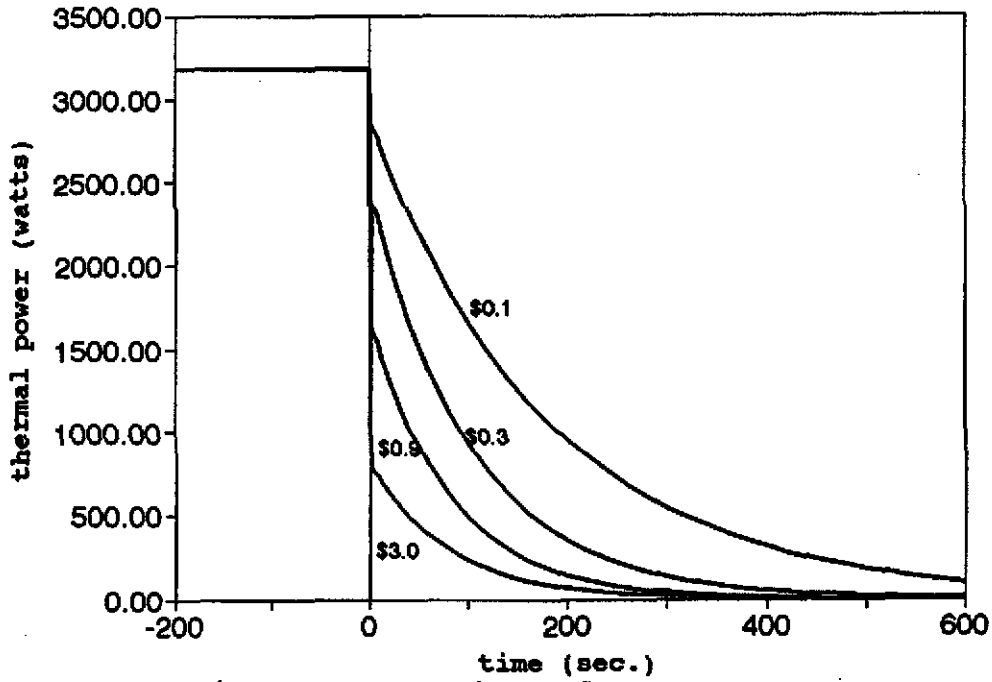


Figure 4.29 Thermal power profile for reactor shut down at different negative reactivity insertions.

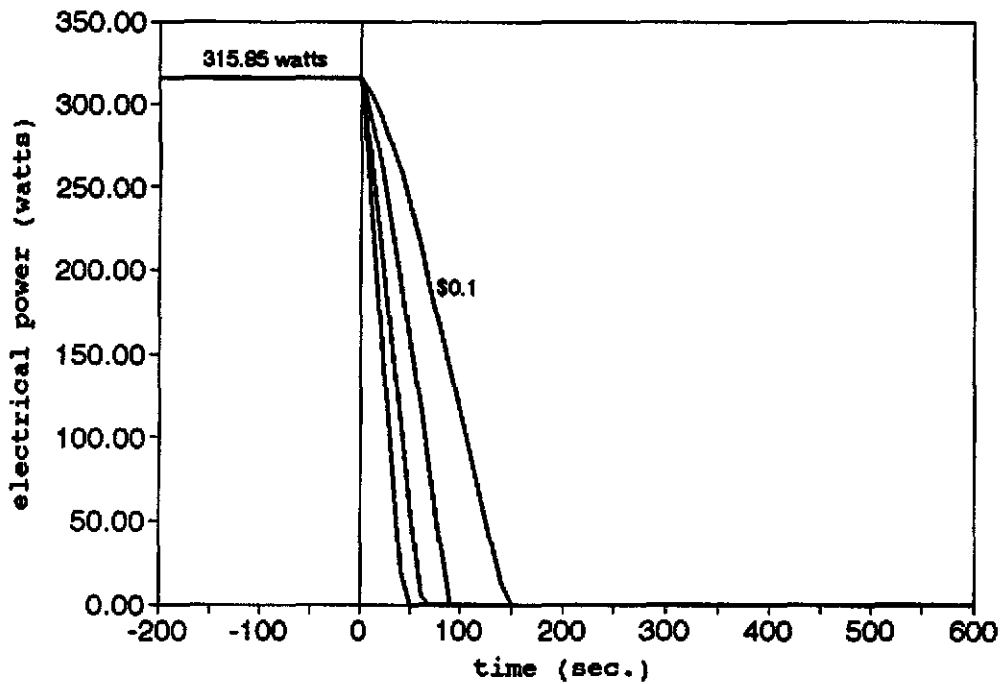


Figure 4.30 Electrical power profile for reactor shut down at different negative reactivity insertions.

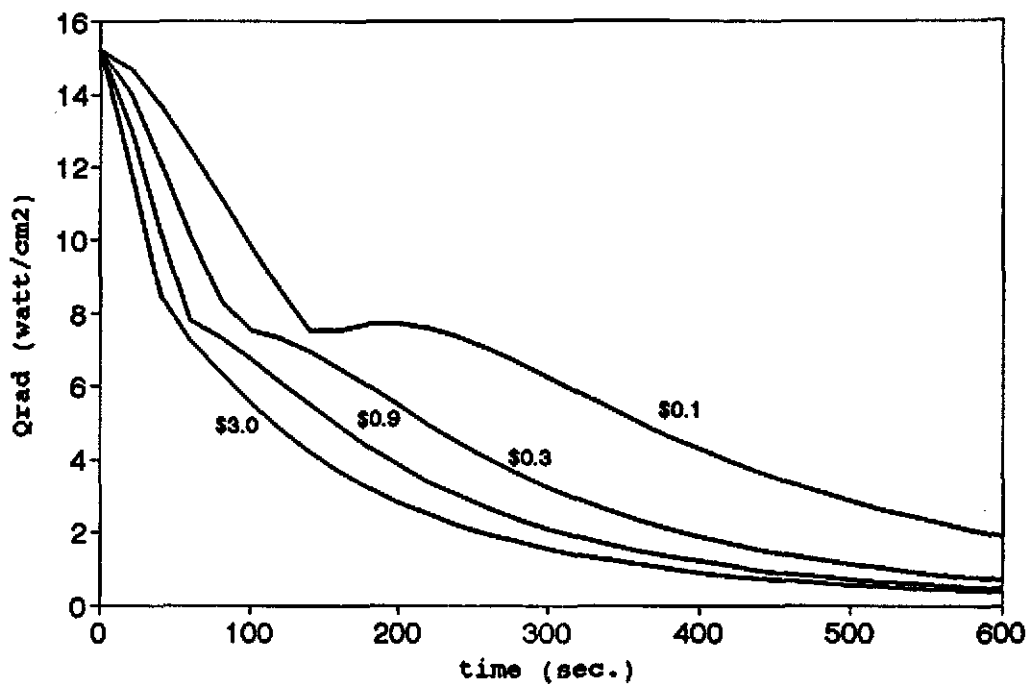


Figure 4.31 Radiation heat flux profile for reactor shut down at different negative reactivity insertions.

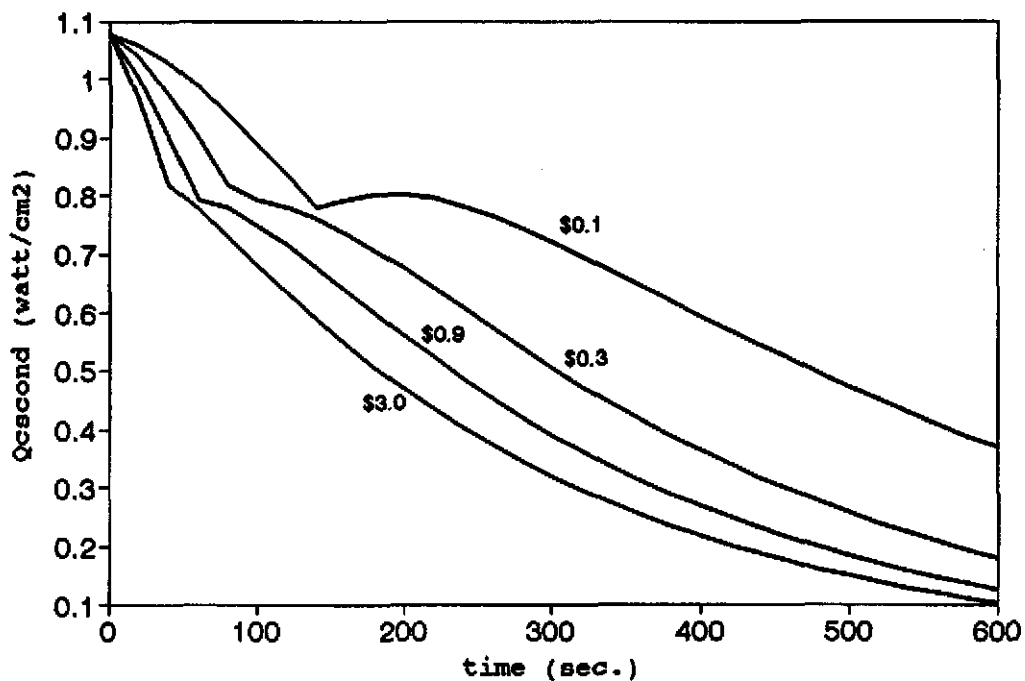


Figure 4.32 Conductive heat flux profile of cesium for reactor shut down at different negative reactivity insertions.

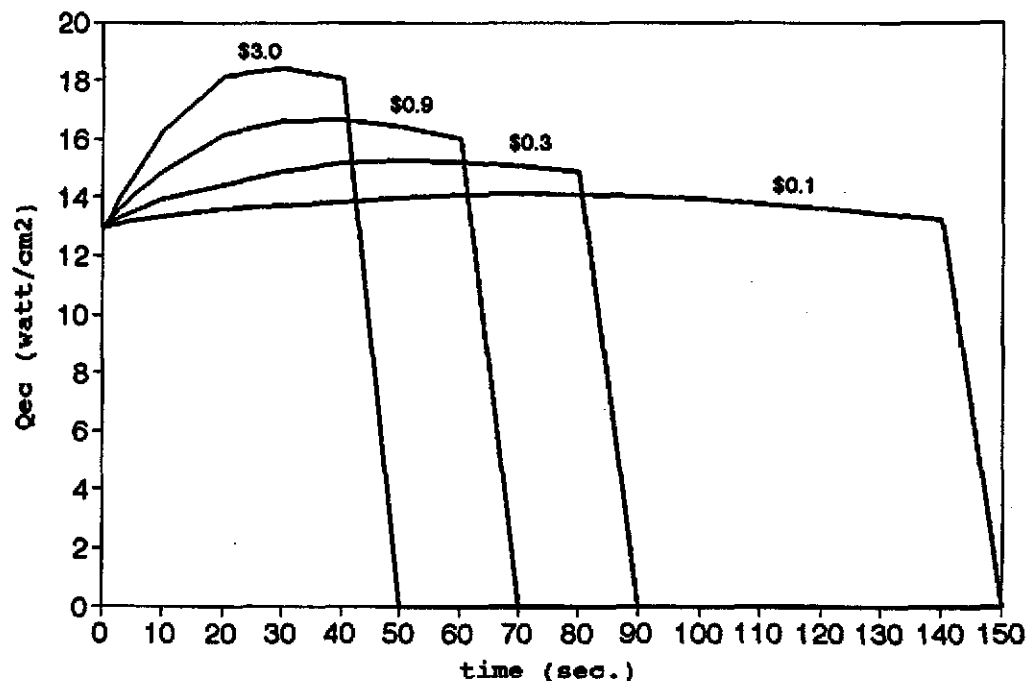


Figure 4.33 Heat flux profile of emitter electron cooling for reactor shut down at different negative reactivity insertions.

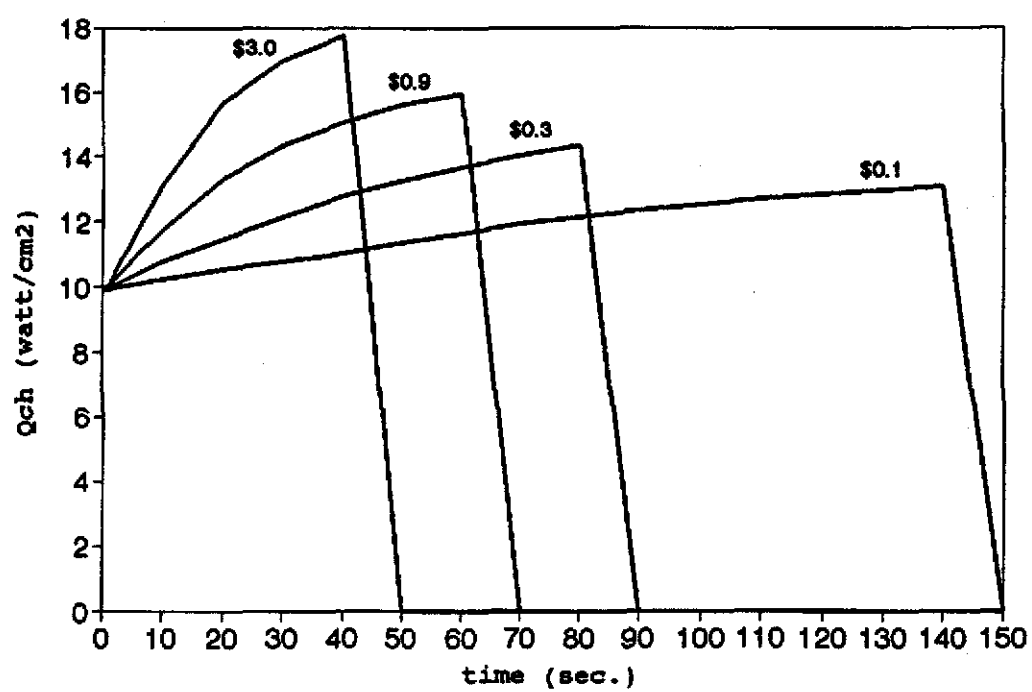


Figure 4.34 Heat flux profile of collector electron heating for reactor shut down at different negative reactivity insertions.

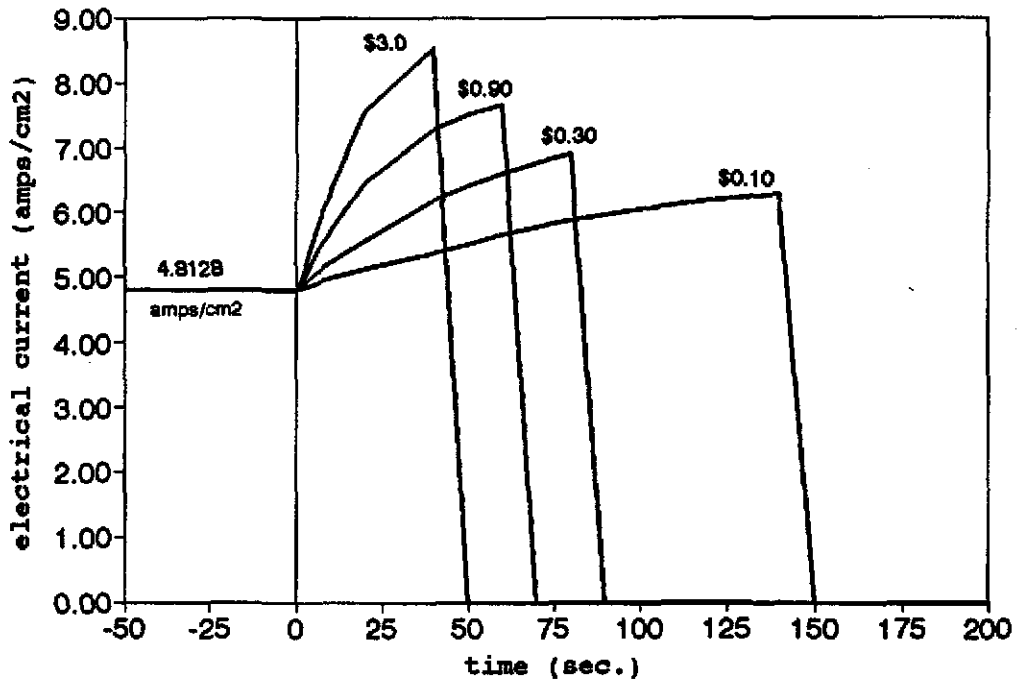


Figure 4.35 Electrical Current profile for reactor shut down at different negative reactivity insertions.

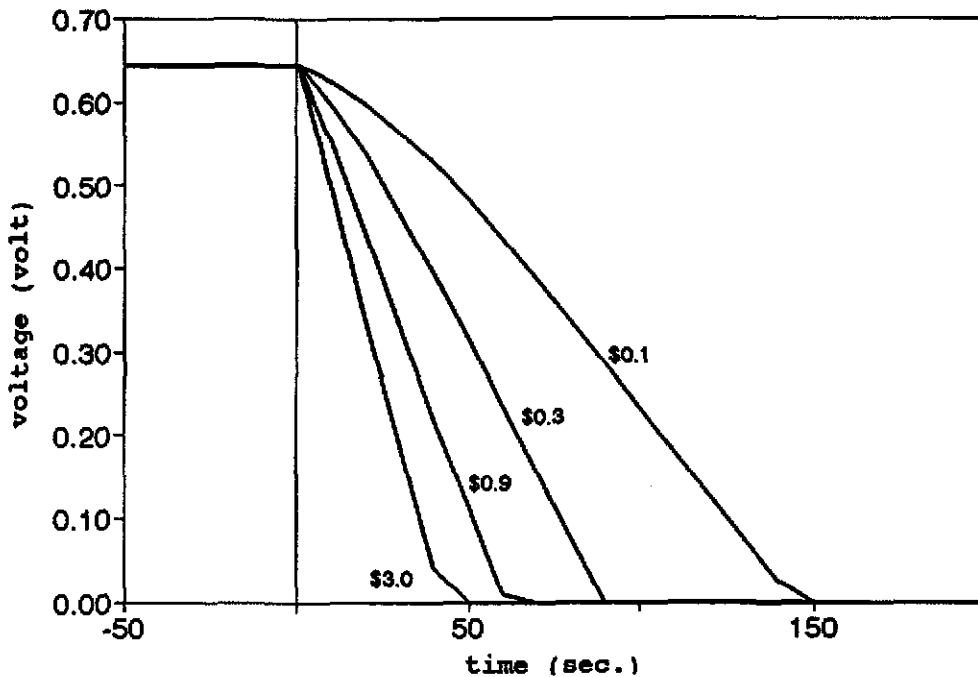


Figure 4.36 Electrical voltage profile for reactor shut down at different negative reactivity insertions.

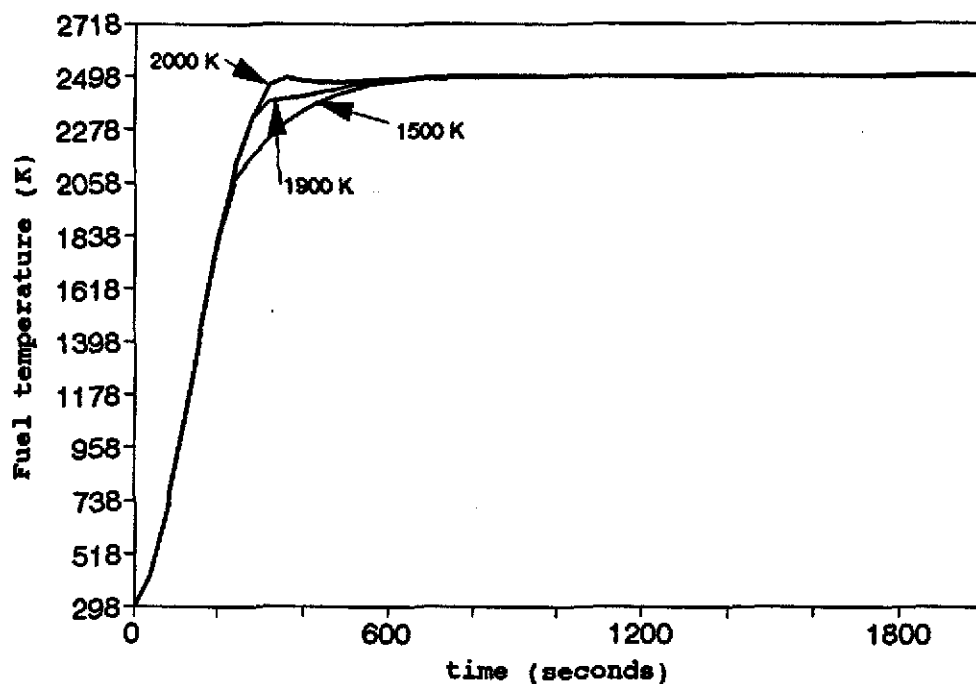


Figure 4.37 Fuel temperature profile for different electron cooling temperatures (Start-up).

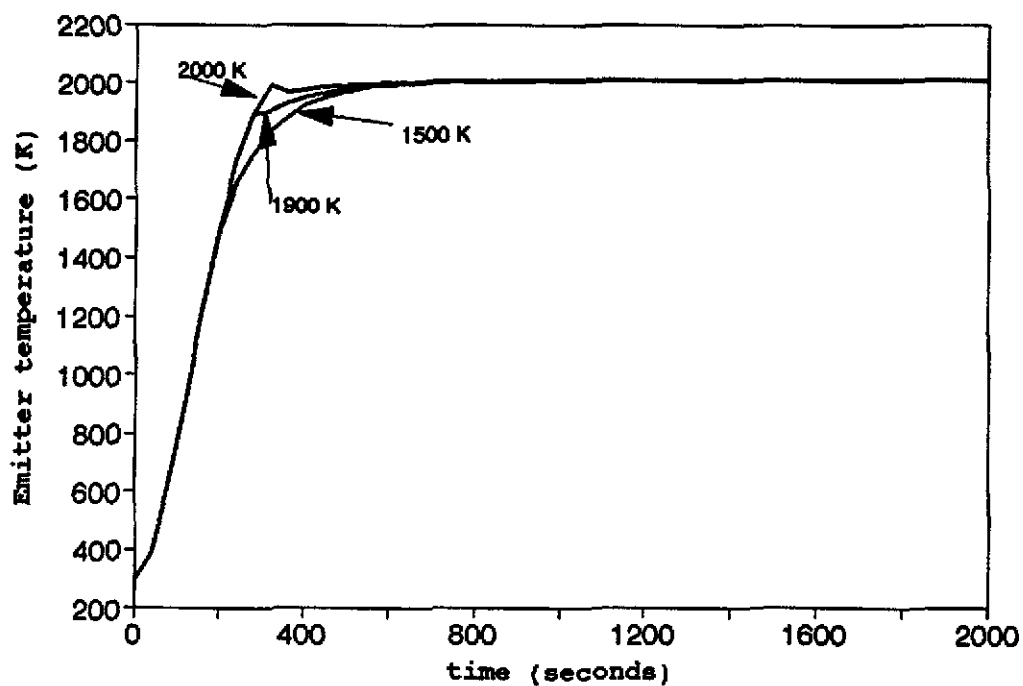


Figure 4.38 Emitter temperature profile for different electron cooling temperatures (Start-up).

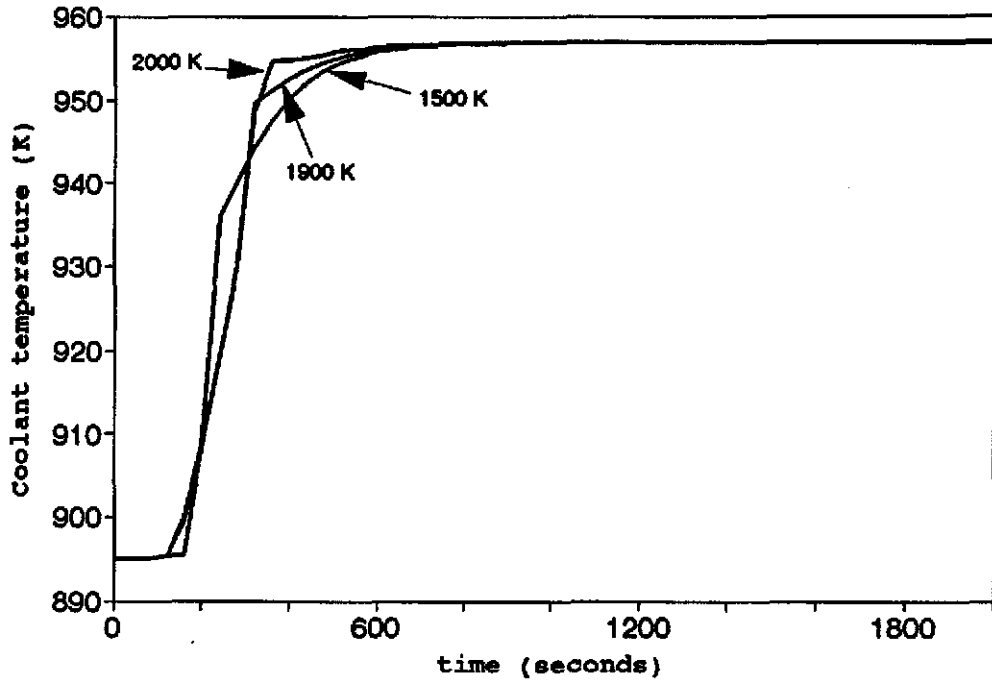


Figure 4.39 Coolant temperature profile for different electron cooling temperatures (Start-up).

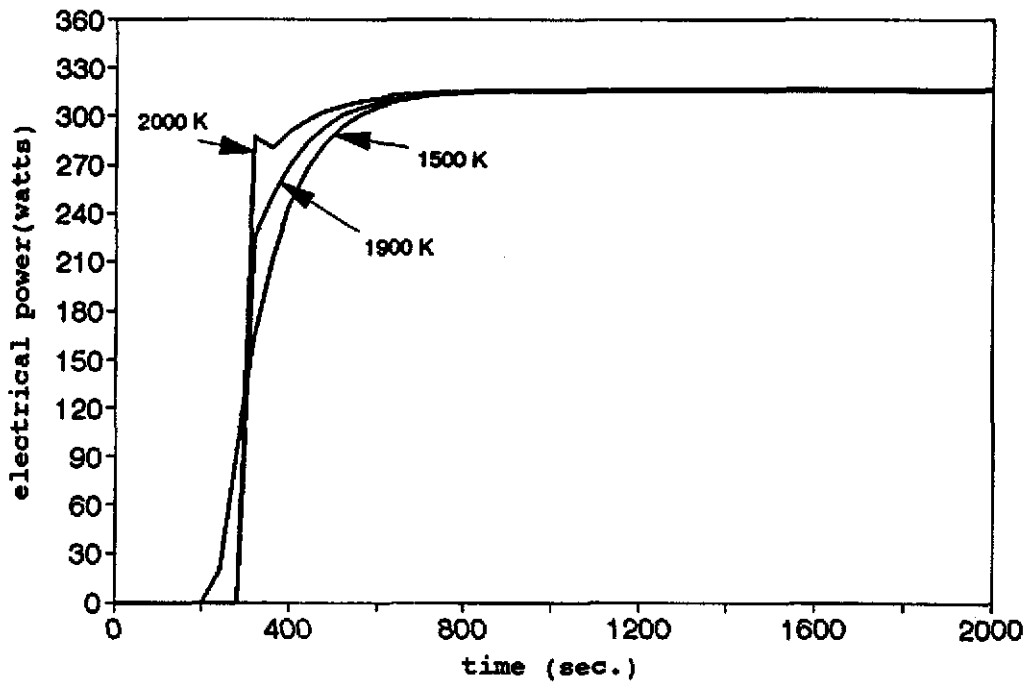


Figure 4.40 Electrical power profile for different electron cooling temperatures (Start-up).

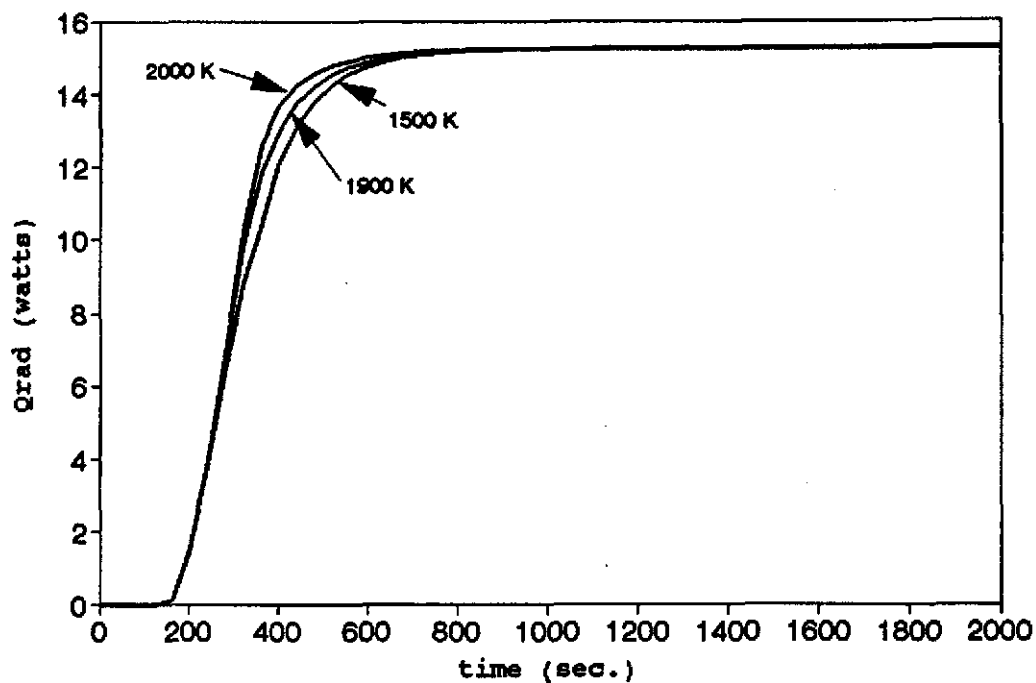


Figure 4.41 Radiation heat flux profile for different electron cooling temperatures (Start-up).

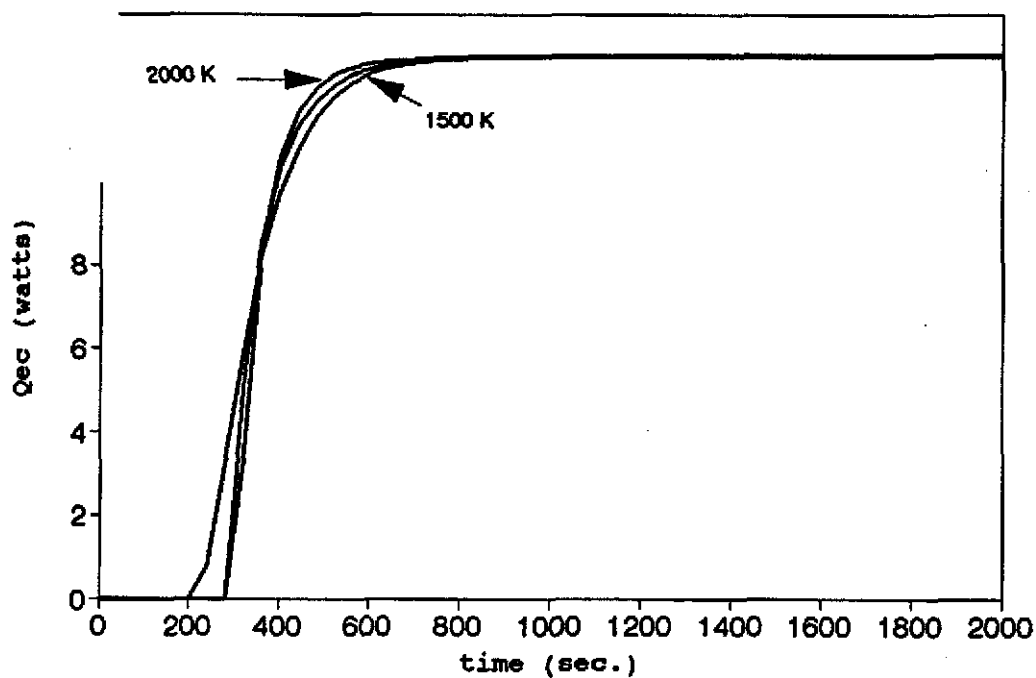


Figure 4.42 Heat flux profile of emitter electron cooling for different electron cooling temperatures (Start-up).

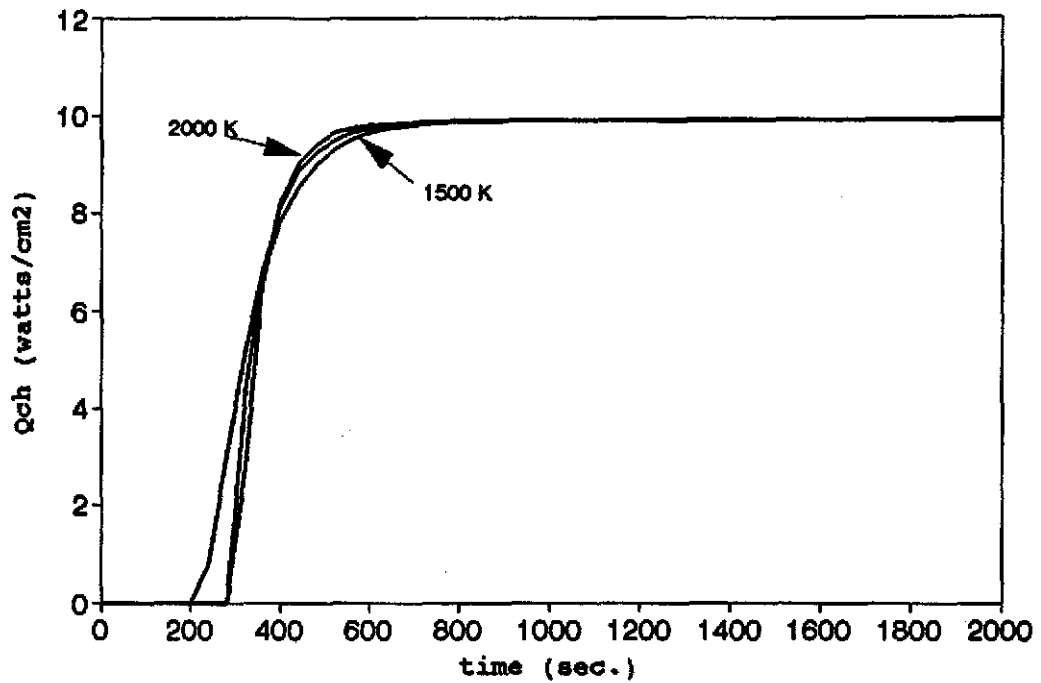


Figure 4.43 Heat flux profile of collector electron heating for different electron cooling temperatures (Start-up).

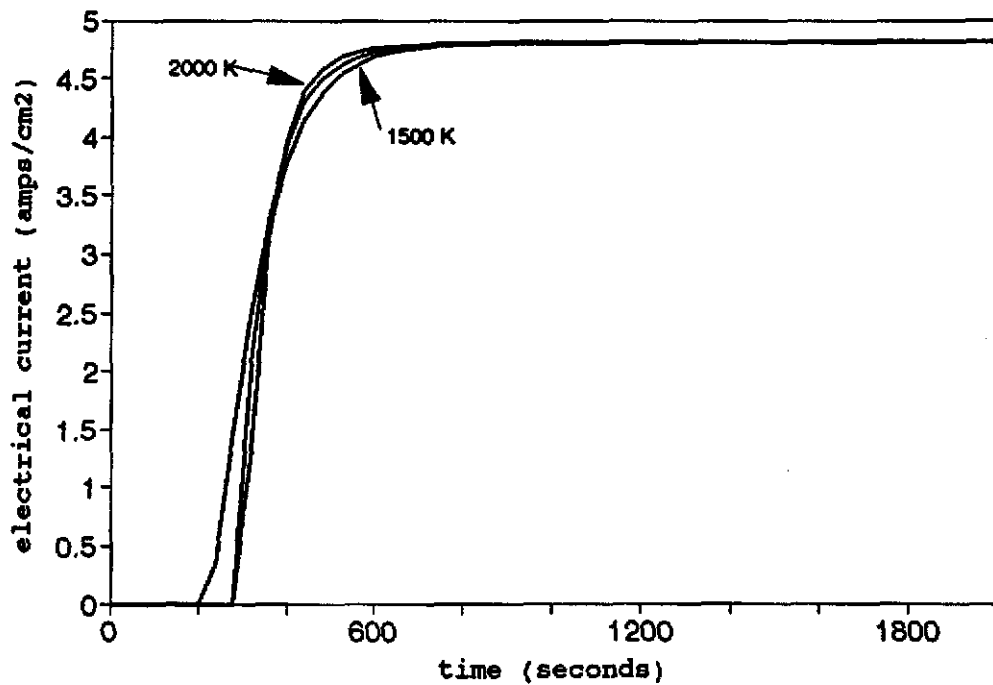


Figure 4.44 Electrical current profile for different electron cooling temperatures (Start-up).

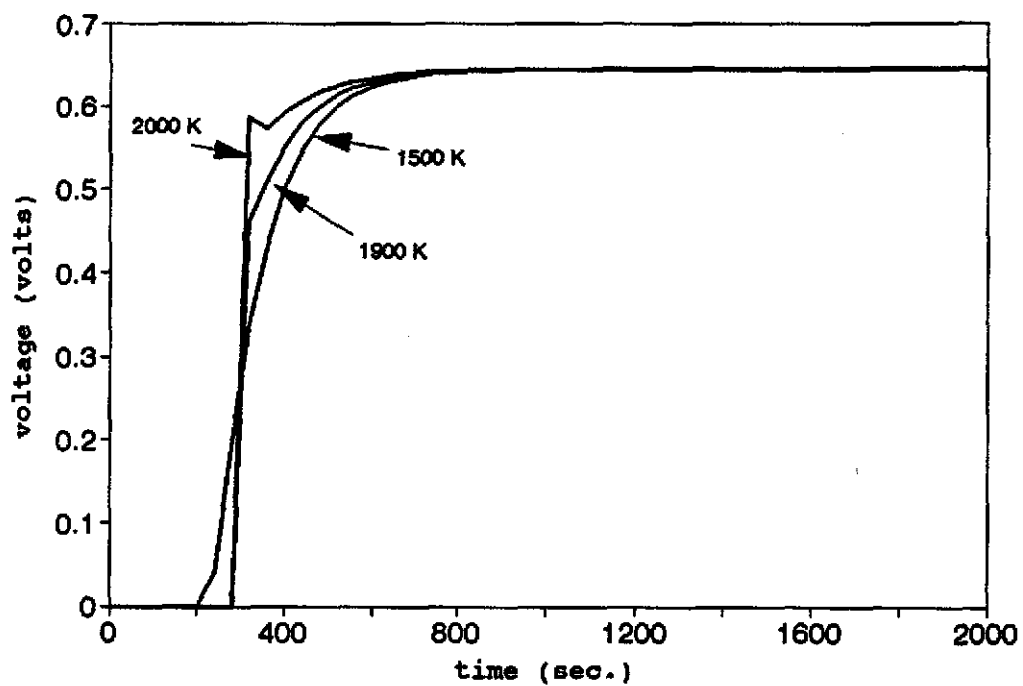


Figure 4.45 Electrical voltage profile for different electron cooling temperatures (Start-up).

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Chapter 5

Conclusions and Recommendations

Conclusions:

A computer model has been developed to simulate the transient temperature distribution of the thermionic fuel element (TFE) for nuclear space reactors. The transient computer code TFETC is based on TFEHX, a steady state code for TFE's.

Presently built into the transient code is the ability to handle the following scenarios: a) start up for user prescribed power rise coefficients; b) loss of flow for different mass loss coefficients and pump failures; and c) shut down for different negative reactivity insertions and total delayed neutron fractions for the UO_2 fuel. The user has the ability to control the helium heating phase through a proper choice of the emitter temperature at which helium heating ends, TSTOP, and likewise for the electron cooling phase through TSTART, the emitter temperature at the onset of electron cooling.

Another feature, in the TFETC code, of great importance is the ability to use more than one solver to solve the linear systems of algebraic equations.

The TFETC has been tested in the case of accidents such as loss of flow and has shown good stability and integrity at

the worst case in which the pump failures are complete. It allows some time, depending on the mass loss coefficient which is part of the input file, to scram the reactor safely. The TFETC model shows that the fuel temperature in a complete LOFA does reach 2497 °K, after the coolant attains its boiling point, in 34 seconds. The fuel temperature may exceed the fuel melting point after a period of time if no appropriate action to trip the reactor is taken. For 1/2, 1/3, and 1/4 pump failures, the fuel temperatures attain steady state values. They never exceed the fuel melting point even if the reactor is not shut down. Also, for the coolant temperature, the boiling point is exceeded in a complete LOFA while for 1/2, 1/3, and 1/4 pump failures, the maximum attainable coolant temperatures are: 1017, 987, 977 °K's respectively.

Recommendations:

The following recommendations for further studies are proposed:

1. The only gap considered in the thermionic fuel element is the emitter/collector gap, otherwise all the TFE regions are stacked next to each other. For further development of the TFETC code, it is recommended to induce some gaps between fuel and emitter or collector and insulator in order to increase the safety margins in the event of an accident.

2. The Gauss elimination methods are not the only technique to solve the unsteady state conduction equations but rather there are some methods that give accurate and reliable results. The round off error in the Gaussian elimination is large. Hence, it will be useful to try the code with other linear system solvers.

3. For more accurate calculations, it is recommended to choose very small time increments. The smaller the Δt , the smaller the truncation error of the implicit method.

4. For a large transient time as in the case of a TFE pin, it is not recommended to use the explicit method due to its deficiency that allows stability for only very small time steps and hence requires an immense period of computer time to study the transient. Other discretization methods can be studied which allow better control of the accuracy and faster execution times.

5. It would be desirable to improve the TFE model which is currently implemented in CYLCON6 to handle transient effects.

6. It is important to test the code results against experiments such as the Thermionic System Evaluation Test (TSET) of the TOPAZ-II system. Also, it is necessary to compare results with single cell test start experiments.

7. To analyze additional accident scenarios such as LOFA with reactor start up and reactor shut down.

8. The heat transfer mechanism is completely

different when the coolant reaches its boiling point, so it is desirable to develop a methodology to be able to handle cases in which boiling occurs in the NaK coolant.

9. It is recommended to decrease Δz , to be less than 1, to reduce the error arising from the implicit method. It is also advisable to replace the subroutine of the Gauss elimination with another subroutine which takes care of the bound error associated with the solution. For example, DGESVX subroutine.

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المؤلف الرئيسي:	Al Kheliewi, Abd Allah S.
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SAMPLE INPUT FILE FOR

*** S T E A D Y S T A T E P R O B L E M ***

4

1

895.0.12 0.78 620.0 245.0 245.0 3177.705

2

0.73 0.425

0.15 0.60 1 3 ! fuel

0.60 0.60 0 ! fuel emitter gap

0.60 0.75 2 0 ! emitter

0.75 0.80 7 0 ! emitter-collector gap

0.80 0.90 3 0 ! collector

0.90 0.90 0 ! collector -insulator gap

0.90 0.95 8 0 ! insulator

0.95 0.95 0 ! insulator-cladding gap

0.95 1.00 3 0 ! cladding

1.00 1.25 ! coolant channel

0.20 0.00 25.40 25.40

SAMPLE INPUT FILE FOR

*** S T A R T U P P R O B L E M ***

1

1

1

2000.0

40.0

0.5

0

900.0

2000.0

100.0

895.0.12 0.78 620.0 245.0 245.0 3177.705

2

0.73 0.425

0.15 0.60 1 3 ! fuel

0.60 0.60 0 ! fuel emitter gap

0.60 0.75 2 0 ! emitter

0.75 0.80 7 0 ! emitter-collector gap

0.80 0.90 3 0 ! collector

0.90 0.90 0 ! collector -insulator gap

0.90 0.95 8 0 ! insulator

0.95 0.95 0 ! insulator-cladding gap

0.95 1.00 3 0 ! cladding

1.00 1.25 ! coolant channel

0.20 0.00 25.40 25.40

SAMPLE INPUT FILE FOR

*** LOSS OF FLOW PROBLEM ***

3

1

1

500

10

0.5

0

0.5 0.5 30.0

895.0.12 0.78 620.0 245.0 245.0 3177.705

2

0.73 0.425

0.15 0.60 1 3

! fuel

0.60 0.60 0

! fuel emitter gap

0.60 0.75 2 0

! emitter

0.75 0.80 7 0

! emitter-collector gap

0.80 0.90 3 0

! collector

0.90 0.90 0

! collector -insulator gap

0.90 0.95 8 0

! insulator

0.95 0.95 0

! insulator-cladding gap

0.95 1.00 3 0

! cladding

1.00 1.250

! coolant channel

0.20 0.00 25.40 25.40

2207.611	2186.197	2131.858	2049.918	1943.400	1939.525	919.364	915.027	902.619	900.716
2261.743	2237.103	2174.669	2080.671	1958.691	1954.265	923.913	919.955	908.548	906.816
2362.666	2333.887	2261.168	2152.020	2010.708	2005.680	932.373	928.077	915.561	913.681
2449.023	2416.885	2335.950	2214.947	2058.707	2053.209	941.053	936.471	922.963	920.958
2496.643	2462.591	2377.041	2249.513	2085.177	2079.421	949.393	944.654	930.523	928.448
2496.923	2462.867	2377.311	2249.774	2085.429	2079.673	956.919	952.191	937.950	935.880
2449.686	2417.542	2336.592	2215.569	2059.308	2053.810	963.355	958.808	944.983	942.992
2363.191	2334.407	2261.677	2152.512	2011.179	2006.151	968.705	964.462	951.458	949.601
2261.853	2237.203	2174.740	2080.698	1958.669	1954.236	973.350	969.444	957.386	955.675
2222.000	2200.541	2144.165	2058.677	1947.356	1943.316	982.179	977.829	964.311	962.414
895.000	901.026	907.582	914.603	921.953	929.398	936.677	943.567	949.961	955.821

SAMPLE INPUT FILE FOR

*** SHUT DOWN PROBLEM ***

2

1

1

5.0

1.0

0.5

0

0.0065

-3.0

895.0.12 0.78 620.0 245.0 245.0 3177.705

2

0.73 0.425

0.15 0.60 1 3

! fuel

0.60 0.60 0

! fuel emitter gap

0.60 0.75 2 0

! emitter

0.75 0.80 7 0

! emitter-collector gap

0.80 0.90 3 0

! collector

0.90 0.90 0

! collector -insulator gap

0.90 0.95 8 0

! insulator

0.95 0.95 0

! insulator-cladding gap

0.95 1.00 3 0

! cladding

1.00 1.25

! coolant channel

0.20 0.00 25.40 25.40

2207.611	2186.197	2131.858	2049.918	1943.400	1939.525	919.364	915.027	902.619	900.716
2261.743	2237.103	2174.669	2080.671	1958.691	1954.265	923.913	919.955	908.548	906.816
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2496.643	2462.591	2377.041	2249.513	2085.177	2079.421	949.393	944.654	930.523	928.448
2496.923	2462.867	2377.311	2249.774	2085.429	2079.673	956.919	952.191	937.950	935.880
2449.686	2417.542	2336.592	2215.569	2059.308	2053.810	963.355	958.808	944.983	942.992
2363.191	2334.407	2261.677	2152.512	2011.179	2006.151	968.705	964.462	951.458	949.601
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895.000	901.026	907.582	914.603	921.953	929.398	936.677	943.567	949.961	955.821

TFETC INPUT DESCRIPTION (CODE MANUAL)

***** S T E A D Y S T A T E *****

Line 1 A 80 Title (Steady state)

Line 2 I1 must be 4 for steady state

Line 3 I1 Type of solver (must be 1 or 2)

1. Gaussian Elimination Solver
2. Y12M Solver

Line 4 7F10.0 Tinlet, Mdot, W, Tr, Itop, Ibottom, PowerTh

- Tinlet : Temperature of the NaK coolant as it enters the coolant channel of the TFE (K).
- Mdot : Mass Flowrate of the NaK coolant within the TFE coolant channel (Kg/s).
- W : Weight Fraction of Potassium within the NaK coolant. Range: $0 \leq W \leq 1.0$. Standard value: 0.78 (Eutectic NaK)
- Tr : Cesium reservoir temperature (K), $Tr \geq 0$
- Itop : Current flow at the top connection of the TFE is defined as the end at which the coolant exits the TFE coolant channel (Amperes). Range: ≥ 0.0
- Ibottom: Current flow at the bottom connection of the TFE is defined as the end at which the coolant enters the TFE coolant channel (Amperes). Range: ≥ 0.0
- PowerTh: For PowerTh ≥ 0 : Total power produced in the fuel of the TFE (Watts).
For PowerTh < 0 : $ABS(PowerTh) =$

Average Volumetric heat generation rate within the fuel of the TFE (Watts/cm³).

Line 5: I2 If TabFlag = 1, a table of axial power peaking factors versus axial position follows.

If TabFlag = 2, the following line contains coefficients for a correlation for the axial power peaking factors versus axial position.

Other values of TabFlag generate an error condition.

Line 6:2F10.0 Z,G if TabFlag = 2

- If TabFlag = 1, then Z and G are entries in a table of axial power peaking factors.

Z = Axial position of the table entry (cm). Measured from the bottom of the TFE.

G = Ratio of the linear heat generation rate at position Z to the average linear heat generation rate in the TFE fuel.

This line is repeated until G < 0.

OR

A,B if TabFlag = 2.

- If TabFlag = 2, then A and B are coefficients in the following correlation:

$$G = A + B * \text{SIN} ((Z - Z_{\text{min}}) / (Z_{\text{max}} - Z_{\text{min}}) * \text{Pi})$$

where G is the ratio of the linear heat generation rate in the TFE fuel at axial position Z to the average linear heat generation rate.

Zmin is the axial position of the

bottom of the fueled region
(cm).

Zmax is the axial position of the top
of the fueled region (cm).

Pi = 3.1415926

The following line is repeated for each of the nine
internal regions of the TFE excluding the coolant channel.

2F10.0, 2I5 IR(I), OR(I), MatNum(I), Rmest(I).I =
1 to 9

IR(I): Inside radius of region I(cm). IR(I)
must be greater than or equal to zero;
IR(I) must equal OR(I-1) for I = 1
through 9.

OR(I): Outside radius of region I(cm). OR(I)
must equal IR(I+1) for I = 1 through 9.

MatNum(I): Identification number for the material
in region I. The numbers are currently
defined as follows:

MatNum	Material
1	UO ₂
2	Tungsten
3	Niobium
4	Nb1Zr
5	Molybdenum
6	Rhenium
7	Cesium
8	Al ₂ O ₃

Rmesh(I): Rmesh(I) equals the number of radial mesh
intervals within region I minus 1. Mesh
points automatically exist at the interior
and exterior surfaces of each region.

(If $IR(1) = 0$, then the inner most mesh point occurs at the fuel centerline). Specifying $Rmesh(I) > 0$ generates additional mesh points within region I. For instance, consider $Rmesh(1) = 3$. This results in 5 mesh points (4 mesh intervals) within the fueled region of the TFE: one on the interior surface of the fuel, and three equally spaced radially within the fuel. The interior and exterior mesh points are shared with the adjacent regions. For example, if $Rmesh(7) = 0$, the insulator region contains only 2 radial mesh points (1 radial mesh interval covering the entire insulator region) and the interior mesh point is also the exterior mesh point of the collector/insulator gap region, while the exterior mesh point is also the interior mesh point of the insulator/cladding gap region.

Notes:

■ The TFE regions (I = 1 to 9) are as follows:

I	Region
1	Fuel
2	Fuel/Emitter Gap
3	Emitter
4	Emitter/Collector Gap
5	Collector
6	Collector/Insulator Gap
7	Insulator
8	Insulator/Cladding Gap
9	Cladding
10	Coolant Channel

■ The region 2, 6 and 8 are included to allow

for small gaps to be modeled between the solid regions of the TFE.

However, it is recommended that the TFE be modeled with all of the solid regions in close contact, i.e. with the following specifications:

$$\text{OR}(1) = \text{IR}(2) = \text{OR}(2) = \text{IR}(3)$$

$$\text{OR}(5) = \text{IR}(6) = \text{OR}(6) = \text{IR}(7)$$

$$\text{OR}(7) = \text{IR}(8) = \text{OR}(8) = \text{IR}(9)$$

2F10.0 IR(10), OR(10)

IR(10): Inside radius of the coolant channel (cm). Must equal OR(9).

OR(10): Outside radius of the coolant channel (cm)

4F10.0 Ems, Zmin, Zmax, L

Ems: Effective radiative emissivity between the emitter and collector surfaces (across the emitter/collector gap). The heat transfer Q due to radiation across the emitter/collector gap is given by:

$$Q(Z) = \text{Ems} * (\text{Temitter}(Z)** 4 - \text{Tcollector}(Z)** 4)$$

where $\text{Temitter}(Z)$ is the emitter surface temperature at position Z .

$\text{Tcollector}(Z)$ is the collector surface temperature at position Z .

Note: An effective emissivity --- "less than 0.1 is not maintainable, and one greater than 0.2 is undesirable." Hatsopoulos and Gyftopoulos, Thermionic Energy Conversion, Vol. 1, 1975, p.83.

Zmin: The axial position of the bottom of the fueled region of the TFE (cm).

Zmax: The axial position of the top of the fueled region of the TFE (cm).

L: Total length of the TFE, including electrode leads.

Note: TFETC does not model heat conduction away from the TFE via the electrode leads. Therefore, the value of L must equal $Z_{\max} - Z_{\min}$; otherwise an error condition results.

TFETC INPUT DESCRIPTION (CODE MANUAL)

***** S T A R T U P *****

Line 1 A 80 Title (Start up)Line 2 I1 must be 1 for start upLine 3 I1 Type of solver
(must be 1 or 2)

1. Gaussian Elimination Solver
2. Y12M Solver

Line 4 I1 Options:

(must be 1 or 2)

- 1 use default ambient

initial temperature (
i.e. $T = 298 \text{ K}$)

- 2 a table of $T(r,z)$

Other values of options generate an error.

Line 5: F10.0 Transient Test Time, sec.
(Transient Time must be greater than 0 and greater than Print Time Step)Line 6: F10.0 Print Time Step, sec.Line 7: F10.0 delta t, sec.
(must be less than Print Time Step)Line 8: F10.0 printout options
(must be 0 or 1)

- 0 prints everything except the temperature profile

throughout the TFE.

1 prints everything

Line 9: F10.0 temperature at which heating by helium is stopped, K.

(recommended between 700 and 900)

Line 10: F10.0 temperature at which electron cooling starts, K.

(recommended between 1800 and 1950)

Line 11: F10.0 power rise coefficient, tau, sec.
(must be greater than 0)

Line 12: 7F10.0 will be the same as Line 4 in the steady state input file

After Line 11, the startup input file follows the same description of steady state input file starting from Line 4.

TFETC INPUT DESCRIPTION (CODE MANUAL)

***** L O S S O F F L O W *****

Line 1 A 80 Title (Loss of Flow)

Line 2 I1 must be 3 for loss of flow

Line 3 I1 Type of solver
(must be 1 or 2)

1. Gaussian Elimination Solver
2. Y12M Solver

Line 4 I1 Options:
(must be 1 or 2)

1. The steady state temperature distribution is generated by the TFEHX code.
2. a table of $T(r,z)$ can be used by the user as a forcing function.

Other values of options generate an error.

Line 5: F10.0 Transient Test Time, sec.
(Transient Time must be greater than 0 and greater than Print Time Step)

Line 6: F10.0 Print Time Step, sec.

Line 7: F10.0 delta t, sec.
(must be less than Print Time Step)

Line 8: F10.0 printout options
(must be 0 or 1)

- 0 prints everything except the temperature profile

throughout the TFE.

1 prints everything

Line 9: 3F10.0 Loss of mass flowrate coefficients:
A, B, τ (τ should be in seconds)

((A + B) must equal 1)

$$m = m (A + B * \exp(-t/\tau))$$

- 1) 1/1 Pump Failure
 - A = 0.0
 - B = 1.0
 - $\tau > 0.0$
- 2) 1/2 Pump Failure
 - A = 0.5
 - B = 0.5
 - $\tau > 0.0$
- 3) 1/3 Pump Failure
 - A = 0.67
 - B = 0.33
 - $\tau > 0.0$
- 4) 1/4 Pump Failure
 - A = 0.75
 - B = 0.25
 - $\tau > 0.0$

After Line 9, the loss of flow input file follows the same description of steady state input file starting from Line 4.

TFETC INPUT DESCRIPTION (CODE MANUAL)

***** S H U T D O W N *****

Line 1 A 80 Title (Shut down)

Line 2 I1 must be 2 for shut down

Line 3 I1 Type of solver
(must be 1 or 2)

1. Gaussian Elimination Solver
2. Y12M Solver

Line 4 I1 Options:
(must be 1 or 2)

1. The steady state temperature distribution is generated by the TFEHX code.
2. a table of $T(r,z)$ can be used by the user as a forcing function.

Other values of options generate an error.

Line 5: F10.0 Transient Test Time, sec.
(Transient Time must be greater than 0 and greater than Print Time Step)

Line 6: F10.0 Print Time Step, sec.

Line 7: F10.0 delta t, sec.
(must be less than Print Time Step)

Line 8: F10.0 printout options
(must be 0 or 1)

- 0 prints everything except the temperature profile throughout the TFE.
- 1 prints everything

Line 9: F10.0 Total delayed fraction, β

$\beta = 0.0065$ for ^{235}U
 $\beta = 0.0026$ for ^{233}U
 $\beta = 0.0021$ for ^{239}Pu
 $\beta = 0.0203$ for ^{232}Th

Line 10:F10.0 Negative Reactivity Coefficient
must be less than 0.0, \$ unit.

After Line 10, the loss of flow input file follows the same description of steady state input file starting from Line 4.

```

1***** TFETC *****
**** INPUT DATA SUMMARY FOR THE FOLLOWING CASE:
*** S T A R T U P P R O B L E M ***
****
**** Start Up Problem ****
Linear Equations solved using Gaussian elimination
Simulation Period, TIME = 20.00 Secs.
Print Time Step, TPRINT = 10.00 Secs.
Time Step Increment, delta t = 0.5000 Secs.
Print Option, ipout = 1.
Stop helium heating at the emitter temperature, Tstop = 900.00.
Start Electron cooling at the emitter temperature, Tstart = 2000.00.
Power-rise coefficient, tau = 0.100E+03,
P(t) = P(0) * [ 1 - Exp ( - t / tau ) ] .

COOLANT TYPE Molten Sodium-Potassium Alloy (NaK)
Potassium composition = 78%
COOLANT MASS FLOW RATE: 0.12 kilograms per second.
TEMPERATURE OF COOLANT AT CHANNEL INLET. 895.0 K.

TEMPERATURE OF CESIUM RESERVOIR 620.0 K.
PRESSURE OF CESIUM VAPOR: 5.6 Torr.

EFFECTIVE EMISSIVITY FOR RADIANT HEAT TRANSFER FROM
THE EMITTER SURFACE TO THE COLLECTOR SURFACE: 0.200000

OUTPUT CURRENT FROM THE TOP OF THE TFE: 245.0 Amperes.
OUTPUT CURRENT FROM THE BOTTOM OF THE TFE: 245.0 Amperes

TOTAL THERMAL POWER PRODUCED IN THE TFE FUEL 3177.7 Watts.
AVERAGE VOLUMETRIC HEAT GENERATION RATE FOR THE TFE FUEL 118.0 Watts.
CORRELATION FOR THE RATIO OF THE HEAT GENERATION RATE
AT POSITION Z TO THE AVERAGE HEAT GENERATION RATE IN
THE TFE FUEL:

F = 0.7300+ 0.4250 * SIN((Z-Zmin)/(Zmax-Zmin)*3.14159)

```

AXIAL PEAK-TO-AVERAGE RATIO FOR HEAT GENERATION IS: 1.1543

```

1***** TFETC *****
**** INPUT DATA SUMMARY FOR THE FOLLOWING CASE:
*** S T A R T U P P R O B L E M ***
****
**** GEOMETRY DATA EDIT ****
**** RADIAL GEOMETRY ****

```

Region	Inside Radius (cm)	Outside Material (cm)	Number of Interior Mesh Points
fuel	0.150000	0.600000	uo2 3
emitter	0.600000	0.750000	w 0
emitter-collector gap	0.750000	0.800000	cs 0
collector	0.800000	0.900000	nb 0
insulator	0.900000	0.950000	al2o3 0
cladding	0.950000	1.000000	nb 0
coolant channel	1.000000	1.250000	

**** AXIAL GEOMETRY ****

```

AXIAL POSITION OF THE UPPER LIMIT FOR
THE FUELED REGION OF THE TFE 0.000000 (cm)
AXIAL POSITION OF THE LOWER LIMIT FOR
THE FUELED REGION OF THE TFE. 25.400000 (cm)
AXIAL EXTENT OF THE FUELED REGION OF THE TFE: 25.400000 (cm)
TOTAL LENGTH OF THE TFE, INCLUDING ELECTRODE LEADS: 25.400000 (cm)

```

```

1***** TFETC *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S T A R T U P P R O B L E M ***
TIME = 0.00000000

```

TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

```

t( 1, 1) = 298.0000000
t( 1, 2) = 298.0000000
t( 1, 3) = 298.0000000
t( 1, 4) = 298.0000000
t( 1, 5) = 298.0000000
t( 1, 6) = 298.0000000
t( 1, 7) = 298.0000000
t( 1, 8) = 298.0000000
t( 1, 9) = 298.0000000
t( 1, 10) = 298.0000000
t( 2, 1) = 298.0000000
t( 2, 2) = 298.0000000
t( 2, 3) = 298.0000000

```

```
t( 2, 4) = 298.0000000
t( 2, 5) = 298.0000000
t( 2, 6) = 298.0000000
t( 2, 7) = 298.0000000
t( 2, 8) = 298.0000000
t( 2, 9) = 298.0000000
t( 2, 10) = 298.0000000
t( 3, 1) = 298.0000000
t( 3, 2) = 298.0000000
t( 3, 3) = 298.0000000
t( 3, 4) = 298.0000000
t( 3, 5) = 298.0000000
t( 3, 6) = 298.0000000
t( 3, 7) = 298.0000000
t( 3, 8) = 298.0000000
t( 3, 9) = 298.0000000
t( 3, 10) = 298.0000000
t( 4, 1) = 298.0000000
t( 4, 2) = 298.0000000
t( 4, 3) = 298.0000000
t( 4, 4) = 298.0000000
t( 4, 5) = 298.0000000
t( 4, 6) = 298.0000000
t( 4, 7) = 298.0000000
t( 4, 8) = 298.0000000
t( 4, 9) = 298.0000000
t( 4, 10) = 298.0000000
t( 5, 1) = 298.0000000
t( 5, 2) = 298.0000000
t( 5, 3) = 298.0000000
t( 5, 4) = 298.0000000
t( 5, 5) = 298.0000000
t( 5, 6) = 298.0000000
t( 5, 7) = 298.0000000
t( 5, 8) = 298.0000000
t( 5, 9) = 298.0000000
t( 5, 10) = 298.0000000
t( 6, 1) = 298.0000000
t( 6, 2) = 298.0000000
t( 6, 3) = 298.0000000
t( 6, 4) = 298.0000000
t( 6, 5) = 298.0000000
t( 6, 6) = 298.0000000
t( 6, 7) = 298.0000000
t( 6, 8) = 298.0000000
t( 6, 9) = 298.0000000
t( 6, 10) = 298.0000000
t( 7, 1) = 298.0000000
t( 7, 2) = 298.0000000
t( 7, 3) = 298.0000000
t( 7, 4) = 298.0000000
t( 7, 5) = 298.0000000
t( 7, 6) = 298.0000000
t( 7, 7) = 298.0000000
t( 7, 8) = 298.0000000
t( 7, 9) = 298.0000000
t( 7, 10) = 298.0000000
t( 8, 1) = 298.0000000
t( 8, 2) = 298.0000000
t( 8, 3) = 298.0000000
t( 8, 4) = 298.0000000
t( 8, 5) = 298.0000000
t( 8, 6) = 298.0000000
t( 8, 7) = 298.0000000
t( 8, 8) = 298.0000000
t( 8, 9) = 298.0000000
t( 8, 10) = 298.0000000
t( 9, 1) = 298.0000000
t( 9, 2) = 298.0000000
t( 9, 3) = 298.0000000
t( 9, 4) = 298.0000000
t( 9, 5) = 298.0000000
t( 9, 6) = 298.0000000
t( 9, 7) = 298.0000000
t( 9, 8) = 298.0000000
t( 9, 9) = 298.0000000
t( 9, 10) = 298.0000000
t( 10, 1) = 298.0000000
t( 10, 2) = 298.0000000
t( 10, 3) = 298.0000000
t( 10, 4) = 298.0000000
t( 10, 5) = 298.0000000
t( 10, 6) = 298.0000000
t( 10, 7) = 298.0000000
t( 10, 8) = 298.0000000
t( 10, 9) = 298.0000000
```

```
t( 10, 10) = 298.0000000
tcool( 1) = 895.0000000
tcool( 2) = 895.0000000
tcool( 3) = 895.0000000
tcool( 4) = 895.0000000
tcool( 5) = 895.0000000
tcool( 6) = 895.0000000
tcool( 7) = 895.0000000
tcool( 8) = 895.0000000
tcool( 9) = 895.0000000
tcool( 10) = 895.0000000
```

```
Temperature of coolant at core exit: 895.000 degrees K.
Voltage across bottom of cell: 0.0000000
Voltage across top of cell: 0.0000000
Output current = 0.0000000
Output electrical power = 0.0000000
Total Thermal power = 0.0000000
```

Z	V	Qec	Jdens
0.00000000	0.00000000	0.00000000	0.00000000
2.82222222	0.00000000	0.00000000	0.00000000
5.64444444	0.00000000	0.00000000	0.00000000
8.46666667	0.00000000	0.00000000	0.00000000
11.28888889	0.00000000	0.00000000	0.00000000
14.11111111	0.00000000	0.00000000	0.00000000
16.93333333	0.00000000	0.00000000	0.00000000
19.75555556	0.00000000	0.00000000	0.00000000
22.57777778	0.00000000	0.00000000	0.00000000
25.40000000	0.00000000	0.00000000	0.00000000

Z	EmHeat	ColHeat
0.00000000	0.00000000	0.00000000
2.82222222	0.00000000	0.00000000
5.64444444	0.00000000	0.00000000
8.46666667	0.00000000	0.00000000
11.28888889	0.00000000	0.00000000
14.11111111	0.00000000	0.00000000
16.93333333	0.00000000	0.00000000
19.75555556	0.00000000	0.00000000
22.57777778	0.00000000	0.00000000
25.40000000	0.00000000	0.00000000

Z	Qch	Qrad	QCCond
0.00000000	0.00000000	0.00000000	0.00000000
2.82222222	0.00000000	0.00000000	0.00000000
5.64444444	0.00000000	0.00000000	0.00000000
8.46666667	0.00000000	0.00000000	0.00000000
11.28888889	0.00000000	0.00000000	0.00000000
14.11111111	0.00000000	0.00000000	0.00000000
16.93333333	0.00000000	0.00000000	0.00000000
19.75555556	0.00000000	0.00000000	0.00000000
22.57777778	0.00000000	0.00000000	0.00000000
25.40000000	0.00000000	0.00000000	0.00000000

1***** TFETC *****

***** RESULTS FOR THE FOLLOWING CASE:

*** S T A R T U P P R O B L E M ***

TIME = 10.0000000

TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

```
t( 1, 1) = 302.8718008
t( 1, 2) = 304.9487739
t( 1, 3) = 306.0289744
t( 1, 4) = 306.7853917
t( 1, 5) = 307.1854458
t( 1, 6) = 307.1843456
t( 1, 7) = 306.7823554
t( 1, 8) = 306.0245954
t( 1, 9) = 304.9437831
t( 1, 10) = 303.0465792
t( 2, 1) = 302.6851613
t( 2, 2) = 304.8625006
t( 2, 3) = 305.9377254
t( 2, 4) = 306.6858891
t( 2, 5) = 307.0813961
t( 2, 6) = 307.0803280
```

```

t( 2, 7) = 306.6829409
t( 2, 8) = 305.9334694
t( 2, 9) = 304.8577151
t( 2, 10) = 302.8713899
t( 3, 1) = 302.1843453
t( 3, 2) = 304.6326810
t( 3, 3) = 305.6944395
t( 3, 4) = 306.4205951
t( 3, 5) = 306.8039771
t( 3, 6) = 306.8029909
t( 3, 7) = 306.4178717
t( 3, 8) = 305.6905006
t( 3, 9) = 304.6283846
t( 3, 10) = 302.3549294
t( 4, 1) = 301.3532343
t( 4, 2) = 304.2518257
t( 4, 3) = 305.2917614
t( 4, 4) = 305.9814804
t( 4, 5) = 306.3447454
t( 4, 6) = 306.3438835
t( 4, 7) = 305.9790991
t( 4, 8) = 305.2883162
t( 4, 9) = 304.2485143
t( 4, 10) = 301.4856964
t( 5, 1) = 300.1233274
t( 5, 2) = 303.6884295
t( 5, 3) = 304.6972746
t( 5, 4) = 305.3331979
t( 5, 5) = 305.6666669
t( 5, 6) = 305.6659676
t( 5, 7) = 305.3312647
t( 5, 8) = 304.6945012
t( 5, 9) = 303.6870040
t( 5, 10) = 300.1934887
t( 6, 1) = 300.0115130
t( 6, 2) = 303.6476278
t( 6, 3) = 304.6519975
t( 6, 4) = 305.2837096
t( 6, 5) = 305.6149047
t( 6, 6) = 305.6142110
t( 6, 7) = 305.2817920
t( 6, 8) = 304.6492483
t( 6, 9) = 303.6462754
t( 6, 10) = 300.0763484
t( 7, 1) = 887.0273947
t( 7, 2) = 893.8633088
t( 7, 3) = 893.9128826
t( 7, 4) = 893.9132047
t( 7, 5) = 893.9132066
t( 7, 6) = 893.9132066
t( 7, 7) = 893.9132025
t( 7, 8) = 893.9126478
t( 7, 9) = 893.8454120
t( 7, 10) = 887.0264901
t( 8, 1) = 887.5363084
t( 8, 2) = 893.9263743
t( 8, 3) = 893.9726393
t( 8, 4) = 893.9729389
t( 8, 5) = 893.9729408
t( 8, 6) = 893.9729407
t( 8, 7) = 893.9729369
t( 8, 8) = 893.9724191
t( 8, 9) = 893.9094610
t( 8, 10) = 887.5354542
t( 9, 1) = 890.5895308
t( 9, 2) = 894.5193399
t( 9, 3) = 894.5403220
t( 9, 4) = 894.5404529
t( 9, 5) = 894.5404537
t( 9, 6) = 894.5404537
t( 9, 7) = 894.5404520
t( 9, 8) = 894.5402253
t( 9, 9) = 894.5117879
t( 9, 10) = 890.5889927
t( 10, 1) = 891.2092255
t( 10, 2) = 894.6369246
t( 10, 3) = 894.6530197
t( 10, 4) = 894.6531194
t( 10, 5) = 894.6531200
t( 10, 6) = 894.6531200
t( 10, 7) = 894.6531187
t( 10, 8) = 894.6529464
t( 10, 9) = 894.6312302
t( 10, 10) = 891.2087526
tcool( 1) = 895.0000000
tcool( 2) = 895.0000000

```

```
tcool( 3) = 895.0000000
tcool( 4) = 895.0000000
tcool( 5) = 895.0000000
tcool( 6) = 895.0000000
tcool( 7) = 895.0000000
tcool( 8) = 895.0000000
tcool( 9) = 895.0000000
tcool(10) = 895.0000000
```

```
Temperature of coolant at core exit: 895.000 degrees K.
Voltage across bottom of cell: 0.0000000
Voltage across top of cell: 0.0000000
Output current = 0.0000000
Output electrical power = 0.0000000
Total Thermal power = 302.3986125
```

Z	V	Qec	Jdens
0.00000000	0.00000000	0.00000000	0.00000000
2.82222222	0.00000000	0.00000000	0.00000000
5.64444444	0.00000000	0.00000000	0.00000000
8.46666667	0.00000000	0.00000000	0.00000000
11.28888889	0.00000000	0.00000000	0.00000000
14.11111111	0.00000000	0.00000000	0.00000000
16.93333333	0.00000000	0.00000000	0.00000000
19.75555556	0.00000000	0.00000000	0.00000000
22.57777778	0.00000000	0.00000000	0.00000000
25.40000000	0.00000000	0.00000000	0.00000000

Z	EmHeat	ColHeat
0.00000000	0.00000000	0.00000000
2.82222222	0.00000000	0.00000000
5.64444444	0.00000000	0.00000000
8.46666667	0.00000000	0.00000000
11.28888889	0.00000000	0.00000000
14.11111111	0.00000000	0.00000000
16.93333333	0.00000000	0.00000000
19.75555556	0.00000000	0.00000000
22.57777778	0.00000000	0.00000000
25.40000000	0.00000000	0.00000000

Z	Qch	Qrad	QCCond
0.00000000	0.00000000	0.00000000	0.00000000
2.82222222	0.00000000	0.00000000	0.00000000
5.64444444	0.00000000	0.00000000	0.00000000
8.46666667	0.00000000	0.00000000	0.00000000
11.28888889	0.00000000	0.00000000	0.00000000
14.11111111	0.00000000	0.00000000	0.00000000
16.93333333	0.00000000	0.00000000	0.00000000
19.75555556	0.00000000	0.00000000	0.00000000
22.57777778	0.00000000	0.00000000	0.00000000
25.40000000	0.00000000	0.00000000	0.00000000

1***** TFETC *****

***** RESULTS FOR THE FOLLOWING CASE:

*** S T A R T U P P R O B L E M ***

TIME = 20.00000000

TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

```
t( 1, 1) = 314.3188972
t( 1, 2) = 323.8055061
t( 1, 3) = 328.0695175
t( 1, 4) = 330.8827027
t( 1, 5) = 332.3510992
t( 1, 6) = 332.3372837
t( 1, 7) = 330.8439274
t( 1, 8) = 328.0099727
t( 1, 9) = 323.7156140
t( 1,10) = 314.8662271
t( 2, 1) = 313.8481635
t( 2, 2) = 323.5737879
t( 2, 3) = 327.8365972
t( 2, 4) = 330.6305580
t( 2, 5) = 332.0876954
t( 2, 6) = 332.0741236
t( 2, 7) = 330.5924504
t( 2, 8) = 327.7779808
t( 2, 9) = 323.4857544
```

```

t( 2, 10) - 314.4124792
t( 3, 1) - 312.6150764
t( 3, 2) - 322.9732739
t( 3, 3) - 327.2312886
t( 3, 4) - 329.9751740
t( 3, 5) - 331.4030291
t( 3, 6) - 331.3900775
t( 3, 7) - 329.9387688
t( 3, 8) - 327.1750775
t( 3, 9) - 322.8900245
t( 3, 10) - 313.1308168
t( 4, 1) - 310.6686031
t( 4, 2) - 322.0224680
t( 4, 3) - 326.2736928
t( 4, 4) - 328.9383730
t( 4, 5) - 330.3197435
t( 4, 6) - 330.3077369
t( 4, 7) - 328.9045654
t( 4, 8) - 326.2212440
t( 4, 9) - 321.9478092
t( 4, 10) - 311.0827745
t( 5, 1) - 307.9729533
t( 5, 2) - 320.6966308
t( 5, 3) - 324.9407257
t( 5, 4) - 327.4952554
t( 5, 5) - 328.8116071
t( 5, 6) - 328.8008465
t( 5, 7) - 327.4648822
t( 5, 8) - 324.8934389
t( 5, 9) - 320.6361492
t( 5, 10) - 308.2334946
t( 6, 1) - 307.7350411
t( 6, 2) - 320.6104272
t( 6, 3) - 324.8470828
t( 6, 4) - 327.3932048
t( 6, 5) - 328.7049117
t( 6, 6) - 328.6941956
t( 6, 7) - 327.3629555
t( 6, 8) - 324.7999906
t( 6, 9) - 320.5504811
t( 6, 10) - 307.9838412
t( 7, 1) - 894.9136469
t( 7, 2) - 894.9967241
t( 7, 3) - 894.9977590
t( 7, 4) - 894.9977702
t( 7, 5) - 894.9977703
t( 7, 6) - 894.9977703
t( 7, 7) - 894.9977702
t( 7, 8) - 894.9977578
t( 7, 9) - 894.9966875
t( 7, 10) - 894.9136327
t( 8, 1) - 894.9192991
t( 8, 2) - 894.9969118
t( 8, 3) - 894.9978826
t( 8, 4) - 894.9978931
t( 8, 5) - 894.9978932
t( 8, 6) - 894.9978932
t( 8, 7) - 894.9978931
t( 8, 8) - 894.9978815
t( 8, 9) - 894.9968773
t( 8, 10) - 894.9192858
t( 9, 1) - 894.9538973
t( 9, 2) - 894.9986310
t( 9, 3) - 894.9990637
t( 9, 4) - 894.9990683
t( 9, 5) - 894.9990684
t( 9, 6) - 894.9990684
t( 9, 7) - 894.9990683
t( 9, 8) - 894.9990632
t( 9, 9) - 894.9986157
t( 9, 10) - 894.9538897
t( 10, 1) - 894.9606406
t( 10, 2) - 894.9989646
t( 10, 3) - 894.9992939
t( 10, 4) - 894.9992973
t( 10, 5) - 894.9992974
t( 10, 6) - 894.9992974
t( 10, 7) - 894.9992973
t( 10, 8) - 894.9992935
t( 10, 9) - 894.9989531
t( 10, 10) - 894.9606341
tcool( 1) - 895.0000000
tcool( 2) - 895.0000000
tcool( 3) - 895.0000000
tcool( 4) - 895.0000000
tcool( 5) - 895.0000000

```

```

tcool( 6) = 895.0000000
tcool( 7) = 895.0000000
tcool( 8) = 895.0000000
tcool( 9) = 895.0000000
tcool(10) = 895.0000000

```

```

Temperature of coolant at core exit: 895.000 degrees K.
Voltage across bottom of cell: 0.0000000
Voltage across top of cell: 0.0000000
Output current = 0.0000000
Output electrical power = 0.0000000
Total Thermal power = 576.0201923

```

Z	V	Qec	Jdens
0.00000000	0.00000000	0.00000000	0.00000000
2.82222222	0.00000000	0.00000000	0.00000000
5.64444444	0.00000000	0.00000000	0.00000000
8.46666667	0.00000000	0.00000000	0.00000000
11.28888889	0.00000000	0.00000000	0.00000000
14.11111111	0.00000000	0.00000000	0.00000000
16.93333333	0.00000000	0.00000000	0.00000000
19.75555556	0.00000000	0.00000000	0.00000000
22.57777778	0.00000000	0.00000000	0.00000000
25.40000000	0.00000000	0.00000000	0.00000000

Z	EmHeat	ColHeat
0.00000000	0 00000000	0 00000000
2.82222222	0 00000000	0 00000000
5.64444444	0 00000000	0 00000000
8.46666667	0 00000000	0 00000000
11.28888889	0 00000000	0 00000000
14.11111111	0 00000000	0 00000000
16.93333333	0 00000000	0 00000000
19.75555556	0 00000000	0 00000000
22.57777778	0 00000000	0 00000000
25.40000000	0 00000000	0 00000000

Z	Qch	Qrad	QCsCond
0.00000000	0.00000000	0.00000000	0.00000000
2.82222222	0.00000000	0.00000000	0.00000000
5.64444444	0.00000000	0.00000000	0.00000000
8.46666667	0.00000000	0.00000000	0.00000000
11.28888889	0.00000000	0.00000000	0.00000000
14.11111111	0.00000000	0.00000000	0.00000000
16.93333333	0.00000000	0.00000000	0.00000000
19.75555556	0.00000000	0.00000000	0.00000000
22.57777778	0.00000000	0.00000000	0.00000000
25.40000000	0.00000000	0.00000000	0.00000000


```

1***** TFETC *****
**** INPUT DATA SUMMARY FOR THE FOLLOWING CASE:
*** L O S S   O F   F L O W   P R O B L E M   ***
****
**** Loss of Flow Problem ****
Linear Equations solved using Gaussian elimination
Simulation Period, TIME = 20.00 Secs.
Print Time Step, TPRINT = 10.00 Secs.
Time Step Increment, delta t = 0.5000 Secs.
Print Option, ipout = 1.
Mass-loss coefficients, A = 0.5000, B = 0.5000, tau = 0.300E+02.
Mdot(t) = Mdot(0) * [ A + B * Exp(- t / tau) ]

COOLANT TYPE: Molten Sodium-Potassium Alloy (NaK)
Potassium composition = 78%
COOLANT MASS FLOW RATE: 0.12 kilograms per second.
TEMPERATURE OF COOLANT AT CHANNEL INLET: 895.0 K.

TEMPERATURE OF CESIUM RESERVOIR: 620.0 K.
PRESSURE OF CESIUM VAPOR: 5 6 Torr

EFFECTIVE EMISSIVITY FOR RADIANT HEAT TRANSFER FROM
THE EMITTER SURFACE TO THE COLLECTOR SURFACE: 0.200000

OUTPUT CURRENT FROM THE TOP OF THE TFE 245.0 Amperes.
OUTPUT CURRENT FROM THE BOTTOM OF THE TFE 245.0 Amperes.

TOTAL THERMAL POWER PRODUCED IN THE TFE FUEL. 3177.7 Watts.
AVERAGE VOLUMETRIC HEAT GENERATION RATE FOR THE TFE FUEL: 118.0 Watts.
CORRELATION FOR THE RATIO OF THE HEAT GENERATION RATE
AT POSITION Z TO THE AVERAGE HEAT GENERATION RATE IN
THE TFE FUEL:

F = 0.7300+ 0.4250 * SIN((Z-Zmin)/(Zmax-Zmin)*3.14159)

```

AXIAL PEAK-TO-AVERAGE RATIO FOR HEAT GENERATION IS: 1.1543

```

1***** TFETC *****
**** INPUT DATA SUMMARY FOR THE FOLLOWING CASE:
*** L O S S   O F   F L O W   P R O B L E M   ***
****
**** GEOMETRY DATA EDIT ****
**** RADIAL GEOMETRY ****

      Region              Inside      Outside      Material      Number of
      -----              Radius      Radius      -----      Interior
                          (cm)        (cm)                               Mesh Points
-----
fuel                      0.150000    0.600000    uo2           3
emitter                   0.600000    0.750000    w             0
emitter-collector gap    0.750000    0.800000    cs            0
collector                 0.800000    0.900000    nb            0
insulator                 0.900000    0.950000    al2o3         0
cladding                 0.950000    1.000000    nb            0
coolant channel          1.000000    1.250000

```

**** AXIAL GEOMETRY ****

```

AXIAL POSITION OF THE UPPER LIMIT FOR
THE FUELED REGION OF THE TFE: 0.000000 (cm)
AXIAL POSITION OF THE LOWER LIMIT FOR
THE FUELED REGION OF THE TFE: 25.400000 (cm)
AXIAL EXTENT OF THE FUELED REGION OF THE TFE: 25.400000 (cm)
TOTAL LENGTH OF THE TFE, INCLUDING ELECTRODE LEADS: 25.400000 (cm)

```

```

Temperature of coolant at core exit: 911.2 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** L O S S   O F   F L O W   P R O B L E M   ***
ITERATION HISTORY --
Converging the RMS error to less than 0.1 K.
Iteration : 1 RMS error = 352.3744542 Ave Diff. = 244.0701024
Max. Error = 836.2653934

```

```

Temperature of coolant at core exit: 935.1 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** L O S S   O F   F L O W   P R O B L E M   ***
ITERATION HISTORY --
Converging the RMS error to less than 0.1 K.
Iteration : 2 RMS error = 120.6911636 Ave Diff. = 82.8249886
Max. Error = 262.7163942

```

```

Temperature of coolant at core exit: 946.3 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:

```

```

*** LOSS OF FLOW PROBLEM ***
ITERATION HISTORY --
      Converting the RMS error to less than 0.1 K.
Iteration : 3  RMS error =  48.0790538 Ave Diff. =  28.9756862
              Max. Error = 124.2231601

Temperature of coolant at core exit:  951.7 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
ITERATION HISTORY --
      Converting the RMS error to less than 0.1 K.
Iteration : 4  RMS error =  22.1990022 Ave Diff. =  15.0890168
              Max. Error =  47.7020788

Temperature of coolant at core exit:  954.4 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
ITERATION HISTORY --
      Converting the RMS error to less than 0.1 K.
Iteration : 5  RMS error =  10.5703466 Ave Diff. =   6.1852238
              Max. Error =  24.5401210

Temperature of coolant at core exit:  955.7 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
ITERATION HISTORY --
      Converting the RMS error to less than 0.1 K.
Iteration : 6  RMS error =   5.3631696 Ave Diff. =   2.8889611
              Max. Error =  10.0539319

Temperature of coolant at core exit:  956.3 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
ITERATION HISTORY --
      Converting the RMS error to less than 0.1 K.
Iteration : 7  RMS error =   2.7477195 Ave Diff. =   1.1581796
              Max. Error =   5.1710185

Temperature of coolant at core exit:  956.6 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
ITERATION HISTORY --
      Converting the RMS error to less than 0.1 K.
Iteration : 8  RMS error =   1.4849013 Ave Diff. =   0.4761796
              Max. Error =   2.9321308

Temperature of coolant at core exit:  956.8 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
ITERATION HISTORY --
      Converting the RMS error to less than 0.1 K.
Iteration : 9  RMS error =   0.8003439 Ave Diff. =   0.1667677
              Max. Error =   1.6387800

Temperature of coolant at core exit:  956.9 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
ITERATION HISTORY --
      Converting the RMS error to less than 0.1 K.
Iteration : 10 RMS error =   0.4468618 Ave Diff. =   0.0509478
              Max. Error =   0.9027483

Temperature of coolant at core exit:  956.9 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
ITERATION HISTORY --
      Converting the RMS error to less than 0.1 K.
Iteration : 11 RMS error =   0.2453117 Ave Diff. =   0.0066867
              Max. Error =   0.4927094

Temperature of coolant at core exit:  956.9 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
ITERATION HISTORY --
      Converting the RMS error to less than 0.1 K.
Iteration : 12 RMS error =   0.1374013 Ave Diff. =  -0.0057550
              Max. Error =   0.2662746

```

Temperature of coolant at core exit: 956.9 degrees K
 1***** TFEHX *****
 ***** RESULTS FOR THE FOLLOWING CASE:
 *** LOSS OF FLOW PROBLEM ***
 ITERATION HISTORY --
 Converging the RMS error to less than 0.1 K.
 Iteration : 13 RMS error = 0.0754500 Ave Diff. = -0.0080428
 Max. Error = 0.1428042
 1***** TFEHX *****
 ***** RESULTS FOR THE FOLLOWING CASE:
 *** LOSS OF FLOW PROBLEM ***
 TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

T(1, 1) = 2207.6099799
 T(1, 2) = 2261.7498155
 T(1, 3) = 2362.6692432
 T(1, 4) = 2449.0244839
 T(1, 5) = 2496.6438504
 T(1, 6) = 2496.9186250
 T(1, 7) = 2449.6735003
 T(1, 8) = 2363.1763020
 T(1, 9) = 2261.8518754
 T(1, 10) = 2221.9650827
 T(2, 1) = 2186.1929268
 T(2, 2) = 2237.1053504
 T(2, 3) = 2333.8847952
 T(2, 4) = 2416.8802095
 T(2, 5) = 2462.5836797
 T(2, 6) = 2462.8553788
 T(2, 7) = 2417.5228984
 T(2, 8) = 2334.3872511
 T(2, 9) = 2237.1977085
 T(2, 10) = 2200.5034192
 T(3, 1) = 2131.8455701
 T(3, 2) = 2174.6616482
 T(3, 3) = 2261.1536691
 T(3, 4) = 2335.9307086
 T(3, 5) = 2377.0188307
 T(3, 6) = 2377.2839338
 T(3, 7) = 2336.5595171
 T(3, 8) = 2261.6454175
 T(3, 9) = 2174.7248924
 T(3, 10) = 2144.1203825
 T(4, 1) = 2049.8943113
 T(4, 2) = 2080.6498301
 T(4, 3) = 2151.9899401
 T(4, 4) = 2214.9105351
 T(4, 5) = 2249.4727497
 T(4, 6) = 2249.7299490
 T(4, 7) = 2215.5219128
 T(4, 8) = 2152.4669546
 T(4, 9) = 2080.6711635
 T(4, 10) = 2058.6227204
 T(5, 1) = 1943.3652400
 T(5, 2) = 1958.6571780
 T(5, 3) = 2010.6630404
 T(5, 4) = 2058.6554004
 T(5, 5) = 2085.1206973
 T(5, 6) = 2085.3690260
 T(5, 7) = 2059.2461008
 T(5, 8) = 2011.1211889
 T(5, 9) = 1958.6304420
 T(5, 10) = 1947.2927154
 T(6, 1) = 1939.4898721
 T(6, 2) = 1954.2307309
 T(6, 3) = 2005.6346468
 T(6, 4) = 2053.1568933
 T(6, 5) = 2079.3647793
 T(6, 6) = 2079.6131762
 T(6, 7) = 2053.7478765
 T(6, 8) = 2006.0928726
 T(6, 9) = 1954.1970618
 T(6, 10) = 1943.2526925
 T(7, 1) = 919.3693636
 T(7, 2) = 923.9247743
 T(7, 3) = 932.3917029
 T(7, 4) = 941.0796696
 T(7, 5) = 949.4278157
 T(7, 6) = 956.9612147
 T(7, 7) = 963.4052389
 T(7, 8) = 968.7628206
 T(7, 9) = 973.4131859
 T(7, 10) = 982.2504182
 T(8, 1) = 915.0295911
 T(8, 2) = 919.9643110
 T(8, 3) = 928.0941405

```

T( 8, 4) = 936.4957394
T( 8, 5) = 944.6864194
T( 8, 6) = 952.2318028
T( 8, 7) = 958.8557014
T( 8, 8) = 964.5168861
T( 8, 9) = 969.5054473
T( 8, 10) = 977.8976175
T( 9, 1) = 902.6200325
T( 9, 2) = 908.5560904
T( 9, 3) = 915.5751364
T( 9, 4) = 922.9840447
T( 9, 5) = 930.5510512
T( 9, 6) = 937.9848177
T( 9, 7) = 945.0246739
T( 9, 8) = 951.5067375
T( 9, 9) = 957.4406258
T( 9, 10) = 964.3720872
T( 10, 1) = 900.7165965
T( 10, 2) = 906.8230273
T( 10, 3) = 913.6950848
T( 10, 4) = 920.9783348
T( 10, 5) = 928.4762371
T( 10, 6) = 935.9152912
T( 10, 7) = 943.0341280
T( 10, 8) = 949.6493791
T( 10, 9) = 955.7301540
T( 10, 10) = 962.4749495
Voltage across bottom of cell: 0.6427667
Voltage across top of cell: 0.6465651
Output current = 490.0000000
Output electrical power = 315.8862832

```

Z	V	Qec	Jdens
0.0000000	0.64276668	12.99430163	4.81276691
2.8222222	0.73959046	10.19453024	3.65189375
5.6444444	0.81543279	11.26422623	3.93880029
8.4666667	0.86809799	11.79150175	4.05750063
11.2888889	0.89565457	12.06399812	4.11770336
14.1111111	0.89685880	12.08239618	4.12389963
16.9333333	0.87147959	11.85322300	4.07907171
19.7555556	0.82030557	11.39452654	3.98658183
22.5777778	0.74481487	10.47748564	3.75821204
25.4000000	0.64656509	13.89597476	5.16933972

Z	EmHeat	ColHeat
0.0000000	14.49810519	12.78456733
2.8222222	8.68565016	7.62157940
5.6444444	4.81674372	4.12394584
8.4666667	1.87878625	1.57487539
11.2888889	0.24869437	0.20682254
14.1111111	0.15331479	0.12842295
16.9333333	1.60678297	1.37606431
19.7555556	4.41224414	3.91338449
22.5777778	8.23791408	7.58845246
25.4000000	14.53486721	13.59574866

Z	Qch	Qrad	QCCond
0.0000000	9.90081543	15.23808053	1.07744326
2.8222222	7.49362446	15.71537048	1.08777951
5.6444444	8.05239930	17.49574903	1.13124448
8.4666667	8.26919362	19.26610657	1.17042804
11.2888889	8.37595830	20.28345587	1.18841945
14.1111111	8.38384050	20.26435874	1.18111695
16.9333333	8.29839525	19.20286184	1.14859681
19.7555556	8.12431126	17.37203651	1.09503360
22.5777778	7.67831344	15.52319973	1.03762210
25.4000000	10.55366016	15.11997007	1.01755208

```

Total computational time required: 1 min., 0.37 sec.
Time spent in Convect/CoolantTemp: 0 min., 0.00 sec. ( 0.0%)
Time spent in CYLCON6: 1 min., 27.10 sec. (84.3%)
Time spent in Gauss: 0 min., 15.33 sec. (14.8%)
1***** TFETC *****

```

```

***** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
TIME = 0.00000000

```

TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

t(1, 1) = 2207.6106582
t(1, 2) = 2261.7426054
t(1, 3) = 2362.6664057
t(1, 4) = 2449.0229475
t(1, 5) = 2496.6433830
t(1, 6) = 2496.9234677
t(1, 7) = 2449.6863479
t(1, 8) = 2363.1914258
t(1, 9) = 2261.8530039
t(1, 10) = 2221.9998042
t(2, 1) = 2186.1971281
t(2, 2) = 2237.1025284
t(2, 3) = 2333.8873935
t(2, 4) = 2416.8852771
t(2, 5) = 2462.5906059
t(2, 6) = 2462.8674079
t(2, 7) = 2417.5418559
t(2, 8) = 2334.4072952
t(2, 9) = 2237.2029112
t(2, 10) = 2200.5411066
t(3, 1) = 2131.8581104
t(3, 2) = 2174.6690550
t(3, 3) = 2261.1684885
t(3, 4) = 2335.9499908
t(3, 5) = 2377.0411968
t(3, 6) = 2377.3109644
t(3, 7) = 2336.5916177
t(3, 8) = 2261.6765124
t(3, 9) = 2174.7395541
t(3, 10) = 2144.1652664
t(4, 1) = 2049.9178867
t(4, 2) = 2080.6705441
t(4, 3) = 2152.0199439
t(4, 4) = 2214.9465505
t(4, 5) = 2249.5126048
t(4, 6) = 2249.7739613
t(4, 7) = 2215.5694463
t(4, 8) = 2152.5116847
t(4, 9) = 2080.6980165
t(4, 10) = 2058.6768568
t(5, 1) = 1943.4002334
t(5, 2) = 1958.6914577
t(5, 3) = 2010.7078927
t(5, 4) = 2058.7072181
t(5, 5) = 2085.1766716
t(5, 6) = 2085.4286152
t(5, 7) = 2059.3079608
t(5, 8) = 2011.1788302
t(5, 9) = 1958.6693771
t(5, 10) = 1947.3555271
t(6, 1) = 1939.5252885
t(6, 2) = 1954.2654800
t(6, 3) = 2005.6800497
t(6, 4) = 2053.2093102
t(6, 5) = 2079.4213757
t(6, 6) = 2079.6733825
t(6, 7) = 2053.8103232
t(6, 8) = 2006.1510542
t(6, 9) = 1954.2364049
t(6, 10) = 1943.3159623
t(7, 1) = 919.3642134
t(7, 2) = 923.9127148
t(7, 3) = 932.3725376
t(7, 4) = 941.0528808
t(7, 5) = 949.3930788
t(7, 6) = 956.9185405
t(7, 7) = 963.3549215
t(7, 8) = 968.7053012
t(7, 9) = 973.3498345
t(7, 10) = 982.1790161
t(8, 1) = 915.0268697
t(8, 2) = 919.9545935
t(8, 3) = 928.0772959
t(8, 4) = 936.4712201
t(8, 5) = 944.6539122
t(8, 6) = 952.1913380
t(8, 7) = 958.8076000
t(8, 8) = 964.4616232
t(8, 9) = 969.4443033
t(8, 10) = 977.8286091
t(9, 1) = 902.6190560
t(9, 2) = 908.5484778
t(9, 3) = 915.5611828
t(9, 4) = 922.9632337
t(9, 5) = 930.5231087
t(9, 6) = 937.9496898

t(9, 7) = 944.9825023
t(9, 8) = 951.4578048
t(9, 9) = 957.3857064
t(9, 10) = 964.3110205
t(10, 1) = 900.7157871
t(10, 2) = 906.8155358
t(10, 3) = 913.6812466
t(10, 4) = 920.9576199
t(10, 5) = 928.4483757
t(10, 6) = 935.8802369
t(10, 7) = 942.9920328
t(10, 8) = 949.6005390
t(10, 9) = 955.6753043
t(10, 10) = 962.4140332
tcool(1) = 895.0000000
tcool(2) = 901.5697693
tcool(3) = 908.1042149
tcool(4) = 915.1116661
tcool(5) = 922.4532633
tcool(6) = 929.8935392
tcool(7) = 937.1691484
tcool(8) = 944.0572319
tcool(9) = 950.4384966
tcool(10) = 956.8961135

Temperature of coolant at core exit: 956.896 degrees K.

Mass flow rate = 0.120
Voltage across bottom of cell: 0.6427047
Voltage across top of cell: 0.6464798
Output current = 490.0000000
Output electrical power = 315.8501975
Total Thermal power = 3177.7050000

Z	V	Qec	Jdens
0.00000000	0.64270471	12.99420332	4.81284388
2.82222222	0.73952756	10.19447559	3.65196351
5.64444444	0.81536882	11.26434223	3.93893884
8.46666667	0.86803225	11.79162961	4.05764643
11.28888889	0.89558633	12.06404159	4.11782102
14.11111111	0.89678741	12.08230457	4.12396904
16.93333333	0.87140461	11.85295220	4.07907416
19.75555556	0.82022683	11.39399910	3.98648550
22.57777778	0.74473245	10.47667932	3.75799840
25.40000000	0.64647977	13.89467367	5.16896030

Z	EmHeat	ColHeat
0.00000000	14.49777300	12.78461813
2.82222222	8.68536675	7.62158438
5.64444444	4.81644251	4.12387927
8.46666667	1.87853834	1.57475799
11.28888889	0.24858863	0.20674847
14.11111111	0.15340144	0.12850539
16.93333333	1.60703735	1.37639999
19.75555556	4.41255720	3.91401618
22.57777778	8.23815769	7.58931886
25.40000000	14.53427214	13.59664908

Z	Qch	Qrad	QCsCond
0.00000000	9.90096591	15.23808053	1.07744326
2.82222222	7.49374791	15.71537048	1.08777951
5.64444444	8.05265430	17.49574903	1.13124448
8.46666667	8.26946163	19.26610657	1.17042804
11.28888889	8.37617736	20.28345587	1.18841945
14.11111111	8.38398105	20.26435874	1.18111695
16.93333333	8.29842819	19.20286184	1.14859681
19.75555556	8.12417673	17.37203651	1.09503360
22.57777778	7.67797598	15.52319973	1.03762210
25.40000000	10.55304538	15.11997007	1.01755208

1***** TFETC *****

***** RESULTS FOR THE FOLLOWING CASE:

*** LOSS OF FLOW PROBLEM ***

TIME = 10.0000000

TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

t(1, 1) = 2207.6297829

t(1, 2) = 2261.7641721
t(1, 3) = 2362.6880617
t(1, 4) = 2449.0488481
t(1, 5) = 2496.6740644
t(1, 6) = 2496.9572843
t(1, 7) = 2449.7220171
t(1, 8) = 2363.2304574
t(1, 9) = 2261.9027013
t(1, 10) = 2222.0225448
t(2, 1) = 2186.2143660
t(2, 2) = 2237.1206139
t(2, 3) = 2333.9039784
t(2, 4) = 2416.9060295
t(2, 5) = 2462.6173644
t(2, 6) = 2462.8999423
t(2, 7) = 2417.5798142
t(2, 8) = 2334.4526150
t(2, 9) = 2237.2644789
t(2, 10) = 2200.5666713
t(3, 1) = 2131.8710108
t(3, 2) = 2174.6781620
t(3, 3) = 2261.1724539
t(3, 4) = 2335.9592115
t(3, 5) = 2377.0612400
t(3, 6) = 2377.3448834
t(3, 7) = 2336.6409831
t(3, 8) = 2261.7445697
t(3, 9) = 2174.8402423
t(3, 10) = 2144.2013789
t(4, 1) = 2049.9254129
t(4, 2) = 2080.6649284
t(4, 3) = 2152.0040485
t(4, 4) = 2214.9398358
t(4, 5) = 2249.5276965
t(4, 6) = 2249.8194352
t(4, 7) = 2215.6499137
t(4, 8) = 2152.6331210
t(4, 9) = 2080.8843339
t(4, 10) = 2058.7403573
t(5, 1) = 1943.4031565
t(5, 2) = 1958.6637339
t(5, 3) = 2010.6631867
t(5, 4) = 2058.6793966
t(5, 5) = 2085.1903829
t(5, 6) = 2085.5023466
t(5, 7) = 2059.4522923
t(5, 8) = 2011.4049191
t(5, 9) = 1959.0177440
t(5, 10) = 1947.4791499
t(6, 1) = 1939.5280559
t(6, 2) = 1954.2365168
t(6, 3) = 2005.6337608
t(6, 4) = 2053.1802724
t(6, 5) = 2079.4348273
t(6, 6) = 2079.7483491
t(6, 7) = 2053.9577586
t(6, 8) = 2006.3824265
t(6, 9) = 1954.5936576
t(6, 10) = 1943.4423966
t(7, 1) = 919.4722115
t(7, 2) = 924.8298080
t(7, 3) = 934.3335273
t(7, 4) = 944.1024127
t(7, 5) = 953.4961673
t(7, 6) = 961.9822995
t(7, 7) = 969.2421922
t(7, 8) = 975.2606102
t(7, 9) = 980.4302251
t(7, 10) = 989.5514930
t(8, 1) = 915.1332143
t(8, 2) = 920.8723737
t(8, 3) = 930.0429403
t(8, 4) = 939.5302137
t(8, 5) = 948.7715572
t(8, 6) = 957.2746355
t(8, 7) = 964.7189533
t(8, 8) = 971.0451129
t(8, 9) = 976.5581917
t(8, 10) = 985.2621260
t(9, 1) = 902.7227612
t(9, 2) = 909.4779268
t(9, 3) = 917.5496337
t(9, 4) = 926.0581396
t(9, 5) = 934.6935765
t(9, 6) = 943.1080631
t(9, 7) = 950.9967511

```

t( 9, 8) = 958.1765717
t( 9, 9) = 964.6739118
t( 9, 10) = 972.0118532
t( 10, 1) = 900.8194385
t( 10, 2) = 907.7517064
t( 10, 3) = 915.6834329
t( 10, 4) = 924.0739195
t( 10, 5) = 932.6482095
t( 10, 6) = 941.0758875
t( 10, 7) = 949.0510420
t( 10, 8) = 956.3709359
t( 10, 9) = 963.0220593
t( 10, 10) = 970.1901425
tcool( 1) = 895.0000000
tcool( 2) = 902.6347593
tcool( 3) = 910.1883199
tcool( 4) = 918.2672600
tcool( 5) = 926.7017600
tcool( 6) = 935.2141737
tcool( 7) = 943.4954344
tcool( 8) = 951.2829759
tcool( 9) = 958.4410535
tcool( 10) = 965.6293706
    
```

Temperature of coolant at core exit: 965.629 degrees K.

```

Mass flow rate = 0.103
Voltage across bottom of cell: 0.6429185
Voltage across top of cell: 0.6449749
Output current = 490.0000000
Output electrical power = 315.5338830
Total Thermal power = 3177.7050000
    
```

Z	V	Qec	Jdens
0.00000000	0.64291849	12.98885191	4.81062783
2.82222222	0.73977079	10.20737706	3.65700034
5.64444444	0.81563836	11.28544589	3.94727532
8.46666667	0.86828479	11.81524599	4.06689152
11.28888889	0.89574570	12.08521675	4.12589394
14.11111111	0.89675829	12.09609826	4.12886904
16.93333333	0.87108999	11.85549180	4.07924725
19.75555556	0.81954415	11.38162494	3.98043695
22.57777778	0.74362737	10.43377433	3.73960942
25.40000000	0.64497491	13.85338112	5.14996506

Z	EmHeat	ColHeat
0.00000000	14.49779980	12.78601378
2.82222222	8.68348115	7.62714921
5.64444444	4.80880364	4.12555855
8.46666667	1.86859828	1.57119688
11.28888889	0.24311790	0.20301259
14.11111111	0.15887757	0.13374339
16.93333333	1.62602413	1.40046217
19.75555556	4.44130449	3.96374542
22.57777778	8.26320266	7.66211558
25.40000000	14.53545285	13.69156969

Z	Qch	Qrad	QCcCond
0.00000000	9.89601033	15.23661496	1.07730135
2.82222222	7.50203502	15.71022427	1.88683681
5.64444444	8.06589674	17.48567689	1.12927056
8.46666667	8.28402594	19.25199444	1.16742285
11.28888889	8.38946499	20.26641525	1.18444564
14.11111111	8.39350072	20.24542832	1.17627858
16.93333333	8.30210035	19.18281780	1.14302871
19.75555556	8.11948112	17.35171400	1.08889198
22.57777778	7.65289841	15.50449963	1.03109522
25.40000000	10.53178287	15.09135130	1.01051432

```

1***** TFETC *****
***** RESULTS FOR THE FOLLOWING CASE:
*** LOSS OF FLOW PROBLEM ***
TIME = 20.00000000
    
```

TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

```

t( 1, 1) = 2207.6383214
t( 1, 2) = 2261.7421265
    
```


t(1, 3) - 2362.6588720
t(1, 4) - 2449.0365761
t(1, 5) - 2496.6933684
t(1, 6) - 2497.0195192
t(1, 7) - 2449.8388375
t(1, 8) - 2363.4213240
t(1, 9) - 2262.2112551
t(1, 10) - 2222.1673669
t(2, 1) - 2186.2213254
t(2, 2) - 2237.0905596
t(2, 3) - 2333.8657641
t(2, 4) - 2416.8866620
t(2, 5) - 2462.6346318
t(2, 6) - 2462.9684996
t(2, 7) - 2417.7140760
t(2, 8) - 2334.6743344
t(2, 9) - 2237.6209227
t(2, 10) - 2200.7382163
t(3, 1) - 2131.8735725
t(3, 2) - 2174.6269389
t(3, 3) - 2261.1107292
t(3, 4) - 2335.9213815
t(3, 5) - 2377.0729640
t(3, 6) - 2377.4292534
t(3, 7) - 2336.8197844
t(3, 8) - 2262.0456400
t(3, 9) - 2175.3198330
t(3, 10) - 2144.4446130
t(4, 1) - 2049.9199520
t(4, 2) - 2080.5796496
t(4, 3) - 2151.9052960
t(4, 4) - 2214.8728090
t(4, 5) - 2249.5297206
t(4, 6) - 2249.9264560
t(4, 7) - 2215.8956128
t(4, 8) - 2153.0549764
t(4, 9) - 2081.5510899
t(4, 10) - 2059.1017282
t(5, 1) - 1943.3842160
t(5, 2) - 1958.5313956
t(5, 3) - 2010.5144355
t(5, 4) - 2058.5724956
t(5, 5) - 2085.1771698
t(5, 6) - 2085.6352703
t(5, 7) - 2059.7811099
t(5, 8) - 2011.9798525
t(5, 9) - 1959.9215982
t(5, 10) - 1948.0077430
t(6, 1) - 1939.5087211
t(6, 2) - 1954.1021747
t(6, 3) - 2005.4829891
t(6, 4) - 2053.0717478
t(6, 5) - 2079.4208803
t(6, 6) - 2079.8820188
t(6, 7) - 2054.2894057
t(6, 8) - 2006.9627433
t(6, 9) - 1955.5069482
t(6, 10) - 1943.9769048
t(7, 1) - 919.5871032
t(7, 2) - 925.9585206
t(7, 3) - 936.5041239
t(7, 4) - 947.3822243
t(7, 5) - 957.9259656
t(7, 6) - 967.5616307
t(7, 7) - 975.9265021
t(7, 8) - 982.9699304
t(7, 9) - 989.0588224
t(7, 10) - 999.0991141
t(8, 1) - 915.2463400
t(8, 2) - 922.0004452
t(8, 3) - 932.2143452
t(8, 4) - 942.8125886
t(8, 5) - 953.2057394
t(8, 6) - 962.8600849
t(8, 7) - 971.4109915
t(8, 8) - 978.7637224
t(8, 9) - 985.1993488
t(8, 10) - 994.8282434
t(9, 1) - 902.8243304
t(9, 2) - 910.5826400
t(9, 3) - 919.6798213
t(9, 4) - 929.2800708
t(9, 5) - 939.0487149
t(9, 6) - 948.5994633
t(9, 7) - 957.5858610
t(9, 8) - 965.7904454

```

t( 9, 9) = 973.2189328
t( 9, 10) = 981.4816996
t( 10, 1) = 900.9191634
t( 10, 2) = 908.8556674
t( 10, 3) = 917.8130995
t( 10, 4) = 927.2957086
t( 10, 5) = 937.0036164
t( 10, 6) = 946.5679489
t( 10, 7) = 955.6411876
t( 10, 8) = 963.9862458
t( 10, 9) = 971.5696672
t( 10, 10) = 979.6660120
tcool( 1) = 895.0000000
tcool( 2) = 903.6649141
tcool( 3) = 912.2331384
tcool( 4) = 921.3938151
tcool( 5) = 930.9535666
tcool( 6) = 940.5974077
tcool( 7) = 949.9752122
tcool( 8) = 958.7897911
tcool( 9) = 966.8859962
tcool( 10) = 975.0037525

```

Temperature of coolant at core exit: 975.004 degrees K.

```

Mass flow rate = 0.091
Voltage across bottom of cell: 0.6427620
Voltage across top of cell: 0.6422057
Output current = 490.0000000
Output electrical power = 314.8171011
Total Thermal power = 3177.7050000

```

Z	V	Qec	Jdens
0.00000000	0.64276201	12.99809452	4.81446777
2.82222222	0.73963081	10.23212465	3.66692499
5.64444444	0.81548281	11.31532518	3.95931168
8.46666667	0.86804489	11.84626533	4.07923207
11.28888889	0.89532345	12.11261159	4.13647415
14.11111111	0.89603864	12.11412424	4.13529262
16.93333333	0.86995761	11.85830471	4.07908370
19.75555556	0.81790157	11.36436099	3.97157466
22.57777778	0.74140948	10.37823873	3.71464933
25.40000000	0.64220575	13.77511295	5.11377653

Z	EmHeat	ColHeat
0.00000000	14.49761917	12.78749844
2.82222222	8.67431180	7.62844859
5.64444444	4.79182512	4.12030308
8.46666667	1.85091109	1.56147227
11.28888889	0.23435304	0.19654217
14.11111111	0.16762173	0.14185401
16.93333333	1.65554048	1.43472696
19.75555556	4.48632671	4.03182268
22.57777778	8.30599548	7.76005390
25.40000000	14.54047118	13.81384544

Z	Qch	Qrad	QCsCond
0.00000000	9.90353754	15.23565582	1.07716729
2.82222222	7.51995396	15.70179082	1.08555797
5.64444444	8.08657457	17.47227288	1.12692305
8.46666667	8.30530880	19.23527965	1.16400256
11.28888889	8.40912926	20.24834296	1.17996203
14.11111111	8.40874226	20.22804197	1.17077627
16.93333333	8.30967482	19.16764175	1.13658820
19.75555556	8.11600383	17.33960623	1.08162785
22.57777778	7.62416252	15.49730457	1.02319164
25.40000000	10.49101626	15.06581421	1.00127424

```

1***** TFETC *****
**** INPUT DATA SUMMARY FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
****
**** Shutdown Problem ****
Linear Equations solved using Gaussian elimination
Simulation Period, TIME = 6.00 Secs.
Print Time Step, TPRINT = 3.00 Secs.
Time Step Increment, delta t = 0.5000 Secs.
Print Option, ipout = 1.
Total delayed neutron fraction, BETA = 0.00650.
Negative Reactivity insertion in $, dollar = -3.00.
Reactor period, T = 80.00 Secs.
P(t) = P(0) [(1 - BETA * RHO)/(1 - RHO)] * Exp(- t / Period)

```

```

COOLANT TYPE: Molten Sodium-Potassium Alloy (NaK)
Potassium composition = 79%
COOLANT MASS FLOW RATE: 0.12 kilograms per second.
TEMPERATURE OF COOLANT AT CHANNEL INLET: 895.0 K.

```

```

TEMPERATURE OF CESIUM RESERVOIR: 620.0 K.
PRESSURE OF CESIUM VAPOR: 5.6 Torr.

```

```

EFFECTIVE EMISSIVITY FOR RADIANT HEAT TRANSFER FROM
THE EMITTER SURFACE TO THE COLLECTOR SURFACE: 0.200000

```

```

OUTPUT CURRENT FROM THE TOP OF THE TFE: 245.0 Amperes.
OUTPUT CURRENT FROM THE BOTTOM OF THE TFE: 245.0 Amperes.

```

```

TOTAL THERMAL POWER PRODUCED IN THE TFE FUEL: 3177.7 Watts.
AVERAGE VOLUMETRIC HEAT GENERATION RATE FOR THE TFE FUEL: 118.0 Watts.
CORRELATION FOR THE RATIO OF THE HEAT GENERATION RATE
AT POSITION Z TO THE AVERAGE HEAT GENERATION RATE IN
THE TFE FUEL:

```

$$F = 0.7300 + 0.4250 * \sin((Z-Z_{min})/(Z_{max}-Z_{min})*3.14159)$$

```

AXIAL PEAK-TO-AVERAGE RATIO FOR HEAT GENERATION IS: 1.1543

```

```

1***** TFETC *****
**** INPUT DATA SUMMARY FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***

```

```

**** GEOMETRY DATA EDIT ****
**** RADIAL GEOMETRY ****

```

Region	Inside Radius (cm)	Outside Radius (cm)	Material	Number of Interior Mesh Points
fuel	0.150000	0.600000	uo2	3
emitter	0.600000	0.750000	w	0
emitter-collector gap	0.750000	0.800000	cs	0
collector	0.800000	0.900000	nb	0
insulator	0.900000	0.950000	al2o3	0
cladding	0.950000	1.000000	nb	0
coolant channel	1.000000	1.250000		

```

**** AXIAL GEOMETRY ****

```

```

AXIAL POSITION OF THE UPPER LIMIT FOR
THE FUELED REGION OF THE TFE: 0.000000 (cm)
AXIAL POSITION OF THE LOWER LIMIT FOR
THE FUELED REGION OF THE TFE: 25.400000 (cm)
AXIAL EXTENT OF THE FUELED REGION OF THE TFE: 25.400000 (cm)
TOTAL LENGTH OF THE TFE, INCLUDING ELECTRODE LEADS: 25.400000 (cm)

```

```

Temperature of coolant at core exit: 911.2 degrees K.

```

```

1***** TFEHX *****

```

```

**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --

```

```

Converging the RMS error to less than 0.1 K.
Iteration : 1 RMS error = 352.3744542 Ave Diff. = 244.0701024
Max. Error = 836.2653934

```

```

Temperature of coolant at core exit: 935.1 degrees K.

```

```

1***** TFEHX *****

```

```

**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --

```

```

Converging the RMS error to less than 0.1 K.
Iteration : 2 RMS error = 120.6911636 Ave Diff. = 82.8249886
Max. Error = 262.7163942

```

```

Temperature of coolant at core exit: 946.3 degrees K.

```

```

1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --
      Converging the RMS error to less than 0.1 K.
Iteration : 3 RMS error = 48.0790538 Ave Diff. = 28.9756862
              Max. Error = 124.2231601

Temperature of coolant at core exit: 951.7 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --
      Converging the RMS error to less than 0.1 K.
Iteration : 4 RMS error = 22.1990022 Ave Diff. = 15.0890168
              Max. Error = 47.7020788

Temperature of coolant at core exit: 954.4 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --
      Converging the RMS error to less than 0.1 K.
Iteration : 5 RMS error = 10.5703466 Ave Diff. = 6.1852238
              Max. Error = 24.5401210

Temperature of coolant at core exit: 955.7 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --
      Converging the RMS error to less than 0.1 K.
Iteration : 6 RMS error = 5.3631696 Ave Diff. = 2.8889611
              Max. Error = 10.0539319

Temperature of coolant at core exit: 956.3 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --
      Converging the RMS error to less than 0.1 K.
Iteration : 7 RMS error = 2.7477195 Ave Diff. = 1.1581796
              Max. Error = 5.1710185

Temperature of coolant at core exit: 956.6 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --
      Converging the RMS error to less than 0.1 K.
Iteration : 8 RMS error = 1.4849013 Ave Diff. = 0.4761796
              Max. Error = 2.9321308

Temperature of coolant at core exit: 956.8 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --
      Converging the RMS error to less than 0.1 K.
Iteration : 9 RMS error = 0.8003439 Ave Diff. = 0.1667677
              Max. Error = 1.6387800

Temperature of coolant at core exit: 956.9 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --
      Converging the RMS error to less than 0.1 K.
Iteration : 10 RMS error = 0.4468618 Ave Diff. = 0.0509478
              Max. Error = 0.9027483

Temperature of coolant at core exit: 956.9 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --
      Converging the RMS error to less than 0.1 K.
Iteration : 11 RMS error = 0.2453117 Ave Diff. = 0.0066867
              Max. Error = 0.4927094

Temperature of coolant at core exit: 956.9 degrees K.
1***** TFEHX *****
**** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***
ITERATION HISTORY --
      Converging the RMS error to less than 0.1 K.

```

Iteration : 12 RMS error = 0.1374013 Ave Diff. = -0.0057550
 Max. Error = 0.2662746

Temperature of coolant at core exit: 956.9 degrees K.

1***** TFEHX *****

***** RESULTS FOR THE FOLLOWING CASE:

*** S H U T D O W N P R O B L E M ***

ITERATION HISTORY --

Converging the RMS error to less than 0.1 K.

Iteration : 13 RMS error = 0.0754500 Ave Diff. = -0.0080428
 Max. Error = 0.1428042

1***** TFEHX *****

***** RESULTS FOR THE FOLLOWING CASE:

*** S H U T D O W N P R O B L E M ***

TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

T(1, 1) = 2207.6099799
 T(1, 2) = 2261.7498155
 T(1, 3) = 2362.6692432
 T(1, 4) = 2449.0244839
 T(1, 5) = 2496.6438504
 T(1, 6) = 2496.9186250
 T(1, 7) = 2449.6735003
 T(1, 8) = 2363.1763020
 T(1, 9) = 2261.8518754
 T(1, 10) = 2221.9650827
 T(2, 1) = 2186.1929268
 T(2, 2) = 2237.1053504
 T(2, 3) = 2333.8847952
 T(2, 4) = 2416.8802095
 T(2, 5) = 2462.5836797
 T(2, 6) = 2462.6553788
 T(2, 7) = 2417.5228984
 T(2, 8) = 2334.3872511
 T(2, 9) = 2237.1977085
 T(2, 10) = 2200.5034192
 T(3, 1) = 2131.8455701
 T(3, 2) = 2174.6616482
 T(3, 3) = 2261.1536691
 T(3, 4) = 2335.9307086
 T(3, 5) = 2377.0188307
 T(3, 6) = 2377.2839338
 T(3, 7) = 2336.5595171
 T(3, 8) = 2261.6454175
 T(3, 9) = 2174.7248924
 T(3, 10) = 2144.1203825
 T(4, 1) = 2049.8943113
 T(4, 2) = 2080.6498301
 T(4, 3) = 2151.9899401
 T(4, 4) = 2214.9105351
 T(4, 5) = 2249.4727497
 T(4, 6) = 2249.7299490
 T(4, 7) = 2215.5219128
 T(4, 8) = 2152.4669546
 T(4, 9) = 2080.6711635
 T(4, 10) = 2058.6227204
 T(5, 1) = 1943.3652400
 T(5, 2) = 1958.6571780
 T(5, 3) = 2010.6630404
 T(5, 4) = 2058.6554004
 T(5, 5) = 2085.1206973
 T(5, 6) = 2085.3690260
 T(5, 7) = 2059.2461008
 T(5, 8) = 2011.1211889
 T(5, 9) = 1958.6304420
 T(5, 10) = 1947.2927154
 T(6, 1) = 1939.4898721
 T(6, 2) = 1954.2307309
 T(6, 3) = 2005.6346468
 T(6, 4) = 2053.1568933
 T(6, 5) = 2079.3647793
 T(6, 6) = 2079.6131762
 T(6, 7) = 2053.7478765
 T(6, 8) = 2006.0928726
 T(6, 9) = 1954.1970618
 T(6, 10) = 1943.2526925
 T(7, 1) = 919.3693636
 T(7, 2) = 923.9247743
 T(7, 3) = 932.3917029
 T(7, 4) = 941.0796696
 T(7, 5) = 949.4278157
 T(7, 6) = 956.9612147
 T(7, 7) = 963.4052389
 T(7, 8) = 968.7628206
 T(7, 9) = 973.4131859
 T(7, 10) = 982.2504182

```

T( 8, 1) = 915.0295911
T( 8, 2) = 919.9643110
T( 8, 3) = 928.0941405
T( 8, 4) = 936.4957394
T( 8, 5) = 944.6864194
T( 8, 6) = 952.2318028
T( 8, 7) = 958.8557014
T( 8, 8) = 964.3168861
T( 8, 9) = 969.5054473
T( 8, 10) = 977.8976175
T( 9, 1) = 902.6200325
T( 9, 2) = 908.5560904
T( 9, 3) = 915.5751364
T( 9, 4) = 922.9840447
T( 9, 5) = 930.5510512
T( 9, 6) = 937.9848177
T( 9, 7) = 945.0246739
T( 9, 8) = 951.5067375
T( 9, 9) = 957.4406258
T( 9, 10) = 964.3720872
T( 10, 1) = 900.7165965
T( 10, 2) = 906.8230273
T( 10, 3) = 913.6950848
T( 10, 4) = 920.9783348
T( 10, 5) = 928.4762371
T( 10, 6) = 935.9152912
T( 10, 7) = 943.0341280
T( 10, 8) = 949.6493791
T( 10, 9) = 955.7301540
T( 10, 10) = 962.4749495
Voltage across bottom of cell: 0.6427667
Voltage across top of cell: 0.6465651
Output current = 490.0000000
Output electrical power = 315.8862832

```

Z	V	Qec	Jdens
0.00000000	0.64276668	12.99430163	4.81276691
2.82222222	0.73959046	10.19453024	3.65189375
5.64444444	0.81543279	11.26422623	3.93880029
8.46666667	0.86809799	11.79150175	4.05750063
11.28888889	0.89565457	12.06399812	4.11770336
14.11111111	0.89685880	12.08239618	4.12389963
16.93333333	0.87147959	11.85322300	4.07907171
19.75555556	0.82030557	11.39452654	3.98658183
22.57777778	0.74481487	10.47748564	3.75821204
25.40000000	0.64656509	13.89597476	5.16933972

Z	EmHeat	ColHeat
0.00000000	14.49810519	12.78456733
2.82222222	8.68565016	7.62157940
5.64444444	4.81674372	4.12394584
8.46666667	1.87878625	1.57487539
11.28888889	0.24869437	0.20682254
14.11111111	0.15331479	0.12842295
16.93333333	1.60678297	1.37606431
19.75555556	4.41224414	3.91338449
22.57777778	8.23791408	7.58845246
25.40000000	14.53486721	13.59574866

Z	Qch	Qrad	QCCond
0.00000000	9.90081543	15.23808053	1.07744326
2.82222222	7.49362446	15.71537048	1.08777951
5.64444444	8.05239930	17.49574903	1.13124448
8.46666667	8.26919362	19.26610657	1.17042804
11.28888889	8.37595830	20.28345587	1.18841945
14.11111111	8.38384050	20.26435874	1.18111695
16.93333333	8.29839525	19.20286184	1.14859681
19.75555556	8.12431126	17.37203651	1.09503360
22.57777778	7.67831344	15.52319973	1.03762210
25.40000000	10.55366016	15.11997007	1.01755208

```

Total computational time required: 1 min., 0.47 sec.
Time spent in Convect/CoolantTemp: 0 min., 0.00 sec. ( 0.0%)
Time spent in CYLCON6 1 min., 27.17 sec. (84.2%)
Time spent in Gauss 0 min., 15.20 sec. (14.7%)

```

***** TFETC *****

***** RESULTS FOR THE FOLLOWING CASE:
*** S H U T D O W N P R O B L E M ***

TIME - 0.0000000

TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

t(1, 1)	=	2207.6106582
t(1, 2)	=	2261.7426054
t(1, 3)	=	2362.6664057
t(1, 4)	=	2449.0229475
t(1, 5)	=	2496.6433830
t(1, 6)	=	2496.9234677
t(1, 7)	=	2449.6863479
t(1, 8)	=	2363.1914258
t(1, 9)	=	2261.8530039
t(1, 10)	=	2221.9998042
t(2, 1)	=	2186.1971281
t(2, 2)	=	2237.1025284
t(2, 3)	=	2333.8873935
t(2, 4)	=	2416.8852771
t(2, 5)	=	2462.5906059
t(2, 6)	=	2462.8674079
t(2, 7)	=	2417.5418559
t(2, 8)	=	2334.4072952
t(2, 9)	=	2237.2029112
t(2, 10)	=	2200.5411066
t(3, 1)	=	2131.8581104
t(3, 2)	=	2174.6690550
t(3, 3)	=	2261.1684885
t(3, 4)	=	2335.9499908
t(3, 5)	=	2377.0411968
t(3, 6)	=	2377.3109644
t(3, 7)	=	2336.5916177
t(3, 8)	=	2261.6765124
t(3, 9)	=	2174.7395541
t(3, 10)	=	2144.1652664
t(4, 1)	=	2049.9178867
t(4, 2)	=	2080.6705441
t(4, 3)	=	2152.0199439
t(4, 4)	=	2214.9465505
t(4, 5)	=	2249.5126048
t(4, 6)	=	2249.7739613
t(4, 7)	=	2215.5694463
t(4, 8)	=	2152.5116847
t(4, 9)	=	2080.6980165
t(4, 10)	=	2058.6768568
t(5, 1)	=	1943.4002334
t(5, 2)	=	1958.6914577
t(5, 3)	=	2010.7078927
t(5, 4)	=	2058.7072181
t(5, 5)	=	2085.1766716
t(5, 6)	=	2085.4286152
t(5, 7)	=	2059.3079608
t(5, 8)	=	2011.1788302
t(5, 9)	=	1958.6693771
t(5, 10)	=	1947.3555271
t(6, 1)	=	1939.5252885
t(6, 2)	=	1954.2654800
t(6, 3)	=	2005.6800497
t(6, 4)	=	2053.2093102
t(6, 5)	=	2079.4213757
t(6, 6)	=	2079.6733825
t(6, 7)	=	2053.8103232
t(6, 8)	=	2006.1510542
t(6, 9)	=	1954.2364049
t(6, 10)	=	1943.3159623
t(7, 1)	=	919.3642134
t(7, 2)	=	923.9127148
t(7, 3)	=	932.3725376
t(7, 4)	=	941.0528808
t(7, 5)	=	949.3930788
t(7, 6)	=	956.9185405
t(7, 7)	=	963.3549215
t(7, 8)	=	968.7053012
t(7, 9)	=	973.3498345
t(7, 10)	=	982.1790161
t(8, 1)	=	915.0268697
t(8, 2)	=	919.9545935
t(8, 3)	=	928.0772959
t(8, 4)	=	936.4712201
t(8, 5)	=	944.6539122
t(8, 6)	=	952.1913380
t(8, 7)	=	958.8076000
t(8, 8)	=	964.4616232
t(8, 9)	=	969.4443033
t(8, 10)	=	977.8286091
t(9, 1)	=	902.6190560
t(9, 2)	=	908.5484778

t(9, 3) = 915.5611828
 t(9, 4) = 922.9632337
 t(9, 5) = 930.5231087
 t(9, 6) = 937.9496898
 t(9, 7) = 944.9825023
 t(9, 8) = 951.4578048
 t(9, 9) = 957.3857064
 t(9, 10) = 964.3110205
 t(10, 1) = 900.7157871
 t(10, 2) = 906.8155358
 t(10, 3) = 913.6812466
 t(10, 4) = 920.9576199
 t(10, 5) = 928.4483757
 t(10, 6) = 935.8802369
 t(10, 7) = 942.9920328
 t(10, 8) = 949.6005390
 t(10, 9) = 955.6753043
 t(10, 10) = 962.4140332
 tcool(1) = 895.0000000
 tcool(2) = 901.5697693
 tcool(3) = 908.1042149
 tcool(4) = 915.1116661
 tcool(5) = 922.4532633
 tcool(6) = 929.8935392
 tcool(7) = 937.1691484
 tcool(8) = 944.0572319
 tcool(9) = 950.4384966
 tcool(10) = 956.8961135

Temperature of coolant at core exit: 956.896 degrees K.
 Voltage across bottom of cell: 0.6427047
 Voltage across top of cell: 0.6464798
 Output current = 490.0000000
 Output electrical power = 315.8501975
 Total Thermal power = 3177.7050000

Z	V	Qec	Jdens
0.00000000	0.64270471	12.99420332	4.81284388
2.82222222	0.73952756	10.19447559	3.65196351
5.64444444	0.81536882	11.26434223	3.93893884
8.46666667	0.86803225	11.79162961	4.05764643
11.28888889	0.89558633	12.06404159	4.11782102
14.11111111	0.89678741	12.08230457	4.12396904
16.93333333	0.87140461	11.85295220	4.07907416
19.75555556	0.82022683	11.39399910	3.98648550
22.57777778	0.74473245	10.47667932	3.75799840
25.40000000	0.64647977	13.89467367	5.16896030

Z	EmHeat	ColHeat
0.00000000	14.49777300	12.78461813
2.82222222	8.68536675	7.62158438
5.64444444	4.81644251	4.12387927
8.46666667	1.87853834	1.57475799
11.28888889	0.24858863	0.20674847
14.11111111	0.15340144	0.12850539
16.93333333	1.60703735	1.37639999
19.75555556	4.41255720	3.91401618
22.57777778	8.23815769	7.58931886
25.40000000	14.53427214	13.59664908

Z	Qch	Qrad	QCCond
0.00000000	9.90096591	15.23808053	1.07744326
2.82222222	7.49374791	15.71537048	1.08777951
5.64444444	8.05265430	17.49574903	1.13124448
8.46666667	8.26946163	19.26610657	1.17042804
11.28888889	8.37617736	20.28345587	1.18841945
14.11111111	8.38398105	20.26435874	1.18111695
16.93333333	8.29842819	19.20286184	1.14859681
19.75555556	8.12417673	17.37203651	1.09503360
22.57777778	7.67797598	15.52319973	1.03762210
25.40000000	10.55304538	15.11997007	1.01755208

1***** TFETC *****

***** RESULTS FOR THE FOLLOWING CASE:

*** S H U T D O W N P R O B L E M ***

TIME = 3.0000000

TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

t(1, 1) = 2175.2091168
t(1, 2) = 2224.4941554
t(1, 3) = 2321.5539056
t(1, 4) = 2406.2573295
t(1, 5) = 2453.6435868
t(1, 6) = 2454.5622991
t(1, 7) = 2408.6250986
t(1, 8) = 2324.1860239
t(1, 9) = 2226.0284061
t(1, 10) = 2188.8984176
t(2, 1) = 2153.9197566
t(2, 2) = 2199.6888875
t(2, 3) = 2292.4566360
t(2, 4) = 2373.6281585
t(2, 5) = 2418.9759244
t(2, 6) = 2419.8541150
t(2, 7) = 2375.8863134
t(2, 8) = 2294.9454717
t(2, 9) = 2201.1036342
t(2, 10) = 2167.0138313
t(3, 1) = 2100.8278294
t(3, 2) = 2137.3601775
t(3, 3) = 2219.5099990
t(3, 4) = 2292.0662889
t(3, 5) = 2332.5036905
t(3, 6) = 2333.2754037
t(3, 7) = 2294.0380708
t(3, 8) = 2221.6295496
t(3, 9) = 2138.4733762
t(3, 10) = 2111.7750324
t(4, 1) = 2024.4381794
t(4, 2) = 2045.6193771
t(4, 3) = 2112.3681245
t(4, 4) = 2172.6792992
t(4, 5) = 2206.2624914
t(4, 6) = 2206.8712683
t(4, 7) = 2174.2175042
t(4, 8) = 2113.9377039
t(4, 9) = 2046.3165153
t(4, 10) = 2032.0477657
t(5, 1) = 1934.5739920
t(5, 2) = 1932.1721604
t(5, 3) = 1979.9686793
t(5, 4) = 2025.4903420
t(5, 5) = 2050.9792358
t(5, 6) = 2051.3987602
t(5, 7) = 2026.5290091
t(5, 8) = 1980.8912098
t(5, 9) = 1932.4543528
t(5, 10) = 1938.2045205
t(6, 1) = 1931.9105523
t(6, 2) = 1928.3942892
t(6, 3) = 1975.6567174
t(6, 4) = 2020.7490227
t(6, 5) = 2046.0120942
t(6, 6) = 2046.4283126
t(6, 7) = 2021.7787669
t(6, 8) = 1976.5621809
t(6, 9) = 1928.6648864
t(6, 10) = 1935.4357084
t(7, 1) = 919.6834321
t(7, 2) = 922.9062992
t(7, 3) = 931.3488388
t(7, 4) = 940.0559262
t(7, 5) = 948.3270923
t(7, 6) = 955.7868239
t(7, 7) = 962.1640739
t(7, 8) = 967.3831763
t(7, 9) = 971.8382477
t(7, 10) = 982.1357663
t(8, 1) = 915.2734764
t(8, 2) = 919.1136182
t(8, 3) = 927.2221537
t(8, 4) = 935.6381489
t(8, 5) = 943.7602506
t(8, 6) = 951.2288734
t(8, 7) = 957.7717363
t(8, 8) = 963.2889378
t(8, 9) = 968.0846745
t(8, 10) = 977.7028604
t(9, 1) = 902.6938868
t(9, 2) = 908.1276375
t(9, 3) = 915.1181665
t(9, 4) = 922.5250416
t(9, 5) = 930.0375575
t(9, 6) = 937.3797742

```
t( 9, 7) = 944.2951952
t( 9, 8) = 950.6094306
t( 9, 9) = 956.3519517
t( 9, 10) = 963.8994377
t( 10, 1) = 900.7660353
t( 10, 2) = 906.4540152
t( 10, 3) = 913.2935346
t( 10, 4) = 920.5702153
t( 10, 5) = 928.0133501
t( 10, 6) = 935.3566712
t( 10, 7) = 942.3432381
t( 10, 8) = 949.7856105
t( 10, 9) = 954.6735845
t( 10, 10) = 961.9558884
tcool( 1) = 895.0000000
tcool( 2) = 901.5016237
tcool( 3) = 907.8243883
tcool( 4) = 914.6487377
tcool( 5) = 921.8235578
tcool( 6) = 929.1103884
tcool( 7) = 936.2558890
tcool( 8) = 943.0329490
tcool( 9) = 949.3114083
tcool( 10) = 955.8092844
```

```
Temperature of coolant at core exit: 955.809 degrees K.
Voltage across bottom of cell: 0.6054920
Voltage across top of cell: 0.6098648
Output current = 490.0000000
Output electrical power = 297.7624247
Total Thermal power = 780.1080744
```

Z	V	Qec	Jdens
0.0000000	0.60549203	13.97631552	5.24725793
2.8222222	0.70021916	9.58456395	3.47982406
5.6444444	0.77484743	10.77465962	3.81891060
8.4666667	0.82722199	11.66113025	4.06688624
11.2888889	0.85470084	11.94602880	4.13241495
14.1111111	0.85603961	11.97170440	4.14127668
16.9333333	0.83098788	11.74628298	4.09712193
19.7555556	0.78029598	11.01423062	3.90594247
22.5777778	0.70598699	9.86219958	3.58501651
25.4000000	0.60986480	14.83566770	5.59654031

Z	EmHeat	ColHeat
0.0000000	14.42058898	12.78828925
2.8222222	8.38173326	7.47437845
5.6444444	4.73827708	4.13186324
8.4666667	1.89148833	1.60812593
11.2888889	0.25599615	0.21713951
14.1111111	0.14332497	0.12243004
16.9333333	1.56198780	1.36341936
19.7555556	4.28108126	3.86541502
22.5777778	7.88786912	7.37976079
25.4000000	14.45428255	13.59554922

Z	Qch	Qrad	QCCond
0.0000000	10.79914265	15.04593000	1.07132425
2.8222222	7.14792448	15.02346659	1.06741982
5.6444444	7.81558657	16.63043851	1.10755816
8.4666667	8.29691251	18.26547716	1.14485593
11.2888889	8.41405029	19.21336909	1.16211976
14.1111111	8.42660754	19.19909208	1.15496288
16.9333333	8.34162432	18.21457766	1.12341254
19.7555556	7.96643941	16.51971006	1.07178535
22.5777778	7.33122457	14.84062511	1.01767785
25.4000000	11.42253475	14.91919756	1.01129477

1***** TFEIC *****

***** RESULTS FOR THE FOLLOWING CASE:

*** S H U T D O W N P R O B L E M ***

TIME = 6.00000000

TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---

```
t( 1, 1) = 2137.1537602
t( 1, 2) = 2178.7763202
t( 1, 3) = 2270.3424920
```

t(1, 4) = 2352.2058158
t(1, 5) = 2398.8105113
t(1, 6) = 2400.4207526
t(1, 7) = 2356.3709744
t(1, 8) = 2275.0686959
t(1, 9) = 2181.5979032
t(1, 10) = 2149.4854712
t(2, 1) = 2117.4182109
t(2, 2) = 2154.7121441
t(2, 3) = 2241.9155529
t(2, 4) = 2320.0969459
t(2, 5) = 2364.5500674
t(2, 6) = 2366.0542532
t(2, 7) = 2323.9814644
t(2, 8) = 2246.2862579
t(2, 9) = 2157.2737901
t(2, 10) = 2129.0996137
t(3, 1) = 2069.0376110
t(3, 2) = 2094.8966270
t(3, 3) = 2171.4240386
t(3, 4) = 2240.6737363
t(3, 5) = 2280.0103436
t(3, 6) = 2281.2625374
t(3, 7) = 2243.8909742
t(3, 8) = 2174.9459411
t(3, 9) = 2096.8532271
t(3, 10) = 2078.6792651
t(4, 1) = 2000.9933116
t(4, 2) = 2008.3847474
t(4, 3) = 2069.7767331
t(4, 4) = 2126.4120062
t(4, 5) = 2158.7897204
t(4, 6) = 2159.7142171
t(4, 7) = 2128.7577585
t(4, 8) = 2072.1758999
t(4, 9) = 2009.5969578
t(4, 10) = 2007.6816471
t(5, 1) = 1921.0854419
t(5, 2) = 1902.9221561
t(5, 3) = 1946.3163071
t(5, 4) = 1987.5966110
t(5, 5) = 2011.9647916
t(5, 6) = 2012.5569247
t(5, 7) = 1989.0427574
t(5, 8) = 1947.5315793
t(5, 9) = 1903.4461349
t(5, 10) = 1924.3583482
t(6, 1) = 1918.6167527
t(6, 2) = 1899.3746759
t(6, 3) = 1942.3047530
t(6, 4) = 1983.1087120
t(6, 5) = 2007.2524160
t(6, 6) = 2007.8376664
t(6, 7) = 1984.5345570
t(6, 8) = 1943.4912502
t(6, 9) = 1899.8799782
t(6, 10) = 1921.7948770
t(7, 1) = 920.2385783
t(7, 2) = 921.7163918
t(7, 3) = 929.4294905
t(7, 4) = 938.0418324
t(7, 5) = 945.9787956
t(7, 6) = 953.1670869
t(7, 7) = 959.3564472
t(7, 8) = 964.0893700
t(7, 9) = 968.6705203
t(7, 10) = 980.8985011
t(8, 1) = 915.7287224
t(8, 2) = 918.1148562
t(8, 3) = 925.5615558
t(8, 4) = 933.8362900
t(8, 5) = 941.6269111
t(8, 6) = 948.8196982
t(8, 7) = 955.1623723
t(8, 8) = 960.2351176
t(8, 9) = 965.0904933
t(8, 10) = 976.3451849
t(9, 1) = 902.8580353
t(9, 2) = 907.7025904
t(9, 3) = 914.2278019
t(9, 4) = 921.3640554
t(9, 5) = 928.5614262
t(9, 6) = 935.6157394
t(9, 7) = 942.2880032
t(9, 8) = 948.2706591
t(9, 9) = 953.8761746

t(9, 10) = 962.1157834
 t(10, 1) = 900.8866062
 t(10, 2) = 906.1150878
 t(10, 3) = 912.5154417
 t(10, 4) = 919.4995424
 t(10, 5) = 926.6273554
 t(10, 6) = 933.6785544
 t(10, 7) = 940.4136359
 t(10, 8) = 946.5380125
 t(10, 9) = 952.2604084
 t(10, 10) = 960.1015218
 tcool(1) = 895.0000000
 tcool(2) = 901.4203347
 tcool(3) = 907.3837013
 tcool(4) = 913.8438917
 tcool(5) = 920.6952541
 tcool(6) = 927.6682153
 tcool(7) = 934.5241628
 tcool(8) = 941.0033013
 tcool(9) = 947.0140176
 tcool(10) = 953.5389272

Temperature of coolant at core exit: 953.539 degrees K.
 Voltage across bottom of cell: 0.5582231
 Voltage across top of cell: 0.5635919
 Output current = 490.0000000
 Output electrical power = 274.8446806
 Total Thermal power = 751.3957425

Z	V	Qec	Jdens
0.00000000	0.55822307	14.99565931	5.72925528
2.82222222	0.65062244	9.13030960	3.37249491
5.64444444	0.72343508	9.97983511	3.59903814
8.46666667	0.77550410	11.44195623	4.05955636
11.28888889	0.80303253	11.85489062	4.17155476
14.11111111	0.80453951	11.89502216	4.18592555
16.93333333	0.77974177	11.59297690	4.11436851
19.75555556	0.72952052	10.23862522	3.69467618
22.57777778	0.65720277	9.42946520	3.48799570
25.40000000	0.56359195	15.87532742	6.09624958

Z	EmHeat	ColHeat
0.00000000	14.29456808	12.79484983
2.82222222	8.00458752	7.26845157
5.64444444	4.61603461	4.10566820
8.46666667	1.88868670	1.65001363
11.28888889	0.26574308	0.23041701
14.11111111	0.13489302	0.11774609
16.93333333	1.52509930	1.35933496
19.75555556	4.10780373	3.77755644
22.57777778	7.45534498	7.08832947
25.40000000	14.32488978	13.57887468

Z	Qch	Grad	QCsCond
0.00000000	11.79745682	14.63163961	1.05785902
2.82222222	6.93608875	14.08628468	1.03882279
5.64444444	7.37616467	15.47006236	1.07511735
8.46666667	8.29375361	16.87667920	1.10846876
11.28888889	8.50499643	17.73199865	1.12501096
14.11111111	8.52727965	17.72460964	1.11826101
16.93333333	8.38483192	16.84259733	1.08813083
19.75555556	7.54328311	15.37355212	1.04080057
22.57777778	7.13714477	13.91962742	0.99108494
25.40000000	12.43953024	14.49800445	0.99904635

```

program TFETC
implicit double precision (a-h,o-z)

```

```

*****
*
*           Thermionic Fuel Element Transient Code (TFETC)
*         written by : Abdullah S. Al-Kheliewi
*
*****

Parameter (Imax = 10, Jmax = 10)
Integer Prob, Options
double precision Time, Tprint
Integer J, TabFlag, ipout, Isolver
double precision T(Imax,Jmax), msave, Current
double precision Tcoolant(Jmax), Zmin, Qec(jmax), Jdens(jmax)
double precision Tinlet, dt, Tstop, Tstart, Qch(jmax), QcsCond(jmax)
double precision Rbound(10), Ems, Tr, EmHeat(jmax), ColHeat(jmax)
double precision QTable(Jmax), De, Gl, W, PhiE, Qrad(jmax)
double precision Zmax, Itop, Ibottom, powerTh
double precision Dout, Din, Q3ave, PowerTabl(2,100)
double precision mdot, A, B, tau
Integer I, Rmesh(9), K2, Mat(5)
Character*80 Title
Common /Rdata/ Rbound, Rmesh, Mat
Common /Zdata/ Zmin, Zmax, K2
Common /QTAB/ QTable
Common /Input/ Tr, Ems, PhiE, Itop, Ibottom, Title
Common /CoolProp/ Tinlet, De, Gl, W, Dout, Din, mdot
Common /Steady/ Emheat, ColHeat, Qch, Qrad, QcsCond, Qec, Jdens,
& Current
* Common /PowerData/ Q3ave, PowerTabl, TabFlag
Data Pi/3.1415926D0/

c
c ... read input data for TFETC
call input(Prob,Options,Time,Tprint,T,dt,Tstop,Tstart,
& tcoolant,powerTh,A,B,tau,ipout,Isolver)

c
c ... ***** run steady state problem *****
if ( Prob .eq. 4 ) then
    print*, ' Calculating steady state temperature profile ... '
    print*
    call tfhx(tcoolant,t,Isolver)
    stop
end if

c
c ... ***** run start up problem *****
if ( Prob .eq. 1 ) then
    if ( Options .eq. 1 ) then
c use default ambient conditions for start-up
        do 10 j=1,jmax
            do 10 i=1,imax
                T(i,j) = 298.0d0
                Tcoolant(j) = Tinlet
10          continue
            end if
        print*, ' Calculating transient temperature profile ... '
        print*
        call timplicit(T,Time,Tprint,dt,Prob,tcoolant,msave,
& Tstop,Tstart,options,powerTh,A,B,tau,
& ipout,Isolver)
        end if
c
c ... ** run shutdown problem or loss of flow problem ***
if ( Prob .eq. 2 .or. Prob .eq. 3 ) then
    if ( Options .eq. 1 ) then
c use steady state solution as forcing function
        print*, ' Calculating steady state temperature profile ... '
        print*
        call tfhx(tcoolant,t,Isolver)
        end if
        if ( prob .eq. 3 ) then
c
c ... if loss of flow, set flow-rate at t=0 to msave
            msave = mdot
        end if
    end if

```

```

print*, ' Calculating transient temperature profile ... '
print*

call timplicit(T,Time,Tprint,dt,Prob,tcoolant,msave,
$           Tstop,Tstart,options,powerTh,A,B,tau,
$           ipout,Isolver)
end if

stop
end

subroutine gdot(tnow,msave,A,B,tau)
double precision Tinlet, De, G1, W, Dout, Din, mdot, tnow, msave
double precision ir(10), or(10), A, B, tau, Pi
Common /CoolProp/ Tinlet, De, G1, W, Dout, Din, mdot
Common /ggdot/ ir, or
Data Pi/3.1415926D0/
c
c
mdot = msave * (A + B*dexp(-tnow/tau) )
g1 = mdot/(or(10)**2.0d0-ir(10)**2.0d0)/pi

return
end
subroutine timplicit(t,time,tprint,dt,prob,tcoolant,msave,
$           Tstop,Tecool,option,powerTh,Aa,B,tau,
$           ipout,Isolver)
implicit double precision (a-h,o-z)
*****
*
*   This subroutine does transient calculations.
*   It is part of the TFETC code.
*   Written by : Abdullah S. Al-Kheliewi (June 1993)
*
*****
parameter ( imax = 10, jmax = 10 )
integer prob, N, icmax, itnow, Isolver
double precision t(imax,jmax),time,tprint,mdot
integer j, j2, j3, loff, option, istart, ipout, iprint
double precision A(imax*jmax+1,imax*jmax), X(imax*jmax)
double precision c1, kcond, r, z, r1, z1, msave,Aa,B
double precision r2,z2,r3,z3,temp3,h,t1,temm(jmax),tau
double precision deltax,c3,t2,tcoolant(jmax),v(jmax),zmin
double precision tinlet,v0,c4,cpl,dt,rho1,tnow,dmax1,minv
double precision rbound(10),sig,ems,gapcond,tr,qch(jmax)
double precision heffe(jmax),heffc(jmax), current,qec(jmax)
double precision jdens(jmax),gtran,ccp,rho,pi,teaav,tcol(jmax)
double precision qtable(jmax),de,g1,w,phie,emheat(jmax)
double precision colheat(jmax),zmax,itop,ibottom,cden_av1,cden_av2
double precision vguess(jmax),teav(jmax),tcav(jmax),Tstop,Tecool
double precision dout,din,ThPower,Power
double precision qrad(jmax),qcscond(jmax),tstart, powerTh
integer i, k, il, i2, i3, i4, rmesh(9), k2, i9, mat(5)
character*80 title
Common /GaussMAIN/ A, X, N
common /rdata/ rbound,rmesh,mat
common /zdata/ zmin,zmax,k2
common /qtab/ qtable
common /input/ tr, ems, phie, itop, ibottom, title
common /coolprop/ tinlet, de, g1, w, dout, din, mdot
Common /Steady/ Emheat,ColHeat,Qch,Qrad,QcsCond,Qec,Jdens,
$           Current
Data Pi/3.1415926D0/
c
c ... set the stefan-boltzman constant (watts/cm^2 k^4) sig
sig = 5.67d-12
N = imax*jmax
ioff = 0
istart = 0
c
c ... set the initial guess value of the interelectrode voltage.
v0 = 0.6d0
do k=1, jmax
vguess(k) = v0
end do
c
c ... initialize loop parameters
tstart = 0.0d0
icmax = idint( time/dt ) + 1
c
c ... start major loop for transient calculations
do itnow = 1,icmax
tnow = dble( float(itnow-1) ) * dt
if (itnow .eq. icmax ) tnow = time
c

```

```

c ... update mass-flow-rate and mass-velocity
  if ( prob .eq. 3 ) then
    call gdot(tnow,msave,Aa,B,tau)
  end if
c
c ... form a table for calculating the heatflux
  do k=1,jmax
    qtable(k) = kcond(imax,r(imax),t(imax,k))
    a      *(t(imax-1,k) - t(imax,k))/(r(imax) - r(imax-1))
    if (qtable(k) .lt. 0.d0 ) qtable(k) = 0.d0
  end do
c
c ... solve for the axial coolant temperature distribution
  call tconvect(tnow,dt,tcoolant)
  call coolanttemp(tcoolant)
c
c ... compute average emitter and collector temperatures (axial)
  i1 = 1
  do i9=1,2
    i1 = i1 + rmesh(i9)
  end do
  i2 = 1
  do i9=1,3
    i2 = i2 + rmesh(i9)
  end do
  i3 = i2+1
  i4 = 1
  do i9=1,5
    i4 = i4 + rmesh(i9)
  end do
  teaav = 0.d0
  do k=1,jmax
    temm(k) = t(i2,k)
    teaav = teaav + temm(k)
    tcol(k) = t(i2+1,k)
    teav(k) = t(i1,k)*(r(i1+1)**2+2*r(i1+1)*r(i1)-3*r(i1)**2)/4
    tcav(k) = t(i3,k)*(r(i3+1)**2+2*r(i3+1)*r(i3)-3*r(i3)**2)/4
    do i=i1+1,i2-1
      a      teav(k) = teav(k) + t(i,k)*(r(i+1)**2+2*r(i)*
        (r(i+1)-r(i-1))-r(i-1)**2)/4
    end do
    do i=i3+1,i4-1
      a      tcav(k) = tcav(k) + t(i,k)*(r(i+1)**2+2*r(i)*
        (r(i+1)-r(i-1))-r(i-1)**2)/4
    end do
    a      teav(k) = teav(k) + t(i2,k)*(3*r(i2)**2-2*r(i2)*r(i2-1)
      -r(i2-1)**2)/4
    a      tcav(k) = tcav(k) + t(i4,k)*(3*r(i4)**2-2*r(i4)*r(i4-1)
      -r(i4-1)**2)/4
    a      teav(k) = teav(k)/(r(i2)**2-r(i1)**2)
      tcav(k) = tcav(k)/(r(i4)**2-r(i3)**2)
  end do
c
c ... compute the axially-averaged emitter temperature at the outer
c ... surface
  teaav = teaav/dbl(float(jmax))
c
c ... compute voltage and current density distribution along the length
c ... of the thermionic converter
  cden_av1 = ibottom/(pi*r(i2)**2*(zmax-zmin)/2)
  cden_av2 = itop/(pi*r(i2)**2*(zmax-zmin)/2)
c
c ... calculate the transient cesium reservoir temperature
  if ( (Prob .eq. 1 .and. Teaav .lt. Tecoal .and. istart .eq. 0)
    .or. (Prob .eq. 2 .and. ioff .eq. 1) ) then
    .or. itnow .lt. 2 ) then
    call helium(v,qec,qch,jdens,emheat,colheat)
  else
    print*, ' calling cylcon '
    call cylcon6(temm,teav,tcol,tcav,tr,phie,r(i3)-r(i2),cden_av1,
      1 cden_av2,zmax-zmin,2*r(i2),r(i2)-r(i1),r(i4)-r(i3),jmax,
      2 vguess, v, qec, jdens, emheat, colheat)
    current = itop+ibottom
    do k=1,jmax
      vguess(k) = v(k)
      qch(k) = qec(k)-jdens(k)*v(k)
    end do
  end if

```

```

if ( prob .eq. 1 )  istart = 1
if ( minv(v) .lt. 0.0d0 ) then
  call helium(v,qec,qch,jdens,emheat,colheat)
  ioff = 1
end if

end if
if ( prob .ne. 1 .and. option .eq. 2 ) then
  call initial(prob,Tstop,Tecool,tr,sig,ems,
    &          Grad,Qcscnd,t)
end if
Power = ThPower(prob,tau,tnow,powerTh)
c
c ... write output
*
if (iprint(tnow,tprint,dt,time,tstart) .eq. 1) then
  print *, ' Time = ', tnow
  j2 = jmax/2
  j3 = j2 + 1
  print 100, tnow,dmax1(t(i,j2),t(i,j3)),teaav,tcoolant(jmax)
100  format(' Time = ',f9.3,' Tfuel = ',f9.3,' Teav = ',f9.3,
&        ' Tcoolant = ',f9.3)
  call output(tnow,imax,jmax, v, qec, jdens, emheat,
1      tcoolant,colheat, qch, grad, qcscnd,
2      t, current, prob, Power, ipout)
end if

do 2000 j=1, jmax
do 2000 i=1, imax
  i2 = (j-1)*imax + i
  do k=1,N+1
    A(k,i2) = 0.0d0
  end do
**  i = 1, j = 2, jmax -1 ***** (Figure 3.6)
  if ((i.eq.1).and.((j.ne.1).and.(j.ne.jmax))) then
    r1 = r(i)
    r3 = r(i+1)
    r2 = (r3 + r1)/2
    z1 = z(j)
    deltax = (z(j+1)-z(j-1))/2
    t1 = (t(i+1,j) + t(i,j))/2
    c3 = kcond(i,r2,t1)*(r3+r1)/(r3-r1)*deltax
    c1 = c3

    j2 = (j-1)*imax + i + 1
    A(j2,i2) = C3

    temp3 = (r3**2 + 2*r1*r3 - 3*r1**2)/4
    z3 = z(j+1)
    z2 = (z3 + z1)/2
    t1 = (t(i,j+1) + t(i,j))/2
    c3 = kcond(i,r1,t1)/(z3-z1)*temp3
    c1 = c1 + c3
    J2 = j*imax + i
    A(j2,i2) = C3

    z3 = z(j-1)
    z2 = (z3 + z1)/2
    t1 = (t(i,j-1) + t(i,j))/2
    c3 = kcond(i,r1,t1)/(z1-z3)*temp3
    c1 = c1 + c3
    J2 = (j-2)*imax + i
    A(j2,i2) = C3
    rho1 = rho(i,(r1+r2)/2)
    cpl = ccp(i,(r1+r2)/2,t1)
    c4 = rho1 * cpl * deltax * temp3/dt
    c1 = c1 + c4
    A(N+1,i2) = - gtran((r1+r2)/2,z1,prob,tau,tnow)
&      * deltax * temp3 - c4 * t(i,j)

    A(i2,i2) = - c1

    go to 2000
  endif

**  if ((i.eq.1).and.(j.eq.1)) then ***** (Figure 3.5)
  i = 1, j = 1
  r1 = r(i)
  r3 = r(i+1)
  r2 = (r3 + r1)/2
  z1 = z(j)
  z3 = z(j+1)
  deltax = (z3-z1)/2
  t1 = (t(i+1,j) + t(i,j))/2
  c3 = kcond(i,r2,t1)*(r3+r1)/(r3-r1)*deltax

```



```

c1 = c3
J2 = (j-1)*Imax + I+1
A(J2,I2) = C3

temp3 = (r3**2 - 3*r1**2 + 2*r1*r3)/4
z2 = (z3 + z1)/2
t1 = (t(i,j+1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z3-z1)*temp3
c1 = c1 + c3
J2 = j*Imax + I
A(J2,I2) = C3

rho1 = rho(i,(r1+r2)/2)
cpl = ccp(i,(r1+r2)/2,t1)
c4 = rho1 * cpl * deltax * temp3/dt
c1 = c1 + c4
A(N+1,I2) = - gtran((r1+r2)/2,(z1+z2)/2,prob,tau,tnow)
          * deltax * temp3 - c4 * t(i,j)

A(i2,i2) = - c1
go to 2000

end if

**
if ((i.eq.1).and.(j.eq.jmax)) then
i = 1 and j = jmax ***** (Figure 3.4)
r1 = r(i)
r3 = r(i+1)
r2 = (r3 + r1)/2
z1 = z(j)
z3 = z(j-1)
deltaz = (z1-z3)/2
t1 = (t(i+1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r3-r1)*deltaz
c1 = c3
J2 = (j-1)*Imax + I+1
A(J2,I2) = C3

temp3 = (r3**2 - 3*r1**2 + 2*r1*r3)/4
z2 = (z3 + z1)/2
t1 = (t(i,j-1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z1-z3)*temp3
c1 = c1 + c3
J2 = (j-2)*Imax + I
A(J2,I2) = C3

rho1 = rho(i,(r1+r2)/2)
cpl = ccp(i,(r1+r2)/2,t1)
c4 = rho1 * cpl * deltax * temp3/dt
c1 = c1 + c4
A(N+1,I2) = - gtran((r1+r2)/2,(z1+z2)/2,prob,tau,tnow)
          * deltax * temp3 - c4 * t(i,j)

A(i2,i2) = - c1
go to 2000

end if

**
Collector Surface, j = 2, jmax -1 ***** (Figure 3.12)
if ((r(i).eq.rbound(5)).and.((j.ne.1).and.(j.ne.jmax))) then
r1 = r(i)
r3 = r(i+1)
r2 = (r3 + r1)/2
z1 = z(j)
deltaz = (z(j+1)-z(j-1))/2
t1 = (t(i+1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r3-r1)*deltaz
c1 = c3
J2 = (j-1)*Imax + I+1
A(J2,I2) = C3

temp3 = (r3**2 + 2*r1*r3 - 3*r1**2)/4
z3 = z(j+1)
z2 = (z3 + z1)/2
t1 = (t(i,j+1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z3-z1)*temp3
c1 = c1 + c3
J2 = j*Imax + I
A(J2,I2) = C3

z3 = z(j-1)
z2 = (z3 + z1)/2
t1 = (t(i,j-1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z1-z3)*temp3
c1 = c1 + c3
J2 = (j-2)*Imax + I

```

```

A(J2,I2) = C3

t1 = t(i-1,j)-t(i,j)
t2 = dmax1( t1, 1.0d0 )
if ( t1 .le. 0.0d0 ) then
  heffc(j) = qch(j)*2*r(i-1)*deltaz
else
b   heffc(j) = (qch(j)
c   + sig*ems*((t(i-1,j))**4-(t(i,j))**4)*r(i-1)/r(i)
d   + gapcond(t(i-1,j),t(i,j),Tstop,Tecool,Prob,tr,
  r(i)-r(i-1)))*2*r(i-1)*deltaz/t2
end if
C1 = C1 + Heffc(j)
J2 = (j-1)*Imax + I-1
A(J2,I2) = Heffc(j)

rho1 = rho(i,(r1+r2)/2)
t1 = (t(i,j-1) + t(i,j))/2
cpl = ccp(i,(r1+r2)/2,t1)
c4 = rho1 * cpl * deltaz * temp3/dt
c1 = c1 + c4
a   A(N+1,I2) = - (gtran((r1+r2)/2,z1,Prob,tau,tnow) +
  colheat(j))*deltaz * temp3 - c4 * t(i,j)

A(i2,I2) = - c1
go to 2000

end if

** Collector Surface, j = 1 ***** (Figure 3.14)
if ((r(i).eq.rbound(5)).and.(j.eq.1)) then
  r1 = r(i)
  r3 = r(i+1)
  r2 = (r3 + r1)/2
  z1 = z(j)
  z3 = z(j+1)
  deltaz = (z3-z1)/2
  t1 = (t(i+1,j) + t(i,j))/2
  c3 = kcond(i,r2,t1)*(r3+r1)/(r3-r1)*deltaz
  c1 = c3
  J2 = (j-1)*Imax + I+1
  A(J2,I2) = C3

  temp3 = (r3**2 - 3*r1**2 + 2*r1*r3)/4
  z2 = (z3 + z1)/2
  t1 = (t(i,j+1) + t(i,j))/2
  c3 = kcond(i,r1,t1)/(z3-z1)*temp3
  c1 = c1 + c3
  J2 = j*Imax + I
  A(J2,I2) = C3

  t1 = t(i-1,j)-t(i,j)
  t2 = dmax1( t1, 1.0d0 )
  if ( t1 .le. 0.0d0 ) then
    heffc(j) = qch(j)*2*r(i-1)*deltaz
  else
b   heffc(j) = (qch(j)
c   + sig*ems*((t(i-1,j))**4-(t(i,j))**4)*r(i-1)/r(i)
d   + gapcond(t(i-1,j),t(i,j),Tstop,Tecool,Prob,tr,
  r(i)-r(i-1)))*2*r(i-1)*deltaz/t2
end if
C1 = C1 + Heffc(j)
J2 = (j-1)*Imax + I-1
A(J2,I2) = Heffc(j)

rho1 = rho(i,(r1+r2)/2)
t1 = (t(i,j+1) + t(i,j))/2
cpl = ccp(i,(r1+r2)/2,t1)
c4 = rho1 * cpl * 2 * deltaz * temp3/dt
c1 = c1 + c4
a   A(N+1,I2) = - (gtran((r1+r2)/2,z1,Prob,tau,tnow) +
  colheat(j))*deltaz * temp3 - c4 * t(i,j)

A(i2,i2) = - c1
go to 2000

end if

** Collector Surface and j = jmax ***** (Figure 3.13)
if ((r(i).eq.rbound(5)).and.(j.eq.jmax)) then
  r1 = r(i)
  r3 = r(i+1)
  r2 = (r3 + r1)/2
  z1 = z(j)
  z3 = z(j-1)
  deltaz = (z1-z3)/2

```

```

t1 = (t(i+1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r3-r1)*deltaz
c1 = c3
J2 = (j-1)*Imax + I+1
A(J2,I2) = C3

temp3 = (r3**2 - 3*r1**2 + 2*r1*r3)/4
z2 = (z3 + z1)/2
t1 = (t(i,j-1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z1-z3)*temp3
c1 = c1 + c3
J2 = (j-2)*Imax + I
A(J2,I2) = C3

t1 = t(i-1,j)-t(i,j)
t2 = dmax1( t1, 1.0d0 )
if ( t1 .le. 0.0d0 ) then
  heffc(j) = qch(j)*2*r(i-1)*deltaz
else
  heffc(j) = (qch(j)
+ sig*ems*{(t(i-1,j))**4-(t(i,j))**4}*r(i-1)/r(i)
+ gapcond(t(i-1,j),t(i,j),Tstop,Tecool,Prob,tr,
r(i)-r(i-1)))*2*r(i-1)*deltaz/t2
end if
C1 = C1 + Heffc(j)
J2 = (j-1)*Imax + I-1
A(J2,I2) = Heffc(j)

rho1 = rho(i,(r1+r2)/2)
t1 = (t(i,j-1) + t(i,j))/2
cpl = ccp(i,(r1+r2)/2,t1)
c4 = rho1 * cpl * 2 * deltax * temp3/dt
c1 = c1 + c4
a A(N+1,I2) = - (gtran((r1+r2)/2,z1,Prob,tau,tnow) +
colheat(j))*deltaz * temp3 - c4 * t(i,j)

A(i2,i2) = - c1
go to 2000

end if

** Emitter Surface, j = 2, jmax -1 ***** (Figure 3.9)
if ((r(i).eq.rbound(4)).and.((j.ne.1).and.(j.ne.jmax))) then
  r1 = r(i)
  z1 = z(j)
  deltax = (z(j+1)-z(j-1))/2
  r3 = r(i-1)
  r2 = (r3 + r1)/2
  t1 = (t(i-1,j) + t(i,j))/2
  c3 = kcond(i,r2,t1)*(r3+r1)/(r1-r3)*deltaz
  c1 = c3
  J2 = (j-1)*Imax + I-1
  A(J2,I2) = C3

  temp3 = (3*r1**2 - r3**2 - 2*r1*r3)/4
  z3 = z(j+1)
  z2 = (z3 + z1)/2
  t1 = (t(i,j+1) + t(i,j))/2
  c3 = kcond(i,r1,t1)/(z3-z1)*temp3
  c1 = c1 + c3
  J2 = j*Imax + I
  A(J2,I2) = C3

  z3 = z(j-1)
  z2 = (z3 + z1)/2
  t1 = (t(i,j-1) + t(i,j))/2
  c3 = kcond(i,r1,t1)/(z1-z3)*temp3
  c1 = c1 + c3
  J2 = (j-2)*Imax + I
  A(J2,I2) = C3

  t1 = t(i,j)-t(i+1,j)
  t2 = dmax1( t1, 1.0d0 )
  if ( t1 .le. 0.0d0 ) then
    heffe(j) = qec(j)*2*r(i)*deltaz
    grad(j) = 0.0d0
    qcscond(j) = 0.0d0
  else
    heffe(j) = (qec(j)
+ sig*ems*{(t(i,j))**4 - (t(i+1,j))**4}
+ gapcond(t(i,j),t(i+1,j),Tstop,Tecool,Prob,tr,
r(i+1)-r(i))*2*r(i)*deltaz/t2
grad(j) = sig*ems*{(t(i,j))**4 - (t(i+1,j))**4}
qcscond(j) = gapcond(t(i,j),t(i+1,j),Tstop,Tecool,Prob,
tr,r(i+1)-r(i))
end if

```

```

C1 = C1 + HeffE(j)
J2 = (j-1)*Imax + I+1
A(J2,I2) = HeffE(j)

rhol = rho(i,(r1+r2)/2)
t1 = (t(i,j-1) + t(i,j))/2
cpl = ccp(i,(r1+r2)/2,t1)
c4 = rhol * cpl * deltax * temp3/dt
c1 = c1 + c4
A(N+1,I2) = - (gtran((r1+r2)/2,z1,prob,tau,tnow)
+emheat(j))* deltax * temp3 - c4 * t(i,j)
b

A(i2,i2) = - c1
go to 2000

end if

** Emitter Surface, j = 1 ***** (Figure 3.11)
if ((r(i).eq.rbound(4)).and.(j.eq.1)) then
r1 = r(i)
z1 = z(j)
z3 = z(j+1)
deltaz = (z3-z1)/2
r3 = r(i-1)
r2 = (r3 + r1)/2
t1 = (t(i-1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r1-r3)*deltaz
c1 = c3
J2 = (j-1)*Imax + I-1
A(J2,I2) = C3

temp3 = (3*r1**2 - r3**2 + 2*r1*r3)/4
z2 = (z3 + z1)/2
t1 = (t(i,j+1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z3-z1)*temp3
c1 = c1 + c3
J2 = j*Imax + I
A(J2,I2) = C3

t1 = t(i,j)-t(i+1,j)
t2 = dmaxi( t1, 1.0d0 )
if ( t1 .le. 0.0d0 ) then
heffe(j) = qec(j)*2*r(i)*deltaz
grad(j) = 0.0d0
qcscond(j) = 0.0d0
else
heffe(j) = (qec(j)
+ sig*ems*((t(i,j))**4 - (t(i+1,j))**4)
+ gapcond(t(i,j),t(i+1,j),Tstop,Tecool,Prob,tr,
r(i+1)-r(i))*2*r(i)*deltaz/t2
grad(j) = sig*ems*((t(i,j))**4 - (t(i+1,j))**4)
qcscond(j) = gapcond(t(i,j),t(i+1,j),Tstop,Tecool,Prob,
tr,r(i+1)-r(i))
end if
b
c
d
a
C1 = C1 + HeffE(j)
J2 = (j-1)*Imax + I+1
A(J2,I2) = HeffE(j)

rhol = rho(i,(r1+r2)/2)
t1 = (t(i,j+1) + t(i,j))/2
cpl = ccp(i,(r1+r2)/2,t1)
c4 = rhol * cpl * 2 * deltax * temp3/dt
c1 = c1 + c4
a
A(N+1,I2) = - (gtran((r1+r2)/2,(z1+z2)/2,prob,tau,tnow)
+emheat(j))*deltaz * temp3 - c4 * t(i,j)

A(i2,i2) = - c1
go to 2000

end if

** Emitter Surface, j = jmax ***** (Figure 3.10)
if ((r(i).eq.rbound(4)).and.(j.eq.jmax)) then
r1 = r(i)
z1 = z(j)
z3 = z(j-1)
deltaz = (z1-z3)/2
r3 = r(i-1)
r2 = (r3 + r1)/2
t1 = (t(i-1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r1-r3)*deltaz
c1 = c3
J2 = (j-1)*Imax + I-1
A(J2,I2) = C3

temp3 = (3*r1**2 - r3**2 + 2*r1*r3)/4

```

```

z2 = (z3 + z1)/2
t1 = (t(i,j-1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z1-z3)*temp3
c1 = c1 + c3
J2 = (j-2)*Imax + I
A(J2,I2) = C3

t1 = t(i,j)-t(i+1,j)
t2 = dmax1( t1, 1.0d0 )
if ( t1 .le. 0.0d0 ) then
  heffe(j) = qec(j)*2*r(i)*deltaz
  grad(j) = 0.0d0
  qcscond(j) = 0.0d0
else
  heffe(j) = (qec(j)
+ sig*ems*(t(i,j))**4 - (t(i+1,j))**4)
+ gapcond(t(i,j),t(i+1,j),Tstop,Tecool,Prob,tr,
d r(i+1)-r(i)))*2*r(i)*deltaz/t2
  grad(j) = sig*ems*(t(i,j))**4 - (t(i+1,j))**4)
  qcscond(j) = gapcond(t(i,j),t(i+1,j),Tstop,Tecool,Prob,
a tr,r(i+1)-r(i))
end if
C1 = C1 + HeffE(j)
J2 = (j-1)*Imax + I+1
A(J2,I2) = HeffE(j)

rhol = rho(i,(r1+r2)/2)
t1 = (t(i,j-1) + t(i,j))/2
cpl = ccp(i,(r1+r2)/2,t1)
c4 = rhol * cpl * 2 * deltaz * temp3/dt
c1 = c1 + c4
a A(N+1,I2) = - (gtran((r1+r2)/2,(z1+z2)/2,prob,tau,tnow)
+emheat(j))*deltaz * temp3 - c4 * t(i,j)

A(i2,i2) = - c1
go to 2000

end if

** if (((i.ne.1).and.(i.ne.imax)).and.(j.eq.1)) then
j = 1 and i = 2, imax -1 ***** (Figure 3.8)
r1 = r(i)
r3 = r(i+1)
r2 = (r3 + r1)/2
z1 = z(j)
z3 = z(j+1)
deltaz = (z3-z1)/2
t1 = (t(i+1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r3-r1)*deltaz
c1 = c3
J2 = (j-1)*Imax + I+1
A(J2,I2) = C3

r3 = r(i-1)
r2 = (r3 + r1)/2
t1 = (t(i-1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r1-r3)*deltaz
c1 = c1 + c3
J2 = (j-1)*Imax + I-1
A(J2,I2) = C3

r2 = r(i+1)
temp3 = (r2**2 - r3**2 + 2*r1*(r2-r3))/4
z2 = (z3 + z1)/2
t1 = (t(i,j+1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z3-z1)*temp3
c1 = c1 + c3
J2 = j*Imax + I
A(J2,I2) = C3

rhol = rho(i,r1)
cpl = ccp(i,r1,t1)
c4 = rhol * cpl * deltaz * temp3/dt
c1 = c1 + c4
a A(N+1,I2) = - gtran(r1,(z1+z2)/2,prob,tau,tnow)
* deltaz * temp3 - c4 * t(i,j)

A(i2,i2) = - c1
go to 2000

end if

** if (((i.ne.1).and.(i.ne.imax)).and.(j.eq.jmax)) then
j = jmax and i = 2, imax -1 ***** (Figure 3.7)
r1 = r(i)
r3 = r(i+1)

```

```

r2 = (r3 + r1)/2
z1 = z(j)
z3 = z(j-1)
deltaz = (z1-z3)/2
t1 = (t(i+1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r3-r1)*deltaz
c1 = c3
J2 = (j-1)*Imax + I+1
A(J2,I2) = C3

r3 = r(i-1)
r2 = (r3 + r1)/2
t1 = (t(i-1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r1-r3)*deltaz
c1 = c1 + c3
J2 = (j-1)*Imax + I-1
A(J2,I2) = C3

r2 = r(i+1)
temp3 = (r2**2 - r3**2 + 2*r1*(r2-r3))/4
z2 = (z3 + z1)/2
t1 = (t(i,j-1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z1-z3)*temp3
c1 = c1 + c3
J2 = (j-2)*Imax + I
A(J2,I2) = C3

rho1 = rho(i,r1)
cp1 = ccp(i,r1,t1)
c4 = rho1 * cp1 * deltaz * temp3/dt
c1 = c1 + c4
a A(N+1,I2) = - gtran(r1,z2,prob,tau,tnow)*deltaz * temp3
      - c4 * t(i,j)

A(i2,i2) = - c1
go to 2000

endif

** if ((i.eq.imax).and.((j.ne.1).and.(j.ne.jmax))) then (Figure 3.15)
i = imax, j = 2, jmax -1 *****
r1 = r(i)
z1 = z(j)
deltaz = (z(j+1)-z(j-1))/2
t2 = tcoolant(j)
c3 = h(t2)*r1*deltaz*2
c1 = c3
A(N+1,I2) = -C3*T2

r3 = r(i-1)
r2 = (r3 + r1)/2
t1 = (t(i-1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r1-r3)*deltaz
c1 = c1 + c3
J2 = (j-1)*Imax + I-1
A(J2,I2) = C3

temp3 = (3*r1**2 - r3**2 - 2*r1*r3)/4
z3 = z(j+1)
z2 = (z3 + z1)/2
t1 = (t(i,j+1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z3-z1)*temp3
c1 = c1 + c3
J2 = j*Imax + I
A(J2,I2) = C3

z3 = z(j-1)
z2 = (z3 + z1)/2
t1 = (t(i,j-1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z1-z3)*temp3
c1 = c1 + c3
J2 = (j-2)*Imax + I
A(J2,I2) = C3

rho1 = rho(i,r2)
cp1 = ccp(i,r2,t1)
c4 = rho1 * cp1 * deltaz * temp3/dt
c1 = c1 + c4
a A(N+1,I2) = A(N+1,I2) - gtran(r2,z1,prob,tau,tnow)
      + deltaz * temp3 - c4 * t(i,j)

A(i2,i2) = - c1
go to 2000

endif

```

```

**      if ((i.eq.imax).and.(j.eq.1)) then
i = imax, j = 1 ***** (Figure 3.17)
      r1 = r(i)
      z1 = z(j)
      z3 = z(j+1)
      deltaz = (z3-z1)/2
      t1 = t(i,j)
      t2 = tcoolant(j)
      c3 = h(t2)*r1*deltaz*2
      c1 = c3
      A(N+1,I2) = - c3 * t2

      r3 = r(i-1)
      r2 = (r3 + r1)/2
      t1 = (t(i-1,j) + t(i,j))/2
      c3 = kcond(i,r2,t1)*(r3+r1)/(r1-r3)*deltaz
      c1 = c1 + c3
      J2 = (j-1)*Imax + I-1
      A(J2,I2) = C3

      temp3 = (3*r1**2 - r3**2 + 2*r1*r3)/4
      z2 = (z3 + z1)/2
      t1 = (t(i,j+1) + t(i,j))/2
      c3 = kcond(i,r1,t1)/(z3-z1)*temp3
      c1 = c1 + c3
      J2 = j*Imax + I
      A(J2,I2) = C3

      rho1 = rho(i,r1)
      cpl = ccp(i,r1,t1)
      c4 = rho1 * cpl * deltaz * temp3/dt
      c1 = c1 + c4
      A(N+1,I2) = A(N+1,I2) - gtran(r2,z2,prob,tau,tnow)
a          * deltaz * temp3 - c4 * t(i,j)

      A(i2,i2) = - c1
      go to 2000

endif

**      if ((i.eq.imax).and.(j.eq.jmax)) then
i = imax, j = jmax ***** (Figure 3.16)
      r1 = r(i)
      z1 = z(j)
      z3 = z(j-1)
      deltaz = (z1-z3)/2
      t1 = t(i,j)
      t2 = tcoolant(j)
      c3 = h(t2)*r1*deltaz*2
      c1 = c3
      A(N+1,I2) = - c3 * t2

      r3 = r(i-1)
      r2 = (r3 + r1)/2
      t1 = (t(i-1,j) + t(i,j))/2
      c3 = kcond(i,r2,t1)*(r3+r1)/(r1-r3)*deltaz
      c1 = c1 + c3
      J2 = (j-1)*Imax + I-1
      A(J2,I2) = C3

      temp3 = (3*r1**2 - r3**2 + 2*r1*r3)/4
      z2 = (z3 + z1)/2
      t1 = (t(i,j-1) + t(i,j))/2
      c3 = kcond(i,r1,t1)/(z1-z3)*temp3
      c1 = c1 + c3
      J2 = (j-2)*Imax + I
      A(J2,I2) = C3

      rho1 = rho(i,r2)
      cpl = ccp(i,r2,t1)
      c4 = rho1 * cpl * deltaz * temp3/dt
      c1 = c1 + c4
      A(N+1,I2) = A(N+1,I2) - gtran(r2,z2,prob,tau,tnow)
a          * deltaz * temp3 - c4 * t(i,j)

      A(i2,i2) = - c1
      go to 2000

endif

**      all other points ***** (Figure 3.1)
      r1 = r(i)
      r3 = r(i+1)
      r2 = (r3 + r1)/2
      z1 = z(j)
      deltaz = (z(j+1)-z(j-1))/2

```

```

t1 = (t(i+1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r3-r1)*deltaz
c1 = c3
J2 = (j-1)*Imax + I+1
A(J2,I2) = C3

r3 = r(i-1)
r2 = (r3 + r1)/2
t1 = (t(i-1,j) + t(i,j))/2
c3 = kcond(i,r2,t1)*(r3+r1)/(r1-r3)*deltaz
c1 = c1 + c3
J2 = (j-1)*Imax + I-1
A(J2,I2) = C3

r2 = r(i+1)
temp3 = (r2**2 - r3**2 + 2*r1*(r2-r3))/4
z3 = z(j+1)
z2 = (z3 + z1)/2
t1 = (t(i,j+1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z3-z1)*temp3
c1 = c1 + c3
J2 = j*Imax + I
A(J2,I2) = C3

z3 = z(j-1)
z2 = (z3 + z1)/2
t1 = (t(i,j-1) + t(i,j))/2
c3 = kcond(i,r1,t1)/(z1-z3)*temp3
c1 = c1 + c3
J2 = (j-2)*Imax + I
A(J2,I2) = C3

rho1 = rho(i,r1)
cp1 = ccp(i,r1,t1)
c4 = rho1 * cp1 * deltaz * temp3/dt
c1 = c1 + c4
A(N+1,I2) = - gtran(r1,z1,prob,tau,tnow)*deltaz * temp3
- c4 * t(i,j)
a
    A(i2,i2) = - c1
2000 continue

if ( Isolver .eq. 1 ) then
    Call Gauss
else
    Call SGauss
end if

do j=1, jmax
do i=1, imax
    I2 = (j-1)*Imax + I
    if ( prob .eq. 1 ) then
        T(I,j) = (T(I,J)+X(I2))/2.0
    else
        T(I,j) = X(I2)
    end if
end do
end do
do i=1,N
    X(i) = 0.0d0
    do j=1,N
        A(i,j) = 0.0d0
    end do
    A(N+1,i) = 0.0d0
end do

end do

return
end

double precision function gtran(r,z,prob,tau,tnow)
parameter ( eps = 1.1d-16 )
double precision r, z, g, tau, tnow, beta, period, dollar, de
integer prob
common /prompt/ beta, period, dollar

if ( tau .le. 1.1d-16 ) then
    de = 0.0d0
else
    de = dexp(-tnow/tau)
end if

c
c ... if startup problem, increase the heat generation exponentially
if ( prob .eq. 1 ) then
    gtran = g(r,z) * ( 1.0d0 - de )

```



```

c
c ... if shutdown problem, decrease the heat generation to zero
elseif ( prob .eq. 2 ) then
  if ( tau .ne. 0.0d0 ) then
    * ... exponential shutdown
    gtran = g(r,z) * de
  *
  else
    ... prompt jump shutdown
    if ( tnow .gt. 0.0d0 ) then
      gtran = g(r,z) * (1.0-dollar*beta)/(1.0-dollar)
      * dexp(- tnow/period)
    else
      gtran = g(r,z)
    end if
  end if
else
  gtran = g(r,z)
end if
return
end

double precision function ThPower(prob,tau,tnow,powerTh)
parameter ( eps = 1.1d-16 )
double precision tau, tnow, beta, period, dollar, powerTh, de
integer prob
common /prompt/ beta, period, dollar

if ( tau .le. 1.1d-16 ) then
  de = 0.0d0
else
  de = dexp(-tnow/tau)
end if

c
c ... if startup problem, increase the thermal power exponentially
if ( prob .eq. 1 ) then
  Thpower = powerTh * ( 1.0d0 - de )
c
c ... if shutdown problem, decrease the thermal power to zero
elseif ( prob .eq. 2 ) then
  if ( tau .ne. 0.0d0 ) then
    * ... exponential shutdown
    Thpower = powerTh * de
  *
  else
    ... prompt jump shutdown
    if ( tnow .gt. 0.0d0 ) then
      Thpower = powerTh * (1.0-dollar*beta)/(1.0-dollar)
      * dexp(- tnow/period)
    else
      Thpower = powerTh
    end if
  end if
else
  Thpower = powerTh
end if
return
end

integer function iprint(tnow,tprint,dt,time,tstart)
double precision tnow, tprint, dt, time, tol, tstart, dmin1
double precision a, b

iprint = 0
if (tnow .eq. tstart .or. tnow .eq. time) then
  iprint = 1
  return
end if
tol = dmin1(dt,1.0d-5)
a = dmod(tnow,tprint)
b = tnow/tprint
if(a .le. tol .and. idint(b) .ge. 1) then
  iprint = 1
  return
end if

end

double precision function minv(v)
parameter ( jmax = 10 )
double precision v(jmax)

minv = v(1)
do j=2,jmax
  minv = dmin1(minv,v(j))
end do

```

```

return
end
subroutine input(prob,options,time,tprint,ffun,dt,
*          Tstop,Tstart,tcoolant,powerTh,
*          A, B, tau,ipout,Isolver)

integer numofmats, j
parameter (numofmats = 8, imax = 10, jmax = 10)
double precision tinlet, mdot, w, tr, itop, ibottom, powerth
double precision pwrtabl(2,100),ir(10),or(10),ems,phi0(numofmats)
double precision zmin,zmax,l,phie,z,g,trl,pcs,rbound(10),pi,Tstop
double precision de, gl, d2, dl, fuelvol, q3ave, totmesh, paratio
integer rmesh(9),mat(5),k2
integer prob, options, ipout,Isolver
double precision time, tprint, ffun(imax,jmax),dt,Tstart
double precision beta, period, dollar, Tcoolant(jmax)
double precision tau, A, B, rperiod
integer tabflag, matnum(9), meshpt(9), i, tablen
character*80 title
character*21 regname(10)
character*5 matname(numofmats)
logical deckerror
common /input/ tr, ems, phie, itop, ibottom, title
common /rdata/ rbound,rmesh,mat
common /zdata/ zmin,zmax,k2
common /powerdata/ q3ave, pwrtabl, tabflag
Common /ggdot/ ir, or
common /prompt/ beta, period, dollar
common /coolprop/ tinlet, de, gl, w, d2, dl, mdot
data matname/'uo2 ','w ','nb ','nbizr','mo ','re ','
a          'cs ','al2o3'/
data phi0/0.0d0,4.9d0,6*0.0d0/
data regname/'fuel          ','fuel-emitter gap          ',
a          'emitter          ','emitter-collector gap          ',
a          'collector          ','collector-insulator gap          ',
c          'insulator          ','insulator-cladding gap          ',
b          'cladding          ','coolant channel          '/
data pi/3.1415926d0/

open (7, file='tfetc.inp', status='old')
open (8, file='tfetc.out')

deckerror=.false.
Read (7,10) Title
Read (7,*) Prob
if (Prob .lt. 1 .or. Prob .gt. 4 .or. mod(Prob,1) .ne. 0) then
Write(8,9010) 'Invalid problem specification.'
Write(8,9120) 'Prob',1,2,3,4
DeckError = .True.
end if
Read (7,*) Isolver
if (Isolver .ne. 1 .and. Isolver .ne. 2) then
Write(8,9010) 'Invalid Isolver specification.'
Write(8,9020) 'Isolver',1,2
DeckError = .True.
end if
if (Prob .ne. 4) then
Read (7,*) Options
if (Options .ne. 1 .and. Options .ne. 2) then
Write(8,9010) 'Invalid Options specification.'
Write(8,9020) 'Options',1,2
DeckError = .True.
end if
Read (7,*) Time
Read (7,*) Tprint
Read (7,*) dt
Read (7,*) ipout
if (dt .gt. Tprint .or. Tprint .gt. Time
* .or. Time .le. 0.0 .or. dt .gt. 1.0d0) then
Write(8,9010) ' Invalid Timing Specification.'
Write(8,9290) 'DT',Tprint,1.0d0,'Tprint',Time,'Time',0.0d0
DeckError = .True.
end if
if ( ipout .ne. 0 .and. ipout .ne. 1 ) then
Write(8,9010) ' Invalid Print Option.'
Write(8,9020) 'IPOINT',0,1
DeckError = .True.
end if
end if
if ( prob .eq. 3 ) then
Read(7,*) A, B, tau
if (A .lt. 0.0d0 .or. B .le. 0.0d0 .or. A+B .ne. 1.0d0) then
Write(8,9010) ' Invalid mass-loss coefficients '
Write(8,9280) ' A ',0.0d0,' B ',0.0d0,' A+B ',1.0d0
DeckError = .True.
end if

```



```

else
  Write(8,9010) 'Invalid output current at the bottom of the',
  a   ' pin.'
  Write(8,9040) 'Ibottom', 0.0D0
  DeckError=.True.
end if
if (PowerTh.GE.0.0D0) then
  Write(8,710) PowerTh
else
  PowerTh = -PowerTh*(Zmax-Zmin)*Pi*(OR(1)**2-IR(1)**2)
  Write(8,710) PowerTh
end if
FuelVol = Pi*(OR(1)**2.0D0-IR(1)**2.0D0)*(Zmax-Zmin)
Q3ave = PowerTh/FuelVol
Write(8,720) Q3ave
if (TabFlag.EQ 1) then
  Write(8,810)
  Do 9 I=1, TabLen
9    Write(8,820) PwrTabl(1,I), PwrTabl(2,I)
  else
    Write(8,830) PwrTabl(1,1), PwrTabl(2,1)
    PARatio = (PwrTabl(1,1)+PwrTabl(2,1))/(PwrTabl(1,1) +
  a    2.0D0*PwrTabl(2,1)/Pi)
    PwrTabl(1,1) = PwrTabl(1,1)/PARatio
    PwrTabl(2,1) = PwrTabl(2,1)/PARatio
    Write(8,835) PARatio
  end if
  Write(8,100)
  Write(8,10) Title
  Write(8,910)
  TotMesh = 1
  Do 70 I=1,9
    if (MatNum(I).NE.0) then
      Write(8,920) RegName(I), IR(I), OR(I),
  a    MatName(MatNum(I)), MeshPt(I)
    end if
    if (IR(I).GT.OR(I)) then
      Write(8,9010) 'Invalid geometry data.'
      Write(8,9060) RegName(I)
      DeckError = .True.
    end if
    if (I.GT.1) then
      if (IR(I).NE.OR(I-1)) then
        Write(8,9010) 'Invalid geometry data.'
        Write(8,9070) RegName(I), RegName(I-1)
        DeckError = .True.
      end if
    end if
    if (I.EQ.3) then
      PhiE = Phi0(MatNum(I))
      if (PhiE.EQ.0.0D0) then
        Write(8,9010) 'Invalid emitter material specification'
        Write(8,9080) MatName(MatNum(I))
        DeckError = .True.
      end if
    end if
    if (IR(I).NE.OR(I)) MeshPt(I) = MeshPt(I) + 1
    TotMesh = TotMesh + MeshPt(I)
70  Continue
  if (TotMesh.NE.Imax) then
    Write(8,9010) 'Invalid mesh point specification.'
    Write(8,9090) Imax
    DeckError = .True.
  end if
  Write(8,930) RegName(10), IR(10), OR(10)
  Write(8,1110) Zmin, Zmax, Zmax-Zmin, L
  if (ABS(Zmax-Zmin).GT.L) then
    Write(8,9010) 'Invalid geometry data.'
    Write(8,9100)
    DeckError = .True.
  end if
  if ((Zmax-Zmin).LE.0.0D0) then
    Write(8,9010) 'Invalid geometry data.'
    Write(8,9105)
    DeckError = .True.
  end if

  if (Prob .lt. 4 .and. Options .eq. 2) then
    Write(8,9010) 'Forcing Function: Temperature Distribution for
  c the Transient Case'
    Do 11 j=1, Jmax
      Write(8,80) (Ffun(i,j), i=1,Imax)
11  Continue
  end if
end if
c ... write initial coolant temperature profile

```

KHEL 4/11/93
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 KHEL 4/11/93
 KHEL 4/11/93
 KHEL 4/11/93

KHEL 7/5/93

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if ( (prob .eq. 2 .or. prob .eq. 3) .and. options .eq. 2 ) then KHEL 7/5/93
  Write(8,9010) ' Initial coolant temperature profile ' KHEL 7/5/93
  Write(8,80) (Tcoolant(j), j=1, jmax) KHEL 7/5/93
end if

if (DeckError) then
  Write(8,9110)
  Stop
end if

10 Format (A80)
20 Format (7F10.0)
30 Format (I2)
40 Format (2F10.0)
50 Format (2F10.0,2I5)
55 Format (2F10.0)
60 Format (4F10.0)
80 format (10F10.0)

100 Format ('1',20(' '), ' TFEFC ',20(' ')/
a ' ***** INPUT DATA SUMMARY FOR THE FOLLOWING CASE:')
110 Format (/)
120 Format (' COOLANT TYPE: Molten Sodium-Potassium Alloy (NaK)',/
a ' 15X,'Potassium composition =',I3,'%')
130 Format (' COOLANT TYPE Molten Potassium')
140 Format (' COOLANT TYPE Molten Sodium')
210 Format (' COOLANT MASS FLOW RATE:',F7.2,' kilograms per second.')
310 Format (' TEMPERATURE OF COOLANT AT CHANNEL INLET:',F7.1,' K.')
410 Format (' TEMPERATURE OF CESIUM RESERVOIR:',F7.1,' K.')
420 Format (' PRESSURE OF CESIUM VAPOR:',F7.1,' Torr.')
510 Format (' OUTPUT CURRENT FROM THE TOP OF THE TFE: ',F7.1,
a ' Amperes ')
610 Format (' OUTPUT CURRENT FROM THE BOTTOM OF THE TFE:',F7.1,
a ' Amperes ')
710 Format (' TOTAL THERMAL POWER PRODUCED IN THE TFE FUEL:',F7.1,
a ' Watts ')
720 Format (' AVERAGE VOLUMETRIC HEAT GENERATION RATE FOR THE TFE',
a ' FUEL:',F7.1,' Watts.')
810 Format ('// AXIAL POWER PROFILE TABLE -----')
a '//5X,'R is the ratio of the volumetric heat generation rate'/
b 8X,'at point Z to the average volumetric heat generation'/
c 8X,'rate for the TFE fuel.'//
d 8X,'Z is measured from the ends of the emitter and collector'
e 8X,'leads at the end of the TFE where the coolant enters.'//
g 6X,'Z (cm)',8X,'R/2(5X,8('-'))')
820 Format (6X,F5.1,7X,F6.3)
830 Format (' CORRELATION FOR THE RATIO OF THE HEAT GENERATION RATE'/
a 10X,' AT POSITION Z TO THE AVERAGE HEAT GENERATION RATE IN '/
b 10X,' THE TFE FUEL:'//10X,' F = ',F10.4,'+',F10.4,
c ' * SIN((Z-Zmin)/(Zmax-Zmin)*3.14159)')
835 Format (' AXIAL PEAK-TO-AVERAGE RATIO FOR HEAT GENERATION IS:',
a F7.4/)
910 Format (' ***** GEOMETRY DATA EDIT *****')
a ' ***** RADIAL GEOMETRY *****')
a 30X,'Inside',9X,'Outside',17X,'Number of'/
b 9X,'Region',15X,'Radius',9X,'Radius',6X,'Material',5X,
c 'Interior',31X,'(cm)',11X,'(cm)',18X,'Mesh Points',1X,
d 23('-'),4X,10('-'),5X,10('-'),4X,8('-'),3X,11('-')
920 Format (A23,4X,F10.6,5X,F10.6,8X,A5,5X,I3)
930 Format (A23,4X,F10.6,5X,F10.6)
1010 Format ('// EFFECTIVE EMISSIVITY FOR RADIANT HEAT TRANSFER FROM'/
a 10X,' THE EMITTER SURFACE TO THE COLLECTOR SURFACE:',F10.6)
1110 Format (' ***** AXIAL GEOMETRY *****')
a ' AXIAL POSITION OF THE UPPER LIMIT FOR'/10X'THE FUELED'
b ' REGION OF THE TFE:',F10.6,' (cm)'/ ' AXIAL POSITION OF'
c ' THE LOWER LIMIT FOR'/10X'THE FUELED REGION OF THE TFE:'
d F10.6,' (cm)'/ ' AXIAL EXTENT OF THE FUELED REGION OF THE'
e ' TFE:',F10.6,' (cm)'/ ' TOTAL LENGTH OF THE TFE,'
f ' INCLUDING ELECTRODE LEADS ',F10.6,' (cm)')

9010 Format (' ***** ',A66,' ***** ')
9020 Format (10X,A23,' must be either',I2,' or',I2,'.')
9030 Format (10X,A23,' should be between',F5.2,' and',F5.2,
a ', inclusive.')
9040 Format (10X,A23,' should be greater than',F5.2,'.')
9050 Format (10X,A23,' should be greater than or equal to',F5.2,'.')
9060 Format (10X,'The inside radius for the ',A23,' region must be',
a ' less',10X,' than the outside radius.')
9070 Format (10X,'The inside radius for the ',A23,' region must be',
a ' equal'/10X,' to the outside radius of the ',A23,' region.')
9080 Format (10X,'No bare work function data is available for the '
a 'material'/10X,A23,'. Please add the necessary data to the '
b 'Phi0 DATA'/10X,' statement in the Input subroutine.')
9090 Format (10X,'There must be a total of',I3,' interior and'
a ' interfacial mesh points.')
9100 Format (10X,'L should be greater than or equal to Zmax - Zmin.')

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9105 Format (10X,'Zmax should be greater than Emin.')
9110 Format (//' ***** EXECUTION HALTED DUE TO ERRORS IN THE',
      & ' INPUT DECK *****//')
9120 Format (10X,A23,' must be one of ',I2,1X,I2,1X,I2,1X,I2,1X) KHEL 4/11/93
9130 Format (10X,'Tstop = ',F7.2,' must be less than Tstart = ',F7.2) KHEL 6/26/93
9140 Format (10X,' Print Time Step, TPRINT = ',F7.2,' Secs.') KHEL 6/26/93
9150 Format (10X,' Time Step Increment, delta t = ',F10.4,' Secs.') KHEL 6/26/93
9160 Format (10X,' Stop helium heating at the emitter temperature, Tst
      & 'op = ',F7.2,') KHEL 6/26/93
9170 Format (10X,' Start Electron cooling at the emitter temperature,
      & 'Tstart = ',F7.2,') KHEL 6/26/93
9180 Format (10X,' Simulation Period, TIME = ',F7.2,' Secs.') KHEL 6/26/93
9190 Format (10X,' Power-rise coefficient, tau = ',D9.3,','/,10X,
      & ' P(t) = P(0) * [ 1 - Exp ( - t / tau ) ] ',') KHEL 7/6/93
*9200 Format (10X,' Power-loss coefficient, PLOSS = ',F7.4,') KHEL 6/26/93
9210 Format (10X,' Mass-loss coefficients, A = ',F7.4,','/, B = ',F7.4,
      & 'tau = ',D9.3,','/,10X, ' Mdot(t) = Mdot(0) * [ ' KHEL 7/6/93
      & ' A + B * Exp(- t / tau ) ] ' ) KHEL 7/6/93
9220 Format (10X,A23,' should be less than ',F5.2,') KHEL 6/26/93
9230 Format (10X,' Total delayed neutron fraction, BETA = ',F9.5,') KHEL 6/26/93
9240 Format (10X,' Negative Reactivity insertion in $, dollar = ',F7.2,
      & ' ') KHEL 6/26/93
9250 Format (10X,' Reactor period, T = ',F7.2,' Secs.',/,10X,
      & ' P(t) = P(0) [(1 - BETA * RHO)/(1 - RHO)] * Exp(- t / Period) ') KHEL 7/7/93
9260 Format (' ***** ',A20, ' ***** ') KHEL 6/26/93
9280 Format (10X,A5,' should be greater than or equal to',F7.2,','/,
      & ',A5,' should be greater than',F7.2,','/,
      & ',A5,' should be equal to',F7.2,') KHEL 7/7/93
9290 Format (10X,A6,' should be less than or equal to',F7.2,','/,F7.2,
      & ',A6,' should be less than or equal to',F7.2,','/,
      & ',A6,' should be greater than',F7.2,') KHEL 7/7/93
9300 Format (10X,' Print Option, ipout = ',I1,') KHEL 7/7/93
9310 Format (10X,' Linear Equations solved using Gaussian elimination') KHEL 7/19/93
9320 Format (10X,' Linear Equations solved using Y12M Sparse solver') KHEL 7/19/93
      D1 = 2.0D0*IR(10)
      D2 = 2.0D0*OR(10)
      Ds = D2-D1
      G1 = Mdot/(OR(10)**2.0D0-IR(10)**2.0D0)/P1
      Do 2010 I = 1,10
2010      Rbound(I) = IR(I)
      Do 2020 I=1,9
2020      Rmesh(I) = MeshPt(I)
      Do 2030 I=1,9,2
2030      Mat(INT((I+1)/2)) = MatNum(I)

Return
end

double precision function rperiod(dollar)
implicit double precision (a-h,o-z)
double precision dollar, result, period(14), rho(14), x
data period /700.0, 400.0, 280.0, 200.0, 180.0, 125.0, 93.0,
& 90.0, 80.0, 80.0, 80.0, 80.0, 80.0, 80.0 /
data rho / 0.02, 0.04, 0.06, 0.08, 0.10, 0.20, 0.40,
& 0.60, 1.00, 10.0, 100.0, 200.0, 300.0, 600.0 /

x = - dollar
call intrpl(8,14,rho,period,1,x,result)
rperiod = result

return
end
double precision Function ccp(I,R2,T)
*** Units = J/Kg.K ***

Integer I,Rmesh(9),M(5)
double precision R, Rbound(10), Temp, R2
double precision T, ccpl
Common /Rdata/ Rbound,Rmesh,M

if (R2.LT.Rbound(1)) then
*   *** Void ( assumed to be air )
      Temp = 1.00488d3
      Goto 100
endif
if (R2.EQ.Rbound(1)) then
*   *** Void/Pellet boundary
      Temp = (1.00488d3 + ccpl(T,M(1)))/2
      Goto 100
endif
if ((R2.GT.Rbound(1)).AND.(R2.LT.Rbound(2))) then
*   Temp = ccpl(T,M(1))
*   *** Fuel pellet
      Goto 100
endif
if (R2.EQ.Rbound(2)) then

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```

*
*      *** Fuel Pellet outer surface
*** Does a gap exist between the fuel and the emitter? ***
if (Rbound(2).NE.Rbound(3)) then
*
*      *** Gap
a      Temp = (1.00488d3*(R(I+1)-R(I)) +
b      ccpl(T,M(1))*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
*
*      else
*      *** No Gap
a      Temp = (ccpl(T,M(2))*(R(I+1)-R(I)) +
b      ccpl(T,M(1))*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
*
*      endif
*      Goto 100
endif
if ((R2.EQ.Rbound(3)).AND.(R2.GT.Rbound(2))
*      .AND.(R2.LT.Rbound(3))) then
*
*      *** Gap
a      Temp = 1.00488d3
*      Goto 100
endif
if ((R2.EQ.Rbound(3)).AND.(Rbound(2).NE.Rbound(3))) then
*
*      Temp = (ccpl(T,M(2))*(R(I+1)-R(I)) + 1.00488d3*(R(I)-R(I-1)))
a      / (R(I+1)-R(I-1))
*
*      *** Emitter inner surface
*      Goto 100
endif
if ((R2.GT.Rbound(3)).AND.(R2.LT.Rbound(4))) then
*
*      Temp = ccpl(T,M(2))
*      *** Emitter
*      Goto 100
endif
if (R2.EQ.Rbound(4)) then
*
*      *** Emitter outer surface (Cs vapor used in gap)
a      Temp = (1.9D-3*(R(I+1)-R(I)) + ccpl(T,M(2))*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
*
*      Goto 100
endif
if ((R2.GT.Rbound(4)).AND.(R2.LT.Rbound(5))) then
*
*      *** Gap (Cesium vapor)
a      Temp = 1.9D-3
*      Goto 100
endif
if (R2.EQ.Rbound(5)) then
*
*      *** Collector inner surface
a      Temp = (ccpl(T,M(3))*(R(I+1)-R(I)) + 1.9D-3*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
*
*      Goto 100
endif
if ((R2.GT.Rbound(5)).AND.(R2.LT.Rbound(6))) then
*
*      *** Collector
a      Temp = ccpl(T,M(3))
*      Goto 100
endif
if (R2.EQ.Rbound(6)) then
*
*      *** Collector outer surface
*** Does a gap exist between the collector and the insulator? ***
if (Rbound(6).NE.Rbound(7)) then
*
*      *** Gap
a      Temp = (1.00488d3*(R(I+1)-R(I)) +
b      ccpl(T,M(3))*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
*
*      else
*      *** No Gap
a      Temp = (ccpl(T,M(4))*(R(I+1)-R(I)) +
b      ccpl(T,M(3))*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
*
*      endif
*      Goto 100
endif
if ((Rbound(6).NE.Rbound(7)).AND.(R2.GT.Rbound(6))
*      .AND.(R2.LT.Rbound(7))) then
*
*      *** Gap
a      Temp = 1.00488d3
*      Goto 100
endif
if ((R2.EQ.Rbound(7)).AND.(Rbound(6).NE.Rbound(7))) then
*
*      *** Insulator inner surface
a      Temp = (ccpl(T,M(4))*(R(I+1)-R(I)) + 1.0D-2*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
*
*      Goto 100
endif
if ((R2.GT.Rbound(7)).AND.(R2.LT.Rbound(8))) then
*
*      *** Insulator
a      Temp = ccpl(T,M(4))
*      Goto 100
endif

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```

endif
if (R2.EQ.Rbound(8)) then
*
*** Insulator outer surface
*** Does a gap exist between the insulator and the clad? ***
if (Rbound(8).NE.Rbound(9)) then
*
*** Gap
a      Temp = (1.00488d3*(R(I+1)-R(I)) +
a      ccpl(T,M(4))*(R(I)-R(I-1)))
a      / (R(I+1)-R(I-1))
*
else
*** No Gap
a      Temp = (ccpl(T,M(5))*(R(I+1)-R(I)) +
a      ccpl(T,M(4))*(R(I)-R(I-1)))
a      / (R(I+1)-R(I-1))
endif
Goto 100
endif
if ((Rbound(8).NE.Rbound(9)).AND.((R2.GT.Rbound(8))
a      .AND.(R2.LT.Rbound(9)))) then
*
*** Gap
Temp = 1.00488d3
Goto 100
endif
if ((R2.EQ.Rbound(9)).AND.(Rbound(8).NE.Rbound(9))) then
*
*** Clad inner surface
a      Temp = (ccpl(T,M(5))*(R(I+1)-R(I)) + 1.00488d3*(R(I)-R(I-1)))
a      / (R(I+1)-R(I-1))
Goto 100
endif
if ((R2.GT.Rbound(9)).AND.(R2.LT.Rbound(10))) then
*
*** Clad
Temp = ccpl(T,M(5))
Goto 100
endif
if (R2.EQ.Rbound(10)) then
*
*** Clad outer surface
*
Temp = ccpl(T,M(5))
Goto 100
endif
100 ccp = Temp

return
end

*** double precision Function ccpl(T,M1)
Units = J/Kg.K ***

Integer M1
double precision Cpdata(8), MOcp(11), MOTm(11), Recp(10)
double precision Retm(10), Alcp(7), Altm(7), wcp, ncp
double precision k1, k2, k3, theta, ed, y, Rc, fcp, T1
double precision T

*
*      Material #1 = UO2          Specific Heat J/Kg.K
*      Material #2 = W            0.23d3
*      Material #3 = Nb          1.33984d2
*      Material #4 = Nb12r       2.72155d2
*      Material #5 = Mo          2.55407d2
*      Material #6 = Re          1.38171d2
*      Material #7 = Cs          2.17724d2
*      Material #8 = Al2O3       8.374d2
*

Data Cpdata/
1      2.3d2      , 1.33984d2, 2.72155d2,
2      0          , 2.55407d2, 1.38171d2,
3      2.17724d2, 8.374d2/

Data k1, k2, k3/296.7, 2.43d-2, 8.745d7/

Data theta,ed, Rc,y/535.285, 1.577d5, 8.3143, 2.0/

Data MOcp/141.0, 224.0, 251.0, 261.0, 275.0, 285.0, 295.0,
&      308.0, 330.0, 380.0, 459.0/

Data MOTm/100.0, 200.0, 300.0, 400.0, 600.0, 800.0, 1000.0,
&      1200.0, 1500.0, 2000.0, 2500.0/

Data Recp/97.0, 127.0, 136.0, 139.0, 145.0, 151.0, 156.0, 162.0,
&      171.0, 186.0/

Data Retm/100.0, 200.0, 300.0, 400.0, 600.0, 800.0, 1000.0,
&      1200.0, 1500.0, 2000.0/

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Data Alcp/778.782, 929.514, 1025.815, 1109.555, 1172.36,
4 1256.100, 1306.344/

Data Altm/293.15, 373.15, 473.15, 573.15, 773.15,
4 1173.15, 1973.15/

fcp(T1) = k1 * theta * theta * dexp(theta/T1) /
4 ( T1*T1 * ( dexp(theta/T1) - 1.0 )**2.0 ) + k2 * T1 +
4 ( y * k3 * ed / (2.0 * Rc + T1 * T1) ) * dexp(-ed/Rc/T1)

wcp(T1) = 135.76 * (1.0d0 - 4805.0d0/T1/T1) + 9.1159d-3 * T1 +
4 2.3134d-9 * (T1**3.0)

ncp(T1) = ( 6.43d-2 + 0.772766d-5 * T1 + 0.234774d-8 * T1 * T1 )
4 * 4187.0d0

*
if ( M1 .eq. 1 ) then
* ... UO2
  ccpl = fcp(T)
  return
*
else if ( M1 .eq. 2 ) then
* ... W
  ccpl = wcp(T)
  return
*
else if ( M1 .eq. 3 ) then
* ... Nb
  ccpl = ncp(T)
  return
*
else if ( M1 .eq. 4 ) then
* ... Nb1Zr
  ccpl = Cpdata(4)
  return
*
else if ( M1 .eq. 5 ) then
* ... Mo
  call intrpl(8,11,Motm,Mocp,1,T,ccpl)
  return
*
else if ( M1 .eq. 6 ) then
* ... Re
  call intrpl(8,10,Retm,Recp,1,T,ccpl)
  return
*
else if ( M1 .eq. 7 ) then
* ... Cs
  ccpl = Cpdata(7)
  return
*
else if ( M1 .eq. 8 ) then
* ... Al2O3
  call intrpl(8,7,Altm,Alcp,1,T,ccpl)
*
else
100 write(8,100) 'Invalid material'
  format(10x,'****',a22,'****')
  stop
end if

return
end
*** double precision Function rho(I,R2)
  Units = Kg/cm^3 ***

Integer I,Rmesh(9),M(5)
double precision R, Rbound(10), Temp, R2, Rhdata(8)
Common /Rdata/ Rbound,Rmesh,M

*
* Material #1 = UO2 Density Kg/cm^3
* Material #2 = W 1.098d-2
* Material #3 = Nb 19.3d-3
* Material #4 = Nb1Zr 8.57d-3
* Material #5 = Mo 10.2d-3
* Material #6 = Re 20.d-3
* Material #7 = Cs 1.9d-3
* Material #8 = Al2O3 3.6264d-3
*

Data Rhdata/1.098d-2, 19.3d-3 , 8.57d-3,
2 0.d0 , 10.2d-3 , 20.0d-3,
3 1.9d-3 , 3.6264d-3/

*
if (R2.LT.Rbound(1)) then
* *** Void ( assumed to be air )
  Temp = 1.293d-6
  Goto 100
endif
*
if (R2.EQ.Rbound(1)) then
* *** Void/Pellet boundary
  Temp = (1.293d-6 + Rhdata(M(1)))/2
  Goto 100
endif

```

```

if ((R2.GT.Rbound(1)).AND.(R2.LT.Rbound(2))) then
  Temp = Rhdata(M(1))
  *** Fuel pellet
  Goto 100
endif
if (R2.EQ.Rbound(2)) then
  *** Fuel Pellet outer surface
  *** Does a gap exist between the fuel and the emitter? ***
  if (Rbound(2).NE.Rbound(3)) then
    *** Gap
    a
    b
    Temp = (1.293D-6*(R(I+1)-R(I)) +
            Rhdata(M(1))*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
    else
    *** No Gap
    a
    b
    Temp = (Rhdata(M(2))*(R(I+1)-R(I)) +
            Rhdata(M(1))*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
    endif
    Goto 100
  endif
  if ((Rbound(2).NE.Rbound(3)).AND.((R2.GT.Rbound(2))
  a
  .AND.(R2.LT.Rbound(3)))) then
    *** Gap
    Temp = 1.293d-6
    Goto 100
  endif
  if ((R2.EQ.Rbound(3)).AND.(Rbound(2).NE.Rbound(3))) then
    a
    Temp = (Rhdata(M(2))*(R(I+1)-R(I)) + 1.293D-6*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
    *** Emitter inner surface
    Goto 100
  endif
  if ((R2.GT.Rbound(3)).AND.(R2.LT.Rbound(4))) then
    Temp = Rhdata(M(2))
    *** Emitter
    Goto 100
  endif
  if (R2.EQ.Rbound(4)) then
    *** Emitter outer surface (Cs vapor used in gap)
    a
    Temp = (1.9D-3*(R(I+1)-R(I)) + Rhdata(M(2))*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
    Goto 100
  endif
  if ((R2.GT.Rbound(4)).AND.(R2.LT.Rbound(5))) then
    *** Gap (Cesium vapor)
    Temp = 1.9D-3
    Goto 100
  endif
  if (R2.EQ.Rbound(5)) then
    *** Collector inner surface
    a
    Temp = (Rhdata(M(3))*(R(I+1)-R(I)) + 1.9D-3*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
    Goto 100
  endif
  if ((R2.GT.Rbound(5)).AND.(R2.LT.Rbound(6))) then
    *** Collector
    Temp = Rhdata(M(3))
    Goto 100
  endif
  if (R2.EQ.Rbound(6)) then
    *** Collector outer surface
    *** Does a gap exist between the collector and the insulator? ***
    if (Rbound(6).NE.Rbound(7)) then
    *** Gap
    a
    a
    Temp = (1.293d-6*(R(I+1)-R(I)) +
            Rhdata(M(3))*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
    else
    *** No Gap
    a
    a
    a
    Temp = (Rhdata(M(4))*(R(I+1)-R(I)) +
            Rhdata(M(3))*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))
    endif
    Goto 100
  endif
  if ((Rbound(6).NE.Rbound(7)).AND.((R2.GT.Rbound(6))
  a
  .AND.(R2.LT.Rbound(7)))) then
    *** Gap
    Temp = 1.293D-6
    Goto 100
  endif
  if ((R2.EQ.Rbound(7)).AND.(Rbound(6).NE.Rbound(7))) then
    *** Insulator inner surface
    a
    Temp = (Rhdata(M(4))*(R(I+1)-R(I)) + 1.0D-2*(R(I)-R(I-1)))
          / (R(I+1)-R(I-1))

```

```

        Goto 100
    endif
    if ((R2.GT.Rbound(7)).AND.(R2.LT.Rbound(8))) then
*       *** Insulator
        Temp = Rhdata(M(4))
        Goto 100
    endif
    if (R2.EQ.Rbound(8)) then
*       *** Insulator outer surface
***     Does a gap exist between the insulator and the clad? ***
        if (Rbound(8).NE.Rbound(9)) then
*           *** Gap
            Temp = (1.293D-6*(R(I+1)-R(I)) +
a             Rhdata(M(4))*(R(I)-R(I-1)))
a             / (R(I+1)-R(I-1))
*           else
***     No Gap
            Temp = (Rhdata(M(5))*(R(I+1)-R(I)) +
a             Rhdata(M(4))*(R(I)-R(I-1)))
a             / (R(I+1)-R(I-1))
            endif
            Goto 100
        endif
        if ((Rbound(8).NE.Rbound(9)).AND.((R2.GT.Rbound(8))
a         .AND.(R2.LT.Rbound(9)))) then
*           *** Gap
            Temp = 1.293D-6
            Goto 100
        endif
        if ((R2.EQ.Rbound(9)).AND.(Rbound(8).NE.Rbound(9))) then
*           *** Clad inner surface
            Temp = (Rhdata(M(5))*(R(I+1)-R(I)) + 1.293D-6*(R(I)-R(I-1)))
a             / (R(I+1)-R(I-1))
            Goto 100
        endif
        if ((R2.GT.Rbound(9)).AND.(R2.LT.Rbound(10))) then
*           *** Clad
            Temp = Rhdata(M(5))
            Goto 100
        endif
        if (R2.EQ.Rbound(10)) then
*           *** Clad outer surface
*           *** Clad
            Temp = Rhdata(M(5))
            Goto 100
        endif
    endif
100 rho = Temp

    end
    subroutine output(time,imax,jmax, v, qec, jdens, emheat,
1      tcoolant, colheat, qch, grad, qcscond,
2      t, current, prob, ThPower, ipout)
    implicit double precision (a-h,o-z)
*****
*
*       Write the results to the file tfeh.x.out
*
*****

    double precision tr, itop, ibottom, tcoolant(jmax)
    double precision ems, phie, v(jmax), z, qec(jmax), jdens(jmax)
    double precision emheat(jmax), colheat(jmax), qch(jmax), current
    double precision grad(jmax), qcscond(jmax), time, t(imax,jmax)
    double precision Tinlet, De, Gl, W, Dout, Din, mdot, ThPower
    integer i, j, prob, ipout
    character*80 title
    common /input/ tr, ems, phie, itop, ibottom, title
    common /coolprop/ tinlet, de, gl, w, dout, din, mdot

    write(8,1300)
    write(8,1400) title
    write(8,1500) time
    if ( ipout .eq. 1 ) then
        write(8,1600)
    endif
c
c... output temp. distribution for fuel
    do i=1,imax
        do j=1,jmax
            write(8,200) i,j, t(i,j)
        end do
    end do
200  format (' t(',i3,',',i3,') = ',f13.7)
    do j=1,jmax
        write(8,1900) j,tcoolant(j)
    end do

```

```

end if
write(8,1700) tcoolant(jmax)
if ( prob .eq. 3 ) then
  write(8,1800) mdot
end if
write(8,300) v(1),v(jmax)
write(8,400) current, v(1)*ibottom+v(jmax)*itop
300 format(' Voltage across bottom of cell: ',F13.7/
a      ' Voltage across top of cell: ',F13.7)
400 format('/8X,'Z',19X,'V',18X,'Qec',16X,'Jdens'/X,3(15('-'),5X),
a      F13.7)
  write(8,450) ThPower
450 format(' Total Thermal power = ',F13.7)
  write(8,500)
500 format('/8X,'Z',19X,'V',18X,'Qec',16X,'Jdens'/X,3(15('-'),5X),
A      15('-')/)
  do 600 j=1,jmax
    write(8,700) Z(j), V(j), Qec(j), Jdens(j)
600 continue
700 format(X,3(F15.8,5X),F15.8)
  write(8,800)
800 format('/8X,'Z',17X,'EmHeat',13X,'ColHeat'/X,2(15('-'),5X),
A      15('-')/)
  do 900 j=1,jmax
    write(8,1000) z(j), emheat(j), colheat(j)
900 continue
1000 format(X,2(F15.8,5X),F15.8)
  write(8,1100)
1100 format('/8X,'Z',18X,'Qch',16X,'Qrad',15X,'QCsCond'/
A      X,3(15('-'),5X),15('-')/)
  do 1200 j=1,jmax
    write(8,700) Z(j), Qch(j), Qrad(j), QCsCond(j)
1200 continue

1300 format ('1',20('*'), 'TFETC ',20('*')/
a      ' ***** RESULTS FOR THE FOLLOWING CASE:')
1400 format (A80)
1500 format ( ' TIME = ',f15.8,/)
1600 format (' TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---'/)
1700 Format (/ ' Temperature of coolant at core exit: ',F10.3,
a      ' degrees K.')
1800 Format (/ ' Mass flow rate = ', F10.3 )
1900 Format (' tcool(',i3,') = ',f13.7 )

return
end
subroutine helium(v,qec,qch,jdens,emheat,colheat)
parameter ( jmax = 10 )
implicit double precision (a-h,o-z)
double precision v(jmax),qec(jmax)
double precision jdens(jmax),emheat(jmax),colheat(jmax)
double precision qch(jmax)
integer i

do i=1,jmax
  qec(i) = 0.d0
  v(i) = 0.d0
  jdens(i) = 0.d0
  emheat(i) = 0.d0
  colheat(i) = 0.d0
  qch(i) = 0.d0
end do

return
end

double precision Function GapCond(Te,Tc,Tstop,Tstart,Prob,Tr,D)

integer Prob
double precision Te,Tc,Tstop,Tr,Trl,D,Pcs,K,Hcond,Tstart
external Hcond

if ( Prob .eq. 1 .and. Te .le. Tstop ) then
*   ... helium heating phase
  Trl = (Te+Tc)/2.0d0
  K = Hcond(Trl)
  GapCond = K*(Te-Tc)/D
*   if ( GapCond .lt. 0.0d0 ) GapCond = 0.0d0
else
*   K = 5.5D-5
  ... electron-cooling phase
  if ( Te .lt. Tstart ) then
    Trl = Te + Tr/Tstart
  else

```

```

      Tr1 = Tr
    end if
    Pcs = 2.45D+8 + exp(-8910.D0/Tr1)/SQRT(Tr1)
    GapCond = K*(Te-Tc)/(D + 1.15D-5*(Te-Tc)/Pcs)
*   if ( GapCond .lt. 0.0d0 ) GapCond = 0.0d0
  end if

  End

  double precision function HCond(T)
*****
*
*   Calculate the thermal conductivity of helium as a function of
*   temperature T, in Kelvin. Data is taken from "Introduction to
*   Heat Transfer", by F. P. Incropera and D. P. DeWitt,
*   Table A.4 page 683.
*
*   Units are in W/cm.K
*****

  double precision k(22), temp(22), result, T
  data temp / 100.0d0, 120.0d0, 140.0d0, 160.0d0, 180.0d0, 200.0d0,
&           220.0d0, 240.0d0, 260.0d0, 280.0d0, 300.0d0, 350.0d0,
&           400.0d0, 450.0d0, 500.0d0, 600.0d0, 650.0d0, 700.0d0,
&           750.0d0, 800.0d0, 900.0d0,1000.0d0 /
  data k    / 73.0d0, 81.9d0, 90.7d0, 99.2d0, 107.2d0, 115.1d0,
&           123.1d0, 130.0d0, 137.0d0, 145.0d0, 152.0d0, 170.0d0,
&           187.0d0, 204.0d0, 220.0d0, 252.0d0, 264.0d0, 278.0d0,
&           291.0d0, 304.0d0, 330.0d0, 354.0d0 /

  C
  C
  call intrpl(8,22,temp,k,1,T,result)
  HCond = result * 1.0d-5

  return
  end
  Subroutine TConvect(tnow,dt,tfcool)
*****
*
*   Subroutine TConvect
*   -----
*   6/10/1993
*
*   Computes the temperature of the coolant within
*   cylindrical flow channels by solving the transient
*   partial differential equation for temperature rise
*   through the core ( equation 6.8.6 in Elements of
*   Nuclear Reactor Design, J. Weisman ed., Kreiger
*   Publishing Company, 1983, with Cpdt substituted
*   for dh.) An explicit finite difference scheme is
*   solve the partial differential equation.
*   This treatment allows the temperature dependences
*   of the coolant properties to be included in the
*   analysis. The output for this module is the axial
*   temperature profile of the coolant within the
*   flow channel.
*
*
*****

  implicit double precision (a-h,o-z)
  parameter ( N = 500 , jmax = 10 )
*   double precision T, Told, Tinlet, h, z, mdot
  double precision T, Tinlet, h, z, mdot,tfcool(jmax)
  double precision Cp, HeatFlux, Rbound(10), zcool(jmax), hcool
  double precision De, G, W, CoolTbl(2000,2), Zmax, Zmin, D2, D1
  double precision tnow, dt, rhonak, dum1, dum2, dum3, dum4, dum5
  double precision TOLD(N), HF(N), dt1
  Integer i, j, Kmax, M
  Integer Rmesh(9), Mat(5)
  Common /CoolProp/ Tinlet, De, G, W, D2, D1, mdot
  Common /TTAB/ CoolTbl
  Common /Zdata/ Zmin, Zmax, Kmax
  Common /Rdata/ Rbound, Rmesh, Mat
  external rhonak

  dt1 = 0.5
  if ( dt .lt. dt1 ) dt1 = dt/10.0d0
  Kmax = 10
  h = (Zmax-Zmin)/(N-1)
  CoolTbl(1,1) = Zmin
  CoolTbl(1,2) = Tinlet

```

```

hcool = (Zmax-Zmin)/(Jmax-1)
do j=1,jmax
  zcool(j) = (j-1)*hcool + Zmin
end do

if ( tnow .lt. dt ) then
  do j=1,N
    z = (j-1)*h + Zmin
    CoolTbl(j,1) = z
  end do
  call intrpl(8,jmax,zcool,tfcool,N,CoolTbl(1,1),CoolTbl(1,2))
end if

do j=1,n
  z = (j-1)*h + Zmin
  HF(j) = HeatFlux(z)
end do

M = idint( dt/dt1 )
do i=1,M

  do j=1,N
    TOLD(j) = CoolTbl(j,2)
  end do

  do 100 j=2, N
    dum1 = HF(j)
    dum2 = Cp(TOLD(j),W)
    dum3 = RhoNaK(TOLD(j),W)
    dum4 = dum3/dt1
    dum5 = G/h

    T = ( 4.0*dum1/dum2/De + dum4*TOLD(j) + dum5*CoolTbl(j-1,2) )
    a / ( dum4 + dum5 )

    CoolTbl(j,2) = T

100 Continue

  end do

End
double precision Function RhoNaK(T,W)
*****
* Uses correlations from the Sodium-NaK Engineering *
* Handbook (O. Foust, ed.; vol. 1 pp. 16-17) to return *
* the value of the density of the NaK-78 coolant for *
* a given temperature T and potassium weight fraction W *
* for the coolant (e.g. eutectic NaK-78 has W=78.) *
* Only single phase coolants are modeled. If the *
* temperature of the coolant is higher than the boiling *
* point of NaK at the given sodium-potassium composition,*
* this routine reports the error and halts the program. *
* *
* Units are in kilogram/cm^3 *
* *
*****
double precision T, BoilingPt, W

BoilingPt = ((756.5-881.4)*W + 881.4) + 273.1
If (T.GT BoilingPt) then
c Write(*,100) T, INT(W*100)
  Write(8,100) T, INT(W*100)
  Stop
EndIf

RhoNaK = 9.4971d-4 - 2.473d-7 * T

100 Format(' The temperature T=',F7.1,' degrees K is higher than ' /
a ' the boiling point for NaK-',I3, //
b ' Execution terminated in RhoNaK.' //)
End
Subroutine TFEHX(Tcoolant,t,Isolver)

C Implicit NONE
Integer Imax, Kmax, N, J, TabFlag, Isolver KHEL 7/18/93
Parameter (Imax = 10, Kmax = 10)
Real*8 T(Imax,Kmax), C1, Kcond, R, Z, Temp, R1, Z1
C Real*8 DeltaT
Real*8 R2, Z2, R3, Z3, Temp3, G, H, T1, Temm(Kmax), Tcol(Kmax)
Real*8 DeltaZ, C3, T2, Tcoolant(Kmax), ErrSqr, V(Kmax), Zmin
Real*8 A(Imax*Kmax+1,Imax*Kmax), X(Imax*Kmax), Tinlet, V0
Real*8 Rbound(10), Sig, Ems, QGapCond, Tr, Qch(Kmax), mdot KHEL 4/26/93
Real*8 HeffE(Kmax), HeffC(Kmax), Current, Qec(Kmax), Jdens(Kmax)
Real*8 QTable(Kmax), De, G1, W, Pi, PhiE, EmHeat(Kmax)
Real*8 ColHeat(Kmax), Zmax, Itop, Ibottom, Cden_av1, Cden_av2

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```

Real*8 Vguess(Kmax), Te0, Tc0, TeAv(Kmax), TcAv(Kmax)
Real*8 Dout, Din, Q3ave, Error, PowerTabl(2,100), Seconds
Real*8 Qrad(Kmax), QCsCond(Kmax), MaxError, Timer(3), TotalTime
Integer I, K, IC, I1, I2, I3, I4, J2, Rmesh(9), K2, I9, Mat(5)
Character*11 Start, Step1, Step2, Stop
Character*80 Title
Common /GaussMAIN/ A, X, N
Common /Rdata/ Rbound, Rmesh, Mat
Common /Zdata/ Zmin, Zmax, K2
Common /QTAB/ QTable
Common /Input/ Tr, Ems, PhiE, Itop, Ibottom, Title
Common /CoolProp/ Tinlet, De, G1, W, Dout, Din, mdot
Common /Steady/ Emheat, ColHeat, Qch, Qrad, QcsCond, Qec, Jdens,
        Current
Common /PowerData/ Q3ave, PowerTabl, TabFlag
Data Pi/3 1415926D0/

Call TIME(Start)
Do 10 I=1,3
10   Timer(I)=0

Te0 = 1900D0
Tc0 = 880D0
Sig = 5.67D-12
V0 = 0.60D0
N = Imax*Kmax
IC = 1

Do 100 K=1, Kmax
  Temp = Tinlet
  Do 100 I=1, Imax
    If (R(I).EQ.Rbound(5)) then
      T(I,K) = Tc0
    ElseIf (R(I).GT.Rbound(5)) then
      T(I,K) = (2.0D0)*{Rbound(10)-R(I)}
a      /{Rbound(10)-Rbound(5)} + Temp
    Else
      T(I,K) = Te0
    EndIf
100  Continue
  Do 101 K=1, Kmax
101   Vguess(K) = V0
102  Do 105 K=1, Kmax
    QTable(K) = Kcond(Imax, R(Imax), T(Imax, K))
a      *(T(Imax-1, K) - T(Imax, K)) / (R(Imax) - R(Imax-1))
105  Continue
*   Write(*,107)
  Call TIME(Step1)
  Call Convect
  Call CoolantTemp(Tcoolant)
*   Write(*,108)
  Call TIME(Step2)
* 107 Format(' Entering Convect/CoolantTemp.....')
* 108 Format(' .....Leaving Convect/CoolantTemp')
  Timer(1) = Timer(1) + Seconds(Step2) - Seconds(Step1)

110 I1 = 1
  Do 120 I9=1,2
120   I1 = I1 + Rmesh(I9)
    I2 = 1
    Do 125 I9=1,3
125   I2 = I2 + Rmesh(I9)
      I3 = I2+1
      I4 = 1
      Do 128 I9=1,5
128   I4 = I4 + Rmesh(I9)
        Do 150 K=1, Kmax
          Temm(K) = T(I2, K)
          Tcol(K) = T(I2+1, K)
          TeAv(K) = T(I1, K) * {R(I1+1)**2+2*R(I1+1)*R(I1)-3*R(I1)**2} / 4
          TcAv(K) = T(I3, K) * {R(I3+1)**2+2*R(I3+1)*R(I3)-3*R(I3)**2} / 4
          Do 130 I=I1+1, I2-1
            TeAv(K) = TeAv(K) + T(I, K) * {R(I+1)**2+2*R(I)*
a              {R(I+1)-R(I-1)}-R(I-1)**2} / 4
130   Continue
          Do 140 I=I3+1, I4-1
            TcAv(K) = TcAv(K) + T(I, K) * {R(I+1)**2+2*R(I)*
a              {R(I+1)-R(I-1)}-R(I-1)**2} / 4
140   Continue
          TeAv(K) = TeAv(K) + T(I2, K) * {3*R(I2)**2-2*R(I2)*R(I2-1)
a              -R(I2-1)**2} / 4
          TcAv(K) = TcAv(K) + T(I4, K) * {3*R(I4)**2-2*R(I4)*R(I4-1)
a              -R(I4-1)**2} / 4
          TeAv(K) = TeAv(K) / {R(I2)**2-R(I1)**2}

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      TcAv(K) = TcAv(K)/(R(I4)**2-R(I3)**2)
150  Continue
      Cden_av1 = Ibottom/(Pi*R(I2)**2*(Zmax-Zmin)/2)
      Cden_av2 = Itop/(Pi*R(I2)**2*(Zmax-Zmin)/2)
*
*   Write(*,154)
      Call TIME(Step1)
      Call Cylcon6(Temm,TeAv,Tcol,TcAv,Tr,PhiE,R(I3)-R(I2),Cden_av1,
1   Cden_av2,Zmax-Zmin,2*R(I2),R(I2)-R(I1),R(I4)-R(I3),Kmax,
2   Vguess, V, Qec, Jdens, EmHeat, ColHeat)
      Call TIME(Step2)
*   Write(*,155)
* 154 Format(' Entering CYLCON6.....')
* 155 Format(' .....Leaving CYLCON6')
      Timer(2) = Timer(2) + Seconds(Step2) - Seconds(Step1)

      Current = Itop+Ibottom
      Do 180 K=1,Kmax
          Vguess(K) = V(K)
180   Qch(K) = Qec(K)-Jdens(K)*V(K)

      Do 2005 K=1, Kmax
      Do 2000 I=1, Imax
          I2 = (K-1)*Imax + I
          Do 250 J=1,Imax*Kmax+1
              A(J,I2) = 0.0D000
250   Continue
**   I = 1, K = 2, Kmax -1 ****
      If ((I.EQ.1).AND.(K.NE.1).AND.(K.NE.Kmax)) Then
          R1 = R(I)
          R3 = R(I+1)
          R2 = (R3 + R1)/2
          Z1 = Z(K)
          DeltaZ = (Z(K+1)-Z(K-1))/2
          T1 = (T(I+1,K) + T(I,K))/2
          C3 = Kcond(I,R2,T1)*(R3+R1)/(R3-R1)*DeltaZ
          C1 = C3
          J2 = (K-1)*Imax + I+1
          A(J2,I2) = C3

          Temp3 = (R3**2 + 2*R1*R3 - 3*R1**2)/4
          Z3 = Z(K+1)
          Z2 = (Z3 + Z1)/2
          T1 = (T(I,K+1) + T(I,K))/2
          C3 = Kcond(I,R1,T1)/(Z3-Z1)*Temp3
          C1 = C1 + C3
          J2 = K*Imax + I
          A(J2,I2) = C3

          Z3 = Z(K-1)
          Z2 = (Z3 + Z1)/2
          T1 = (T(I,K-1) + T(I,K))/2
          C3 = Kcond(I,R1,T1)/(Z1-Z3)*Temp3
          C1 = C1 + C3
          J2 = (K-2)*Imax + I
          A(J2,I2) = C3

          A(Imax*Kmax+1,I2) = - G((R1+R2)/2,Z1)*DeltaZ + Temp3

          Goto 1000
      EndIf

**   If ((I.EQ.1).AND.(K.EQ.1)) Then
      I = 1, K = 1 ****
          R1 = R(I)
          R3 = R(I+1)
          R2 = (R3 + R1)/2
          Z1 = Z(K)
          Z3 = Z(K+1)
          DeltaZ = (Z3-Z1)/2
          T1 = (T(I+1,K) + T(I,K))/2
          C3 = Kcond(I,R2,T1)*(R3+R1)/(R3-R1)*DeltaZ
          C1 = C3
          J2 = (K-1)*Imax + I+1
          A(J2,I2) = C3

          Temp3 = (R3**2 - 3*R1**2 + 2*R1*R3)/4
          Z2 = (Z3 + Z1)/2
          T1 = (T(I,K+1) + T(I,K))/2
          C3 = Kcond(I,R1,T1)/(Z3-Z1)*Temp3
          C1 = C1+C3
          J2 = K*Imax + I
          A(J2,I2) = C3

```

```

      A(Imax*Kmax+1,I2) = - G((R1+R2)/2,(Z1+Z2)/2)*DeltaZ
a      * Temp3
      Goto 1000

      EndIf

      If ((I.EQ.1).AND.(K.EQ.Kmax)) Then
**      I = 1 and K = Kmax ****
          R1 = R(I)
          R3 = R(I+1)
          R2 = (R3 + R1)/2
          Z1 = Z(K)
          Z3 = Z(K-1)
          DeltaZ = (Z1-Z3)/2
          T1 = (T(I+1,K) + T(I,K))/2
          C3 = Kcond(I,R2,T1)*(R3+R1)/(R3-R1)*DeltaZ
          C1 = C3
          J2 = (K-1)*Imax + I+1
          A(J2,I2) = C3

          Temp3 = (R3**2 - 3*R1**2 + 2*R1*R3)/4
          Z2 = (Z3 + Z1)/2
          T1 = (T(I,K-1) + T(I,K))/2
          C3 = Kcond(I,R1,T1)/(Z1-Z3)*Temp3
          C1 = C1 + C3
          J2 = (K-2)*Imax + I
          A(J2,I2) = C3

      A(Imax*Kmax+1,I2) = - G((R1+R2)/2,(Z1+Z2)/2)*DeltaZ
a      * Temp3
      Goto 1000

      EndIf

***** Start of appended text *****
**      Collector surface, K = 2, Kmax -1 ****
      If ((R(I).EQ.Rbound(5)).AND.((K.NE.1).AND.(K.NE.Kmax))) Then
          R1 = R(I)
          R3 = R(I+1)
          R2 = (R3 + R1)/2
          Z1 = Z(K)
          DeltaZ = (Z(K+1)-Z(K-1))/2
          T1 = (T(I+1,K) + T(I,K))/2
          C3 = Kcond(I,R2,T1)*(R3+R1)/(R3-R1)*DeltaZ
          C1 = C3
          J2 = (K-1)*Imax + I+1
          A(J2,I2) = C3

          Temp3 = (R3**2 + 2*R1*R3 - 3*R1**2)/4
          Z3 = Z(K+1)
          Z2 = (Z3 + Z1)/2
          T1 = (T(I,K+1) + T(I,K))/2
          C3 = Kcond(I,R1,T1)/(Z3-Z1)*Temp3
          C1 = C1 + C3
          J2 = K*Imax + I
          A(J2,I2) = C3

          Z3 = Z(K-1)
          Z2 = (Z3 + Z1)/2
          T1 = (T(I,K-1) + T(I,K))/2
          C3 = Kcond(I,R1,T1)/(Z1-Z3)*Temp3
          C1 = C1 + C3
          J2 = (K-2)*Imax + I
          A(J2,I2) = C3

          HeffC(K) = (Qch(K)
b          + Sig*Ems*((T(I-1,K))**4-(T(I,K))**4)*R(I-1)/R(I)
c          + QGapCond(T(I-1,K),T(I,K),Tr,R(I)-R(I-1)))
d          *2*R(I-1)*DeltaZ/(T(I-1,K)-T(I,K))
          C1 = C1 + HeffC(K)
          J2 = (K-1)*Imax + I-1
          A(J2,I2) = HeffC(K)

      A(Imax*Kmax+1,I2) = -(G((R1+R2)/2,Z1)+ColHeat(K))
a      *DeltaZ*Temp3
      Goto 1000

      EndIf

**      Collector surface, K = 1 ****
      If ((R(I).EQ.Rbound(5)).AND.(K.EQ.1)) Then
          R1 = R(I)
          R3 = R(I+1)
          R2 = (R3 + R1)/2
          Z1 = Z(K)
          Z3 = Z(K+1)

```

```

DeltaZ = (Z3-Z1)/2
T1 = (T(I+1,K) + T(I,K))/2
C3 = Kcond(I,R2,T1)*(R3+R1)/(R3-R1)*DeltaZ
C1 = C3
J2 = (K-1)*Imax + I+1
A(J2,I2) = C3

Temp3 = (R3**2 - 3*R1**2 + 2*R1*R3)/4
Z2 = (Z3 + Z1)/2
T1 = (T(I,K+1) + T(I,K))/2
C3 = Kcond(I,R1,T1)/(Z3-Z1)*Temp3
C1 = C1+C3
J2 = K*Imax + I
A(J2,I2) = C3

HeffC(K) = (Qch(K)
+ Sig*Ems*((T(I-1,K))**4-(T(I,K))**4)*R(I-1)/R(I)
+ QGapCond(T(I-1,K),T(I,K),Tr,R(I)-R(I-1)))
*2*R(I-1)*DeltaZ/(T(I-1,K)-T(I,K))
C1 = C1 + HeffC(K)
J2 = (K-1)*Imax + I-1
A(J2,I2) = HeffC(K)

a
A(Imax*Kmax+1,I2) = -(G((R1+R2)/2,Z1)+ColHeat(K))
*DeltaZ*Temp3
Goto 1000

EndIf

**
Collector surface and K = Kmax ****
If ((R(I).EQ.Rbound(5)).AND.(K.EQ.Kmax)) Then
R1 = R(I)
R3 = R(I+1)
R2 = (R3 + R1)/2
Z1 = Z(K)
Z3 = Z(K-1)
DeltaZ = (Z1-Z3)/2
T1 = (T(I+1,K) + T(I,K))/2
C3 = Kcond(I,R2,T1)*(R3+R1)/(R3-R1)*DeltaZ
C1 = C3
J2 = (K-1)*Imax + I+1
A(J2,I2) = C3

Temp3 = (R3**2 - 3*R1**2 + 2*R1*R3)/4
Z2 = (Z3 + Z1)/2
T1 = (T(I,K-1) + T(I,K))/2
C3 = Kcond(I,R1,T1)/(Z1-Z3)*Temp3
C1 = C1 + C3
J2 = (K-2)*Imax + I
A(J2,I2) = C3

HeffC(K) = (Qch(K)
+ Sig*Ems*((T(I-1,K))**4-(T(I,K))**4)*R(I-1)/R(I)
+ QGapCond(T(I-1,K),T(I,K),Tr,R(I)-R(I-1)))
*2*R(I-1)*DeltaZ/(T(I-1,K)-T(I,K))
C1 = C1 + HeffC(K)
J2 = (K-1)*Imax + I-1
A(J2,I2) = HeffC(K)

a
A(Imax*Kmax+1,I2) = -(G((R1+R2)/2,Z1)+ColHeat(K))
*DeltaZ*Temp3
Goto 1000

EndIf

**
Emitter surface, K = 2, Kmax -1 ****
If ((R(I).EQ.Rbound(4)).AND.({K.NE.1}.AND.(K.NE.Kmax))) Then
R1 = R(I)
Z1 = Z(K)
DeltaZ = (Z(K+1)-Z(K-1))/2
R3 = R(I-1)
R2 = (R3 + R1)/2
T1 = (T(I-1,K) + T(I,K))/2
C3 = Kcond(I,R2,T1)*(R3+R1)/(R1-R3)*DeltaZ
C1 = C3
J2 = (K-1)*Imax + I-1
A(J2,I2) = C3

Temp3 = (3*R1**2 - R3**2 - 2*R1*R3)/4
Z3 = Z(K+1)
Z2 = (Z3 + Z1)/2
T1 = (T(I,K+1) + T(I,K))/2
C3 = Kcond(I,R1,T1)/(Z3-Z1)*Temp3
C1 = C1 + C3
J2 = K*Imax + I
A(J2,I2) = C3

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```

Z3 = Z(K-1)
Z2 = (Z3 + Z1)/2
T1 = (T(I,K-1) + T(I,K))/2
C3 = Kcond(I,R1,T1)/(Z1-Z3)*Temp3
C1 = C1 + C3
J2 = (K-2)*Imax + I
A(J2,I2) = C3

b HeffE(K) = (Qec(K)
+ Sig*Ems*((T(I,K))**4 - (T(I+1,K))**4)
c + QGapCond(T(I,K),T(I+1,K),Tr,R(I+1)-R(I)))
d *2*R(I)*DeltaZ/(T(I,K)-T(I+1,K))
Qrad(K) = Sig*Ems*((T(I,K))**4 - (T(I+1,K))**4)
QCsCond(K) = QGapCond(T(I,K),T(I+1,K),Tr,R(I+1)-R(I))
C1 = C1 + HeffE(K)
J2 = (K-1)*Imax + I+1
A(J2,I2) = HeffE(K)

a A(Imax*Kmax+1,I2) = -(G((R1+R2)/2,Z1)+EmHeat(K))
*DeltaZ*Temp3
Goto 1000

EndIf

** Emitter surface, K = 1 ****
If ((R(I).EQ.Rbound(4)).AND.(K.EQ.1)) Then
R1 = R(I)
Z1 = Z(K)
Z3 = Z(K+1)
DeltaZ = (Z3-Z1)/2
R3 = R(I-1)
R2 = (R3 + R1)/2
T1 = (T(I-1,K) + T(I,K))/2
C3 = Kcond(I,R2,T1)*(R3+R1)/(R1-R3)*DeltaZ
C1 = C3
J2 = (K-1)*Imax + I-1
A(J2,I2) = C3

Temp3 = (3*R1**2 - R3**2 + 2*R1*R3)/4
Z2 = (Z3 + Z1)/2
T1 = (T(I,K+1) + T(I,K))/2
C3 = Kcond(I,R1,T1)/(Z3-Z1)*Temp3
C1 = C1 + C3
J2 = K*Imax + I
A(J2,I2) = C3

b HeffE(K) = (Qec(K)
+ Sig*Ems*((T(I,K))**4 - (T(I+1,K))**4)
c + QGapCond(T(I,K),T(I+1,K),Tr,R(I+1)-R(I)))
d *2*R(I)*DeltaZ/(T(I,K)-T(I+1,K))
Qrad(K) = Sig*Ems*((T(I,K))**4 - (T(I+1,K))**4)
QCsCond(K) = QGapCond(T(I,K),T(I+1,K),Tr,R(I+1)-R(I))
C1 = C1 + HeffE(K)
J2 = (K-1)*Imax + I+1
A(J2,I2) = HeffE(K)

a A(Imax*Kmax+1,I2) = -(G((R1+R2)/2,(Z1+Z2)/2)+EmHeat(K))
*DeltaZ*Temp3
Goto 1000

EndIf

** Emitter surface, K = Kmax ****
If ((R(I).EQ.Rbound(4)).AND.(K.EQ.Kmax)) Then
R1 = R(I)
Z1 = Z(K)
Z3 = Z(K-1)
DeltaZ = (Z1-Z3)/2
R3 = R(I-1)
R2 = (R3 + R1)/2
T1 = (T(I-1,K) + T(I,K))/2
C3 = Kcond(I,R2,T1)*(R3+R1)/(R1-R3)*DeltaZ
C1 = C3
J2 = (K-1)*Imax + I-1
A(J2,I2) = C3

Temp3 = (3*R1**2 - R3**2 + 2*R1*R3)/4
Z2 = (Z3 + Z1)/2
T1 = (T(I,K-1) + T(I,K))/2
C3 = Kcond(I,R1,T1)/(Z1-Z3)*Temp3
C1 = C1 + C3
J2 = (K-2)*Imax + I
A(J2,I2) = C3

b HeffE(K) = (Qec(K)
+ Sig*Ems*((T(I,K))**4 - (T(I+1,K))**4)

```

```

c      + QGapCond(T(I,K),T(I+1,K),Tr,R(I+1)-R(I))
d      *2*R(I)*DeltaZ/(T(I,K)-T(I+1,K))
      Qrad(K) = Sig*Ems*{(T(I,K))**4 - (T(I+1,K))**4}
      QCsCond(K) = QGapCond(T(I,K),T(I+1,K),Tr,R(I+1)-R(I))
      C1 = C1 + HeffE(K)
      J2 = (K-1)*Imax + I+1
      A(J2,I2) = HeffE(K)

a      A(Imax*Kmax+1,I2) = -(G*((R2+R1)/2, (Z1+Z2)/2)+EmHeat(K))
      *DeltaZ*Temp3
      Goto 1000

      EndIf

**      If ((I.NE.1).AND.(I.NE.Imax)).AND.(K.EQ.1) Then
      K = 1 and I = 2, Nmax -1 ****
      R1 = R(I)
      R3 = R(I+1)
      R2 = (R3 + R1)/2
      Z1 = Z(K)
      Z3 = Z(K+1)
      DeltaZ = (Z3-Z1)/2
      T1 = (T(I+1,K) + T(I,K))/2
      C3 = Kcond(I,R2,T1)*(R3+R1)/(R3-R1)*DeltaZ
      C1 = C3
      J2 = (K-1)*Imax + I+1
      A(J2,I2) = C3

      R3 = R(I-1)
      R2 = (R3 + R1)/2
      T1 = (T(I-1,K) + T(I,K))/2
      C3 = Kcond(I,R2,T1)*(R3+R1)/(R1-R3)*DeltaZ
      C1 = C1 + C3
      J2 = (K-1)*Imax + I-1
      A(J2,I2) = C3

      R2 = R(I+1)
      Temp3 = (R2**2 - R3**2 + 2*R1*(R2-R3))/4
      Z2 = (Z3 + Z1)/2
      T1 = (T(I,K+1) + T(I,K))/2
      C3 = Kcond(I,R1,T1)/(Z3-Z1)*Temp3
      C1 = C1 + C3
      J2 = K*Imax + I
      A(J2,I2) = C3

      A(Imax*Kmax+1,I2) = - G(R1, (Z1+Z2)/2)*DeltaZ * Temp3

      Goto 1000

      EndIf

**      If (((I.NE.1).AND.(I.NE.Imax)).AND.(K.EQ.Kmax)) Then
      K = Kmax and I = 2, Imax -1 ****
      R1 = R(I)
      R3 = R(I+1)
      R2 = (R3 + R1)/2
      Z1 = Z(K)
      Z3 = Z(K-1)
      DeltaZ = (Z1-Z3)/2
      T1 = (T(I+1,K) + T(I,K))/2
      C3 = Kcond(I,R2,T1)*(R3+R1)/(R3-R1)*DeltaZ
      C1 = C3
      J2 = (K-1)*Imax + I+1
      A(J2,I2) = C3

      R3 = R(I-1)
      R2 = (R3 + R1)/2
      T1 = (T(I-1,K) + T(I,K))/2
      C3 = Kcond(I,R2,T1)*(R3+R1)/(R1-R3)*DeltaZ
      C1 = C1 + C3
      J2 = (K-1)*Imax + I-1
      A(J2,I2) = C3

      R2 = R(I+1)
      Temp3 = (R2**2 - R3**2 + 2*R1*(R2-R3))/4
      Z2 = (Z3 + Z1)/2
      T1 = (T(I,K-1) + T(I,K))/2
      C3 = Kcond(I,R1,T1)/(Z1-Z3)*Temp3
      C1 = C1 + C3
      J2 = (K-2)*Imax + I
      A(J2,I2) = C3

      A(Imax*Kmax+1,I2) = - G(R1,Z2)*DeltaZ * Temp3

      Goto 1000

```

```

EndIf
** If ((I.EQ.Imax).AND.(K.NE.1).AND.(K.NE.Kmax)) Then
I = Imax, K = 2, Kmax - 1 ****
  R1 = R(I)
  Z1 = Z(K)
  DeltaZ = (Z(K+1)-Z(K-1))/2
  T2 = Tcoolant(K)
  C3 = H(T2)*R1*DeltaZ*2
  C1 = C3
  A(Imax*Kmax+1,I2) = -C3*T2

  R3 = R(I-1)
  R2 = (R3 + R1)/2
  T1 = (T(I-1,K) + T(I,K))/2
  C3 = Kcond(I,R2,T1)*(R3+R1)/(R1-R3)*DeltaZ
  C1 = C1 + C3
  J2 = (K-1)*Imax + I-1
  A(J2,I2) = C3

  Temp3 = (3*R1**2 - R3**2 - 2*R1*R3)/4
  Z3 = Z(K+1)
  Z2 = (Z3 + Z1)/2
  T1 = (T(I,K+1) + T(I,K))/2
  C3 = Kcond(I,R1,T1)/(Z3-Z1)*Temp3
  C1 = C1 + C3
  J2 = K*Imax + I
  A(J2,I2) = C3

  Z3 = Z(K-1)
  Z2 = (Z3 + Z1)/2
  T1 = (T(I,K-1) + T(I,K))/2
  C3 = Kcond(I,R1,T1)/(Z1-Z3)*Temp3
  C1 = C1 + C3
  J2 = (K-2)*Imax + I
  A(J2,I2) = C3

  A(Imax*Kmax+1,I2) = A(Imax*Kmax+1,I2)
  - G(R2,Z1)*DeltaZ + Temp3
a
  Goto 1000
EndIf
** If ((I.EQ.Imax).AND.(K.EQ.1)) Then
I = Imax, K = 1 ****
  R1 = R(I)
  Z1 = Z(K)
  Z3 = Z(K+1)
  DeltaZ = (Z3-Z1)/2
  T1 = T(I,K)
  T2 = Tcoolant(K)
  C3 = H(T2)*R1*DeltaZ*2
  C1 = C3
  A(Imax*Kmax+1,I2) = -C3*T2

  R3 = R(I-1)
  R2 = (R3 + R1)/2
  T1 = (T(I-1,K) + T(I,K))/2
  C3 = Kcond(I,R2,T1)*(R3+R1)/(R1-R3)*DeltaZ
  C1 = C1 + C3
  J2 = (K-1)*Imax + I-1
  A(J2,I2) = C3

  Temp3 = (3*R1**2 - R3**2 + 2*R1*R3)/4
  Z2 = (Z3 + Z1)/2
  T1 = (T(I,K+1) + T(I,K))/2
  C3 = Kcond(I,R1,T1)/(Z3-Z1)*Temp3
  C1 = C1 + C3
  J2 = K*Imax + I
  A(J2,I2) = C3

  A(Imax*Kmax+1,I2) = A(Imax*Kmax+1,I2)
  - G(R2,Z2)*DeltaZ + Temp3
a
  Goto 1000
EndIf
** If ((I.EQ.Imax).AND.(K.EQ.Kmax)) Then
I = Imax, K = Kmax ****
  R1 = R(I)
  Z1 = Z(K)
  Z3 = Z(K-1)
  DeltaZ = (Z1-Z3)/2
  T1 = T(I,K)

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```

T2 = Tcoolant(K)
C3 = H(T2)*R1*DeltaZ*2
C1 = C3
A(Imax*Kmax+1,I2) = -C3*T2

R3 = R(I-1)
R2 = (R3 + R1)/2
T1 = (T(I-1,K) + T(I,K))/2
C3 = Kcond(I,R2,T1)*(R3+R1)/(R1-R3)*DeltaZ
C1 = C1 + C3
J2 = (K-1)*Imax + I-1
A(J2,I2) = C3

Temp3 = (3*R1**2 - R3**2 + 2*R1*R3)/4
Z2 = (Z3 + Z1)/2
T1 = (T(I,K-1) + T(I,K))/2
C3 = Kcond(I,R1,T1)/(Z1-Z3)*Temp3
C1 = C1 + C3
J2 = (K-2)*Imax + I
A(J2,I2) = C3

a
A(Imax*Kmax+1,I2) = A(Imax*Kmax+1,I2)
- G(R2,Z2)*DeltaZ * Temp3

Goto 1000

Endif

** All other points ***
R1 = R(I)
R3 = R(I+1)
R2 = (R3 + R1)/2
Z1 = Z(K)
DeltaZ = (Z(K+1)-Z(K-1))/2
T1 = (T(I+1,K) + T(I,K))/2
C3 = Kcond(I,R2,T1)*(R3+R1)/(R3-R1)*DeltaZ
C1 = C3
J2 = (K-1)*Imax + I+1
A(J2,I2) = C3

R3 = R(I-1)
R2 = (R3 + R1)/2
T1 = (T(I-1,K) + T(I,K))/2
C3 = Kcond(I,R2,T1)*(R3+R1)/(R1-R3)*DeltaZ
C1 = C1 + C3
J2 = (K-1)*Imax + I-1
A(J2,I2) = C3

R2 = R(I+1)
Temp3 = (R2**2 - R3**2 + 2*R1*(R2-R3))/4
Z3 = Z(K+1)
Z2 = (Z3 + Z1)/2
T1 = (T(I,K+1) + T(I,K))/2
C3 = Kcond(I,R1,T1)/(Z3-Z1)*Temp3
C1 = C1 + C3
J2 = K*Imax + I
A(J2,I2) = C3

Z3 = Z(K-1)
Z2 = (Z3 + Z1)/2
T1 = (T(I,K-1) + T(I,K))/2
C3 = Kcond(I,R1,T1)/(Z1-Z3)*Temp3
C1 = C1 + C3
J2 = (K-2)*Imax + I
A(J2,I2) = C3

A(Imax*Kmax+1,I2) = - G(R1,Z1)*DeltaZ * Temp3

1000 A(I2,I2) = - C1
2000 Continue
2005 Continue

c Do 2015 J=1,Imax*Kmax
c Do 2010 I=1,Imax*Kmax+1
c Write (6,2020) I,J, A(I,J)
c 2010 Continue
c 2015 Continue
c 2020 Format (' A(',I3,',',I3,') =',F15.5)

* Write(*,2024)
Call TIME(Step1)
if ( Isolver .eq. 1 ) then
Call Gauss
else
Call SGauss
end if

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*      Write(*,2025)
      Call TIME(Step2)
*2024 Format(' Entering GAUSS.....')
*2025 Format(' .....Leaving GAUSS')
      Timer(3) = Timer(3) + Seconds(Step2) - Seconds(Step1)

      MaxError = 0.000
      Error = 0.000
      ErrSqr = 0.00000
      Do 2500 K=1,Kmax
      Do 2500 I=1,Imax
          I2 = (K-1)*Imax + I
          MaxError = MAX(MaxError,X(I2)-T(I,K))
          Error = Error + (X(I2) - T(I,K))
2500      ErrSqr = ErrSqr + (X(I2) - T(I,K))**2.000

      Do 2600 I=1,Imax
      Do 2600 K=1,Kmax
          I2 = (K-1)*Imax + I
          T(I,K) = (T(I,K)+X(I2))/2.000
      Write(8,2620) I,K,T(I,K)
C      2600 Continue
2620 Format (' T(',I3,',',I3,') =',G15.5)
C      DeltaT = 100.000
C      If (ABS(X(I2)-T(I,K)).LT.DeltaT) DeltaT =
C      a      ABS(X(I2)-T(I,K))
C      If (X(I2).LT.T(I,K)) DeltaT = -DeltaT
C 2600      T(I,K) = T(I,K) + DeltaT

C ***** OUTPUT RESULTS TO THE FILE TFEHX.OUT *****

      Write(8,4100)
      Write(8,4110) Title
      Write(8,4120)
      c      Write(*,2550) IC, SQRT(ErrSqr/(Imax*Kmax)), Error/(Imax*Kmax),
      a      MaxError
      Write(8,2550) IC, SQRT(ErrSqr/(Imax*Kmax)), Error/(Imax*Kmax),
      a      MaxError
2550 Format (' Iteration :,I3,' RMS error = ',F13.7,' Ave Diff. = ',
      a      F13.7/20X,' Max. Error = ',F13.7)
      IC = IC + 1

      If (SQRT(ErrSqr/(Imax*Kmax)).LT.1.0D-1) Goto 2900
      Goto 102
2900 Write(8,4100)
      Write(8,4110) Title
      Write(8,4130)
C***** Output Temp. distribution for fuel *****
      Do 3000 I=1,Imax
      Do 3000 K=1,Kmax
          I2 = (K-1)*Imax + I
3000      Write(8,3010) I,K, X(I2)
3010 Format (' T(',I3,',',I3,') = ',F13.7)
      Write (8,3015) V(1),V(Kmax)
      Write(8,3020) Current, V(1)*Ibottom+V(Kmax)*Itop
3015 Format(' Voltage across bottom of cell: ',F13.7/
      a      ' Voltage across top of cell: ',F13.7)
3020 Format(' Output current = ',F13.7/' Output electrical power = ',
      a      F13.7)
      Write(8,3030)
3030 Format(//8X,'2',19X,'V',18X,'Qec',16X,'Jdens'/X,3(15('-'),5X),
      A      15('-')/)
      Do 3040 K=1,Kmax
          Write(8,3050) Z(K), V(K), Qec(K), Jdens(K)
3040 Continue
3050 Format(X,3(F15.8,5X),F15.8)
      Write(8,3060)
3060 Format(//8X,'2',17X,'EmHeat',13X,'ColHeat'/X,2(15('-'),5X),
      A      15('-')/)
      Do 3070 K=1,Kmax
          Write(8,3080) Z(K), EmHeat(K), ColHeat(K)
3070 Continue
3080 Format(X,2(F15.8,5X),F15.8)
      Write(8,3090)
3090 Format(//8X,'2',18X,'Qch',16X,'Qrad',15X,'QCsCond'/
      A      X,3(15('-'),5X),15('-')/)
      Do 3095 K=1,Kmax
          Write(8,3050) Z(K), Qch(K), Qrad(K), QCsCond(K)
3095 Continue
      Call TIME(Stop)
      TotalTime = Seconds(Stop)-Seconds(Start)
      Write(8,4000) INT(TotalTime/60),TotalTime-INT(TotalTime)
      Write(8,4010) 'Convect/CoolantTemp', INT(Timer(1)/60),
      a      Timer(1)-INT(Timer(1)/60)*60, Timer(1)/TotalTime*100D0
      Write(8,4020) 'CYLCON5', INT(Timer(2)/60),

```



```

a      Timer(2)-INT(Timer(2)/60)*60, Timer(2)/TotalTime*100D0
Write(8,4030) 'Gauss', INT(Timer(3)/60),
a      Timer(3)-INT(Timer(3)/60)*60,Timer(3)/TotalTime*100D0

4000 Format(' Total computational time required:',I3,' min.,',F6.2,
a      ' sec.')
4010 Format(' Time spent in ',A19,':',I3,' min.,',F6.2,' sec. ('
a      F4.1,'%')')
4020 Format(' Time spent in ',A7,':',I3,' min.,',F6.2,' sec. ('
a      F4.1,'%')')
4030 Format(' Time spent in ',A5,':',I3,' min.,',F6.2,' sec. ('
a      F4.1,'%')')
4100 Format ('1',20('*')), ' TFEHX ',20('*')/
a      ' ***** RESULTS FOR THE FOLLOWING CASE:'
4110 Format (A80)
4120 Format (' ITERATION HISTORY -- '/20X,'Converging the RMS error to'
a      'less than 0.1 K.')
4130 Format (' TEMPERATURE DISTRIBUTION FOR THE FUEL REGION ---'/)
4140 Format (3X,'R='3X,9(F4.2,4X:))
4142 Format (2X,'Z='',3X,9(A6,2X:))
4150 Format (X,F5.2,X,'',9(X,F6.1,X:))

Return
End
Real*8 Function Seconds(Time)
Character*11 Time

Seconds = (ICHAR(Time(1:1))-48)*36D3 + (ICHAR(Time(2:2))-48)*36D2
a      + (ICHAR(Time(4:4))-48)*60D0 + (ICHAR(Time(5:5))-48)*60D0
b      + (ICHAR(Time(7:7))-48)*10D0 + (ICHAR(Time(8:8))-48)
c      + (ICHAR(Time(10:10))-48)*.1 + (ICHAR(Time(11:11))-48)*.01

End
Subroutine GAUSS

Integer Imax, Kmax
Parameter (Imax = 10,Kmax = 10)
Real*8 A(Imax*Kmax+1,Imax*Kmax), X(Imax*Kmax)
INTEGER PIVOT_ROW, N
COMMON /GaussMAIN/ A,X,N

DO 10 PIVOT_ROW=1,N
CALL PAR_PIVOT(PIVOT_ROW)
CALL FWD_ELIM(PIVOT_ROW)
10 CONTINUE

CALL BACK_SOLN

c DO 20 INDEX=1,N
c WRITE(UNIT=*,FMT=25) INDEX,X(INDEX)
c 25 FORMAT(' X(',I2,')= ',F16.10)
c 20 CONTINUE

END
SUBROUTINE PAR_PIVOT(K)

Integer Imax, Kmax
Parameter (Imax = 10,Kmax = 10)
Real*8 A(Imax*Kmax+1,Imax*Kmax), X(Imax*Kmax), SCRATCH
INTEGER L,I,K,N
COMMON /GaussMAIN/ A,X,N

DO 10 L=K+1,N
IF (ABS(A(K,L)).GT.ABS(A(K,K))) THEN
DO 20 I=K,N+1
SCRATCH=A(I,K)
A(I,K)=A(I,L)
A(I,L)=SCRATCH
20 CONTINUE
ENDIF

10 CONTINUE

RETURN
END
SUBROUTINE FWD_ELIM(K)

Integer Imax, Kmax
Parameter (Imax = 10,Kmax = 10)
Real*8 A(Imax*Kmax+1,Imax*Kmax), X(Imax*Kmax)
INTEGER I,J,K,N
COMMON /GaussMAIN/A,X,N

DO 10 J=K+1,N+1
A(J,K)=A(J,K)/A(K,K)
10 CONTINUE

```

```

DO 20 J=K+1,N
DO 30 I=K+1,N+1
      A(I,J)=A(I,J)-A(K,J)*A(I,K)
30 CONTINUE
20 CONTINUE

```

```

RETURN
END
SUBROUTINE BACK_SOLN

```

```

Integer Imax, Kmax
Parameter (Imax = 10, Kmax = 10)
Real*8 A(Imax*Kmax+1, Imax*Kmax), X(Imax*Kmax)
INTEGER I, J, N
COMMON /GaussMAIN/ A, X, N

```

```

DO 20 J=N, 1, -1
      X(J)=A(N+1, J)
      DO 10 I=J+1, N
            X(J)-X(J)-A(I, J)*X(I)
10 CONTINUE
20 CONTINUE

```

```

RETURN
END
Real*8 Function H(T)

```

```

C*****
C
C   for the convective heat transfer correlations given
C   for liquid metal flows through annular channels, as
C   presented in M.M. El-Wakil, Nuclear Heat Transport,
C   p. 269, equations 10-6 and 10-7.
C*****

```

```

Real*8 T, K, A, B, C, D, T1, Cp
Real*8 Tinlet, De, G, W, D2, D1
Real*8 Nu, Pe, mdot
Common /CoolProp/ Tinlet, De, G, W, D2, D1, mdot
Data A/6.20D-2/, B/7.204D-4/, C/-8.343D-7/, D/3.060D-10/
K(T1) = A + B*T1 + C*T1**2 + D*T1**3

```

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```

Pe = De*G*Cp(T,W)/K(T)

```

```

If (D2/D1.LT.1.4) then
  Nu = 5.8D0 + 0.02D0*(Pe**0.8D0)
Else
  Nu = 5.25D0 + 0.0188D0*(Pe**0.8D0)*(D2/D1)**0.3D0
EndIf

```

```

H = Nu*K(T)/De

```

```

End
Real*8 Function G(R, Z)

```

```

Integer Imax
Parameter (Imax = 10)
Real*8 R, Z, Rbound(10), Zmin, Zmax, Pi, Temp, A, B
Real*8 Gave, PowerTabl(2,100)
Integer TabFlag, I
Integer Rmesh(9), Kmax, M(5)
Common /Rdata/ Rbound, Rmesh, M
Common /Zdata/ Zmin, Zmax, Kmax
Common /PowerData/ Gave, PowerTabl, TabFlag
Data Pi/3.1414526/

```

```

If ((R.GE.Rbound(1)).AND.(R.LE.Rbound(2))) then
  If (TabFlag.EQ.1) then
    I=0
5    I=I+1
    If ((Z.GE.PowerTabl(1,I)).AND.
a    (Z.LT.PowerTabl(1,I+1))) then
      Temp=Gave*(PowerTabl(2,I+1)-PowerTabl(2,I))/
a      (PowerTabl(1,I+1)-PowerTabl(1,I))*
b      (Z - PowerTabl(1,I))
    Else
      Goto 5
    EndIf
  Else
    A = PowerTabl(1,1)
    B = PowerTabl(2,1)
    Temp = Gave*(A + B*SIN((Z-Zmin)*Pi/(Zmax-Zmin)))
  EndIf
Else
  Temp = 0.00D0
EndIf
G = Temp

```

```

End
Real*8 Function Kcond(I,R2,T)
***      Units = W/cm/K      ***

Integer Imax
Parameter (Imax = 10)
Integer I,Rmesh(9),M(5), M1
Real*8 T, R, Rbound(10), Temp, R2, T1
Real*8 K, Kdata(4,8)
Common /Rdata/ Rbound,Rmesh,M

*
*   Material #1 = UO2
*   Material #2 = W
*   Material #3 = Nb
*   Material #4 = Nb1Zr
*   Material #5 = Mo
*   Material #6 = Re
*   Material #7 = Cs
*   Material #8 = Al2O3
*

Data Kdata/2.414D-2, - 2.478D-5, 1.094D-8, - 1.67D-12,
a      0.4886D0, - 3.057D-4, 1.237D-7, - 1.72D-11,
b      0.11104D0,  4.870D-6, 1.281D-8,    0.0D0,
c      0.11104D0,  4.870D-6, 1.281D-8,    0.0D0,
d      0.3602D0, - 1.141D-4, 2.050D-8,    0.0D0,
e      0.0D0,    0.0D0,    0.0D0,    0.0D0,
f      0.0D0,    0.0D0,    0.0D0,    0.0D0,
g      0.1858D0, - 4.169D-4, 3.469D-7, - 9.74D-11/

K(T1,M1) = (Kdata(1,M1) + Kdata(2,M1)*T1 + Kdata(3,M1)*T1**2
a          + Kdata(4,M1)*T1**3)*4.184

If (R2.LT.Rbound(1)) then
*      *** Void
      Temp = 1.0D-2
      Goto 100
EndIf
If (R2.EQ.Rbound(1)) then
*      *** Void/Pellet boundary
      Temp = (1.0D-2 + K(T,M(1)))/2
      Goto 100
EndIf
If ((R2.GT.Rbound(1)).AND.(R2.LT.Rbound(2))) then
*      *** Fuel pellet
      Temp = K(T,M(1))
      Goto 100
EndIf
If (R2.EQ.Rbound(2)) then
*      *** Fuel Pellet outer surface
***      Does a gap exist between the fuel and the emitter? ***
      If (Rbound(2).NE.Rbound(3)) then
*          *** Gap
          Temp = (1.0D-2*(R(I+1)-R(I)) +
a              K(T,M(1))*(R(I)-R(I-1)))
b              /(R(I+1)-R(I-1))
          Else
*          *** No Gap
          Temp = (K(T,M(2))*(R(I+1)-R(I)) +
a              K(T,M(1))*(R(I)-R(I-1)))
b              /(R(I+1)-R(I-1))
          EndIf
          Goto 100
        EndIf
      If ((Rbound(2).NE.Rbound(3)).AND.((R2.GT.Rbound(2))
a          .AND.(R2.LT.Rbound(3)))) then
*          *** Gap
          Temp = 1.0D-2
          Goto 100
        EndIf
      If ((R2.EQ.Rbound(3)).AND.(Rbound(2).NE.Rbound(3))) then
a          Temp = (K(T,M(2))*(R(I+1)-R(I)) + 1.0D-2*(R(I)-R(I-1)))
          /(R(I+1)-R(I-1))
*          *** Emitter inner surface
          Goto 100
        EndIf
      If ((R2.GT.Rbound(3)).AND.(R2.LT.Rbound(4))) then
*          *** Emitter
          Temp = K(T,M(2))
          Goto 100
        EndIf
      If (R2.EQ.Rbound(4)) then
*          *** Emitter outer surface
a          Temp = (1.0D-3*(R(I+1)-R(I)) + K(T,M(2))*(R(I)-R(I-1)))
          /(R(I+1)-R(I-1))
          Goto 100

```

```

EndIf
If ((R2.GT.Rbound(4)).AND.(R2.LT.Rbound(5))) then
*
  *** Gap
  Temp = 1.0D-3
  Goto 100
EndIf
If (R2.EQ.Rbound(5)) then
*
  *** Collector inner surface
  Temp = (K(T,M(3))*(R(I+1)-R(I)) + 1.0D-3*(R(I)-R(I-1)))
a
  / (R(I+1)-R(I-1))
  Goto 100
EndIf
If ((R2.GT.Rbound(5)).AND.(R2.LT.Rbound(6))) then
*
  *** Collector
  Temp = K(T,M(3))
  Goto 100
EndIf
If (R2.EQ.Rbound(6)) then
*
  *** Collector outer surface
  *** Does a gap exist between the collector and the insulator? ***
  If (Rbound(6).NE.Rbound(7)) then
  *
    *** Gap
    Temp = (1.0D-2*(R(I+1)-R(I)) + K(T,M(3))*(R(I)-R(I-1)))
a
    / (R(I+1)-R(I-1))
  *
    Else
    *** No Gap
    Temp = (K(T,M(4))*(R(I+1)-R(I)) + K(T,M(3))*(R(I)-R(I-1)))
a
    / (R(I+1)-R(I-1))
  *
    EndIf
  Goto 100
EndIf
If ((Rbound(6).NE.Rbound(7)).AND.((R2.GT.Rbound(6))
a
  .AND.(R2.LT.Rbound(7)))) then
  *
    *** Gap
    Temp = 1.0D-2
    Goto 100
  EndIf
  If ((R2.EQ.Rbound(7)).AND.(Rbound(6).NE.Rbound(7))) then
  *
    *** Insulator inner surface
    Temp = (K(T,M(4))*(R(I+1)-R(I)) + 1.0D-2*(R(I)-R(I-1)))
a
    / (R(I+1)-R(I-1))
    Goto 100
  EndIf
  If ((R2.GT.Rbound(7)).AND.(R2.LT.Rbound(8))) then
  *
    *** Insulator
    Temp = K(T,M(4))
    Goto 100
  EndIf
  If (R2.EQ.Rbound(8)) then
  *
    *** Insulator outer surface
    *** Does a gap exist between the insulator and the clad? ***
    If (Rbound(8).NE.Rbound(9)) then
    *
      *** Gap
      Temp = (1.0D-2*(R(I+1)-R(I)) + K(T,M(4))*(R(I)-R(I-1)))
a
      / (R(I+1)-R(I-1))
    *
      Else
      *** No Gap
      Temp = (K(T,M(5))*(R(I+1)-R(I)) + K(T,M(4))*(R(I)-R(I-1)))
a
      / (R(I+1)-R(I-1))
    *
      EndIf
    Goto 100
  EndIf
  If ((Rbound(8).NE.Rbound(9)).AND.((R2.GT.Rbound(8))
a
  .AND.(R2.LT.Rbound(9)))) then
  *
    *** Gap
    Temp = 1.0D-2
    Goto 100
  EndIf
  If ((R2.EQ.Rbound(9)).AND.(Rbound(8).NE.Rbound(9))) then
  *
    *** Clad inner surface
    Temp = (K(T,M(5))*(R(I+1)-R(I)) + 1.0D-2*(R(I)-R(I-1)))
a
    / (R(I+1)-R(I-1))
    Goto 100
  EndIf
  If ((R2.GT.Rbound(9)).AND.(R2.LT.Rbound(10))) then
  *
    *** Clad
    Temp = K(T,M(5))
    Goto 100
  EndIf
  If (R2.EQ.Rbound(10)) then
  *
    *** Clad outer surface
    *** Clad
    Temp = K(T,M(5))
    Goto 100
  EndIf

```

```

100 Kcond = Temp
      End
      Real*8 Function Z(K)

      Integer K, Kmax
      Real*8 Zmin, Zmax
      Common /Zdata/ Zmin, Zmax, Kmax
      Kmax = 10

      Z = (Zmax-Zmin)*(K-1)/(Kmax-1) + Zmin

      End
      Real*8 Function R(I)

      Integer I, Mesh1, Mesh2, Rmesh(9), J, Imax
      Parameter (Imax = 10)
      Integer Mat(5)
      Real*8 Rbound(10), Temp

      Common /Rdata/ Rbound, Rmesh, Mat

      Mesh2=1
      J=1

10 Temp = Rbound(J)

      Mesh1 = Mesh2
      Mesh2 = Mesh2 + Rmesh(J)

      If ((I.GE.Mesh1).AND.(I.LE.Mesh2)) then
         R = (Rbound(J+1) - Rbound(J))/(Mesh2-Mesh1)*(I-Mesh1) + Temp
         Goto 1000
      Endif

      J=J+1
      Goto 10

1000 Return
      End
      Subroutine CoolantTemp(Tcoolant)
      *****
      * Uses linear interpolation between values in a table to *
      * return the value of the NaK coolant temperature at the *
      * given axial position Z. If the axial position is out *
      * of the range of the table, this routine returns the *
      * coolant temperature at the bottom or the top of the *
      * core, whichever is appropriate. *
      *
      * Units are degrees K. *
      *****
      Integer Kmax
      Parameter (Kmax = 10)
      Real*8 Z, CoolTbl(2000,2), Zh, Zl, Th, Tl, Tcoolant(Kmax)
      Integer K, Kl
      Common /TTAB/ CoolTbl

      Do 500 Kl=1, Kmax
      If (CoolTbl(1,1).GE.Z(Kl)) then
         Tcoolant(1) = CoolTbl(1,2)
         Goto 500
      Endif

      K = 2

10 If (CoolTbl(K,1).GE.Z(Kl)) then
      Zh = CoolTbl(K,1)
      Zl = CoolTbl(K-1,1)
      Th = CoolTbl(K,2)
      Tl = CoolTbl(K-1,2)
      Tcoolant(Kl) = (Th-Tl)/(Zh-Zl)*(Z(Kl)-Zl) + Tl
      Goto 500
      Else
         K = K+1
      Endif
      Goto 10
500 Continue
      End
      SUBROUTINE cylcon6(te, teav, tc, tcav, tr, phi0, gap, cden_av1,
      & cden_av2, length, edout, ethick, cthick, n, vguess, v, qe1, curden,
      & emheat, colheat)
C      IMPLICIT NONE
      INTEGER n, Kmax
      PARAMETER(Kmax=10)
      REAL*8 te(Kmax), teav(Kmax), tc(Kmax), tcav(Kmax), tr, phi0, gap,
      & cden_av1, cden_av2, length, edout, ethick, cthick, vguess(Kmax),

```

```

      6 v(Kmax),qel(Kmax),curden(Kmax),PI,emheat(Kmax),colheat(Kmax)
      PARAMETER(PI=3.141592654)
C
C     Uses relax, resis_w, resis_nb
C
C*****
C     CYLCON6 cylindrical converter model
C     Control #C-853-001-A-100290
C     Author: John B. McVey
C     Rasor Associates, Inc.
C     (408) 734-1622
C
C     Model to solve for the voltage and current density
C     distributions along the length of a long cylindrical
C     thermionic converter with non-negligible resistance in the
C     converter electrodes. Emitter and collector temperature
C     distributions are specified. Boundary conditions use
C     specified currents at cell ends.
C
C     INPUTS:
C     te      vector of length n holding emitter temper-
C            ature (K) values at mesh points (temper-
C            ature of emitter outer surface)
C     teav    vector holding values of radially averaged
C            emitter temperatures (K)
C     tc      vector of length n holding collector
C            inner surface temperature (K) values at
C            mesh points
C     tcav    vector of radially averaged collector
C            temperatures (K)
C     tr      cesium reservoir temperature in K
C     phi0    emitter bare work function in eV
C     gap     interelectrode gap in cm.
C     cden_av1 total current at z=0 end divided by the
C            area of a half-cell. (A/cm2)
C     cden_av2 total current at z=L end divided by the
C            area of a half-cell. (A/cm2)
C     length  total length L of a cell in cm.
C     edout   emitter outer diameter (cm)
C     ethick  emitter clad thickness (cm)
C     cthick  collector clad thickness (cm)
C     n       number of mesh points
C     vguess  vector of length n holding initial
C            guesses for values of v at mesh points
C
C     OUTPUTS:
C     v       vector of converged values of inter-
C            electrode voltage
C     qel     vector of values for emitter electron
C            cooling (W/cm2)
C     curden  vector of values of current density at
C            mesh points (A/cm2)
C     emheat  volumetric heat generation rate in
C            emitter clad due to ohmic heating (W/cm3)
C     colheat volumetric heat generation rate in
C            collector due to ohmic heating (W/cm3)
C*****
C
C     INTEGER i
C     REAL*8 c(Kmax),p(Kmax),dz,edav,cdin,cdav,resis_w,resis_nb,
C     6 param1,param2,s(Kmax),rhoe(Kmax),rhoc(Kmax),emcur(Kmax)
C
C     dz=length/(n-1)
C     edav=edout-ethick
C     cdin=edout+2.d0*gap
C     cdav=cdin+cthick
C.....Compute "C" coefficients using local resistivities.....
C     do i=1,n
C         rhoe(i)=resis_w(teav(i))
C         rhoc(i)=resis_nb(tcav(i))
C         c(i)=rhoe(i)*edout/(ethick*edav)+rhoc(i)*edout/(cthick*cdav)
C     end do
C.....Compute "P" coefficients using expressions for derivative
C     of "C".....
C     p(1)=(-3.d0*c(1)+4.d0*c(2)-c(3))/(4.d0*c(1))
C     do i=2,n-1
C         p(i)=(c(i+1)-c(i-1))/(4.d0*c(i))
C     end do
C     p(n)=(3.d0*c(n)-4.d0*c(n-1)+c(n-2))/(4.d0*c(n))
C.....v is initially set to vguess.....
C     do i=1,n
C         v(i)=vguess(i)
C     end do
C.....Boundary condition parameters.....

```

```

      param1=c(1)*cden_av1*length*dz
      param2=c(N)*cden_av2*length*dz
C.....Call primary routine for solution of differential equations.....
      call relax(v,c,p,dz,param1,param2,n,te,tc,tr,phi0,gap,qel,
      & curden)
C.....Compute ohmic heat generation rates.....
      s(1)=0.d0
      emcur(1)=-cden_av1*PI*edout*length/2.d0
      emcur(n)=-cden_av2*PI*edout*length/2.d0
      do i=2,n-1
        s(i)=(curden(i)+curden(i-1))*dz/2.d0+s(i-1)
        emcur(i)=PI*edout*s(i)+emcur(1)
      end do
      do i=1,n
C***** Changed by Ron Pawlowski 11/14/90
C      emheat(i)=emcur(i)*emcur(i)*rhoe(i)/(PI*edav*ethick)**2
C      colheat(i)=emcur(i)*emcur(i)*rhoc(i)/(PI*cdav*cthick)**2
        emheat(i)=emcur(i)*emcur(i)*rhoe(i)/(PI*edav*ethick)*dz
        colheat(i)=emcur(i)*emcur(i)*rhoc(i)/(PI*cdav*cthick)*dz
C **** End of changes
      end do
C
C      END
C
C      SUBROUTINE relax(v,c,p,dz,param1,param2,n,te,tc,tr,phi0,gap,
      & qel,curden)
C      IMPLICIT NONE
      INTEGER n,Kmax,ITMAX
      PARAMETER(Kmax=10)
      REAL*8 v(Kmax),c(Kmax),p(Kmax),dz,te(Kmax),tc(Kmax),tr,phi0,gap,
      & qel(Kmax),curden(Kmax),ONE,TWO,THREE,FOUR,cden,TOL,SMALLV,
      & param1,param2
      PARAMETER(ONE=1.d0,TWO=2.d0,THREE=3.d0,
      & FOUR=4.d0,ITMAX=100,TOL=1.e-4,SMALLV=1.d-3)
C
C      Uses cden, tridag
C
C*****
C      Primary routine for solving the differential equation
C      and boundary conditions for the interelectrode voltage.
C      Newton-Raphson method is used to solve equation set
C      resulting from discretization.
C
C      INPUTS:
C      v      initial guesses for v(i)'s
C      qel    vector returns converged values on output
C      c      vector of "C" coefficients
C      p      vector of "P" coefficients
C      dz     mesh spacing (cm)
C      param1 a parameter used in the boundary condition
C             at z=0
C      param2 as for param1, for z=L
C      n      number of mesh points
C      te     vector of length n holding emitter temper-
C             ature (K) values at mesh points
C      tc     vector of length n holding collector temp-
C             erature (K) values at mesh points
C      tr     cesium reservoir temperature in K
C      phi0   emitter bare work function in eV
C      gap    interelectrode gap in cm.
C
C      OUTPUTS:
C      v      vector of converged values of inter-
C             electrode voltage
C      qel    vector of values for emitter electron
C             cooling (W/cm2)
C      curden vector of values of current density at
C             mesh points (A/cm2)
C*****
C      INTEGER i,iter
      REAL*8 dif,jguess,djdv(Kmax),curpls,v2
      REAL*8 f(Kmax),aa(Kmax),bb(Kmax),cc(Kmax),delta(Kmax)
      LOGICAL convrg
C **** Commented out by R.A. Pawlowski, 10/31/90 **
C **** jguess will be set to zero for all calls to cden **
C      SAVE jguess
C.....sub-diagonal elements of Jacobian....
      do i=2,n-1
        aa(i)=ONE+p(i)
      end do

```

```

aa(n)=TWO
C.....super-diagonal elements.....
cc(1)=TWO
do i=2,n-1
  cc(i)=ONE-p(i)
end do
C.....Begin iteration.....
do iter=1,ITMAX
C.....diagonal elements, including dJ/dV calculation.....
do i=1,n
  jguess=0.000
  curden(i)=cden(tc(i),tc(i),tr,phi0,gap,v(i),qel(i),jguess)
C
  jguess=curden(i)
  v2=v(i)+SMALLV
  curpls=cden(tc(i),tc(i),tr,phi0,gap,v2,qel(i),jguess)
  djdv(i)=(curpls-curden(i))/SMALLV
  bb(i)=c(i)*dz*dz+djdv(i)-TWO
end do
C.....compute function values.....
do i=2,n-1
  f(i)=(i-1)*(ONE+p(i))+v(i+1)*(ONE-p(i))+c(i)*dz*dz*
& curden(i)-TWO*v(i)
end do
f(1)=TWO*v(2)-param1*(ONE+p(1))+c(1)*curden(1)*dz*dz-
& TWO*v(1)
f(n)=TWO*v(n-1)-param2*(ONE-p(N))+c(n)*dz*dz*curden(n)-
& TWO*v(n)
C.....solve for corrections delta using tridiagonal routine.....
call tridag(1,n,aa,bb,cc,f,delta)
C.....update voltages.....
do i=1,n
C *** Additions by R.A. Pawlowski 11/6/90 ***
  If (ABS(Delta(i)).le.0.1D0) then
    v(i)=v(i)-delta(i)
  else
    v(i)=v(i)-DSIGN(0.1D0,delta(i))
  endif
C
  Write(*,16) i,v(i)
  Format(' V(',I2,') =',F10.7)
C *** End of additions ***
end do
C.....check for convergence.....
convr=.true.
do i=1,n
  dif=dabs(delta(i))
  if (dif.gt.TOL) convr=.false.
end do
if (convr) goto 10
end do
if (iter.gt.ITMAX) pause 'No convergence'
C.....end of routine - calculate current density using converged v's
C 10 jguess=curden(1)
10 jguess=0.000
do i=1,n
  curden(i)=cden(tc(i),tc(i),tr,phi0,gap,v(i),qel(i),jguess)
C
  jguess=curden(i)
end do
C.....jguess updated for any subsequent call to relax, as when
C calculating an I-V curve.....
C **** Commented out by R.A. Pawlowski on 10/31/90 **
C **** Sometimes updating jguess led to problems with calls to UNIG **
C
  jguess=curden(1)
return
END
C
C
REAL*8 FUNCTION resis_w(t)
C
IMPLICIT NONE
REAL*8 t
C
C.....cubic fit to resistivity of tungsten vs. temperature...
C.....input is temperature in K.....
C
REAL*8 a(4),r
DATA a /-.2285507d0,0.01808205d0,6.64431d-6,-7.479135d-10/
r=a(1)+t*(a(2)+t*(a(3)+t*a(4)))
resis_w=1.d-6*r
return
END
C
C
REAL*8 FUNCTION resis_nb(t)
C
IMPLICIT NONE
REAL*8 t
C
C.....quadratic fit to resistivity of niobium vs. temperature...

```



```

C.....input is temperature in K.....
C
  REAL*8 a(3),r
  DATA a /-1.451331d0,0.04999382d0,-4.867492d-6/
  r=a(1)+t*a(2)+t*a(3)
  resis_nb=1.d-6*r
  return
END
C
C
  REAL*8 FUNCTION resis_mo(t)
  IMPLICIT NONE
  REAL*8 t
C.....linear fit to resistivity of molybdenum vs. temperature...
C.....input is temperature in K.....
C.....This is used for cases with a molybdenum collector and is
C.....thrown in free of charge.....
C
  REAL*8 a(2),r
  DATA a /-.506d0,0.022d0/
  r=a(1)+t*a(2)
  resis_mo=1.d-6*r
  return
END
C
C
  SUBROUTINE tridag(f,l,a,b,c,d,v)
  IMPLICIT NONE
  INTEGER f,l,Kmax
  PARAMETER (Kmax=10)
  REAL*8 a(Kmax),b(Kmax),c(Kmax),d(Kmax),v(Kmax)
C.....Subroutine for solving a tridiagonal linear system of
C.....equations.....
C      f = index of first equation
C      l = index of last equation
C      a = sub-diagonal vector
C      b = diagonal vector
C      c = super-diagonal vector
C      d = vector of right-hand side values
C      v = solution
C
  INTEGER fp1,last,k,i
  REAL*8 beta(101),gamma(101)
  beta(f)=b(f)
  gamma(f)=d(f)/beta(f)
  fp1=f+1
  do i=fp1,l
    beta(i)=b(i)-a(i)*c(i-1)/beta(i-1)
    gamma(i)=(d(i)-a(i)*gamma(i-1))/beta(i)
  end do
  v(l)=gamma(l)
  last=l-f
  do k=1,last
    i=l-k
    v(i)=gamma(i)-c(i)*v(i+1)/beta(i)
  end do
  return
END
C
  REAL*8 FUNCTION cden(te,tc,tr,phi0,d,v,qel,jguess)
  IMPLICIT NONE
  REAL*8 te,tc,tr,phi0,d,v,qel,jguess
C
  Uses jvbrac, jvfind, ndsphi
C
C*****
C
C      The function cden returns current density as a function of
C      voltage utilizing thermionic models which compute voltage
C      as a function of current density. A combination of the
C      TECMDL and UNIG thermionic models are used, which are called
C      by the routines jvbrac and jvfind.
C
C      Input values -
C      te      Emitter temperature (K)
C      tc      Collector temperature (K)
C      tr      Cesium reservoir temperature (K)
C      phi0    Emitter bare work function (eV)
C      d       Interelectrode spacing (cm)
C      v       Output voltage
C      jguess  Guess for current density (amps/cm2)
C
C      Output values -
C      cden   Current density (amps/cm2)
C      qel    Emitter electron cooling (watts/cm2)

```

```

C
C*****
C
C      REAL*8 jvfind,phie,phic,j1,j2,f1,f2,ndsphi
C      LOGICAL success
C
C      ...Get the cesiated work functions...
C      phie=ndsphi(te,tr,phi0)
C      phic=1.9104+(tc/tr)*(2.2963+(tc/tr)*(-3.1364+
C      & (tc/tr)*.98039))
C      if ((te.le.1300.d0).and.(v.ge.0.5d0)) then
C          cden=0.d0
C          qel=0.d0
C          return
C      endif
C      ...Try to bracket the desired current density
C      j1=jguess
C      call jvbrac(te,tc,tr,phie,phic,d,v,j1,j2,f1,f2,success)
C      ...Zero in on the correct current density value.....
C      if (success) then
C          cden=jvfind(te,tc,tr,phie,phic,d,v,j1,j2,f1,f2,qel)
C      else
C          pause ' no match'
C      end if
C
C      return
C      END
C
C
C      SUBROUTINE jvbrac(te,tc,tr,phie,phic,d,v0,x1,x2,f1,f2,success)
C      IMPLICIT NONE
C      REAL*8 te,tc,tr,phie,phic,d,v0,x1,x2,f1,f2,XKE,FACTOR
C      LOGICAL success
C      PARAMETER(XKE=8.6175d-5,FACTOR=1.6d0)
C
C      Uses jvcurve
C
C*****
C      The subroutine jvbrac searches for two current density
C      values which will bracket the desired solution for output
C      voltage.
C
C      Input values -
C      te          Emitter temperature (K)
C      tc          Collector temperature (K)
C      tr          Cesium reservoir temperature (K)
C      phie        Cesiated emitter work function (eV)
C      phic        Cesiated collector work function (eV)
C      d           Interelectrode spacing (cm)
C      v0          Desired value for output voltage
C      x1          Input as first guess for current density
C
C      Output values -
C      x1          Output as one of the bracketing values of
C                  current density
C      x2          The other bracketing value of current density*
C      f1          The value of v - v0 at x1
C      f2          The value of v - v0 at x2
C*****
C
C      REAL*8 dx,x3,f3,v,qel,xjc
C      INTEGER bad
C
C      ...First set the search step to 1 A/cm2.....
C      dx=1.
C      ...Call the combined thermionic model.....
C      call jvcurve(te,tc,tr,phie,phic,d,x1,v,qel)
C      f1=v-v0
C      ...Increment current density in the correct direction...
C      x2=x1+dsign(dx,f1)
C      x2=dmax1(x2,0.d0)
C      ...Compute voltage at new current density.....
C      call jvcurve(te,tc,tr,phie,phic,d,x2,v,qel)
C      f2=v-v0
C      bad=0
C      ...Find the back emission current density for lower search limit..
C      xjc=120.d0*tc*tc*dexp(-11604.5d0*phic/tc)
C      ...Continue searching until solution is bracketed.....
C      do while (f1*f2.gt.0.d0)
C      ...Increase size of search step.....
C      dx=dx*FACTOR
C      x3=x2+dsign(dx,f2)
C      ...Count number of times that current density tries to go
C      below the back emission level. If 2 or more, return

```

```

C      without a successful solution.....
C      if (x3.lt.-xjc) bad=bad+1
C      if (bad.ge.2) then
C          success=.false.
C          return
C      end if
C      x3=dmax1(x3,-xjc)
C      call jvcurve(te,tc,tr,phie,phic,d,x3,v,qel)
C      f3=v-v0
C      x1=x2
C      f1=f2
C      x2=x3
C      f2=f3
C      end do
C      success=.true.
C      return
C      END

C
C
C      REAL*8 FUNCTION jvfind(te,tc,tr,phie,phic,d,v0,j1,j2,f1,f2,qel)
C      IMPLICIT NONE
C      REAL*8 te,tc,tr,phie,phic,d,v0,j1,j2,f1,f2,qel,TOL2
C      PARAMETER(TOL2=1.d-5)

C      Uses jvcurve
C
C      *****
C
C      The function jvfind uses the modified regula falsi method
C      to find a value for current density which yields a desired
C      voltage. The solution must already have been bracketed.
C
C      Input values -
C      te      Emitter temperature (K)
C      tc      Collector temperature (K)
C      tr      Cesium reservoir temperature (K)
C      phie    Cesium emitter work function (eV)
C      phic    Cesium collector work function (eV)
C      d      Interelectrode spacing (cm)
C      v0     Desired value for output voltage
C      j1     One of the bracketing values of current
C            density.
C      j2     The other bracketing value of current density*
C      f1     The value of v - v0 at j1
C      f2     The value of v - v0 at j2
C
C      Output values -
C      jvfind  The solution for the current density
C      qel     The electron cooling at the solution point
C
C      *****

C      REAL*8 toll,save_f,j3,f3,v

C      toll=1.d-5
C      save_f=f1
C      10 continue
C          j3=j2-f2*(j2-j1)/(f2-f1)
C          call jvcurve(te,tc,tr,phie,phic,d,j3,v,qel)
C          f3=v-v0
C      C.....Re-assign whichever endpoint has the same sign of f as the most
C      recent point. If an endpoint has been stagnant for 2 passes,
C      replace f with f/2 there.....
C          if (f3*f1.lt.0.d0) then
C              j2=j3
C              f2=f3
C              if (f3*save_f.gt.0.d0) f1=f1/2.d0
C          else
C              j1=j3
C              f1=f3
C              if (f3*save_f.gt.0.d0) f2=f2/2.d0
C          end if
C          save_f=f3
C          if (.not.((dabs(j1-j2).le.toll).or.(dabs(f3).le.TOL2))) goto 10
C          jvfind=j3
C          return
C      END

C
C
C      SUBROUTINE jvcurve(te,tc,tr,phie,phic,dcm,j,v,qel)
C      IMPLICIT NONE
C      REAL*8 te,tc,tr,phie,phic,dcm,j,v,qel,JLOW,JHIGH
C      PARAMETER(JLOW=0.1d0, JHIGH=3.d0)
C      Uses tecmdl, unig
C
C      *****

```

```

C
C The routine jvcurve combines the outputs of TECMDL and UNIG *
C to produce a single, physically reasonable, well-behaved *
C volt-ampere curve. The limits JHIGH and JLOW are used to *
C save computational effort by only calling both models in the *
C interval bounded by these limits. Above JHIGH only TECMDL *
C is called, below JLOW only UNIG is called. *
C
C Input values - *
C te Emitter temperature (K) *
C tc Collector temperature (K) *
C tr Cesium reservoir temperature (K) *
C phie Cesium emitter work function (eV) *
C phic Cesium collector work function (eV) *
C dcm Interelectrode spacing (cm) *
C j Current density (amps/cm2) *
C
C Output values - *
C v Output voltage *
C qel Emitter electron cooling (watts/cm2) *
C
C*****
C INTEGER sheaths
C REAL*8 dmm,vig,qelig,vun,qelun,ji,jel,old
C
C dmm=dcm*10.d0
C if (j.lt.JLOW) then
C   jel=j
C....A simple iteration is necessary when calling unig as it
C accepts the electron current as an independent variable,
C whereas the total current = electron current - ion current....
C 10 continue
C   old=jel
C   call unig(te,tc,tr,dcm,phie,phic,jel,ji,v,qel,sheaths)
C   jel=j+ji
C   if (dabs((jel-old)/jel).gt.1.d-5) go to 10
C   print*,v=',v','unig j =',jel-ji
C else if (j.gt.JHIGH) then
C   call tecmdl(te,tc,tr,phie,phic,dmm,j,v,qel)
C   print*,v=',v','tecmdl j =',j
C else
C   jel=j
C 20 continue
C   old=jel
C   call unig(te,tc,tr,dcm,phie,phic,jel,ji,vun,qelun,sheaths)
C   jel=j+ji
C   if (dabs((jel-old)/jel).gt.1.d-6) go to 20
C   print*,v=',v','unig j =',jel-ji
C   call tecmdl(te,tc,tr,phie,phic,dmm,j,vig,qelig)
C   print*,v=',v','tecmdl j =',j
C....Select whichever voltage (and corresponding electron cooling)
C is higher.....
C   if (vig.ge.vun) then
C     v=vig
C     qel=qelig
C   else
C     v=vun
C     qel=qelun
C   end if
C   print*,v=',v','chosen j =',j
C end if
C return
C END
C SUBROUTINE tecmdl(te,tc,tr,phie,phic,d,j,vout,qel)
C IMPLICIT NONE
C REAL*8 te,tc,tr,phie,phic,d,j,vout,qel,VI,B,H,BP,XK,TWO,
C AR,HALF
C PARAMETER (VI=3.2d0,B=30.d0,H=5.d0,BP=50.d0,XK=8.6175d-5,
C TWO=2.d0,AR=120.d0,HALF=0.5d0)
C
C Uses ndsphi,obstr,obstr2,satur,satur2
C*****
C
C C-563-002-G-082988
C Written by
C John B. McVey
C Razor Associates, Inc.
C (408) 734-1622 X-315
C
C TECMDL is an implementation of the "phenomenological *
C model" of the ignited mode converter described in *
C N.S. Razor, "Thermionic Energy Conversion", Chapter *
C 5 of Applied Atomic Collision Physics, vol. 5, *
C Massey, McDaniel, and Bederson eds., Academic Press, *
C 1982. The article is available on request from *

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C      Razor Associates. The following physics has been *
C      added to the model: *
C      A. Plasma energy loss by radiation. *
C      B. Improved description of saturation *
C      region. *
C      C. Provision for ion-retaining collector *
C      sheath. *
C      The equations are documented in the Razor document *
C      E-563-002-A-063087, which is available on request. *
C      *
C      This routine calls four subroutines, two for the *
C      obstructed mode (positive and negative collector *
C      sheath) and two for the saturation region (positive *
C      and negative collector sheath) as required. It *
C      calculates the output voltage and emitter electron *
C      cooling. *
C      *
C      Input values - *
C      TE      Emitter temperature (K) *
C      TC      Collector temperature (K) *
C      TR      Cesium reservoir temperature (K) *
C      PHIE    Emitter work function (eV). *
C      PHIC    Collector work function (eV). *
C      D      Interelectrode spacing (mm) *
C      J      Current density (amps/cm2) *
C      *
C      Output values - *
C      VOUT    Output voltage (volts) *
C      QEL     Net emitter electron cooling (watts/cm2) *
C      *
C      Version G is special for use in CYLCON6. *
C      - calculation of cesiated work functions removed *
C      - changed to double precision *
C      - parameter jconfdnc removed *
C      *
C      *****
C
      REAL*8 jsp,jc,jcj,pcs,ta,
      &      pd,tee,tec,ve,vc,vd,vrad,jej,je,dv,
      &      js,jij,js,phis
C
C.....Calculate saturation current density.....
      jsp=AR*te*te*dexp(-phie/(XK*te))
C
C.....Calculate back emission current density and ratio.....
      jc=AR*tc*tc*dexp(-phic/(XK*tc))
      jcj=jc/j
C
C.....Calculate cesium pressure in torr.....
      pcs=2.45d+8*dexp(-8910.d0/tr)/dsqrt(tr)
C
C.....Average neutral and ion temperature.....
      ta=(te+tc)/TWO
C
C.....Calculate Pd.....
      pd=pcs*d
C
C.....Call the obstructed region calculation
C      (can't be obstructed if current density is
C      above saturation).....
      if (j.le.jsp) then
C
C.....Calculation for positive collector sheath.....
      call obstr(VI,B,H,j,jcj,te,tc,tr,pd,d,ta,tee,tec,ve,vc,
      &      vd,vrad,jej)
C
C.....If collector sheath was negative in previous calculation,
C      use appropriate calculation.....
      if (vc.lt.0.d0) call obstr2(VI,B,H,j,jcj,te,tc,tr,pd,d,ta,
      &      tee,tec,ve,vc,vd,vrad,jej)
C
C.....Calculate effective emitted current density.....
      je=jej*j
C
C.....Calculate sheath barrier height.....
      dv=XK*te*dlog(jsp/je)
C
C.....Calculate output voltage.....
      vout=phie-phic-vd+dv
C
C.....Calculate net electron cooling from emitter
C      (includes plasma radiation).....
      qel=j*(phie+dv+TWO*XK*tee)-je*TWO*XK*(tee-te)-
      &      HALF*j*vrad
C
      endif

```

```

C
C.....Call the saturation region calculation if above saturation
C      or if obstructed region calculation failed.....
C      if ((j.gt.jsp).or.(dv.lt.0.d0)) then
C
C.....Calculation for positive collector sheath.....
C      call satur(VI,B,EP,H,j,jc,jsp,te,tc,tr,pd,d,ta,tee,tec,
C      ve,vc,vd,vrad,jsj,ji)
C
C.....Calculation for negative collector sheath if previous
C      calculation gave negative value.....
C      if (vc.lt.0.d0) call satur2(VI,B,EP,H,j,
C      jc,jsp,te,tc,tr,pd,d,ta,tee,tec,ve,vc,vd,vrad,jsj,
C      ji)
C
C.....Calculate effective Schottky saturation current density.....
C      js=jsj*j
C
C.....Calculate Schottky reduced emitter work function.....
C      phis=KK*te*dlog(AR*te*te/js)
C
C.....Calculate output voltage.....
C      vout=phis-phis-vc
C
C.....Calculate net emitter electron cooling (includes
C      ion heating and plasma radiation).....
C      qel=j*(phis+TWO*KK*tee)-js*TWO*KK*(tee-te)+j*ji*(ve+3.89d0+
C      TWO*KK*tee)-HALF*j*vrad
C
C      endif
C      return
C      END
C
C
C      SUBROUTINE obstr(vi,b,h,j,jc,j,te,tc,tr,pd,d,ta,tee,tec,ve,vc,
C      vd,vrad,je)
C      IMPLICIT NONE
C      INTEGER MAXITR
C      REAL*8 vi,b,h,j,jc,j,te,tc,tr,pd,d,ta,tee,tec,ve,vc,vd,vrad,
C      je,j,KK,HALF,TOL,AR,EMIS,ONE,TWO,THREE,TINY
C      PARAMETER (XX=8.6175d-5,TWO=2.d0,HALF=.5d0,TOL=1.d-5,AR=120.d0,
C      EMIS=.4d0,MAXITR=50,ONE=1.d0,THREE=3.d0,TINY=1.d-32)
C
C      Uses tsc, ltec
C
C.....*****
C
C      OBSTR is called by TECMDL to implement the
C      phenomenological equations for
C      the obstructed region of the ignited mode volt-
C      ampere curve with a positive (electron retaining)
C      sheath at the collector. This is the formulation
C      described in Massey, McDaniel, and Bederson.
C      Equations (24)-(29) and (31) are used. The emitter
C      side and collector side electron temperatures are
C      subject to LTE (Local Thermodynamic Equilibrium)
C      constraints which are implemented by the function
C      TSC and the subroutine LTE. Equations (24) for
C      JE/J and (25) for Vd are coupled, and are solved
C      iteratively using a secant method search.
C
C      Input values -
C      VI      Effective ionization energy (eV)
C      B      Ionizability factor
C      H      Collector current factor
C      J      Current density (amps/cm2)
C      JCJ     Ratio of back emission to current density
C      TE      Emitter temperature (K)
C      TC      Collector temperature (K)
C      TR      Cesium reservoir temperature (K)
C      PD      Pressure-spacing product (torr-mm)
C      D      Interelectrode spacing (mm)
C      TA      Average neutral and ion temperature (K)
C
C      Output values -
C      TEE     Emitter side electron temperature (K)
C      TEC     Collector side electron temperature (K)
C      VE      Emitter sheath height (eV)
C      VC      Collector sheath height (eV)
C      VD      Arc drop (eV)
C      VRAD    Plasma radiation component of arc drop (eV)
C      JEJ     Ratio JE/J of effective emitted current
C              density to working current density
C.....*****
C

```

```

INTEGER iter
REAL*8 dlea,phinc,jnc,hs,tsc,telect,dl,r,ans,dif,
& oldj,olddif,newj,param1,param2,param3,param4
LOGICAL first,ltec
C
C.....Calculate ratio of spacing to electron-neutral
C mean free path.....
dlea=35.d0/((te+tc)/2000.d0)*pd
C
C.....Calculate emitter side electron temperature.....
tee=VI/(TWO*XK*dlog(B*dlea))
C
C.....Calculate collector side electron temperature.....
tec=(THREE*tee+TWO*tc*jcj)/(dlog((H+HALF)/
& (ONE+jcj))+TWO*jcj+THREE)
C
C.....Calculate neutralization potential and current density.....
phinc=1.7d0+.383d0*tec/tr
jnc=AR*tec*tec*dexp(-phinc/(XK*tec))
C
C.....Assign value to LTE limit for H and check
C to see if LTE limits the electron temperature
C at the collector edge - if so, calculate a new
C TEC value.....
hs=jnc/j
if (hs.lt.h) then
tec=tsc(tee,tc,tr,hs,j,cj)
ltec=.true.
else
ltec=.false.
endif
C
C.....Calculate average electron temperature.....
telect=(tee+tec)/TWO
C
C.....Calculate ratio of spacing to total
C electron mean free path, including
C ion scattering.....
dl=dlea+3.4d+7*j*d/((telect**2.5d0)
C
C.....If LTE has occurred at the collector edge, the routine
C LTE is called to check that the average electron
C temperature is above the bulk LTE limit. If not,
C the LTE routine will calculate new emitter side,
C collector side, and average electron temperatures
C The ratio of spacing to total mean free path is also
C recalculated.....
if (ltec) call lte(tee,tec,telect,tc,tr,hs,j,cj,dl,dlea,d)
C
C.....Calculate collector sheath height.....
vc=THREE*XK*(tee-tec)-TWO*xk*(tec-tc)*jcj
C
C.....Calculate collector reflection factor.....
r=(ONE+jcj)*dexp(vc/(XK*tec))-ONE
C
C.....Calculate radiation component of arc drop.....
vrad=9.65d+5*pd/(j*ta)*dexp(-2.d0/(XK*telect))*(ONE+.069d0
& *dexp(.58d0/(XK*telect))*(EMIS/dsqrt(d/10.d0)+HALF))
C
C.....Guess JEJ and enter secant method iteration.....
jej=TWO
first=.true.
C
C.....First compute some parameters in order to save time in the
C iteration loop.....
param1=TWO*XK*(tec-te+(tec-tc)*jcj)+vrad
param2=TWO*XK*(tee-te)
param3=.75d0*dl+r
param4=-ONE/(XK*tee)
C.....Start iteration.....
do iter=1,MAXITR
C.....Calculate arc drop.....
vd=param2*(jej-ONE)+param1
C
C.....Calculate emitter sheath height.....
ve=vd+vc
C
C.....Calculate answer for JEJ and compute difference from
C guess for JEJ.....
if (ve*param4.le.dlog(TINY)) then
C.....Case for ve so large that the exp function would underflow..
ans=ONE
else
C.....Normal case.....
ans=ONE+param3*dexp(ve*param4)
endif
endif

```

```

      dif=jej-ans
      if (dabs(dif).lt.TOL) go to 10
C
C.....Update value of JEJ until convergence.....
      if (first) then
        oldj=jej
        olddif=dif
        jej=jej-dsign(.2d0,dif)
        first=.false.
      else
        newj=(oldj*dif-jej*olddif)/(dif-olddif)
        oldj=jej
        olddif=dif
        jej=newj
      endif
      if (dabs(jej-oldj).lt.1.d-5*jej) go to 10
    enddo
  10  if (iter.gt.MAXITR) pause 'Exceeded maximum iterations in
      sobstr'
      return
      END
C
C
      SUBROUTINE satur(vi,b,bp,h,j,jcj,jsp,te,tc,tr,pd,d,ta,tee,tec,
& ve,vc,vd,vrad,jsj,jij)
C
      IMPLICIT NONE
      INTEGER MAXITR
      REAL*8 vi,b,bp,h,j,jcj,jsp,te,tc,tr,pd,d,ta,tee,tec,ve,vc,vd,
& vrad,jsj,jij,KK,TWO,HALF,TOL1,TOL2,AR,EMIS,ONE,THREE,TINY
      PARAMETER (KK=8.6175d-5,TWO=2.d0,HALF=.5d0,TOL1=1.d-6,TOL2=1.d-5,
& MAXITR=100,AR=120.d0,EMIS=.4d0,ONE=1.d0,THREE=3.d0,
& TINY=1.d-32)
C
      Uses tsc, ltec
C
C
C.....
C
      SATUR is called by TECMDL to implement the phenom- *
      ological model equations in the saturation region, *
      with a positive collector sheath. The formulation *
      given by eqs. (33) to (35) in Massey, McDaniel, and *
      Bederson has been improved so that is consistent *
      with the level of complexity used in the obstructed *
      region calculation. The ion current into the *
      emitter is now included in all equations in the form *
      of the parameter JIJ (Ji/J). An additional *
      iteration over what was needed in the obstructed *
      mode calculation is required for finding the value *
      of JIJ. A modified linear interpolation method is *
      used. The iteration for finding VD and JEJ is *
      nested within this new iteration. *
      *
      Input values - *
      VI Effective ionization energy (eV) *
      B Ionizability factor *
      BP Temperature increase parameter *
      H Collector current factor *
      J Current density (amps/cm2) *
      JCJ Ratio of back emission to current density *
      TE Emitter temperature (K) *
      TC Collector temperature (K) *
      TR Cesium reservoir temperature (K) *
      PD Pressure-spacing product (torr-mm) *
      D Interelectrode spacing (mm) *
      TA Average neutral and ion temperature (K) *
      *
      Output values - *
      TEE Emitter side electron temperature (K) *
      TEC Collector side electron temperature (K) *
      VE Emitter sheath height (eV) *
      VC Collector sheath height (eV) *
      VD Arc drop (eV) *
      VRAD Plasma radiation component of arc drop (eV) *
      JSJ Ratio JS/J of effective emitted current *
      density to working current density *
      JIJ Ratio Ji/J of additional ion current to *
      the emitter to working current density *
      *
C.....
C
      INTEGER iwch,iter1,iter2
      REAL*8 dlea,phinc,jnc,hs,tsc,telect,dl,r,ans,f,oldj,
& oldf,newj,param1,param2,param3,param4,js,g,
& x1,x2,x3,y1,y2,y3,ys
      LOGICAL first,ltec

```



```

C.....Guess ion current ratio.....
      jij=0.d0
C
C.....Set iteration counter.....
      iwhch=1
C
C.....Calculate ratio of gap to electron-neutral mean free path.....
      dlea=35.d0/((te+tc)/2000.d0)*pd
C
C.....Begin modified linear interpolation search for JIJ.....
C
      do iter1=1,MAXITR
C.....Calculate emitter side electron temperature.....
      tee=vi/(TWO*XK*dlog(b*dlea)-XK*dlog(ONE-bp*jij))
C
C.....Calculate collector side electron temperature.....
      tec=(THREE*tee+TWO*tc*jcj)/(dlog((h+HALF)/
      & (ONE+jcj))+TWO*jcj+THREE)
C
C.....Calculate neutralization potential and current density.....
      phinc=1.7d0+.383d0*tec/tr
      jnc=AR*tec*tec*dexp(-phinc/(XK*tec))
C
C.....Assign value to LTE limit for H and check
C      to see if LTE limits the electron temperature
C      at the collector edge - if so, calculate a new
C      TEC value.....
      hs=jnc/j
      if (hs.lt.h) then
        tec=tsc(tee,tc,tr,hs,j,jcj)
        ltec=.true.
      else
        ltec=.false.
      endif
C
C.....Calculate average electron temperature.....
      telect=(tee+tec)/TWO
C
C.....Calculate ratio of spacing to total
C      electron mean free path, including
C      ion scattering.....
      dl=dlea+3.4d+7*j*d/(telect**2.5d0)
C
C.....If LTE has occurred at the collector edge, the routine
C      LTE is called to check that the average electron
C      temperature is above the bulk LTE limit. If not,
C      the LTE routine will calculate new emitter side,
C      collector side, and average electron temperatures
C      The ratio of spacing to total mean free path is also
C      recalculated.....
      if (ltec) call lte(tee,tec,telect,tc,tr,hs,j,jcj,dl,dlea,d)
C
C.....Calculate collector sheath height.....
      vc=THREE*XK*(tee-tec)-TWO*XK*(tec-tc)*jcj
C
C.....Calculate collector reflection factor.....
      r=(ONE+jcj)*dexp(vc/(XK*tec))-ONE
C
C.....Calculate radiation component of arc drop.....
      vrad=9.65d+5*pd/(j*ta)*dexp(-2.d0/(XK*telect))*
      & (ONE+.069d0*dexp(.58d0/(XK*telect))*
      & (EMIS/dsqrt(d/10.d0)+HALF))
C
C.....Guess JSJ and enter secant method iteration.....
      jsj=2.d0
      first=.true.
C
C.....First compute some parameters in order to save time
C      in the iteration loop
      param1=TWO*XK*(tec-te+(tec-tc)*jcj)+vrad-jij*(vc+
      & 3.89d0+TWO*XK*tee)
      param2=TWO*XK*(tee-te)
      param3=.75d0*dl+r
      param4=-ONE/(XK*tee)
C.....Start iteration.....
      do iter2=1,MAXITR
C.....Calculate arc drop.....
      vd=(param2*(jsj-ONE)+param1)/(ONE+jij)
C
C.....Calculate emitter sheath height.....
      ve=vd+vc
C
C.....Calculate answer for JSJ and compute difference from
C      guess for JSJ ....
      if (ve*param4.le.dlog(TINY)) then
C.....Case for ve so large that exp function would underflow.....

```

```

        ans=ONE+jij
    else
C.....Normal case.....
        ans=ONE+(param3-HALF*jij)*dexp(ve*param4)+jij
    endif
    f=jsj-ans
    if (dabs(f).lt.TOL1) go to 20
C
C.....Update value of JSJ until convergence.....
    if (first) then
        oldj=jsj
        oldf=f
        jsj=jsj-dsign(.2d0,f)
        first=.false.
    else
        newj=(oldj*f-jsj*oldf)/(f-oldf)
        oldj=jsj
        oldf=f
        jsj=newj
    endif
    if (dabs(jsj-oldj).lt.1.d-5*jsj) go to 20
    enddo
20    if (iter2.gt.MAXITR) pause 'Exceeded maximum iterations in
    $SATUR for finding current ratio'
C
C.....Calculate value of JS from eqn. (35) of Massey,
C    McDaniel, and Bederson.....
    js=jsp*dexp(612.d0*dsqrt(dsqrt(-j*jij*dsqrt(ve))))/te)
C
C.....Compute error term.....
    g=js/i-jsj
    if (dabs(g).lt.TOL2) go to 30
C
C.....Update JIJ to make error small.....
    if (iwhch.eq.1) then
        if ((g.gt.0.d0).and.(vc.le.0.d0)) return
        x1=jij
        y1=g
        jij=-.1d0
        x2=jij
        iwhch=2
    else if (iwhch.eq.2) then
        x2=jij
        y2=g
        if (y1*y2.gt.0.d0) then
            x1=x2
            y1=y2
        jij=jij+dsign(.1d0,g)
C.....Prevent jij from becoming equal to -1. Make it the
C    nearest larger number.....
        if (jij.le.-ONE) jij=-.999999d0
    else
        iwhch=3
        ys=y2
        jij=(x1*y2-x2*y1)/(y2-y1)
    endif
    else if (iwhch.eq.3) then
        x3=jij
        y3=g
        if (y3*y1.lt.0.d0) then
            x2=x3
            y2=y3
            if (y3*ys.gt.0.d0) y1=y1/TWO
        else
            x1=x3
            y1=y3
            if (y3*ys.gt.0.d0) y2=y2/TWO
        endif
        ys=y3
        jij=(x1*y2-x2*y1)/(y2-y1)
    endif
    enddo
30    if (iter1.gt.MAXITR) then
c        write(*,'(a)') ' Maximum iterations exceeded in
c        $SATUR2 for finding ion current'
        write(8,'(a)') ' Maximum iterations exceeded in
c        $SATUR2 for finding ion current'
c        write(*,*) j,tr
        write(8,*) j,tr
        stop
    endif
    return
END
C
C
REAL*8 FUNCTION tsc(tee,tc,tr,hs,j,jc)

```

```

C      IMPLICIT NONE
C      INTEGER MAXITR
C      REAL*8 tee,tc,tr,hs,j,jcj,XK,ONE,TWO,THREE,TOL,AR,HALF
C      PARAMETER (XK=8.6175d-5,ONE=1.d0,TWO=2.d0,THREE=3.d0,TOL=
C      1.d-5,AR=120.d0,MAXITR=50,HALF=.5d0)
C
C      *****
C      The function TSC is called by the subroutines OBSTR *
C      and SATUR in order to compute the collector side *
C      electron temperature when LTE conditions exist at the *
C      collector. A secant method iteration is used. *
C      *
C      Input values - *
C      TEE      Emitter side electron temperature (K) *
C      TC       Collector temperature (K) *
C      TR       Cesium reservoir temperature (K) *
C      HS       Ratio of neutralization current Jn to *
C              Current density J *
C      J        Current density (amps/cm2) *
C      JCJ      Ratio of back emission to current den- *
C              sity *
C      *
C      Output values - *
C      TSC      LTE value for electron temperature at *
C              collector edge of plasma *
C      *
C      *****
C
C      INTEGER iter
C      REAL*8 r1,dh,phinc,jnc,param1,param2,hss,dif,oldh,
C      olddif,newh
C      LOGICAL first,goon
C
C      C.....Calculate numerator.....
C      r1=THREE*tee+TWO*tc*jcj
C
C      C.....Enter iteration
C
C      first=.true.
C      goon=.false.
C      dh=ONE
C      param1=TWO*jcj+THREE
C      param2=ONE+jcj
C      do iter=1,MAXITR
C      C.....Calculate collector edge electron temperature.....
C      tsc=r1/(dlog((hs+HALF)/param2)+param1)
C
C      C.....Calculate neutralization work function and current density.....
C      phinc=1.7d0+.383d0*tsc/tr
C      jnc=AR*tsc**2*dexp(-phinc/(XK*tsc))
C
C      C.....Find answer for HS, difference between guess and answer.....
C      hss=jnc/j
C      dif=hs-hss
C      if (dabs(dif).lt.TOL) go to 40
C
C      C.....Update HS to make difference small.....
C      if (first) then
C      oldh=hs
C      olddif=dif
C      hs=hs-dsign(dh,dif)
C      hs=dmax1(hs,1.0d-12)
C      first=.false.
C      dh=dh*1.6d0
C      else
C      if (.not.goon) then
C      if (dif*olddif.gt.0.d0) then
C      newh=hs-dsign(dh,dif)
C      newh=dmax1(newh,1.d-12)
C      dh=1.6d0*dh
C      else
C      goon=.true.
C      newh=(oldh*dif-hs*olddif)/(dif-olddif)
C      endif
C      else
C      newh=(oldh*dif-hs*olddif)/(dif-olddif)
C      endif
C      oldh=hs
C      olddif=dif
C      hs=newh
C      endif
C      if (dabs(hs-oldh).lt.1.d-5*hs) go to 40
C      enddo
C      if (iter.gt.MAXITR) pause 'Exceeded maximum iterations in TSC'
C      return
40

```

```

END
C
C
SUBROUTINE lte(tee,tec,tav,tc,tr,hs,j,jcj,dl,dlea,d)
C
IMPLICIT NONE
C
INTEGER MAXITR
REAL*8 tee,tec,tav,tc,tr,hs,j,jcj,dl,dlea,d,XK,
C
PARAMETER (XK=8.6175d-5,ONE=1.d0,TWO=2.d0,THREE=3.d0,TOL=
C
1.d-5,AR=120.d0,MAXITR=50,HALF=.5d0)
C
C*****
C
C The routine LTE is called by OBSTR and SATUR in order *
C to check, and possibly recalculate, the electron *
C temperatures in order to keep the average electron *
C temperature above the LTE limit for the bulk plasma. *
C This is briefly discussed in Appendix B of Chapter 5 *
C in Massey, McDaniel, and Bederson. *
C
C Input values - *
C TEE Electron temperature at emitter edge (K) *
C TEC Electron temperature at collector edge (K) *
C TAV Average electron temperature (K) *
C TC Collector temperature (K) *
C TR Cesium reservoir temperature (K) *
C HS Ratio of neutralization current to current *
C density *
C J Current density (amps/cm2) *
C JCJ Ratio of back emission to current density *
C DL Ratio of gap to total electron mean free *
C path *
C DLEA Ratio of gap to electron-neutral mean *
C free path *
C D Interelectrode gap (mm) *
C
C Output values (recalculated) - *
C TEE *
C TEC *
C TAV *
C DL *
C*****
C
INTEGER iter1,iter2
REAL*8 ts,dll,tss,dif,oldt,olddif,newt,r1,dh,
C
phinc,jnc,hss,oldh,newh,tsc,param1,param2
LOGICAL first,goon
C
C.....First guess for TS.....
ts=tav
first=.true.
dh=TWO
C
C.....Enter secant method search for TS.....
C
C.....Calculate new value for ratio of gap to mean free path.....
do iter1=1,MAXITR
dll=dlea+3.4d+7*j*d/ts**2.5d0
C
C.....Calculate an answer for TS.....
tss=1.7d0/(XK*dlog((AR*ts*ts)/(j*dll)))-.383d0/tr
C
C.....Find difference between guess and answer.....
dif=ts-tss
if (dabs(dif).lt.TOL) go to 50
C
C.....Update TS to make difference small.....
if (first) then
oldt=ts
olddif=dif
ts=ts-dsign(50.d0,dif)
first=.false.
else
newt=(oldt*dif-ts*olddif)/(dif-olddif)
oldt=ts
olddif=dif
ts=newt
endif
if (dabs(ts-oldt).lt.1.d-5*ts) go to 50
enddo
50 if (iter1.gt.MAXITR) pause 'Max. iterations exceeded in LTE'
C
C.....Check to see if average electron temperature is above
C the limit. If so, return without altering any
C values.....

```

```

      if (tav.ge.ts) return
C
C.....If bulk LTE is in effect, replace TAV and DL with their
C proper LTE values.....
      tav=ts
      dl=dll
C
C.....TEC must now be recalculated, since it depends on TEE,
C which will change to keep the average temperature
C above its limit. An iteration like that in the function
C TSC is used.....
      first=.true.
      goon=.false.
      r1=TWO*THREE*ts+TWO*tc*jcj
      dh=TWO
C
C.....Begin iteration.....
      param1=TWO*(jcj+THREE)
      param2=ONE+jcj
      do iter2=1,MAXITR
C.....Calculate collector edge electron temperature.....
      tsc=r1/(dlog((hs+HALF)/param2)+param1)
      phinc=1.7d0+.383d0*tsc/tr
      jnc=AR*tsc**2*dexp(-phinc/(XK*tsc))
      hss=jnc/j
      dif=hs-hss
      if (dabs(dif).lt.TOL) go to 60
      if (first) then
        oldh=hs
        olddif=dif
        hs=hs-dsign(dh,dif)
        hs=dmax1(hs,1.d-12)
        first=.false.
        dh=1.6d0*dh
      else
        if (.not.goon) then
          if (dif*olddif.gt.0.d0) then
            newh=hs-dsign(dh,dif)
            newh=dmax1(newh,1.d-12)
            dh=1.6d0*dh
          else
            goon=.true.
            newh=(oldh*dif-hs*olddif)/(dif-olddif)
          endif
        else
          newh=(oldh*dif-hs*olddif)/(dif-olddif)
        endif
        oldh=hs
        olddif=dif
        hs=newh
      endif
      if (dabs(hs-oldh).lt.1.d-5*hs) go to 60
    enddo
  60 if (iter2.gt.MAXITR) pause 'Max. iterations exceeded in LTE'
C.....Recompute TEC.....
      tec=tsc
C
C.....Recompute TEE.....
      tee=TWO*ts-tsc
      return
      END
C
C
      SUBROUTINE obstr2(vi,b,h,j,jcj,te,tc,tr,pd,d,ta,tee,tec,ve,vc,
      & vd,vrad,jej)
C
C IMPLICIT NONE
C INTEGER MAXITR
C REAL*8 vi,b,h,j,jcj,te,tc,tr,pd,d,ta,tee,tec,ve,vc,vd,vrad,
      & jej,XK,HALF,TOL,AR,EMIS,ONE,TWO,THREE,TINY
C PARAMETER (XK=8.6175d-5,TWO=2.d0,HALF=.5d0,TOL=1.d-5,AR=120.d0,
      & EMIS=.4d0,MAXITR=50,ONE=1.d0,THREE=3.d0,TINY=1.d-32)
C
C Uses tsc2, ltec2
C
C*****
C
C OBSTR2 is called by TECMDL to implement the
C phenomenological equations for the obstructed
C region of the ignited mode volt-ampere curve with
C a negative (ion retaining) sheath at the collector.
C The emitter side and collector side electron
C temperatures are subject to LTE (Local Thermodynamic
C Equilibrium) constraints which are implemented by
C the function TSC2 and the subroutine LTE2. The sub-
C routine is very similar to OBSTR except that the
C equations for TEC and VC and the LTE routines are

```

```

C      different.
C
C      Input values -
C      VI      Effective ionization energy (eV)
C      B       Ionizability factor
C      H       Collector current factor
C      J       Current density (amps/cm2)
C      JCJ     Ratio of back emission to current density
C      TE      Emitter temperature (K)
C      TC      Collector temperature (K)
C      TR      Cesium reservoir temperature (K)
C      PD      Pressure-spacing product (torr-mm)
C      D       Interelectrode spacing (mm)
C      TA      Average neutral and ion temperature (K)
C
C      Output values -
C      TEE     Emitter side electron temperature (K)
C      TEC     Collector side electron temperature (K)
C      VE      Emitter sheath height (eV)
C      VC      Collector sheath height (eV)
C      VD      Arc drop (eV)
C      VRAD    Plasma radiation component of arc drop (eV)
C      JEJ     Ratio JE/J of effective emitted current
C              density to working current density
C
C*****
C
C      INTEGER iter
C      REAL*8 dlea,zetac,phinc,jnc,hs,tsc2,telect,dl,r,ans,dif,
C      & oldj,olddif,newj,param1,param2,param3,param4
C      LOGICAL first,ltec
C
C.....Calculate ratio of spacing to electron-neutral
C      mean free path.....
C      dlea=35.d0/((te+tc)/2000.d0)*pd
C
C.....Calculate emitter side electron temperature.....
C      tee=vi/(TWO*KK*dlog(b*dlea))
C
C.....Calculate collector sheath attenuation factor.....
C      zetac=(-(h+HALF)+dsqrt((h+HALF)**2+8.d0*jcj*h))/
C      & (TWO*jcj)
C
C.....Calculate collector sheath height.....
C      vc=KK*tc*dlog(zetac)
C
C.....Calculate collector emission factor.....
C      r=jcj*dexp(vc/(KK*tc))
C
C.....Calculate collector side electron temperature.....
C      tec=(THREE*tee+TWO*tc*r)/(TWO*r+THREE)
C
C.....Calculate neutralization potential and current density.....
C      phinc=1.7d0+.383d0*tec/tr
C      jnc=AR*tec*tec*dexp(-phinc/(KK*tec))
C
C.....Assign value to LTE limit for H and check
C      to see if LTE limits the electron temperature
C      at the collector edge - if so, calculate new
C      values for TEC, VC, and R.....
C      hs=jnc/j
C      if ((r+HALF).gt.hs) then
C          tec=tsc2(tee,tc,tr,hs,j,cj,vc)
C          r=hs-HALF
C          ltec=.true.
C      else
C          ltec=.false.
C      endif
C
C.....Calculate average electron temperature.....
C      telect=(tee+tec)/TWO
C
C.....Calculate ratio of spacing to total
C      electron mean free path, including
C      ion scattering.....
C      dl=dlea+3.4d+7*j*d/(telect**2.5d0)
C
C.....If LTE has occurred at the collector edge, the routine
C      LTE is called to check that the average electron
C      temperature is above the bulk LTE limit. If not,
C      the LTE routine will calculate new emitter side,
C      collector side, and average electron temperatures
C      The ratio of spacing to total mean free path is also
C      recalculated.....
C      if (ltec) call lte2(tee,tec,telect,tc,tr,hs,j,cj,vc,dl,dlea,
C      & d,r)

```

```

C
C.....Calculate radiation component of arc drop.....
      vrad=9.65d+5*pd/(j*ta)*dexp(-2.d0/(XK*telect))*
      & (ONE+.069d0*dexp(.58d0/(XK*telect))
      & *(EMIS/dsqrt(d/10.d0)+HALF)
C
C.....Guess JEJ and enter secant method iteration.....
      jej=TWO
      first=.true.
C
C.....First compute some parameters in order to save time in the
C      iteration.....
      param1=TWO*XK*(tec-te+(tec-tc)*r)+vrad
      param2=TWO*XK*(tee-te)
      param3=.75d0*d1+r
      param4=-ONE/(XK*tee)
C.....Start iteration.....
      do iter=1,MAXITR
C.....Calculate emitter sheath height.....
      ve=param2*(jej-ONE)+param1
C
C.....Calculate answer for JEJ and compute difference from
C      guess for JEJ.....
      if (ve*param4.le.dlog(TINY)) then
C.....Case where ve is so large that it would cause exp function
C      to underflow.....
      ans=ONE
      else
C.....Normal case.....
      ans=ONE+param3*dexp(ve*param4)
      endif
      dif=jej-ans
      if (dabs(dif).lt.TOL) go to 70
C
C.....Update value of JEJ until convergence.....
      if (first) then
      oldj=jej
      olddif=dif
      jej=jej-dsign(.2d0,dif)
      first=.false.
      else
      newj=(oldj*dif-jej*olddif)/(dif-olddif)
      oldj=jej
      olddif=dif
      jej=newj
      endif
      if (dabs(jej-oldj).lt.1.d-5*jej) go to 70
      enddo
70 if (iter.gt.MAXITR) pause 'Exceeded maximum iterations in
&OBSTR2'
C
C..Calculate arc drop.....
      vd=ve-vc
      return
      END
C
C
      SUBROUTINE satur2(vi,b,bp,h,j,jcj,jsp,te,tc,tr,pd,d,ta,tee,tec,
      & ve,vc,vd,vrad,jsj,ji)
C      IMPLICIT NONE
      INTEGER MAXITR
      REAL*8 vi,b,bp,h,j,jcj,jsp,te,tc,tr,pd,d,ta,tee,tec,ve,vc,vd,
      & vrad,jsj,ji,XK,TWO,HALF,TOL1,TOL2,AR,EMIS,ONE,THREE,TINY
      PARAMETER (XK=8.6175d-5,TWO=2.d0,HALF=.5d0,TOL1=1.d-6,TOL2=1.d-5,
      & MAXITR=100,AR=120.d0,EMIS=.4d0,ONE=1.d0,THREE=3.d0,
      & TINY=1.d-32)
C
C      Uses tsc2, ltec2
C
C*****
C
C      SATUR2 is called by TECMDL to implement the phenom-
C      ological model equations in the saturation region,
C      with a negative collector sheath. The formulation
C      is very similar to SATUR except that the equations
C      for TEC and VC and the LTE routines are different.
C
C      Input values -
C      VI      Effective ionization energy (eV)
C      B       Ionizability factor
C      BP      Temperature increase parameter
C      H       Collector current factor
C      J       Current density (amps/cm2)
C      JCJ     Ratio of back emission to current density
C      TE      Emitter temperature (K)
C      TC      Collector temperature (K)

```

```

C      TR      Cesium reservoir temperature (K)      *
C      PD      Pressure-spacing product (torr-mm)    *
C      D       Interelectrode spacing (mm)          *
C      TA      Average neutral and ion temperature (K) *
C
C      Output values -
C      TEE     Emitter side electron temperature (K) *
C      TEC     Collector side electron temperature (K) *
C      VE      Emitter sheath height (eV)           *
C      VC      Collector sheath height (eV)         *
C      VD      Arc drop (eV)                       *
C      VRAD    Plasma radiation component of arc drop (eV) *
C      JSJ     Ratio JS/J of effective emitted current *
C              density to working current density    *
C      JIJ     Ratio Ji/J of additional ion current to *
C              the emitter to working current density *
C
C*****
C
C      INTEGER iwhich,iter1,iter2
C      REAL*8 dlea,zetac,phinc,jnc,hs,tsc2,telect,dl,r,ans,f,oldj,
C      &      oldf,newj,param1,param2,param3,param4,js,g,
C      &      xl,x2,x3,y1,y2,y3,ys
C      LOGICAL first,ltec
C
C.....Guess ion current ratio.....
C      jij=0.d0
C
C.....Set iteration counter.....
C      iwhich=1
C
C.....Calculate ratio of gap to electron-neutral mean free path.....
C      dlea=35.d0/((te+tc)/2000.d0)*pd
C
C.....Begin modified linear interpolation search for JIJ.....
C
C      do iter1=1,MAXITR
C.....Calculate emitter side electron temperature.....
C      tee=vi/(TWO*XK*dlog(b*dlea)-XK*dlog(ONE-bp*jij))
C
C.....Calculate collector sheath attenuation factor.....
C      zetac=(-(h+HALF)+dsqrt((h+HALF)**2+8.d0*jcj*h))/
C      &      (2.d0*jcj)
C
C.....Calculate collector sheath height.....
C      vc=XK*tc*dlog(zetac)
C
C.....Calculate collector emission factor.....
C      r=jcj*dexp(vc/(XK*tc))
C
C.....Calculate collector side electron temperature.....
C      tec=(THREE*tee+TWO*tc*r)/(TWO*r+THREE)
C
C.....Calculate neutralization potential and current density.....
C      phinc=1.7d0+.383d0*tec/tr
C      jnc=AR*tec*tec*dexp(-phinc/(XK*tec))
C
C.....Assign value to LTE limit for H and check
C      to see if LTE limits the electron temperature
C      at the collector edge - if so, calculate new
C      values for TEC, VC, and R.....
C      hs=jnc/j
C      if ((r+HALF).gt.hs) then
C          tec=tsc2(tee,tc,tr,hs,j,jcj,vc)
C          r=hs-HALF
C          ltec=.true.
C      else
C          ltec=.false.
C      endif
C
C.....Calculate average electron temperature.....
C      telect=(tee+tec)/TWO
C
C.....Calculate ratio of spacing to total
C      electron mean free path, including
C      ion scattering.....
C      dl=dlea+3.4d+7*j*d/(telect**2.5d0)
C
C.....If LTE has occurred at the collector edge, the routine
C      LTE is called to check that the average electron
C      temperature is above the bulk LTE limit. If not,
C      the LTE routine will calculate new emitter side,
C      collector side, and average electron temperatures
C      The ratio of spacing to total mean free path is also
C      recalculated.....
C      if (ltec) call lte2(tee,tec,telect,tc,tr,hs,j,jcj,vc,dl,dlea,

```



```

& d,r)
C
C.....Calculate radiation component of arc drop.....
      vrad=9.65d+5*pd/(j*ta)*dexp(-2.d0/(XK*telect))*
&      (ONE+.069d0*dexp( 58d0/(XK*telect))*
&      (EMIS/dsqrt(d/10.d0)+HALF))
C
C.....Guess JSJ and enter secant method iteration.....
      jsj=TWO
      first=.true.
C.....First calculate some parameters in order to save time
      in the iteration.....
C
      param1=TWO*XK*(tec-te+(tec-tc)*r)+vrad-j1j*(
&      3.89d0+TWO*XK*tee)
      param2=TWO*XK*(tee-te)
      param3=.75d0*d1+r
      param4=-ONE/(XK*tee)
C.....Begin iteration.....
      do iter2=1,MAXITR
C.....Calculate emitter sheath height.....
      ve=(param2*(jsj-ONE)+param1)/(ONE+j1j)
C
C.....Calculate answer for JSJ and compute difference from
      guess for JSJ.....
      if (ve*param4.le.dlog(TINY)) then
C.....Case where ve is so large that the exp function would
      underflow.....
      ans=ONE+j1j
      else
C.....Normal case.....
      ans=ONE+(param3-HALF*j1j)*dexp(-ve/(XK*tee))+j1j
      endif
      f=jsj-ans
      if (dabs(f).lt.TOL1) go to 80
C
C.....Update value of JSJ until convergence.....
      if (first) then
      oldj=jsj
      oldf=f
      jsj=jsj-dsign(.2d0,f)
      first=.false.
      else
      newj=(oldj+f-jsj*oldf)/(f-oldf)
      oldj=jsj
      oldf=f
      jsj=newj
      endif
      if (dabs(jsj-oldj).lt.1.d-5*jsj) go to 80
      enddo
80      if (iter2.gt.MAXITR) pause 'Max. iterations exceeded in
&SATUR2 for finding current ratio'
C
C.....Calculate value of JS from eqn. (35) of Massey,
      McDaniel, and Bederson.....
      js=jsp*dexp(612.d0*dsqrt(dsqrt(-j*j1j*dsqrt(ve)))/te)
C
C.....Compute error term.....
      g=js/j-jsj
      if (dabs(g).lt.TOL2) go to 90
C
C.....Update JIJ to make error small....
      if (iwhch.eq.1) then
      if ((j1j.eq.0.d0).and.(g.gt.0.d0)) then
      pause ' No solution in SATUR2'
      return
      endif
      x1=j1j
      y1=g
      j1j=-.1d0
      x2=j1j
      iwhch=2
      else if (iwhch.eq.2) then
      x2=j1j
      y2=g
      if (y1*y2.gt.0.d0) then
      x1=x2
      y1=y2
      j1j=j1j+dsign(.1d0,g)
C.....Prevent j1j from becoming equal to -1. Make it the
      nearest larger number.....
      if (j1j.le.-ONE) j1j=-.999999d0
      else
      iwhch=3
      ys=y2
      j1j=(x1*y2-x2*y1)/(y2-y1)
      endif

```

```

else if (iwhch.eq.3) then
  x3=jjj
  y3=g
  if (y3*y1.lt.0.d0) then
    x2=x3
    y2=y3
    if (y3*ys.gt.0.d0) y1=y1/TWO
  else
    x1=x3
    y1=y3
    if (y3*ys.gt.0.d0) y2=y2/TWO
  endif
  ys=y3
  jjj=(x1*y2-x2*y1)/(y2-y1)
endif
enddo
90 if (iter1.gt.MAXITR) then
c   write(*,'(a)') ' Maximum iterations exceeded in
c   $SATUR2 for finding ion current'
c   write(8,'(a)') ' Maximum iterations exceeded in
c   $SATUR2 for finding ion current'
c   write(*,*) j,tr
c   write(8,*) j,tr
  stop
endif
C
C.....Calculate arc drop.....
vd=ve-vc
return
END
C
C
REAL*8 FUNCTION tsc2(tee,tc,tr,hs,j,jcj,vc)
IMPLICIT NONE
INTEGER MAXITR
REAL*8 tee,tc,tr,hs,j,jcj,vc,XK,ONE,TWO,THREE,TOL,AR,HALF
PARAMETER (XK=8.6175d-5,ONE=1.d0,TWO=2.d0,THREE=3.d0,TOL=
c   1d-5,AR=120.d0,MAXITR=50,HALF=.5d0)
C
C*****
C
C   The function TSC2 is called by the subroutines OBSTR2*
C   and SATUR2 in order to compute the collector side
C   electron temperature when LTE conditions exist at the
C   collector and the collector sheath is negative. It
C   is very similar to the function TSC. One difference
C   is that the collector sheath is recalculated by TSC2.*
C
C   Input values -
C   TEE      Emitter side electron temperature (K)
C   TC       Collector temperature (K)
C   TR       Cesium reservoir temperature (K)
C   HS       Ratio of neutralization current Jn to
C   J         Current density J
C   JCJ      Current density (amps/cm2)
C   Ratio of back emission to current den-
C   sity
C   VC       collector sheath height (ev)
C
C   Output values -
C   TSC2     LTE value for electron temperature at
C   collector edge of plasma (K)
C   VC       Recalculated value for collector
C   sheath (eV)
C*****
C
C   INTEGER iter
C   REAL*8 dh,phinc,jnc,hss,dif,oldh,olddif,newh
C   LOGICAL first,goon
C
C.....Enter iteration (first guess for HS has already been
C   calculated by calling routine).....
C
C.....Calculate collector edge electron temperature.....
first=.true.
goon=.false.
dh=ONE
do iter=1,MAXITR
  tsc2=(THREE*tee+(TWO*hs-ONE)*tc)/(TWO*(hs+ONE))
C
C.....Calculate neutralization work function and current density.....
  phinc=1.7d0+.383d0*tsc2/tr
  jnc=AR*tsc2**2*dexp(-phinc/(XK*tsc2))
C
C.....Find answer for HS, difference between guess and answer.....

```

```

      hss=jnc/j
      dif=hs-hss
      if (dabs(dif).lt.TOL) go to 100
C
C.....Update HS to make difference small.....
      if (first) then
        oldh=hs
        olddif=dif
        hs=hs-dsign(dh,dif)
        hs=dmax1(hs,1.d-12)
        first=.false.
        dh=1.6d0*dh
      else
        if (.not.goon) then
          if (dif*olddif.gt.0.d0) then
            newh=hs-dsign(dh,dif)
            newh=dmax1(newh,1.d-12)
            dh=1.6d0*dh
          else
            goon= true
            newh=(oldh*dif-hs*olddif)/(dif-olddif)
          endif
        else
          newh=(oldh*dif-hs*olddif)/(dif-olddif)
        endif
        oldh=hs
        olddif=dif
        hs=newh
      endif
      if (dabs(hs-oldh).lt.1.d-5*hs) go to 100
    enddo
100 if (iter.gt.MAXITR) pause 'Exceeded max. iterations in TSC2'
C
C.....Recalculate VC.....
      vc=XK*tc*dlog((hs-HALF)/jcj)
      return
      END
C
C
SUBROUTINE lte2(tee,tec,tav,tc,tr,hs,j,jcj,vc,dl,dlea,d,r)
C
C  IMPLICIT NONE
C  INTEGER MAXITR
C  REAL*8 tee,tec,tav,tc,tr,hs,j,jcj,vc,dl,dlea,d,r,XK,
C  & ONE,TWO,THREE,TOL,AR,HALF
C  PARAMETER (XK=8.6175d-5,ONE=1.d0,TWO=2.d0,THREE=3.d0,TOL=
C  & 1.d-5,AR=120 d0,MAXITR=50,HALF=.5d0)
C
C*****
C
C  The routine LTE2 is called by OBSTR2 and SATUR2 to
C  perform checking and, if necessary, recomputation of
C  the electron temperatures when the collector sheath
C  is negative. It is very similar to the routine
C  LTE, however, the collector sheath is re-
C  calculated in LTE2.
C
C  Input values -
C  TEE      Electron temperature at emitter edge (K)
C  TEC      Electron temperature at collector edge (K)
C  TAV      Average electron temperature (K)
C  TC       Collector temperature (K)
C  TR       Cesium reservoir temperature (K)
C  HS       Ratio of neutralization current to current
C           density
C  J        Current density (amps/cm2)
C  JCJ      Ratio of back emission to current density
C  VC       Collector sheath height (eV)
C  DL       Ratio of gap to total electron mean free
C           path
C  DLEA     Ratio of gap to electron-neutral mean
C           free path
C  D        Interelectrode gap (mm)
C
C  Output values (recalculated) -
C  TEE
C  TEC
C  TAV
C  DL
C  VC
C*****
C
C  INTEGER iter1,iter2
C  REAL*8 ts,dll,tss,dif,oldt,olddif,newt,dh,
C  & phinc,jnc,hss,oldh,newh,tsc
C  LOGICAL first,goon

```

```

C
C.....First guess for TS.....
  ts=tav
C
C.....Enter secant method search for TS.....
C
  first=.true.
  dh=TWO
  do iter1=1,MAXITR
C.....Calculate new value for ratio of gap to mean free path.....
  dll=dlea+3.4d+7*j*d/ts**2.5d0
C
C.....Calculate an answer for TS.....
  tss=1.7d0/(XK*dlog((120.d0*ts*ts)/(j*dll))-383d0/tr)
C
C.....Find difference between guess and answer.....
  dif=ts-tss
  if (dabs(dif).lt.TOL) go to 110
C
C.....Update TS to make difference small.....
  if (first) then
    oldt=ts
    olddif=dif
    ts=ts-dsign(50.d0,dif)
    first=.false.
  else
    newt=(oldt*dif-ts*olddif)/(dif-olddif)
    oldt=ts
    olddif=dif
    ts=newt
  endif
  if (dabs(ts-oldt).lt.1.d-5*ts) go to 110
enddo
110 if (iter1.gt.MAXITR) pause 'Max. iterations exceeded in LTE'
C
C.....Check to see if average electron temperature is above
C the limit. If so, return without altering any
C values.....
  if (tav.ge.ts) return
C
C.....If bulk LTE is in effect, replace TAV and DL with their
C proper LTE values.....
  tav=ts
  dl=dll
C
C.....TEC must now be recalculated, since it depends on TEE,
C which will change to keep the average temperature
C above its limit. An iteration like that in the function
C TSC2 is used.....
  first=.true.
  goon=.false.
  dh=TWO
C
C.....Begin iteration.....
  do iter2=1,MAXITR
C.....Calculate collector edge electron temperature.....
  tsc=(TWO*THREE*ts+(TWO*hs-ONE)*tc)/(TWO*(hs+ONE)+
  THREE)
  phinc=1.7d0+.383d0*tsc/tr
  jnc=AR*tsc**2*dexp(-phinc/(XK*tsc))
  hss=jnc/j
  dif=hs-hss
  if (dabs(dif).lt.TOL) go to 120
  if (first) then
    oldh=hs
    olddif=dif
    hs=hs-dsign(dh,dif)
    hs=dmax1(hs,1.d-12)
    first=.false.
    dh=1.6d0*dh
  else
    if (.not.goon) then
      if (dif*olddif.gt.0.d0) then
        newh=hs-dsign(hs,dif)
        newh=dmax1(newh,1.d-12)
        dh=1.6d0*dh
      else
        newh=(oldh*dif-hs*olddif)/(dif-olddif)
        goon=.true.
      endif
    else
      newh=(oldh*dif-hs*olddif)/(dif-olddif)
    endif
    oldh=hs
    olddif=dif
    hs=newh
  endif

```

```

endif
if (dabs(hs-oldh).lt.1.d-5*hs) go to 120
enddo
120 if (iter2.gt.MAXITR) pause 'Max. iterations exceeded in LTE2'
C.....Recompute TEC.....
tec=tsc
C.....Recompute VC.....
vc=XK*tc*dlog((hs-HALF)/jcj)
C.....Recompute TEE.....
tee=TWO*ts-tsc
r=hs-HALF
return
END
C
SUBROUTINE unig(te,tc,tr,d,phie,phic,j,ji,v,qe, sheath)
C
IMPLICIT NONE
REAL*8 te,tc,tr,d,phie,phic,ji,v,qe,
+ j,PI,XKE,TFACT,XNFACT,TOL,XK,ME,MI,DEFAULT,AR
INTEGER sheath,TRY,ITMAX
PARAMETER (PI=3.141592654,XKE=8.61753d-5,TFACT=1.05d0,
+ XNFACT=0.8d0,TOL=1 d-5,XK=1.3807d-16,ME=9.1095d-28,
+ MI=2.207d-22,DEFAULT=-99.d0,TRY=4,AR=120.d0,ITMAX=30)
C
UNIG
C
John McVey 30 March 1990
DOCUMENT CONTROL #C-568-006-D-033090
C
Rev. C: Modifications for use in CYLCON6
Calculation of cesiated work functions removed.
Changed to double precision.
C
Rev. D: Eliminated problem with divide by zero in update routine.
C
Unig is a subroutine package for calculating the output voltage of
a thermionic converter operating in the diffusion-dominated
unignited mode.
C
INPUTS:
te Emitter temperature in K
tc Collector temperature in K
tr Cesium reservoir temperature in K.
d Interelectrode gap in centimeters
phie Emitter work function in eV.
phic Collector work function in eV.
j Net electron current density in Amps/sq. cm.
C
OUTPUTS:
ji Ion current density in Amps/sq. cm.
v Output voltage in volts.
qe Electron cooling in Watts/sq. cm.
sheath Integer indicating sheath configuration.
0 - no solution
1 - DU
2 - DD
3 - UU
4 - UD
C
uses du,dd,uu,ud,dn1,dn2,denav,tcalc,update,coefs
C
INTEGER ize, itert, iwhich
REAL*8 taav,na0,nal,naav,veli,nav,r,vele,alpha,
+ dife,difi,lambde,lambdi,e,i,zetae,zetapr,vevc,zetac,
+ zetep,xiepr,nenc,psi,telans,navans,f,g,x1,x2,x3,
+ y1,y2,y3,f1,f2,f3,g1,g2,g3,xnew,ynew,update,tel,
+ ve,vc,vp,js,jie,jc,pcs,dlam,teff,arate,ionprob,
+ mue,mul,emob,imob,jlon,heat
js=AR*te*te*dexp(-phie/(XKE*te))
jc=AR*tc*tc*dexp(-phic/(XKE*tc))
pcs=2.45d+8*dexp(-8910.d0/tr)/dsqrt(tr)
taav=(te+tc)/2.d0
na0=1333.2d0*pcs/(XK*te)
nal=1333.2d0*pcs/(XK*tc)
naav=(na0+nal)/2.d0
veli=dsqrt(8.d0*XK*taav/(PI*MI))
dlam=d*1.2d-14*naav
if (dlam.lt.1.d0) then
teff=taav
else if ((dlam.ge.1.d0).and.(dlam.le.10.d0)) then
teff=taav+(dlam-1.d0)*(te/tc)/18.d0
else
teff=te
end if
arate=1333.2d0*pcs/dsqrt(2.d0*PI*MI*XK*teff)
ionprob=1.d0/(1.d0+2.d0*dexp((3.89d0-phie)/(XKE*te)))

```

```

jie=ionprob*arate*1.6022d-19
tel=1.1d0*te
if (j.lt.-jc) then
  v=DEFAULT
  sheath=0
  return
endif
if (j.gt.js) then
  v=DEFAULT
  sheath=0
  return
endif
nav=1.d+11
izone=0
iwhich=1
do itert=1,ITMAX
  r=tel/taav
  vele=dsqrt(8.d0*XK*tel/(PI*ME))
  alpha=vele/veli
  mue=emob(tel,naav,nav)
  mui=imob(taav,naav,nav)
  dife=mue*tel*XKE
  difi=mui*taav*XKE
  lambde=3.d0*dife/vele
  lambdi=3.d0*difi/veli
  e=.75d0*r/(r+1.d0)*d/lambde
  i=.75d0/(r+1.d0)*d/lambdi
  call du(j,js,jc,jie,tel,te,i,e,alpha,zetae,zetcpr,ve,
+   vc,vevc)
  if ((ve.gt.0.d0).and.(vc.gt.0.d0)) then
    sheath=1
    goto 12
  endif
  call dd(j,js,jc,jie,te,tc,i,e,alpha,zetae,zetac,ve,vc,vevc)
  if ((ve.gt.0.d0).and.(vc.gt.0.d0)) then
    sheath=2
    goto 12
  endif
  call uu(j,js,jc,jie,tel,te,i,e,alpha,zetepr,zetcpr,
+   xiepr,ve,vc,vevc)
  if ((ve.gt.0.d0).and.(vc.gt.0.d0)) then
    sheath=3
    goto 12
  endif
  call ud(j,js,jc,jie,tel,te,tc,i,e,alpha,zetepr,zetac,xiepr,
+   ve,vc,vevc)
  if ((ve.gt.0.d0).and.(vc.gt.0.d0)) then
    sheath=4
    goto 12
  endif
  sheath=0
  izone=izone+1
  if (izone.lt.TRY) then
    tel=TFACT*tel
    nav=XNFACT*nav
    iwhich=1
    goto 100
  else
    v=-dsign(DEFAULT,j)
    return
  endif
12  if ((sheath.eq.2).or.(sheath.eq.4)) then
    call dn1(j,jc,i,e,zetac,lambde,d,nenc,psi)
  else
    call dn2(j,jc,i,e,zetcpr,lambde,d,nenc,psi)
  endif
  vp=XKE*tel*((psi-1.d0)*dlog(nenc))
13  call tcalc(te,tc,j,js,jc,ve,vc,vp,zetae,zetac,telans,sheath)
  call denav(j,jc,zetcpr,zetac,nenc,vele,navans,sheath)
  f=tel-telans
  g=nav-navans
  if (iwhich.eq.1) then
    x1=nav
    y1=tel
    f1=f
    g1=g
    tel=tel-dsign(20.d0,f)
    iwhich=2
  elseif (iwhich.eq.2) then
    x2=nav
    y2=tel
    f2=f
    g2=g
    nav=nav-dsign(1.d+9,g)
    iwhich=3
  elseif (iwhich.eq.3) then

```

```

+   if ((dabs(f/tel).lt.TOL).and.(dabs(g/nav).lt.TOL))
+     goto 200
+   x3=nav
+   y3=tel
+   f3=f
+   g3=g
+   xnew=update(x1,x2,x3,f1,f2,f3,g1,g2,g3)
+   if (xnew.lt.0.d0) xnew=x3
+   ynew=update(y1,y2,y3,f1,f2,f3,g1,g2,g3)
+   if (dabs(ynew-y3).gt.y3/2.d0) ynew=y3*(1.d0+dsign(.5d0,ynew-
+     y3))
+   x1=x2
+   y1=y2
+   f1=f2
+   g1=g2
+   x2=x3
+   y2=y3
+   f2=f3
+   g2=g3
+   nav=xnew
+   tel=ynew
+   endif
100 enddo
C
200 if (itert.gt.ITMAX) then
+   v=-dsign(DEFAULT,j)
+   return
+   end if
+   ji=jion(j,jc,zetcpr,zetac,alpha,sheath)
+   v=phie-phic+vevc-vp
+   qe=heat(j,js,ji,phie,te,tel,ve,zetae,sheath)
C
+   return
+   END
C
C
REAL*8 FUNCTION update(x1,x2,x3,f1,f2,f3,g1,g2,g3)
C
IMPLICIT NONE
REAL*8 x1,x2,x3,f1,f2,f3,g1,g2,g3
C
+   Updates parameters for the two-dimensional secant method
+   iteration in UNIG used to find the average electron temperature
+   and plasma density.
C
REAL*8 r,u
r=x1*(f2*g3-f3*g2)+x2*(f3*g1-f1*g3)+x3*(f1*g2-f2*g1)
u=f2*g3-f3*g2+f3*g1-f1*g3+f1*g2-f2*g1
if (u.eq.0.d0) pause ' U is zero, chuckie!'
update=r/u
return
END
C
C
SUBROUTINE du(j,js,jc,jie,tel,te,i,e,alpha,zetae,zetcpr,ve,
+   vc,vevc)
C
IMPLICIT NONE
REAL*8 j,js,jc,jie,tel,te,i,e,alpha,zetae,zetcpr,ve,vc,vevc,
+   XKE,ZERO,ONE,TWO,DEFAULT
PARAMETER (XKE=8.61753d-5,ZERO=0.d0,ONE=1.d0,TWO=2.d0,
+   DEFAULT=-99.d0)
C
+   Solves for the emitter and collector sheath heights in the
+   condition where an ion retaining sheath is at the emitter
+   and an electron retaining one is at the collector.
C
REAL*8 a,b,c,disc
LOGICAL bad1

bad1 = .false.
a=TWO*i*js
b=TWO*je+(e-i)*j
c--(j*(ONE+TWO*e)+alpha*jie*(ONE+TWO*i))
disc=b*b-4 d0*a*c
if (disc lt ZERO) bad1=.true.
disc=dmax1(disc,ZERO)
zetae=(-b+dsqrt(disc))/(TWO*a)
if ((zetae.le.ZERO).or.(bad1)) then
+   ve=DEFAULT
+   else
+   ve=-XKE*te*dlog(zetae)
+   endif
zetcpr=(j+jc)*(TWO-zetae)/(j-js*zetae*zetae+alpha*jie)
if (zetcpr.gt.ZERO) then
+   vc=-XKE*tel*dlog(zetcpr)
+   else
+   vc=DEFAULT

```

```

endif
vevc=ve+vc
return
END
C
C
SUBROUTINE dd(j,js,jc,jie,te,tc,i,e,alpha,zetae,zetac,ve,
+ vc,vevc)
C
IMPLICIT NONE
INTEGER ITMAX
REAL*8 j,js,jc,jie,te,tc,i,e,alpha,zetae,zetac,ve,vc,vevc,
+ XKE,ZERO,ONE,TWO,DEFAULT,FOUR,TOL
PARAMETER (XKE=8.61753d-5,ZERO=0.d0,ONE=1.d0,TWO=2.d0,
+ DEFAULT=-99.d0,ITMAX=40,FOUR=4.d0,TOL=1.d-5)
C
C
C Solves for the emitter and collector sheath heights in the
C condition where there are ion retaining sheaths at both
C electrodes.
C
INTEGER iter
REAL*8 a,b1,c1,b,c,discl,q,disc2,f,x1,x2,f1,f2
LOGICAL bad1,bad2
a=(TWO*i-ONE)*js
b1=TWO*js+(ONE+e-1)*j
c1=-TWO*((ONE+e)*j+i*alpha*jie)
zetac=ZERO
do iter=1,ITMAX
  bad1=.false
  bad2=.false
  b=b1+jc*zetac
  c=c1-TWO*jc*zetac
  discl=b*b-FOUR*a*c
  if (discl.lt.ZERO) bad1=.true.
  discl=dmax1(discl,ZERO)
  zetae=(-b+dsqrt(discl))/(TWO*a)
  q=(TWO*alpha*jie-zetae*(TWO*js*zetae-j))/(TWO-zetae)
  disc2=(j+q)*(j+q)+16.d0*jc*q
  if (disc2.lt.ZERO) bad2=.true.
  disc2=dmax1(disc2,ZERO)
  f=zetac-(-(j+q)+dsqrt(disc2))/(FOUR*jc)
  if (iter.eq.1) then
    x1=zetac
    f1=f
    zetac=zetac-dsign(.1d0,f)
  else
    x2=zetac
    f2=f
    zetac=x2+f2*(x2-x1)/(f1-f2)
    x1=x2
    f1=f2
  endif
  if (dabs((zetac-x2)/zetac).lt.TOL) goto 100
enddo
100 if (iter.gt.itmax) bad2=.true.
if ((zetae.le.ZERO).or.(bad1)) then
  ve=DEFAULT
else
  ve=-XKE*te*dlog(zetae)
endif
if ((zetac.le.ZERO).or.(bad2)) then
  vc=DEFAULT
else
  vc=-XKE*tc*dlog(zetac)
endif
vevc=ve-vc
return
END
C
C
SUBROUTINE uu(j,js,jc,jie,te,tc,i,e,alpha,zetepr,zetcpr,
+ xiepr,ve,vc,vevc)
C
IMPLICIT NONE
INTEGER ITMAX
REAL*8 j,js,jc,jie,te,tc,i,e,alpha,zetepr,zetcpr,xiepr,ve,
+ vc,vevc,XKE,ZERO,ONE,TWO,DEFAULT,FOUR,TOL
PARAMETER (XKE=8.61753d-5,ZERO=0.d0,ONE=1.d0,TWO=2.d0,
+ DEFAULT=-99.d0,ITMAX=40,FOUR=4.d0,TOL=1.d-5)
C
C
C Solves for the emitter and collector sheath heights in the
C condition where there are electron retaining sheaths at both
C electrodes.
C
C
INTEGER iter
REAL*8 a,b,c,disc,tau,zzx,fmin,f,dfdZ,delta
LOGICAL bad1
a=(TWO*i+ONE)*alpha*jie

```



```

        delta(1)=ZERO
        delta(2)=ZERO
    else
        bad=.false.
        delta(1)=(pderiv(1,2)*f(2)-pderiv(2,2)*f(1))/determ
        delta(2)=(pderiv(2,1)*f(1)-pderiv(1,1)*f(2))/determ
    endif
    if ((dabs(delta(1)).lt.TOL).and.(dabs(delta(2)).lt.
+ TOL)) goto 100
    do ii=1,2
        x(ii)=x(ii)+delta(ii)
    enddo
100 if (iter.gt.itmax) bad=.true.
    zetepr=x(1)
    zetac=x(2)
    xiopr=dsign(dabs(zetepr)**tau,zetepr)
    if ((zetepr le.ZERO).or.(bad)) then
        ve=DEFAULT
    else
        ve=-XKE*te1*dlog(zetepr)
    endif
    if ((zetac le.ZERO).or.(bad)) then
        vc=DEFAULT
    else
        vc=-XKE*tc*dlog(zetac)
    endif
    vevc=-ve-vc
    return
END

C
C
SUBROUTINE dn1(j,jc,i,e,zetac,lambde,d,nenc,psi)
C
C IMPLICIT NONE
C REAL*8 j,jc,i,e,zetac,lambde,d,nenc,psi,ONE,TWO
C PARAMETER(ONE=1.d0,TWO=2.d0)
C
C Evaluates parameters NENC and PSI for computation of the
C plasma drop VP in UNIG. Used for cases in which there is an ion
C retaining collector sheath.
C
REAL*8 jczc
jczc=TWO*jc*zetac+j
nenc=ONE+TWO*e**j/jczc+TWO*zetac*i/(TWO-zetac)
psi=j*(.75d0*d/lambde)/(e**j+jczc*i*zetac/(TWO-zetac))
return
END

C
C
SUBROUTINE dn2(j,jc,i,e,zetcpr,lambde,d,nenc,psi)
C
C IMPLICIT NONE
C REAL*8 j,jc,i,e,zetcpr,lambde,d,nenc,psi,ONE,TWO
C PARAMETER(ONE=1.d0,TWO=2.d0)
C
C Evaluates parameters NENC and PSI for computation of the
C plasma drop VP in UNIG. Used for cases in which there is an
C electron retaining collector sheath.
C
REAL*8 jcj
jcj=TWO*jc+(TWO-zetcpr)*j
nenc=ONE+TWO*zetcpr*e**j/jcj+TWO*i
psi=j*(.75d0*d/lambde)/(e**j+jcj*i/zetcpr)
return
END

C
C
SUBROUTINE denav(j,jc,zetcpr,zetac,nenc,vele,nav,sheath)
C
C IMPLICIT NONE
C INTEGER sheath
C REAL*8 j,jc,zetcpr,zetac,nenc,vele,nav,ONE,TWO,EC
C PARAMETER(ONE=1.d0,TWO=2.d0,EC=1.602d-19)
C
C Calculates the average plasma density in the interelectrode
C space. This is used in UNIG to calculate the amount of
C electron-ion scattering.
C
if (sheath.eq.0) then
    nav=(j+TWO*jc)*(nenc+ONE)/(EC*vele)
elseif ((sheath.eq.1).or.(sheath.eq.3)) then
    nav=(TWO-zetcpr)*j+TWO*jc*(nenc+ONE)/(zetcpr*EC
+ *vele)
elseif ((sheath.eq.2).or.(sheath.eq.4)) then
    nav=(j+TWO*jc*zetac)*(nenc+ONE)/(EC*vele)
endif
return
END

```

```

C
C
SUBROUTINE tcalc(te,tc,j,js,jc,ve,vc,vp,zetae,zetac,tel,sheath)
C
C  IMPLICIT NONE
C  INTEGER sheath
C  REAL*8 te,tc,j,js,jc,ve,vc,vp,zetae,zetac,tel,TWOK
C  PARAMETER (TWOK=5802.5d0)
C
C  Uses energy balance to calculate an average electron temperature
C  in the interelectrode space.
C
C  REAL*8 y
C  if (sheath.eq.1) then
C    y=js*zetae+jc
C    tel=(js*zetae*te+TWOK*j*(vp-vc)+jc*tc)/y
C  elseif (sheath.eq.2) then
C    y=js*zetae+jc*zetac
C    tel=(js*zetae*te+TWOK*j*vp+jc*zetac*tc)/y
C  elseif (sheath.eq.3) then
C    y=js+jc
C    tel=(js*te+TWOK*j*(ve+vp-vc)+jc*tc)/y
C  elseif (sheath.eq.4) then
C    y=js+jc*zetac
C    tel=(js*te+TWOK*j*(ve+vp)+jc*zetac*tc)/y
C  endif
C  return
C  END
C
C
C  REAL*8 FUNCTION jion(j,jc,zetcpr,zetac,alpha,sheath)
C  IMPLICIT NONE
C  REAL*8 j,jc,zetcpr,zetac,alpha,TWO
C  PARAMETER(TWO=2.d0)
C  INTEGER sheath
C
C  if ((sheath.eq.1).or.(sheath.eq.3)) then
C    jion=((TWO-zetcpr)*j+TWO*jc)/(alpha*zetcpr)
C  else if ((sheath.eq.2).or.(sheath.eq.4)) then
C    jion=zetac*(j+TWO*jc*zetac)/(alpha*(TWO-zetac))
C  end if
C  return
C  END
C
C
C  REAL*8 FUNCTION heat(j,js,ji,phie,te,tel,ve,zetae,sheath)
C  IMPLICIT NONE
C  REAL*8 j,js,ji,phie,te,tel,ve,zetae,TK,VI
C  PARAMETER(TK=2.d0/11604.5d0,VI=3.89d0)
C  INTEGER sheath
C
C  if ((sheath.eq.1).or.(sheath.eq.3)) then
C    heat=j*(phie+ve+tel*TK)+js*(te-tel)*TK+ji*(VI-phie)
C  else if ((sheath.eq.2).or.(sheath.eq.4)) then
C    heat=j*(phie+tel*TK)+js*zetae*(te-tel)*TK+ji*(ve+VI-phie)
C  end if
C  return
C  END
C
C
C  REAL*8 FUNCTION emob(tel,na,n)
C  IMPLICIT NONE
C  REAL*8 tel,na,n
C
C  REAL*8 csecea,lnl,nuea,nuei,re,taue,muea,muei,mue
C  Evaluate electron-neutral cross-section (cm2)
C  csecea=1.d-16*(535.d0+tel*(-.27d0+tel*5.2d-5))
C
C  Evaluate the Coulomb logarithm, electron-neutral collision
C  frequency, electron-ion collision frequency, and the ratio.
C  if (n.gt.0.d0) then
C    lnl=dlog(12390.d0*tel**1.5/dsqrt(n))
C  else
C    lnl=dlog(12390.d0*tel**1.5/1.d-16)
C  end if
C  nuea=7.319d+5*na*csecea*dsqrt(tel)
C  nuei=dmax1(1.070d0*n*lnl/tel**1.5,1.d-16)
C  re=nuei/nuea
C
C  Calculate the electron mobility (cm2/volt-sec).
C  taue=(1.d0+re*(14.1d0+re*(30.6d0+re*16.3d0)))/(1.d0+re*
C  + (21.1d0+re*(37.4d0+re*16.3d0)))
C  muea=5.167d+17/nuea
C  muei=3.058d+17/nuei
C  mue=muea*muei/(muea+muei)*taue
C  emob=mue/299.8d0
C
C

```

```

return
END
C
C
REAL*8 FUNCTION imob(ti,na,n)
C
IMPLICIT NONE
REAL*8 ti,na,n
C
REAL*8 csecia,lnl,nua,nui,ri,taui,muia,mui
C
  Evaluate ion-neutral cross-section (cm2)
csecia=1.d-16*(1667.d0+ti*(-.807d0+ti*(4.77d-4-1.047d-7*ti)))
C
  Evaluate the Coulomb logarithm, ion-neutral collision frequency,
C
  ion-ion collision frequency, and the ratio.
if (n.gt.0.d0) then
  lnl=log(12390.d0*ti**1.5/dsqrt(n))
else
  lnl=log(12390.d0*ti**1.5/1.d-16)
end if
nua=1051.d0*na*csecia*dsqrt(ti)
nui=dmax1(1.537d-3*n*lnl/ti**1.5,1.d-16)
ri=nui/nua
C
C
  Calculate the ion mobility (cm2/volt-sec).
taui=(1.d0+ri*(4.2d0+ri*2.86d0))/(1.d0+ri*(4.24d0+ri*2.91d0))
muia=1.959d+12/nua
mui=muia*taui
imob=mui/299.8d0
C
return
END
C
REAL*8 FUNCTION ndsphi(te,tr,phi0)
C
IMPLICIT NONE
INTEGER MAXITR
REAL*8 te,tr,phi0,SMALL,ERRTOL
PARAMETER(SMALL=1.d-5,ERRTOL=1.d-6,MAXITR=100)
C
C
Written by John McVey and Jean-Louis Desplat
Control #C-568-007-D-061290
C
This version uses a value of 1.95 eV for the cesium ion
adsorption energy rather than 2.04 eV (see functions f1 and f2).
C
uses f1,f2
C
*****
C
  The function Nedsphi calculates the cesiated emitter
work function based on the emitter temperature,
cesium reservoir temperature (cesium pressure), and an
effective bare work function of the emitter surface.
The equations are based on the article "Correlation of
Emission Processes for Adsorbed Alkali Films on Metal
Surfaces" by N.S. Rasor and C. Warner, Journal of
Applied Physics, Vol. 35, #9, 1964. This theory is
inaccurate for high bare work functions and low values of
T/TR (Phi0 above 5.5 and T/Tr below 2.5 simultaneously, for
example). The theory does take into account the slight
non-uniqueness in T/Tr.
C
Inputs:
  Te Emitter temperature in K.
  Tr Cesium reservoir temperature in K.
  Phi0 Effective emitter bare work function in eV.
C
Outputs:
  Returns cesiated emitter work function in eV.
Version D is double precision.
*****
C
INTEGER itcnt,i
REAL*8 x(2),f(2),p(2,2),cor(2),cov,dphi,dy,dx,xdx1,s1,
* ydy1,s2,determ,err1,err2,f1,f2
C
C
  if ( te/tr .le. 2.5d0 ) then
  ndsphi = 2.1
  return
  end if
Initial guesses
cov=dmax1((phi0-te/tr)/(phi0-1.d0),1.d-6)
if (cov.le.0.5d0) then
  dphi=2.2d0*(phi0-1.5d0)*cov
else
  dphi=1.1d0*(phi0-1.5d0)
endif

```

KHLE 4/27/93
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```

dphi=dmax1(dphi,1.d-6)
do itcnt=1,MAXITR
  dy=dmax1(SMALL*dphi,1.d-6)
  dx=dmax1(SMALL*cov,1.d-6)
  x(1)=cov
  x(2)=dphi
C   Compute values of two functions which will be zero at solution.
  f(1)=f1(cov,dphi,te,tr,phi0)
  f(2)=f2(cov,dphi,te,phi0)
  if (cov.lt.0.2d0) then
    kdx1=cov-dx
    s1=1.d0
  else
    kdx1=cov+dx
    s1=-1.d0
  endif
  if (dphi.lt.0.2d0) then
    ydy1=dphi-dy
    s2=1.d0
  else
    ydy1=dphi+dy
    s2=-1.d0
  endif
C   Compute partial derivatives of both functions.
  p(1,1)=(f(1)-f1(kdx1,dphi,te,tr,phi0))/(dsign(dx,s1))
  p(1,2)=(f(1)-f1(cov,ydy1,te,tr,phi0))/(dsign(dy,s2))
  p(2,1)=(f(2)-f2(kdx1,dphi,te,phi0))/(dsign(dx,s1))
  p(2,2)=(f(2)-f2(cov,ydy1,te,phi0))/(dsign(dy,s2))
C   Perform Newton-Raphson.
  determ=p(1,1)*p(2,2)-p(2,1)*p(1,2)
  if (dabs(determ).le.1.0d-20) then
    pause 'No convergence in ndsphi'
    ndsphi=-1.0d-12
    return
  else
    cor(1)=(f(2)*p(1,2)-f(1)*p(2,2))/determ
    cor(2)=(f(1)*p(2,1)-f(2)*p(1,1))/determ
  endif
  do i=1,2
    x(i)=x(i)+cor(i)
  enddo
  err1=dabs(cor(1)/x(1))
  err2=dabs(cor(2)/x(2))
  cov=dmini(x(1),.99)
  cov=dmax1(cov,0.)
  dphi=dmax1(x(2),0.)
  if ((err1.lt.ERRTOL).and.(err2.lt.ERRTOL)).or.((dabs(f(1))
  .lt.ERRTOL).and.(dabs(f(2)).lt.ERRTOL)) go to 10
enddo
C   Return value of cesiated work function.
10 if (itcnt.gt.MAXITR) then
  pause 'No convergence in ndsphi'
  ndsphi=-1.0d-12
else
  ndsphi=phi0-dphi
endif
return
END
*****
C   REAL*8 FUNCTION f1(x,y,te,tcs,phi0)
C   IMPLICIT NONE
C   REAL*8 x,y,te,tcs,phi0,PI,K,ONE,TWO,HALF,TPMK,VI,PHIIO
C   PARAMETER (PI=3.141592654,K=1.d0/11604.5d0,ONE=1 d0,TWO=2.d0,
C   TPMK=TWO*PI*2.207d-22*1.381d-16,HALF=0 5d0,VI=3.89d0,PHIIO=
C   1.95d0)
C   *****
C   F1 is called by ndsphi.
C   The value at solution will be near zero.
C   *****
C   REAL*8 phia0,e0,pcs,g,factr1,factr2,mucs,sigfcs
C   phia0=.777d0*dsqrt(phi0)
C   e0=phi0-phia0-VI+PHIIO
C   pcs=2.45d+8*dexp(-8910.d0/tcs)/dsqrt(tcs)
C   mucs=1333.d0*pcs/dsqrt(TPMK*te)
C   g=.18d0+.2d0*x
C   factr1=ONE+HALF*dexp((e0-g*y)/(K*te))
C   factr2=x/(ONE-x)*dexp(x/(ONE-x))
C   sigfcs=HALF*dexp(62.d0+4.8d0*x*(ONE-HALF*x))
C   f1=sigfcs*factr2*dexp(-phia0/(K*te))/(factr1*mucs)-ONE
C   return
C   END
C   *****

```



```

*      k4 = h*f(z+h,T+k3)
*      T = T + (k1 + 2*k2 + 2*k3 + k4)/6
c      T = T + ((HeatFlux(z)*Rbound(10)*Rbound(10)*3.14159D0*h)/
c      a      (Mdot*cp(T,W))
*      T = T + 4.0D0/( De*G*cp(T,W) ) * HeatFlux(z) * h
*
*      CoolTbl(I+1,1) = z+h
*      CoolTbl(I+1,2) = T
100 Continue

If (ABS(T-Told).GE.0.1) then
  Told = T
  N = N*2
  if (N .gt. 2000) then
    write(8,*) ' Nonconvergence in Convect'
    write(8,*) ' Execution Terminated '
    stop
  end if
  Else
    Goto 160
  Endif

Goto 10

160 Write(8,200) T
200 Format (' Temperature of coolant at core exit: ',F10.1,
a      ' degrees K. ')
End
Real*8 Function f(z,T)
*****
* Returns the value of the derivative of T with respect *
* to z (dT/dz), as given by equation 6.6.8 of Weisman *
* (see reference in the comments for the main program). *
*****
Real*8 z, T, G, De, HeatFlux, Cp, Tinlet, W, D1, D2, mdot
Common /CoolProp/ Tinlet, De, G, W, D2, D1, mdot

f = 4.0D0/(G*De*cp(T,W)) * HeatFlux(z)

End
Real*8 Function Cp(T,W)
*****
* Uses correlations from the Sodium-NaK Engineering *
* Handbook (O. Foust, ed.; vol. 1 pp. 52-53) to return *
* the value of the heat capacity of the NaK coolant for *
* a given temperature T and potassium weight fraction W *
* for the coolant (e.g. eutectic NaK-78 has W=78.) *
* Only single phase coolants are modeled. If the *
* temperature of the coolant is higher than the boiling *
* point of NaK at the given sodium-potassium composition, *
* this routine reports the error and halts the program. *
*
* Units are in Joules/(kilogram*K).
*
*****
Real*8 T, BoilingPt, CpNa, CpK, W

BoilingPt = ((756.5-881.4)*W + 881.4) + 273.1
If (T.GT.BoilingPt) then
c      Write(*,100) T, INT(W*100)
c      Write(8,100) T, INT(W*100)
      Stop
Endif

CpNa = (1.43612D0 - 5.80237D-4*T + 4.62081D-7*T**2)*1000.D0
CpK = (0.83850D0 - 3.67230D-4*T + 4.58980D-7*T**2)*1000.D0

Cp = CpNa*(1.0D0 - W) + CpK*W

100 Format(' The temperature T-',F7.1,' degrees K is higher than ' /
a      ' the boiling point for NaK-',I3,//
b      ' Execution terminated in Cp.'//)
End
Real*8 Function HeatFlux(z1)
*****
* Uses linear interpolation between values in a table to *
* return the value of the heat flux at the given axial *
* position z. If the axial position is out of the range *
* of the table, this routine reports the error and halts *
* the program.
*
*****
Integer Kmax
Parameter (Kmax=10)
Real*8 z1, QTable(Kmax), zh, z1, Qh, Ql, Tinlet, De, G
Real*8 W, Z, D1, D2, Zmin, Zmax, mdot

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Integer K, K2
Common /CoolProp/ Tinlet, De, G, W, D2, D1, mdot
Common /QTAB/ Qtable
Common /Zdata/ Zmin, Zmax, K2

K = 1

10 if (z1 .ge. zmax) then
    heatflux = qtable(kmax)
    return
end if
if (Z(K).EQ.z1) then
    HeatFlux = QTable(K)
    Return
elseif (Z(K).GT.z1) then
    zh = Z(K)
    zl = Z(K-1)
    Qh = QTable(K)
    Ql = QTable(K-1)
    HeatFlux = (Qh-Ql)/(zh-zl)*(z1-zl) + Ql
    Return
else
    K = K+1
endif
Goto 10
End
C ALGORITHM 433 COLLECTED ALGORITHMS FROM ACM.
C ALGORITHM APPEARED IN COMM. ACM, VOL. 15, NO. 10,
C P. 914.
SUBROUTINE INTPPL(IU,L,X,Y,N,U,V)
C INTERPOLATION OF A SINGLE-VALUED FUNCTION
C THIS SUBROUTINE INTERPOLATES, FROM VALUES OF THE FUNCTION
C GIVEN AS ORDINATES OF INPUT DATA POINTS IN AN X-Y PLANE
C AND FOR A GIVEN SET OF X VALUES (ABSCISSAS), THE VALUES OF
C A SINGLE-VALUED FUNCTION Y = Y(X).
C THE INPUT PARAMETERS ARE
C IU - LOGICAL UNIT NUMBER OF STANDARD OUTPUT UNIT
C L - NUMBER OF INPUT DATA POINTS
C (MUST BE 2 OR GREATER)
C X - ARRAY OF DIMENSION L STORING THE X VALUES
C (ABSCISSAS) OF INPUT DATA POINTS
C (IN ASCENDING ORDER)
C Y - ARRAY OF DIMENSION L STORING THE Y VALUES
C (ORDINATES) OF INPUT DATA POINTS
C N - NUMBER OF POINTS AT WHICH INTERPOLATION OF THE
C Y VALUE (ORDINATE) IS DESIRED
C (MUST BE 1 OR GREATER)
C U - ARRAY OF DIMENSION N STORING THE X VALUES
C (ABSCISSAS) OF DESIRED POINTS
C THE OUTPUT PARAMETER IS
C V - ARRAY OF DIMENSION N WHERE THE INTERPOLATED Y
C VALUES (ORDINATES) ARE TO BE DISPLAYED
C DECLARATION STATEMENTS
IMPLICIT DOUBLE PRECISION (A-H,O-Z)
DIMENSION X(L),Y(L),U(N),V(N)
EQUIVALENCE (P0,X3),(Q0,Y3),(Q1,T3)
REAL M1,M2,M3,M4,M5
EQUIVALENCE (UK,DX),(IMN,X2,A1,M1),(IMX,X5,A5,M5),
1 (J,SW,SA),(Y2,W2,W4,Q2),(Y5,W3,Q3)
C PRELIMINARY PROCESSING
10 L0=L
LM1=L0-1
LM2=LM1-1
LP1=L0+1
N0=N
IF(LM2 LT.0) GO TO 90
IF(N0.LE.0) GO TO 91
DO 11 I=2,L0
IF(X(I-1)-X(I)) 11,95,96
11 CONTINUE
IPV=0
C MAIN DO-LOOP
DO 80 K=1,N0
UK=U(K)
C ROUTINE TO LOCATE THE DESIRED POINT
20 IF(LM2 EQ.0) GO TO 27
IF(UK GE X(L0)) GO TO 26
IF(UK LT X(1)) GO TO 25
IMN=2
IMX=L0
21 I=(IMN+IMX)/2
IF(UK.GE.X(I)) GO TO 23
22 IMX=I
GO TO 24
23 IMN=I+1
24 IF(IMX.GT.IMN) GO TO 21

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I=IMX
GO TO 30
25 I=1
GO TO 30
26 I=LP1
GO TO 30
27 I=2
C CHECK IF I = IPV
30 IF(I.EQ.IPV) GO TO 70
IPV=I
C ROUTINES TO PICK UP NECESSARY X AND Y VALUES AND
C TO ESTIMATE THEM IF NECESSARY
40 J=I
IF(J.EQ.1) J=2
IF(J.EQ.LP1) J=L0
X3=X(J-1)
Y3=Y(J-1)
X4=X(J)
Y4=Y(J)
A3=X4-X3
M3=(Y4-Y3)/A3
IF(LM2.EQ.0) GO TO 43
IF(J.EQ.2) GO TO 41
K2=X(J-2)
Y2=Y(J-2)
A2=X3-X2
M2=(Y3-Y2)/A2
IF(J.EQ.L0) GO TO 42
41 X5=X(J+1)
Y5=Y(J+1)
A4=X5-X4
M4=(Y5-Y4)/A4
IF(J.EQ.2) M2=M3+M3-M4
GO TO 45
42 M4=M3+M3-M2
GO TO 45
43 M2=M3
M4=M3
45 IF(J.LE.3) GO TO 46
A1=X2-X(J-3)
M1=(Y2-Y(J-3))/A1
GO TO 47
46 M1=M2+M2-M3
47 IF(J.GE.LM1) GO TO 48
A5=X(J+2)-X5
M5=(Y(J+2)-Y5)/A5
GO TO 50
48 M5=M4+M4-M3
C NUMERICAL DIFFERENTIATION
50 IF(I.EQ.LP1) GO TO 52
W2=ABS(M4-M3)
W3=ABS(M2-M1)
SW=W2+W3
IF(SW NE 0.0) GO TO 51
W2=0.5
W3=0.5
SW=1.0
51 T3=(W2*M2+W3*M3)/SW
IF(I.EQ.1) GO TO 54
52 W3=ABS(M5-M4)
W4=ABS(M3-M2)
SW=W3+W4
IF(SW NE 0.0) GO TO 53
W3=0.5
W4=0.5
SW=1.0
53 T4=(W3*M3+W4*M4)/SW
IF(I.NE.LP1) GO TO 60
T3=T4
SA=A2+A3
T4=0.5*(M4+M5-A2*(A2-A3)*(M2-M3)/(SA*SA))
X3=X4
Y3=Y4
A3=A2
M3=M4
GO TO 60
54 T4=T3
SA=A3+A4
T3=0.5*(M1+M2-A4*(A3-A4)*(M3-M4)/(SA*SA))
X3=X3-A4
Y3=Y3-M2*A4
A3=A4
M3=M2
C DETERMINATION OF THE COEFFICIENTS
60 Q2=(2.0*(M3-T3)+M3-T4)/A3
Q3=(-M3-M3+T3+T4)/(A3*A3)

```

```

C COMPUTATION OF THE POLYNOMIAL
  70 DX=UK-P0
  80 V(K)=Q0+DX*(Q1+DX*(Q2+DX*Q3))
      RETURN
C ERROR EXIT
  90 WRITE (IU,2090)
      GO TO 99
  91 WRITE (IU,2091)
      GO TO 99
  95 WRITE (IU,2095)
      GO TO 97
  96 WRITE (IU,2096)
  97 WRITE (IU,2097) I,X(I)
  99 WRITE (IU,2099) LO,NO
      RETURN
C FORMAT STATEMENTS
2090 FORMAT(1X/22H *** L = 1 OR LESS./)
2091 FORMAT(1X/22H *** N = 0 OR LESS./)
2095 FORMAT(1X/27H *** IDENTICAL X VALUES./)
2096 FORMAT(1X/33H *** X VALUES OUT OF SEQUENCE./)
2097 FORMAT(6H I =,I7,10X,6HX(I) =,E12.3)
2099 FORMAT(6H L =,I7,10X,3HN =,I7/
1      36H ERROR DETECTED IN ROUTINE INTRPL)
      END
SUBROUTINE CRVFIT(IU,MD,L,X,Y,M,N,U,V)
C SMOOTH CURVE FITTING
C THIS SUBROUTINE FITS A SMOOTH CURVE TO A GIVEN SET OF IN-
C PUT DATA POINTS IN AN X-Y PLANE. IT INTERPOLATES POINTS
C IN EACH INTERVAL BETWEEN A PAIR OF DATA POINTS AND GENER-
C ATES A SET OF OUTPUT POINTS CONSISTING OF THE INPUT DATA
C POINTS AND THE INTERPOLATED POINTS. IT CAN PROCESS EITHER
C A SINGLE-VALUED FUNCTION OR A MULTIPLE-VALUED FUNCTION.
C THE INPUT PARAMETERS ARE
C IU - LOGICAL UNIT NUMBER OF STANDARD OUTPUT UNIT
C MD - MODE OF THE CURVE (MUST BE 1 OR 2)
C     - 1 FOR A SINGLE-VALUED FUNCTION
C     - 2 FOR A MULTIPLE-VALUED FUNCTION
C L - NUMBER OF INPUT DATA POINTS
C     (MUST BE 2 OR GREATER)
C X - ARRAY OF DIMENSION L STORING THE ABSCISSAS OF
C     INPUT DATA POINTS (IN ASCENDING OR DESCENDING
C     ORDER FOR MD = 1)
C Y - ARRAY OF DIMENSION L STORING THE ORDINATES OF
C     INPUT DATA POINTS
C M - NUMBER OF SUBINTERVALS BETWEEN EACH PAIR OF
C     INPUT DATA POINTS (MUST BE 2 OR GREATER)
C N - NUMBER OF OUTPUT POINTS
C     = (L-1)*M+1
C THE OUTPUT PARAMETERS ARE
C U - ARRAY OF DIMENSION N WHERE THE ABSCISSAS OF
C     OUTPUT POINTS ARE TO BE DISPLAYED
C V - ARRAY OF DIMENSION N WHERE THE ORDINATES OF
C     OUTPUT POINTS ARE TO BE DISPLAYED
C DECLARATION STATEMENTS
      IMPLICIT DOUBLE PRECISION (A-H,O-Z)
      DIMENSION X(L),Y(L),U(N),V(N)
      EQUIVALENCE (M1,B1),(M2,B2),(M3,B3),(M4,B4),
1      (X2,P0),(Y2,Q0),(T2,Q1)
      REAL M1,M2,M3,M4
      EQUIVALENCE (W2,Q2),(W3,Q3),(A1,P2),(B1,P3),
1      (A2,D2),(SW,R,Z)
C PRELIMINARY PROCESSING
10 MD0=MD
   MDM1=MD0-1
   LO=L
   LM1=LO-1
   MO=M
   MM1=MO-1
   NO=N
   IF(MD0.LE.0) GO TO 90
   IF(MD0.GE.3) GO TO 90
   IF(LM1.LE.0) GO TO 91
   IF(MM1.LE.0) GO TO 92
   IF(NO.NE.LM1*MO+1) GO TO 93
   GO TO (11,16),MD0
11 I=2
   IF(X(1)-X(2)) 12,95,14
12 DO 13 I=3,LO
   IF(X(I-1)-X(I)) 13,95,96
13 CONTINUE
   GO TO 18
14 DO 15 I=3,LO
   IF(X(I-1)-X(I)) 96,95,15
15 CONTINUE
   GO TO 18
16 DO 17 I=2,LO

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        IF(X(I-1).NE.X(I)) GO TO 17
        IF(Y(I-1).EQ.Y(I)) GO TO 97
17  CONTINUE
18  K=NO+MO
    I=L0+1
    DO 19 J=1,L0
        K=K-MO
        I=I-1
        U(K)=X(I)
19  V(K)=Y(I)
    RM=MO
    RM=1.0/RM
C MAIN DO-LOOP
20  K5=MO+1
    DO 80 I=1,L0
C ROUTINES TO PICK UP NECESSARY X AND Y VALUES AND
C   TO ESTIMATE THEM IF NECESSARY
    IF(I.GT.1) GO TO 40
30  X3=U(1)
    Y3=V(1)
    X4=U(MO+1)
    Y4=V(MO+1)
    A3=X4-X3
    B3=Y4-Y3
    IF(MDM1.EQ.0) M3=B3/A3
    IF(L0.NE.2) GO TO 41
    A4=A3
    B4=B3
31  GO TO (33,32), MDO
32  A2=A3+A3-A4
    A1=A2+A2-A3
33  B2=B3+B3-B4
    B1=B2+B2-B3
    GO TO (51,56), MDO
40  X2=X3
    Y2=Y3
    X3=X4
    Y3=Y4
    X4=X5
    Y4=Y5
    A1=A2
    B1=B2
    A2=A3
    B2=B3
    A3=A4
    B3=B4
    IF(I.GE.LM1) GO TO 42
41  K5=K5+MO
    X5=U(K5)
    Y5=V(K5)
    A4=X5-X4
    B4=Y5-Y4
    IF(MDM1 EQ.0) M4=B4/A4
    GO TO 43
42  IF(MDM1 NE.0) A4=A3+A3-A2
    B4=B3+B3-B2
43  IF(I.EQ.1) GO TO 31
    GO TO (50,55), MDO
C NUMERICAL DIFFERENTIATION
50  T2=T3
51  W2=ABS(M4-M3)
    W3=ABS(M2-M1)
    SW=W2+W3
    IF(SW NE 0.0) GO TO 52
    W2=0.5
    W3=0.5
    SW=1.0
52  T3=(W2*M2+W3*M3)/SW
    IF(I-1) 80,80,60
55  COS2=COS3
    SIN2=SIN3
56  W2=ABS(A3*B4-A4*B3)
    W3=ABS(A1*B2-A2*B1)
    IF(W2+W3.NE.0.0) GO TO 57
    W2=SQRT(A3*A3+B3*B3)
    W3=SQRT(A2*A2+B2*B2)
57  COS3=W2*A2+W3*A3
    SIN3=W2*B2+W3*B3
    R=COS3*COS3+SIN3*SIN3
    IF(R EQ 0.0) GO TO 58
    R=SQRT(R)
    COS3=COS3/R
    SIN3=SIN3/R
58  IF(I-1) 80,80,65
C DETERMINATION OF THE COEFFICIENTS
60  Q2=(2.0*(M2-T2)+M2-T3)/A2

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      Q3=(-M2-M2+T2+T3)/(A2*A2)
      GO TO 70
65  R=SQRT(A2*A2+B2*B2)
      P1=R*COS2
      P2=3 0*A2-R*(COS2+COS2+COS3)
      P3=A2-P1-P2
      Q1=R*SIN2
      Q2=3 0*B2-R*(SIN2+SIN2+SIN3)
      Q3=B2-Q1-Q2
      GO TO 75
C COMPUTATION OF THE POLYNOMIALS
70  DZ=A2*RM
      Z=0.0
      DO 71  J=1,MM1
          K=K+1
          Z=Z+DZ
          U(K)=P0+Z
71  V(K)=Q0+Z*(Q1+Z*(Q2+Z*Q3))
      GO TO 79
75  Z=0.0
      DO 76  J=1,MM1
          K=K+1
          Z=Z+RM
          U(K)=P0+Z*(P1+Z*(P2+Z*P3))
76  V(K)=Q0+Z*(Q1+Z*(Q2+Z*Q3))
79  K=K+1
80  CONTINUE
      RETURN
C ERROR EXIT
90  WRITE (IU,2090)
      GO TO 99
91  WRITE (IU,2091)
      GO TO 99
92  WRITE (IU,2092)
      GO TO 99
93  WRITE (IU,2093)
      GO TO 99
95  WRITE (IU,2095)
      GO TO 98
96  WRITE (IU,2096)
      GO TO 98
97  WRITE (IU,2097)
98  WRITE (IU,2098)  I,X(I),Y(I)
99  WRITE (IU,2099)  MDO,LO,MO,NO
      RETURN
C FORMAT STATEMENTS
2090 FORMAT(1X/31H  *** MD OUT OF PROPER RANGE./)
2091 FORMAT(1X/22H  *** L = 1 OR LESS./)
2092 FORMAT(1X/22H  *** M = 1 OR LESS./)
2093 FORMAT(1X/25H  *** IMPROPER N VALUE./)
2095 FORMAT(1X/27H  *** IDENTICAL X VALUES./)
2096 FORMAT(1X/33H  *** X VALUES OUT OF SEQUENCE./)
2097 FORMAT(1X/33H  *** IDENTICAL X AND Y VALUES./)
2098 FORMAT(7H  I  =,I4,10X,6HX(I) =,E12.3,
1      10X,6HY(I) =,E12.3)
2099 FORMAT(7H  MD =,I4,8X,3HL =,I5,8X,
1      3HM =,I5,8X,3HN =,I5/
2      36H ERROR DETECTED IN ROUTINE  CRVFIT)
      END
      subroutine initial(prob,Tstop,Tecool,tr,sig,ems,
4      Qrad,Qcscnd,t)
      parameter ( imax = 10, jmax = 10 )
      implicit double precision (a-h,o-z)
      integer prob, i, j, rmesh(9), mat(5)
      double precision tr, sig, ems, Tstop, Tecool
      double precision Qrad(jmax), t(imax,jmax)
      double precision Qcscnd(jmax), rbound(10)
      double precision gapcond, r
      external gapcond, r
      common /rdata/ rbound,rmesh,mat
*****
*
* Calculate initial values of thermal power, conduction and radiation *
*
*****

      do i=1,imax
          if ( r(i).eq.rbound(4) ) then
              do j=1,jmax
                  qrad(j) = sig*ems*((t(i,j))**4 - (t(i+1,j))**4)
                  qcscnd(j) = gapcond(t(i,j),t(i+1,j),Tstop,Tecool,Prob,
a                  tr,r(i+1)-r(i))
              end do
          end if
      end do

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return
end
subroutine sgauss
implicit double precision (a-h,o-z)
integer imax, jmax, nn
double precision zero
parameter (imax = 10, jmax = 10, zero = 0.0d0)
parameter (nn = 10*imax*jmax)
double precision aa(imax*jmax+1,imax*jmax), x(imax*jmax)
double precision a(nn), aflag(8), pivot(imax*jmax)
integer i, j, z, n, snr(nn), rnr(nn), iflag(10)
integer ha(imax*jmax,11), ifail, nml, iha
common /gaussmain/ aa,x,n

z = 0
do j=1,N
  do i=1,N
    if ( aa(i,j) .ne. zero ) then
      z = z + 1
      a(z) = aa(i,j)
      snr(z) = j
      rnr(z) = i
    end if
  end do
  x(j) = aa(n+1,j)
end do
nml = nn
iha = n
* print*, 'nn=', nn, ' z=', z

call y12maf(n, z, a, snr, nn, rnr, nml, pivot, ha,
liha,aflag,iflag,x,ifail)

if ( ifail .ne. 0 ) then
  write(8,10) ifail
10  format(1x, ' Error in sparse gaussian elimination code',/,
  * ' error diagnostic parameter ifail = ', i4 )
  stop
end if

return
end
subroutine y12maf(n, z, a, snr, nn, rnr, nml, pivot, ha,
liha,aflag,iflag,b,ifail)
implicit double precision (a-b,g,p,t-y), integer (c,f,h-n,r-s,z)
double precision a(nn), pivot(n), aflag(8),b(n)
integer snr(nn), rnr(nml), ha(iha,11), iflag(10)
aflag(1)=16.0d0
aflag(2)=1.d-12
aflag(3)=1.d+16
aflag(4)=1.d-12
iflag(2)=2
iflag(3)=1
iflag(4)=0
iflag(5)=1
call y12mbf(n,z,a,snr,nn,rnr,nml,ha,iha,aflag,iflag,ifail)
if(ifail.ne.0)go to 1
call y12mcf(n,z,a,snr,nn,rnr,nml,pivot,b,ha,iha,aflag,iflag,
1 ifail)
if(ifail.ne.0)go to 1
call y12mdf(n,a,nn,b,pivot,snr,ha,iha,iflag,ifail)
return
end
1  subroutine y12mbf(n, z, a, snr, nn, rnr, nml, ha, iha, aflag,
i iflag,ifail)
c
c
c the non-zero elements of a sparse matrix a are prepared in order to
c solve the system ax=b by use of sparse matrix technique/
c
c
implicit double precision(a-b,g,p,t-y),integer(c,f,h-n,r-s,z)
double precision a(nn), aflag(8)
integer snr(nn), rnr(nml), ha(iha,11), iflag(10)
mode=iflag(4)
ifail=0
if(n.lt.2)ifail=12
if(z.le.0)ifail=13
if(nn.lt.2*z)ifail=5
if(nml.lt.z)ifail=6
if(ifail.eq.0.and.n.gt.z)ifail=14
if(iha.lt.n)ifail=15
if(mode.lt.0)ifail=16
if(mode.gt.2)ifail=16
if(ifail.ne.0) go to 22
gt1=0.0d0

```

```

do 10 i=1,n
ha(i,2)=0
ha(i,3)=0
10 ha(i,6)=0
c
c find the number of the non-zero elements in each row and column;move
c the non-zero elements in the end of the arrays a and snr;find the
c largest non-zero element in a(in absolute value).
c
do 20 i=1,z
t=dabs(a(i))
l3=rnr(i)
l4=snr(i)
if(l4.gt.n.or.l4.lt.1)ifail=24
if(l3.gt.n.or.l3.lt.1)ifail=25
ha(l3,3)=ha(l3,3)+1
ha(l4,6)=ha(l4,6)+1
if(t.gt.gt1)gt1=t
a(z+1)=a(i)
20 snr(z+1)=snr(i)
if(ifail.gt.0)go to 22
c
c store the information of the row starts(in ha(i,1))and of the column
c starts(in ha(i,4)).
c
l1=1
l2=1
do 40 i=1,n
l3=ha(i,3)
l4=ha(i,6)
if(l3.gt.0)go to 21
ifail=17
go to 22
21 if(l4.gt.0)go to 23
ifail=18
go to 22
23 if(mode.eq.2)go to 30
ha(i,9)=l3
ha(i,10)=l4
ha(i,11)=0
ha(l3,2)=ha(l3,2)+1
ha(i,5)=l3
30 ha(i,1)=l1
ha(i,4)=l2
l1=l1+l3
l2=l2+l4
ha(i,3)=0
40 ha(i,6)=0
c
c store the non-zero elements of matrix a(ordered in rows) in the
c first z locations of the array a.do the same for their column numbers
c
do 50 i=1,z
l1=z+i
l3=rnr(i)
l2=ha(l3,1)+ha(l3,3)
a(l2)=a(l1)
snr(l2)=snr(l1)
50 ha(l3,3)=ha(l3,3)+1
c
c store the row numbers of the non-zero elements ordered by columns in
c the first z locations of the array rnr. store information about row
c ends(in ha(i,3)).
c
l4=1
do 70 i=1,n
if(mode.eq.2)go to 60
if(ha(i,2).eq.0)go to 60
ha(i,11)=l4
l4=l4+ha(i,2)
ha(i,2)=ha(i,11)
60 ha(i,3)=ha(i,1)+ha(i,3)-1
l1=ha(i,1)
l2=ha(i,3)
do 70 j=l1,l2
l3=snr(j)
r=ha(l3,6)
index=ha(l3,4)+r
rnr(index)=1
if(r.eq.0)go to 70
if(j.eq.l1)go to 70
if(rnr(index-1).ne.i)go to 70
ifail=11
go to 22
70 ha(l3,6)=r+1
do 90 i=1,n

```

```

      if(mode.eq.2)go to 80
      l3=ha(1,5)
      l5=ha(13,2)
      ha(15,8)=i
      ha(1,7)=15
      ha(13,2)=ha(13,2)+1
80  continue
90  ha(i,6)=ha(i,4)+ha(i,6)-1
      aflag(6)=gt1
      iflag(6)=0
      iflag(7)=0
      iflag(8)=z
      iflag(1)=-1
22  return
      end
      subroutine yl2mcf(n,z,a,snr,nn,rnr,nnl,pivot,b,ha,iha, aflag,iflag
*,ifail)
c
c  systems of linear equations are solved by use of sparse matrix tech-
c  nique and by gaussian elimination.
c
c      implicit double precision(a-b,g,p,t-y),integer(c,f,h-n,r-s,z)
c      double precision a(nn),b(n),pivot(n),aflag(8)
c
c  information which is necessary to begin the elimination is stored.
c
c      integer snr(nn),rnr(nnl),ha(iha,11), iflag(10)
c      ifail=0
c      if(iflag(1).ne.-1)ifail=2
c      if(aflag(1).lt.1.0d0)aflag(1)=1.0005 d0
c      if(aflag(3).lt.1.0d+5)aflag(3)=1.0d+5
c      if(aflag(4).lt.0.0d0)aflag(4)=-aflag(4)
c      if(iflag(2).lt.1)ifail=19
c      if(iflag(3).lt.0.or.iflag(3).gt.2)ifail=20
c      if(iflag(5).lt.1.or.iflag(5).gt.3)ifail=21
c      if(iflag(5).eq.3)ifail=22
c      if(ifail.gt.0)go to 1110
c      snr(z+1)=0
c      rnr(z+1)=0
c      n8=n+1
c      n7=n-1
c      u=aflag(1)
c      grmin=aflag(4)*aflag(6)
c
c  use the information about fill-ins if it is possible.
c
c      zz=z
c      nr=n*n
c      if(iflag(4).ne.2)go to 100
c      if(iflag(10).gt.nn)go to 50
c      l1=iflag(10)
c      l5=l1+1
c      if(15.le.nn)snr(15)=0
c      do 40 i=1,n
c      l=n8-i
c      l2=ha(1,3)+1
c      l3=l2-ha(1,1)
c      do 10 j=1,l3
c      snr(15-j)=snr(l2-j)
10  a(15-j)=a(l2-j)
c      ha(1,3)=l1
c      ha(1,1)=15-l3
c      l6=l1-l3
c      l5=15-ha(1,9)
c      if(15.gt.l6)go to 30
c      do 20 j=15,l6
20  snr(j)=0
30  continue
40  l1=15-1
50  if(iflag(9).gt.nnl)go to 100
c      l2=iflag(9)
c      l5=l2+1
c      if(15.le.nnl)rnr(15)=0
c      do 90 i=1,n
c      l=n8-i
c      l1=ha(1,6)+1
c      l4=l1-ha(1,4)
c      do 60 j=1,l4
60  rnr(15-j)=rnr(l1-j)
c      ha(1,4)=15-l4
c      ha(1,6)=l2
c      l6=l2-l4
c      l5=15-ha(1,10)
c      if(15.gt.l6)go to 80
c      do 70 j=15,l6
70  rnr(j)=0

```

```

80 continue
90 l2=l5-1
100 r4=ha(n,3)
    r5=ha(n,6)
    aflag(7)=aflag(6)
    aflag(8)=aflag(6)
    do 110 i=1,n
    pivot(i)=0.0 d0
    ha(i,2)=ha(i,1)
110 ha(i,5)=ha(i,4)
    index=ha(n,8)
c
c start of gaussian elimination.
c
    slut=ha(index,3)-ha(index,2)+1
    do 950 i=1,n7
    rr3=ha(i,2)
    rr4=ha(i,3)
    cl=ha(i,4)
    cr4=ha(i,6)
    if(iflag(3).eq.0)go to 350
    if(iflag(4).ne.2)go to 120
    rrow=ha(i,7)
    rcoll=ha(i,8)
    go to 220
120 l4=ha(i,8)
    if(iflag(3).eq.1)go to 130
    rrow=l4
    rcoll=rrow
    rpivot=i
    go to 170
130 r=nr
    v=0.0 d0
    index=iflag(2)
    do 160 kk=1,index
    ll=i-1+kk
    if(ll.gt.n)go to 170
    j=ha(ll,8)
    r7=ha(j,2)
    r8=ha(j,3)
    r9=r8-r7
    t=0.0 d0
    do 140 k=r7,r8
    td=dabs(a(k))
140 if(t.lt.td)t=td
    t=t/u
    do 160 k=r7,r8
    td=dabs(a(k))
    if(td.lt.t)go to 150
    r6=snr(k)
    r3=r9*(ha(r6,6)-ha(r6,5))
    if(r3.gt.r)go to 150
    if(r3.lt.r)go to 151
    if(v.ge.td)go to 150
151 v=td
    rrow=j
    rcoll=r6
    r=r3
    rpivot=ll
150 continue
160 continue
170 r3=ha(rcoll,10)
    ha(rcoll,10)=ha(i,10)
    ha(i,10)=r3
    r3=ha(rrow,9)
    ha(rrow,9)=ha(i,9)
c
c remove the pivot row of the list where the rows are ordered by
c increasing numbers of non-zero elements.
c
    ha(i,9)=r3
    l1=0
    l=i
    l2=ha(l4,3)-ha(l4,2)+1
180 l=l+1
    if(l2.gt.l1)ha(l2,l1)=1
    if(l.gt.n)go to 190
    l5=ha(l,8)
    l3=ha(l5,3)-ha(l5,2)+1
    if(rpivot.lt.l)go to 190
    ha(l4,7)=1
    ha(l,8)=l4
    l4=l5
    l1=l2
    l2=l3
    l3=n8

```



```

go to 180
190 if(12.eq.11)go to 200
    if(13.eq.12)go to 200
    ha(12,11)=0
200 15=ha(i,7)
    if(rrow.eq.i)go to 210
    ha(15,8)=rrow
    ha(rrow,7)=15
210 ha(i,7)=rrow
c
c row interchanges.
c
    ha(i,8)=rcoll
220 if(rrow.eq.i)go to 290
    t=b(rrow)
    b(rrow)=b(i)
    b(i)=t
    do 250 j=rr3,rr4
        ll=snr(j)
        r=ha(ll,5)-1
        r10=ha(ll,6)
240 r=r+1
    if(rnr(r).ne.i)go to 240
    rnr(r)=rnr(r10)
250 rnr(r10)=rrow
    rr3=ha(rrow,2)
    rr4=ha(rrow,3)
    do 270 j=rr3,rr4
        ll=snr(j)
        r=ha(ll,5)-1
260 r=r+1
    if(rnr(r).ne.rrow)go to 260
270 rnr(r)=i
    do 280 j=1,3
        r3=ha(rrow,j)
        ha(rrow,j)=ha(i,j)
c
c column interchanges.
c
280 ha(i,j)=r3
290 if(rcoll.eq.i)go to 350
    do 310 j=c1,cr4
        ll=rnr(j)
        r=ha(ll,2)-1
        r10=ha(ll,3)
300 r=r+1
    if(snr(r).ne.i)go to 300
    t=a(r10)
    a(r10)=a(r)
    a(r)=t
    snr(r)=snr(r10)
310 snr(r10)=rcoll
    c1=ha(rcoll,4)
    cr4=ha(rcoll,6)
    do 330 j=c1,cr4
        ll=rnr(j)
        r=ha(ll,2)-1
320 r=r+1
    if(snr(r).ne.rcoll)go to 320
330 snr(r)=i
    do 340 j=4,6
        r3=ha(rcoll,j)
        ha(rcoll,j)=ha(i,j)
c
c end of the interchanges.
c the row ordered list and the column ordered list are prepared to
c begin step i of the elimination.
c
340 ha(i,j)=r3
350 r9=rr4-rr3
    do 360 rr=rr3,rr4
        if(snr(rr).eq.i)go to 370
360 continue
    ifail=9
    go to 1110
370 v=a(rr)
    pivot(i)=v
    td=dabs(v)
    if(td.lt.aflag(8))aflag(8)=td
    if(td.ge.grmin)go to 380
    ifail=3
    go to 1110
380 r2=ha(i,1)
    a(rr)=a(rr3)
    snr(rr)=snr(rr3)
    a(rr3)=a(r2)

```

```

    snr(rr3)=snr(r2)
    snr(r2)=0
    z=z-1
    rr3=rr3+1
    ha(i,2)=rr3
    ha(i,1)=r2+1
    cr3=ha(i,5)
    if(r9.le.0)go to 431
    do 430 j=rr3,rr4
    index=snr(j)
430 pivot(index)=a(j)
431 r7=cr4-cr3+1
    do 880 k=1,r7
    r1=rnr(cr3-1+k)
    if(r1.eq.i)go to 870
    i1=ha(r1,1)
    r1=ha(r1,2)
    rr2=ha(r1,3)
    l2=rr2-rr1+1
    l=rr1-1
390 l=l+1
    if(snr(l).ne.i)go to 390
    t=a(l)/v
    if(iflag(5).eq.2)go to 400
    a(l)=a(i1)
    snr(l)=snr(i1)
    snr(i1)=0
    i1=i1+1
    ha(r1,1)=i1
    z=z-1
    go to 410
400 a(l)=a(rr1)
    a(rr1)=t
    r3=snr(rr1)
    snr(rr1)=snr(l)
    snr(i)=r3
410 rr1=rr1+1
    ha(r1,2)=rr1
    b(r1)=b(r1)-b(i)*t
    if(r9.le.0)go to 669
    r=rr1
    if(r.gt.rr2)go to 470
    do 460 l=r,rr2
    l1=snr(l)
    td=pivot(l1)
    if(td.eq.0.0d0)go to 450
    pivot(l1)=0.0 d0
    td=a(l)-td*t
    a(l)=td
    tdl=dabs(td)
    if(tdl.gt.aflag(7))aflag(7)=td1
c
c too small element is created.remove it from the lists.
c
    if(tdl.gt.aflag(2))go to 450
    z=z-1
    a(l)=a(rr1)
    snr(l)=snr(rr1)
    a(rr1)=a(i1)
    snr(rr1)=snr(i1)
    snr(i1)=0
    rr1=rr1+1
    i1=i1+1
    ha(r1,2)=rr1
    ha(r1,1)=i1
    r3=ha(l1,5)
    r2=r3-1
    l4=ha(l1,4)
    l5=rnr(l4)
    l6=rnr(r3)
440 r2=r2+1
    if(rnr(r2).ne.r1)go to 440
    rnr(r2)=l6
    rnr(r3)=l5
    rnr(l4)=0
    ha(l1,5)=r3+1
    ha(l1,4)=l4+1
450 continue
460 continue
470 continue
    do 750 j=1,r9
    r=rr3-1+j
    r2=snr(r)
    tol2=pivot(r2)
    pivot(r2)=a(r)
    if(tol2.eq.0.0d0)go to 740

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```

    tol3=-tol2*t
    toll=dabs(tol3)
    if(toll.lt.aflag(2))go to 740
    c2=ha(r2,4)
    cr2=ha(r2,6)
    cr1=ha(r2,5)
    lfr=rr2-il+2
    lfc=cr2-c2+2
    if(iflag(4).ne.1)go to 480
    if(lfr.gt.ha(r1,9))ha(r1,9)=lfr
    if(lfc.gt.ha(r2,10))ha(r2,10)=lfc
480 if(il.eq.1)go to 490
    if(snr(il-1).eq.0)go to 600
490 if(rr2.eq.nn)go to 500
    if(snr(rr2+1).eq.0)go to 580
c
c collection in row ordered list.
c
500 r10=nn-lfr
    if(r10.ge.r4)go to 560
    iflag(6)=iflag(6)+1
    do 520 jj=1,n
        ll=ha(jj,3)
        if(ll.lt.ha(jj,1))go to 510
        ha(jj,3)=snr(ll)
        snr(ll)--jj
510 continue
520 continue
    l3=0
    l4=1
    do 550 jj=1,r4
        if(snr(jj).eq.0)go to 540
        l3=l3+1
        if(snr(jj).gt.0)go to 530
        l5=-snr(jj)
        snr(jj)=ha(15,3)
        ha(15,3)=l3
        l6=l4+ha(15,2)-ha(15,1)
        ha(15,2)=l6
        ha(15,1)=l4
        l4=l3+1
530 a(l3)=a(jj)
        snr(l3)=snr(jj)
540 continue
550 continue
    r4=l3
    snr(l3+1)=0
    rr3=ha(1,2)
    rr4=ha(1,3)
    il=ha(r1,1)
    rr1=ha(r1,2)
    r=rr3-1+j
    if(r10.ge.r4)go to 560
    ifail=5
c
c fill-in takes place in the row ordered list.
c
    go to 1110
560 r8=lfr-1
    rr2=r4+lfr
    if(r8.le.0)go to 579
    l3=il-1
    do 570 ll=1,r8
        l4=r4+ll
        l5=l3+ll
        a(l4)=a(l5)
        snr(l4)=snr(l5)
570 snr(l5)=0
579 rrl=r4+rr1-1+1
    ha(r1,3)=rr2
    ha(r1,2)=rr1
    il=r4+1
    ha(r1,1)=il
    ll=rr2
    go to 590
580 rr2=rr2+1
    ha(r1,3)=rr2
    ll=rr2
    if(rr2.le.r4)go to 610
590 r4=rr2
    if(r4.lt.nn)snr(r4+1)=0
    go to 610
600 rrl=rr1-1
    il=il-1
    ha(r1,1)=il
    ha(r1,2)=rr1

```

```

l1=rr1
snr(l1)=snr(l1)
a(l1)=a(l1)
610 a(l1)=tol3
snr(l1)=snr(r)
td=dabs(a(l1))
if(td.gt.aflag(7))aflag(7)=td
z=z+1
if(iflag(8).lt.z) iflag(8)=z
if(c2.eq.1)go to 620
if(rnr(c2-1).eq.0)go to 720
620 if(cr2.eq.nn1)go to 630
if(rnr(cr2+1).eq.0)go to 700
c
c collection in column ordered list.
c
630 r10=nn1-lfc
if(r10.ge.r5)go to 680
iflag(7)=iflag(7)+1
do 640 jj=i,n
l1=ha(jj,6)
ha(jj,6)=rnr(l1)
640 rnr(l1)=-jj
l3=0
l4=1
do 670 jj=1,r5
if(rnr(jj).eq.0)go to 660
l3=l3+1
if(rnr(jj).gt.0)go to 650
l5=-rnr(jj)
rnr(jj)=ha(15,6)
ha(15,6)=l3
l6=l4+ha(15,5)-ha(15,4)
ha(15,5)=l6
ha(15,4)=l4
l4=l3+1
650 rnr(l3)=rnr(jj)
660 continue
670 continue
r5=l3
rnr(r5+1)=0
c2=ha(r2,4)
cr3=ha(1,5)
cr4=ha(1,6)
cr1=ha(r2,5)
if(r10.ge.r5)go to 680
ifail=6
c
c fill-in takes place in the column ordered list.
c
go to 1110
680 r8-lfc-1
cr2=r5+lfc
if(r8.le.0)go to 699
l3=c2-1
do 690 l=1,r8
l4=r5+1
l5=l3+1
rnr(l4)=rnr(15)
690 rnr(15)=0
699 cr1=r5+cr1-c2+1
c2=r5+1
ha(r2,6)=cr2
ha(r2,4)=c2
ha(r2,5)=cr1
r=cr2
go to 710
700 cr2=cr2+1
ha(r2,6)=cr2
r=cr2
if(cr2.le.r5)go to 730
710 r5=cr2
if(r5.lt.nn1)rnr(r5+1)=0
go to 730
720 cr1=cr1-1
c2=c2-1
ha(r2,4)=c2
ha(r2,5)=cr1
r=cr1
rnr(c2)=rnr(r)
730 rnr(r)=r1
740 continue
750 continue
669 if(rr1.le.rr2)go to 760
ifail=7
c

```

c update the information in the list where the rows are ordered by
 c increasing numbers of the non-zero elements.

```

c
  go to 1110
760 if(iflag(4).eq.2)go to 870
   if(iflag(3).eq.0)go to 870
   l1=rr2-rr1+1
   if(l1.eq.12)go to 870
   l6=ha(r1,7)
   l4=ha(l2,11)
   if(l1.gt.12)go to 820
   if(l6.gt.14)go to 780
   if(l4.eq.n)go to 770
   l=ha(l4+1,8)
   l5=ha(l,3)-ha(l,2)+1
   if(l5.eq.12)go to 790
770 ha(l2,11)=0
   go to 800
780 l5=ha(l4,8)
   l3=ha(l6,8)
   ha(l4,8)=l3
   ha(l6,8)=l5
   ha(l5,7)=l6
   ha(l3,7)=l4
   l6=l4
790 ha(l2,11)=l4+1
800 if(l4.eq.i+1)go to 810
   l=ha(l6-1,8)
   l2=ha(l,3)-ha(l,2)+1
   l4=ha(l2,11)
   if(l1.lt.12)go to 780
810 if(l1.ne.12)ha(l1,11)=l6
   go to 870
820 if(l6.gt.14)go to 840
   if(l4.eq.n)go to 830
   l=ha(l4+1,8)
   l5=ha(l,3)-ha(l,2)+1
   if(l5.eq.12)go to 840
830 ha(l2,11)=0
840 l2=l2+1
   if(l2.le.slut)go to 850
   l3=n
   slut=l1
   l2=l1
   go to 860
850 l3=ha(l2,11)-1
   if(l3.eq.-1)go to 840
   if(l2.gt.11)l2=l1
860 ha(l2,11)=l3
   l4=ha(l3,8)
   l7=ha(l6,8)
   ha(l3,8)=l7
   ha(l6,8)=l4
   ha(l7,7)=l3
   ha(l4,7)=l6
   l6=l3
   if(l2.lt.11)go to 840
870 continue
880 continue
   if(r9.le.0)go to 882
   do 881 j=rr3,rr4
   index=snr(j)
881 pivot(index)=0.0 d0
882 continue
   cr3=ha(i,4)
   do 890 j=cr3,cr4
890 rnr(j)=0
   if(r9.le.0)go to 930
   l2=ha(i,2)-1
   do 920 l1=1,r9
   r=snr(l2+l1)
   r1=ha(r,5)
   r2=ha(r,6)
   if(r2.gt.r1)go to 900
   ifail=8
   go to 1110
900 ha(r,5)=r1+1
   r3=r1-1
910 r3=r3+1
   if(rnr(r3).ne.1)go to 910
   rnr(r3)=rnr(r1)
920 rnr(r1)=i
930 aflag(5)=aflag(7)/aflag(6)
   if(aflag(5).lt.aflag(3))go to 940
   ifail=4
   go to 1110

```

```

940 continue
c
c preparation to begin the back substitution.
c
950 continue
  index=ha(n,2)
  pivot(n)=a(index)
  a(index)=0.0 d0
  td=dabs(pivot(n))
  if(td.gt.sflag(7))aflag(7)=td
  if(td.lt.aflag(8))aflag(8)=td
  if(td.gt.grmin)go to 960
  ifail=3
  go to 1110
960 if(iflag(4).ne.1)go to 1060
  iflag(10)=ha(n,9)
  iflag(9)=ha(n,10)
  do 990 i=1,n7
    r1=n-i
    iflag(10)=iflag(10)+ha(r1,9)
    iflag(9)=iflag(9)+ha(r1,10)
    if(iflag(3).eq.0)go to 980
    do 970 j=9,10
      r2=ha(r1,j-2)
      r6=ha(r2,j)
      ha(r2,j)=ha(r1,j)
970 ha(r1,j)=r6
980 continue
990 continue
1060 continue
  aflag(5)=aflag(7)/aflag(6)
  iflag(1)=-2
1110 z=zz
  return
  end
  subroutine yl2mdf(n,a,nn,b,pivot,snr,ha,iha,iflag,ifail)
  implicit double precision(a-b,g,p,t-y),integer (c,f,h-n,r-s,z)
  double precision a(nn), pivot(n), b(n)
  integer snr(nn), ha(iha,11), iflag(10)
  ifail=0
  if(iflag(1).eq.-2)go to 1000
  ifail=1
  go to 1110
1000 mode=iflag(4)
  ipiv=iflag(3)
  n8=n+1
  n7=n-1
  state=iflag(5)
c
c solve the system with lower triangular matrix 1 (if the
c lu-factorization is available).
c
  if(state.ne.3)go to 1051
  if(ipiv.eq.0)go to 1020
  do 1010 i=1,n7
    l1=ha(i,7)
    t=b(l1)
    b(l1)=b(i)
    b(i)=t
1010 continue
1020 continue
  do 1050 i=1,n
    rr1=ha(i,1)
    rr2=ha(i,2)-1
    if(rr1.gt.rr2)go to 1040
    do 1030 j=rr1,rr2
      l1=snr(j)
1030 b(i)=b(i)-a(j)*b(l1)
1040 continue
1050 continue
c
c solve the system with upper triagular matrix.
c
1051 continue
  do 1090 i=1,n
    r1=n8-i
    rr1=ha(r1,2)
    rr2=ha(r1,3)
    if(rr2.lt.rr1) go to 1080
    do 1070 j=rr1,rr2
      r2=snr(j)
1070 b(r1)=b(r1)-a(j)*b(r2)
1080 continue
1090 b(r1)=b(r1)/pivot(r1)
c
c if interchanges were used during the elimination then a reordering in

```

```
c lution vector is made.  
c      if(ipiv.eq.0)go to 1110  
      do 1100 i=1,n7  
        r1=n-i  
        r2=ba(r1,8)  
        t=b(r2)  
        b(r2)=b(r1)  
1100  b(r1)=t  
1110  return  
      end
```